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ABSTRACT

Title of Thesis: Process Modelling of The Nitration of Toluene

Nitin K. Shah, M. S. In Chemical Engineering, 1989

Thesis directed by: Dr. Edward C. Roche, Jr.

The thesis on the process modelling of the nitration process focuses specifically on the product separation of the nitrated aromatic material from the reactor and wash section of the process. Included in the text is an overview of the main process steps associated with the production of para and ortho-nitrotoluene. The critical issues concerning the reaction of nitric acid and toluene were summarized, and resulted in this subject being deferred for future work.

The separation of the isomers into pure components is an important part of the MNT process because of the close high boiling points of the isomeric products. The most desirable product in the process is the para isomer even though the ortho isomer is usable. An existing computer model was modified and used to study the batch distillation columns used to recover toluene and the marketable isomers of MNT. A typical washed organic intermediate feed to the separation section (batch columns) was analyzed using the continuous reflux batch distillation model. The results of the modelling program indicate that the separation campaign is a lengthy process, but that high purity products can be obtained.

Process Modelling of The Nitration Of Toluene

by
Nitin K. Shah

Thesis submitted to the Faculty of the Graduate School of
the New Jersey Institute of Technology in partial fulfillment of
the requirements for the degree of
Master of Science in Chemical Engineering.

1989

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CHAPTER I

INTRODUCTION

The nitration of aromatic hydrocarbons is a unit process of considerable industrial importance. Some nitration processes are carried out in the vapor phase but the majority are conducted under liquid conditions, and involve reactions between an organic hydrocarbon phase and an aqueous phase consisting of a mixture of nitric acid, sulfuric acid and water.

The nitration of toluene has been the subject of extensive study for over 100 years, but research continues because of the great synthetic and industrial utility of the nitrated products. Control of the isometric composition of the nitration derivatives of toluene and its homologues has been an important but elusive goal. The 2,4,6-TNT as it is formed creates a need for additional processing steps if a stable and safe explosive is to be made and also generates a major environmental problem in disposal of the products to which the minor isomers are converted. The manufacture of dinitrotoluenes (DNT), which is ultimately converted to toluene di-isocyanate for polyurethanes, is far more significant than that of TNT. A large variety of uses exist for the para and ortho isomers of mononitrotoluene, but seldom has the demand for the individual compounds matched their production.

In past decade paranitrotoluene was most needed, and extensive research is devoted to maximize its production. In recent years new products based on orthonitrotoluene have effected the demand. Application of metanitrotoluene have suffered because, as a minor co-product, its availability always depends

upon changing market conditions. Gaining flexible control of the isomers produced in nitration of toluene continues to be a valid, if difficult, objective providing scientific challenge as well as opportunities to achieve important level of conservation of resources. With improvement in understanding the factors that govern the products of nitration, our prospects for their regulations in production should also improve.

CHAPTER II

DEFINITION OF THE PROCESS

Aromatic nitration has been studied in great detail for several decades, and as a result, it stands as one of the relatively few well understood phenomena in organic chemistry. The reaction is still known only imperfectly and many misconceptions of its nature are widely held. We are primarily interested in the mononitration of toluene.

Liquid phase nitration of toluene has been performed industrially on a large scale for many years. Mononitrotoluenes are produced by the nitration of toluene. It is well known that nitration of aromatic molecules produces a number of isometric products. These mononitro compounds are used as intermediates for manufacture of dyestuffs, pharmaceuticals, etc. The presence of the methyl group on the aromatic ring facilitates the nitration at higher temperature but at the same time it increases the ease of oxidation which sometime results in undesirable products. Thus, the nitration of toluene generally is carried out at a lower temperatures than the nitration of benzene to minimize oxidative side reactions. Toluene is less soluble in the acid phase, thus vigorous agitation of the reaction mixture is necessary to maximize the interfacial area of the two phases and mass transfer of the reactants.

Mononitrotoluenes can be produced by either a batch or continuous process. We will focus our attention on the batch process because better control of the process. A wide range of nitrating agents have been used in laboratory experiments and industrial nitrations. The main consideration for a nitrating

agent is that it be available in quantity, reasonably cheap and relatively stable. The work described below is done using a mixture of nitric acid and sulphuric acid, called mixed acid. This nitrating agent has had wide industrial use for many years. The major steps involved in the process are explained below:

(2.1) Mixed acid preparation:

Nitric acid of a required quantity is first taken into a stainless steel mixing vessel. Sulphuric acid is added slowly with the temperature at 35 to 40 °C. The temperature of the mixture should not go above 40 °C.

(2.2) Nitration of toluene to mononitrotoluene (MNT):

Toluene with the required quantity is charged first in a stainless steel reactor containing a very efficient stirring and cooling arrangement. The mixed acid is then slowly added to it ensure that the temperature of the mass does not exceed 35 °C. It is most important that temperature is controlled by stirring and proper cooling. The temperature of the reaction can also be maintained by adjusting the acid rate of addition. The acid is added below the surface of the toluene. After the addition of required acid, the temperature is raised slowly to 40 °C. The reactor contents are agitated for an additional hour to complete the reaction. After completion of the reaction, the reaction mixture is put into a separator where the mass is allow to settle down for about an hour. The acidic layer is drained from the bottom and is reconcentrated. The crude nitrated organic product from the top layer is transferred to a wash tank.

(2.3) Washing of crude MNT:

Crude mononitrotoluenes after charging to the wash tank is first washed

with water and then washed with dilute alkali. Finally the organic material is washed with water to free it from alkali traces. The wash system is provided with a good stirring arrangement. The product is analyzed using chromatographic equipment for unreacted starting materials (toluene), ortho, meta, and para mononitrotoluenes and for the dinitration product. The crude MNT is stored in a storage tank before processing it for recovery of the toluene and separation of the isomers of mononitrotoluenes.

(2.4) Separation of crude MNT into pure isomers:

The crude MNT is separated into the pure isomers by distillation in various steps. The separation process involved following steps:

(i) Removal of toluene and moisture by distillation:

The crude MNT from the storage tank is charged to the primary batch distillation column in order to remove the unreacted toluene and the traces of water. Water and toluene both will be collected in the overhead receiver. The toluene is recycled to the next nitration campaign. The removal of water and toluene is accomplished easily in the atmospheric batch distillation column.

(ii) Recovery of o-NT from isomer mixture:

Due to the high boiling points of the isomers of MNT, a vacuum batch distillation is carried out in a second column. The batch distillation column has with two overhead condensers and a reboiler. The crude MNT is taken in after vaporizing it in a boiler. The first fraction will be o-NT and is removed via the condenser at the top of the column. It is then crystalized to facilitate the removal of trace quantities of p-NT.

(iii) Recovery of pure p-NT from isomer mixture by crystalization:

The second cut in the column will be m-NT. Since the boiling points of these isomers are very close, a p-NT rich mixture of both isomers will be obtained. The pure p-NT is then recovered by crystallization. The remaining mixture, called mother liquor, still contain all of the three isomers and some of the dinitro products, is transferred to mother liquor tank for a second distillation using the vacuum column as an additional campaign step.

(iv) Mother liquor distillation for m-NT rich fraction:

The mother liquor is charged in the column and remaining part of o-NT is recovered. The p-NT rich stream is directed to the storage tank and transferred to crystallizer for the recovery of pure p-NT. The residual from the column will contain mostly m-NT along with p-NT and dinitro compounds. It is heated and again distilled for the recovery of pure m-NT and the unrecovered part of p-NT. The pure m-NT is then crystallized.

A detailed process block diagram is shown in Figure 1A and 1B.

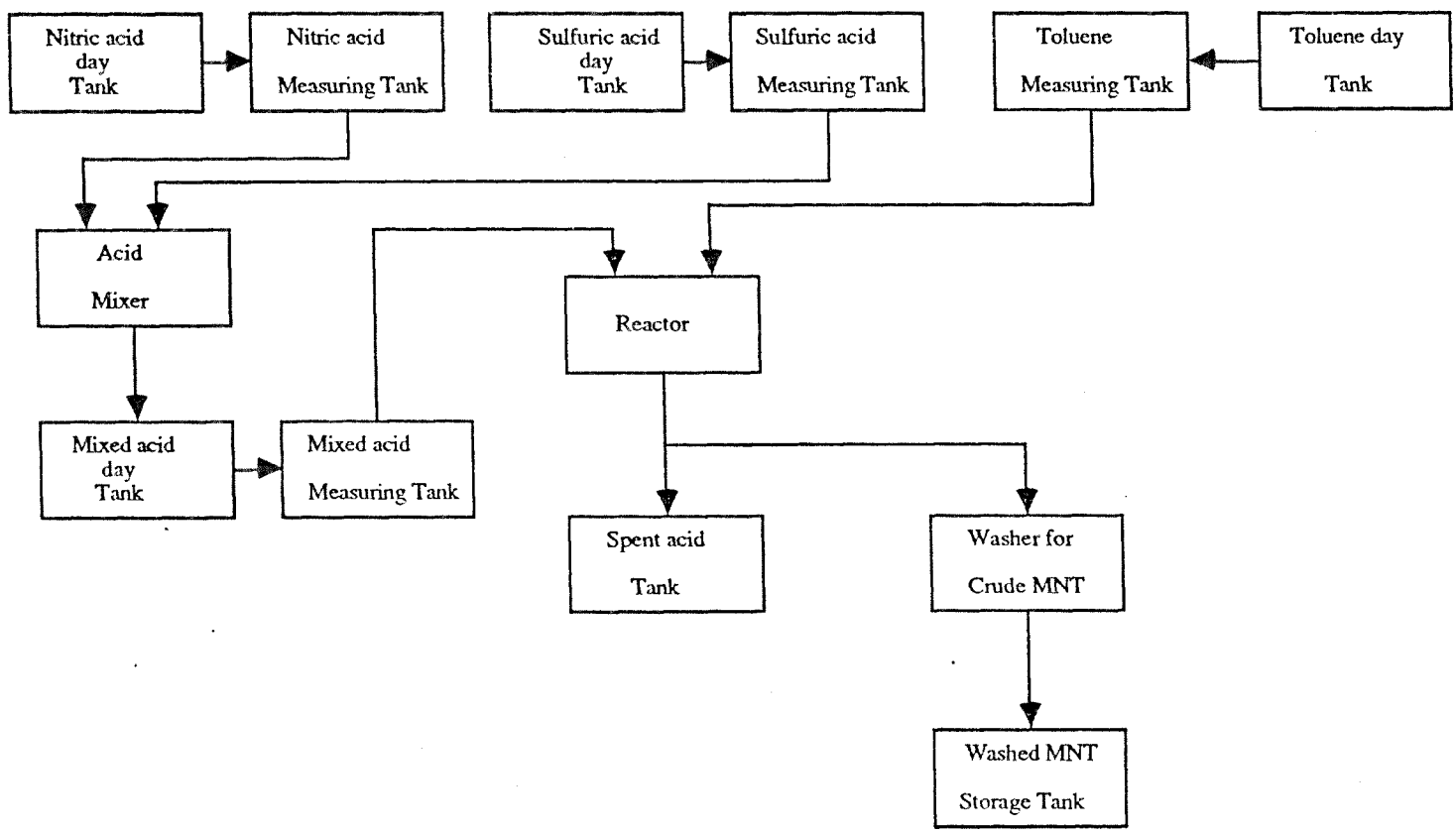


Figure 1A Process Block Diagram

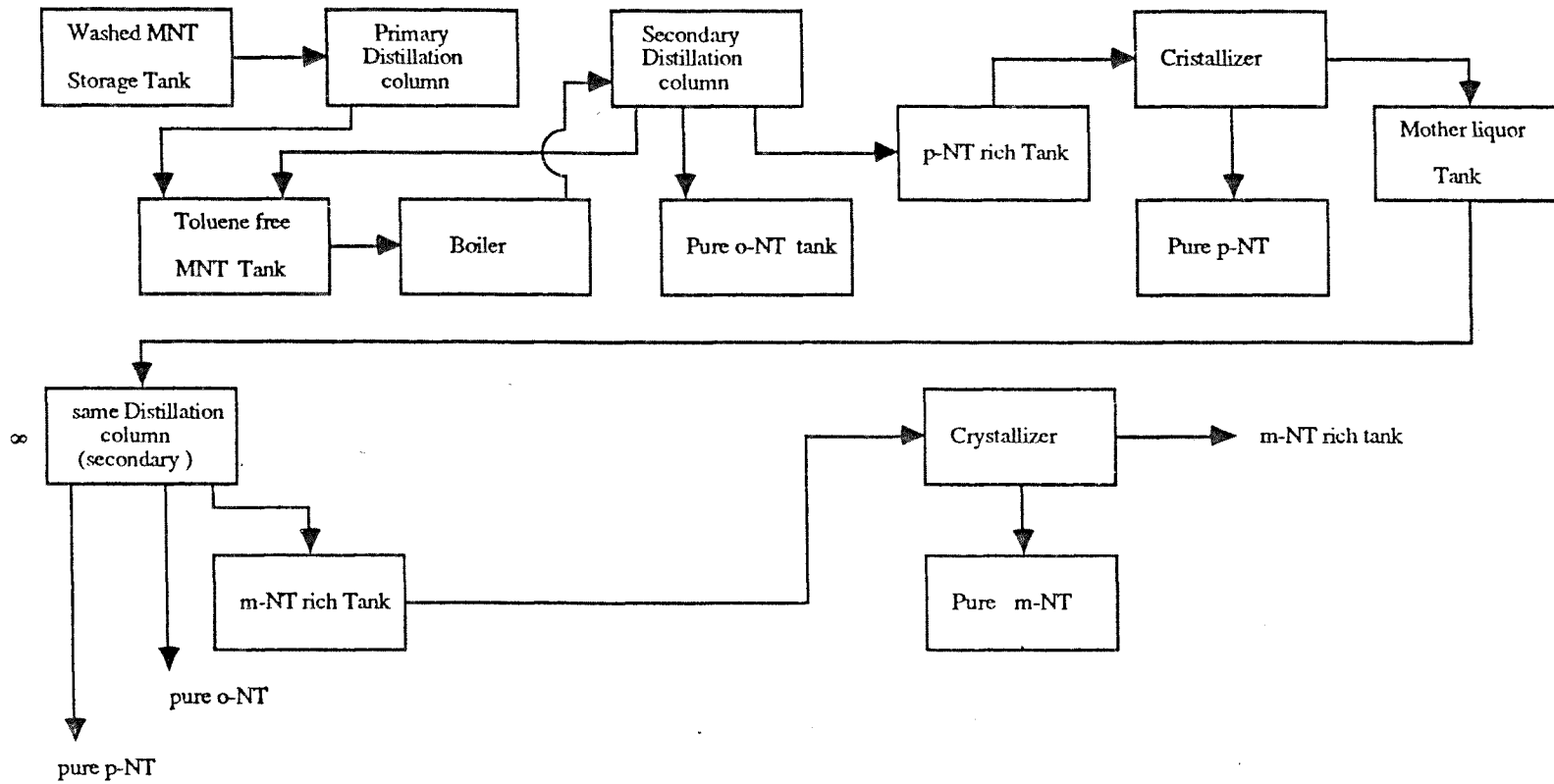


Figure 1B Process Block Diagram

CHAPTER III

TWO PRINCIPAL PROCESS STEPS

The commercial nitration of aromatic substances with mixed acid has been carried out in batch equipment for nearly a century. The process is divided into two major operations

(3.1) Reaction and,

(3.2) Separation of the isomers.

(3.1) Reaction:

For a commercial nitration of several aromatics such as benzene and toluene, the acid phase is a mixture of nitric acid, sulfuric acid and water, known as mixed acid. Mixed acid proportions are generally 52-56% wt. sulfuric acid (H_2SO_4), 28-32% wt. nitric acid (HNO_3) and 12-20% wt. water (H_2O). The design of a batch nitrator has been based mainly on empirical rules and heat transfer rates since it is an exothermic reaction. The nitration reactions certainly occur either in the acid phase or at least at the interface between liquid phases. The aromatic reactant must hence be transferred to the interface and possibly also into the acid phase or vice-versa. Thus the design and scale-up of an industrial nitrator is a problem of simultaneous mass transfer and chemical reaction, and it is essential to know which of these is the limiting step so that the proper parameters for scaleup can be chosen.

(3.2) Separation of the isomers:

Isomers are separated by batch distillation process in sequence. Batch distillation is much simpler in concept than continuous distillation. A mixture

is charged into a boiler (still pot) and is heated to vaporize it. The vapor is continuously condensed and collected in a series of fractions. Because the vapor has a higher concentration of the light component than the corresponding liquid, the condensed fraction has initially higher light concentrations than the original mixture, and the later fractions (or the part left in the reboiler) have lower concentrations. Because the separation from a single equilibrium stage is generally not sufficient, it is usual to incorporate a number of stages by inserting a column between the boiler and condenser, filled with mass transfer internals through which a part of the condensate flows as reflux.

The outstanding advantage of batch distillation is that one column can separate a mixture containing a number of components into relatively pure componential products. To achieve a similar result with a continuous distillation system requires $n-1$ columns for a system of n components. The second advantage of batch distillation is that it is more flexible than a continuous column, and more suitable as general purpose equipment for purification and solvent recovery within a plant where numerous separations are required.

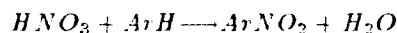
Two batch columns are used in the total separation process. One, known as the primary column, is used for the removal of the unreacted toluene and trace amount of water from the crude mononitrotoluenes. The second column is operated for the separation of the isomers of MNT into the pure compounds and is called the secondary column. Due to the higher boiling points of the products, the distillation is undertaken under vacuum.

CHAPTER IV

REACTION MECHANISM ANALYSIS

Aromatic nitration is one of the oldest and most common industrial reactions. This reaction is still not well understood due to its nature. Only a small amount of useful kinetic data is available to the engineer, and this is restricted to a small range of process operating conditions. The extension and interpretation of the existing data is therefore of importance.

The stoichiometry of the reaction is misleadingly simple:



This chemical reaction is misleading because sulfuric acid does not appear in it, and for this reason sulfuric acid has often been assigned the role of promotor. It has long been known that aromatic nitration is an irreversible reaction. Past studies of the nitration of toluene have shown conclusively that nitration can be considered in many cases as an electrophilic attack of the nitronium ion, NO_2^+ , on the toluene nucleus. A comprehensive survey of this theory has been presented by Gillespie and Millen⁽¹⁾, while Haun and Kobe⁽²⁾ have shown how an understanding of the theory is helpful in the interpretation and correlation of experimental results.

Unfortunately, most of the evidence presented by these workers in support of the nitronium ion mechanism was obtained under homogeneous conditions that could not be compared directly with conditions generally employed in commercial nitration reactors. It is evident that the acids used for mononitration

lie outside the nitronium ion; therefore, it is doubtful that the nitronium ion mechanism applies.

Liquid phase toluene mononitration under normal industrial conditions is an example of mass transfer with simultaneous chemical reaction. The problem of determining the magnitude and the nature of the resistance to interphase transfer has been avoided by much of the research on nitration kinetics, by the simple expedient of working with a solvent where all the reactants are miscible. Early work on the rate of two liquid phase heterogeneous reaction kinetics has been reviewed by Albright and Hanson^(3,4). They pointed out that, contrary to the assumption commonly made, all mass transfer resistance has not necessarily been eliminated if the reaction rate becomes constant at high levels of agitation.

Hanson and co-workers^(5,6) studied the heterogeneous mononitration of the toluene using a nitrating acid typical of that employed in industry i.e. 15 mole % HNO_3 , 30 mole % H_2SO_4 , and 55 mole % H_2O . The results were shown to be inconsistent with a simple kinetic model and it was concluded that diffusional resistances plays a more important part in determining the nitration in the two liquid phase region. This is in agreement with the extensive results for small scale reactors published during the last few years by Strachan and co-workers^(7,8,9), who have demonstrated that the overall rate can be correlated by a simple kinetic model at low sulfuric acid concentrations but that diffusional resistances become important at higher sulfuric acid concentrations. At low concentration of H_2SO_4 , the transition from kinetic to mass transfer control is obtained, and, at the higher concentration, the transition from slow to fast reaction is observed. The concentration of nitric acid becomes less important

as the overall acidity rises. At higher acidity, the concentration of sulfuric acid is more important than the nitric acid concentration. This is consistent with the effect of sulfuric acid on the kinetics of homogeneous nitration reaction. The sulfuric acid is seen as an ionizing medium for nitric acid to the nitronium, ion and so the availability of the latter increases with sulfuric acid concentrations.

As explained above, experimental data with nitrating acids of compositions typical of those employed industrially cannot be reconciled with theoretical models assuming a uniform rate of reaction through either or both phases. Such models will only apply to slow reactions. The other extreme is an instantaneous reactions, which would lead to reaction taking place at the interface. Development of a model to describe the overall rate demands a knowledge of the locale of the reaction. Conflicting opinions have been expressed in the literature as to whether any reaction takes place in the organic phase. Lewis and Suen⁽¹⁰⁾, having been able to separate the two phases rapidly and follow the disappearance of HNO_3 from the organic layer, concluded that some reaction does take place in the organic phase. Barduhn and Kobe⁽¹¹⁾, however, showed that while the HNO_3 disappears from the organic layer, there is no corresponding disappearance of toluene. Sohrabi⁽¹²⁾ has studied reaction in the organic phase and demonstrated that the maximum rate of reaction is many orders of magnitudes less than that in the aqueous phase. Thus, while some reaction may take place in the organic phase during heterogeneous nitration, its contributions to the overall rate will be extremely small ($< 0.001\%$) and can be justifiably neglected.

In the view of the above, the most realistic model to consider for toluene mononitration under these conditions appears to be that of a fast reaction tak-

ing place in a zone in the aqueous phase adjacent to the organic-acid interface. The toluene will diffuse through this zone while reacting. This is illustrated in Figure 2. The mathematical approach for this situation has been developed by Astarita⁽¹³⁾ and Danckwerts⁽¹⁴⁾.

The following steps are envisaged for the mononitration of toluene:

- (1) Toluene diffuses through the organic phase toward the interface.
- (2) From the interface the toluene diffuses into the bulk aqueous phase.
- (3) While diffusing into the aqueous phase the toluene reacts to form mononitrotoluenes.
- (4) The nitrotoluenes formed diffuses back through the aqueous phase to the interface.
- (5) From the interface the nitrotoluenes diffuses into the bulk organic phase.
- (6) Nitric acid diffuses from the bulk aqueous phase towards the interface.
- (7) While diffusing, it reacts with the toluene to form mononitrotoluenes.
- (8) The water formed diffuses back into the bulk aqueous phase.
- (9) Some nitric acid diffuses from the interface into the bulk organic phase.

For the reasons discussed above, processes 2 and 3 are probably rate determining. To simplify derivation of a model, the following assumptions can be made:

- (1) Reaction in the organic phase is negligible.
- (2) The nitronium ion, NO_2^+ , mechanism is partially applicable.
- (3) The water concentration is essentially constant throughout the aqueous phase.
- (4) The nitric acid and nitronium ion (NO_2^+) concentrations are constant

throughout the aqueous phase.

(5) There is a simple distribution relationship between the concentration of toluene in the organic phase (assumed uniform) and the interfacial concentration of toluene in the aqueous phase, i.e.

$$C_{T_o} = \Phi C_{T_A}$$

By material balance over a film of thickness dx in the reaction zone:

$$D \frac{\partial^2 C}{\partial x^2} = r(C)$$

The following boundary conditions are applicable:

At the interface:

$$C = C_{T_A} \text{ when } x = 0$$

In the bulk aqueous phase:

$$\frac{dC}{dx} = 0 \text{ when } C = C_{T_A} = 0$$

Solution of the differential equation gives the rate of reaction per unit volume of reacting mixture:

$$R = A \sqrt{2D \int_0^{C_{T_A}} r(C) dC}$$

The rate of reaction may be represented as:

$$r(C) = kC_{T_A}C_{N_A}$$

Substitution gives:

$$R = A\sqrt{DkC_{N_A}C_{T_A}^*}$$

$$R = \frac{A}{\phi} \sqrt{DkC_{N_A}C_{T_0}}$$

In conclusion it is clear that whether the two phase nitration of toluene is kinetically or mass transfer control depends on the relative values of kC_{N_A} and the mass transfer coefficient. If the value of kC_{N_A} is very much smaller than the mass transfer coefficient, the rate will be kinetically controlled, whereas if it is very much greater than the mass transfer coefficient, the rate will be mass transfer controlled.

In other word most workers are agreed that in the two phase system the toluene nitration occurs almost exclusively in the acid phase. Batch reactor studies show that at low acid strengths the rate is kinetically controlled and given by:

$$R_a = kC_{N_A}C_{T_A}$$

where k is the rate constant for homogeneous nitration in the acid phase, and C_{N_A} and C_{T_A} are the acid phase concentrations of nitric acid and toluene respectively. Over a short range of acid strength a slow reaction diffusional regime in which the rate is given by:

$$R_a = a'k_m C_{T_A}$$

where a' is the interfacial area per unit volume of the acid phase and k_m is the overall mass transfer coefficient. Finally at high acid strengths a fast reaction regime is observed where the rate is given by:

$$R_a = a'\sqrt{Dk_m C_{N_A} C_{T_A}}$$

where D is the diffusivity of toluene in the acid phase.

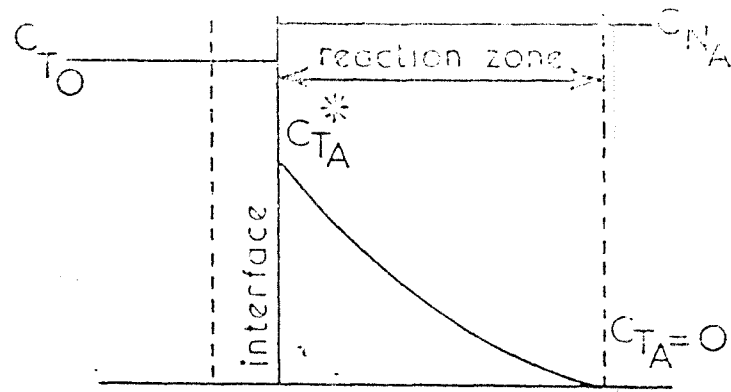


Figure: 2

Interfacial concentration profile assumed
in model

CHAPTER V

MONONITROTOLUENE ISOMER PRODUCTION

It is well known that nitration of aromatic molecules produces a number of isomeric products. According to literature data the mononitration of toluene can yield products in which the ratio of the orthonitrotoluene to pararnitrotoluene varies between 1.41 and 1.62 depending on the nitrating agent and the reaction conditions used.

These mononitrations are carried out industrially on a considerable scale to produce compounds which are required as intermediates for the manufactures of dyestuffs, pharmaceuticals, etc. In most cases the para isomer is required while the ortho and meta products are waste products. Thus, with increasing cost of raw materials and the environmental problems in disposing of waste isomers, any increase in the percentage of the desired isomers represents a considerable process improvement.

A wide range of nitrating agents have been used in industrial scale nitration. The a nitrating agent should be available in sufficient quantity, reasonably cheap and relatively stable. A mixture of nitric acid and sulphuric acid, called mixed acid, is normally used as the nitrating agent for large scale industrial nitrations. The mixture has been used under varying conditions for industrial nitrations for many years. Information on the relationship between the composition of the nitrating mixture and the composition of the reaction product is, however, scarce and tend to be unsystematic.

There are three variables in the composition of the sulfuric/nitric acid nitrating mixture:

- (i) Nitric acid content,
- (ii) Water content,
- (iii) Sulfuric acid concentration.

A few preliminary experiments done by different workers at different times indicate that the concentration of nitric acid did not effect the composition of the reaction product, as long as there was sufficient of nitric acid to mononitrate all of the toluene present. All further experiments were carried out with a slight excess of nitric acid, i.e. 1.04 moles nitric acid/mole of toluene. A series of experiments was then carried out to investigate the effect of water and sulfuric acid concentrations in the nitrating mixture on the composition of the reaction products. The results of these experiments are illustrated by Figures 3-7.

Figure 3 shows a plot of a reaction product composition vs. moles H_2SO_4 for a nitrating mixture which contains too little water for satisfactory mononitration. It is observed in the figure that an excessive amount of dinitration products are produced even at relatively low sulfuric acid concentrations, and consequently considerable quantities of toluene remain unreacted.

Figure 4 show a more satisfactory situation where there is more water (1.78 moles) in the nitrating mixture. The reaction products contain only traces of unreacted toluene and dinitration.

Figure 5 shows the effect of variation in water content in nitrating mixture containing 1.17 moles sulfuric acid -the optimum H_2SO_4 concentration in figure 3. In all of these experiments the amount of ortho- and paranitrotoluenes,

unconverted toluene and dinitration products varied with water or sulfuric acid concentration. Apart from extreme conditions, (Figure 3), the amount of metanitrotoluene remained constant at about 4%.

Figures 6 and 7 show the effect of variation in sulfuric acid and water content of the nitrating mixture on the ortho/para isomer ratio of mononitrotoluenes in the reaction products. The o/p isomer ratio decreases with increase in sulfuric acid content of the mixture and increases with the increase in water concentration. Examination of Figure 3 shows that some of the decrease in o/p ratio with increase in sulfuric acid concentration is due to the fact that the o-nitrotoluene dinitrates more readily than the para isomer. Thus the increase in the amount of para isomer, which can be produced by varying the composition of nitrating mixture, is limited if excessive amount of dinitration products are to be avoided.

The optimum conditions for mononitration are shown in Figure 3 - a nitrating mixture containing 1.17 moles sulfuric acid and 1.78 moles water giving a reaction product containing 36.5% p-nitrotoluene, 59.5% o-nitrotoluene and 4% m-nitrotoluene. $o/p = 1.63$.

1.04 moles HNO_3
0.63 moles H_2O

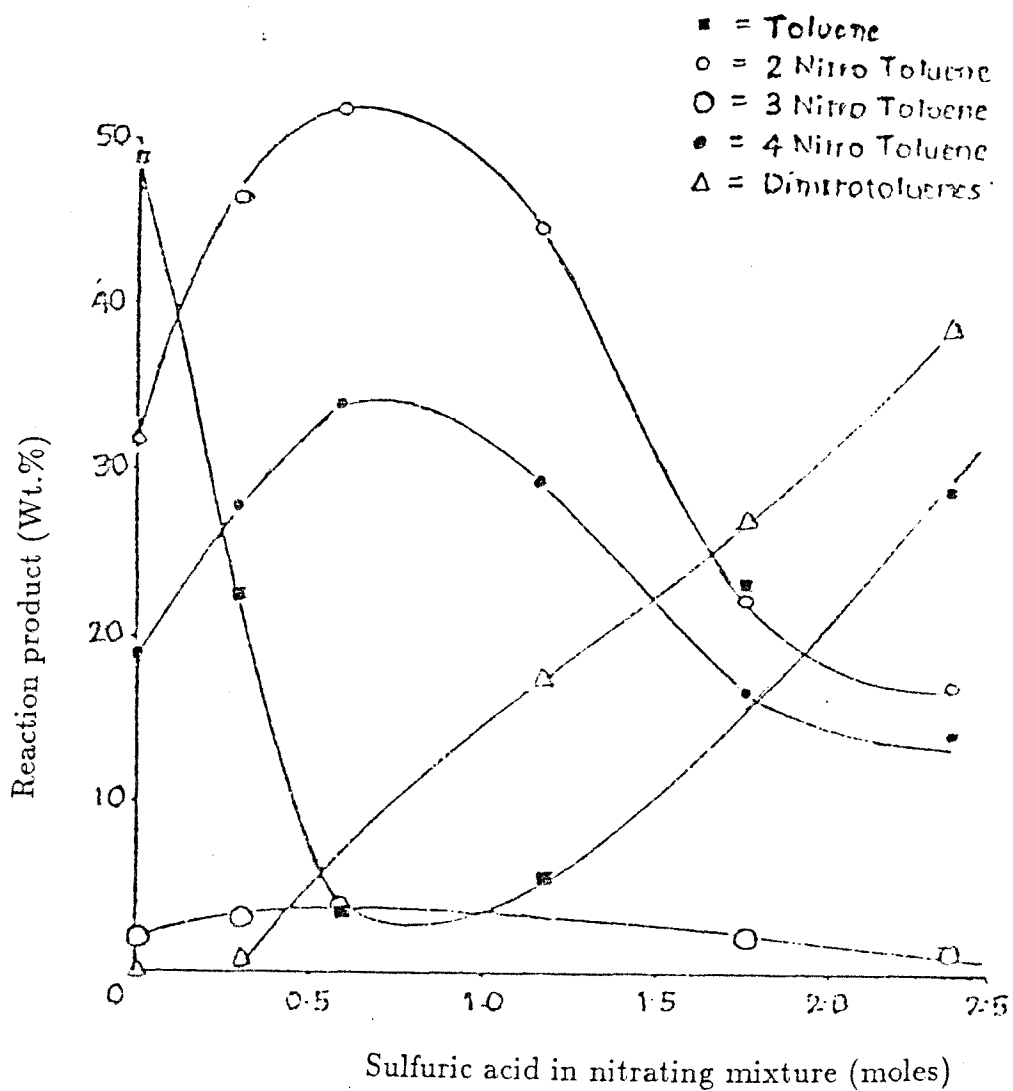


Figure: 3.

Reaction product composition vs. Sulfuric acid content
of nitrating mixture

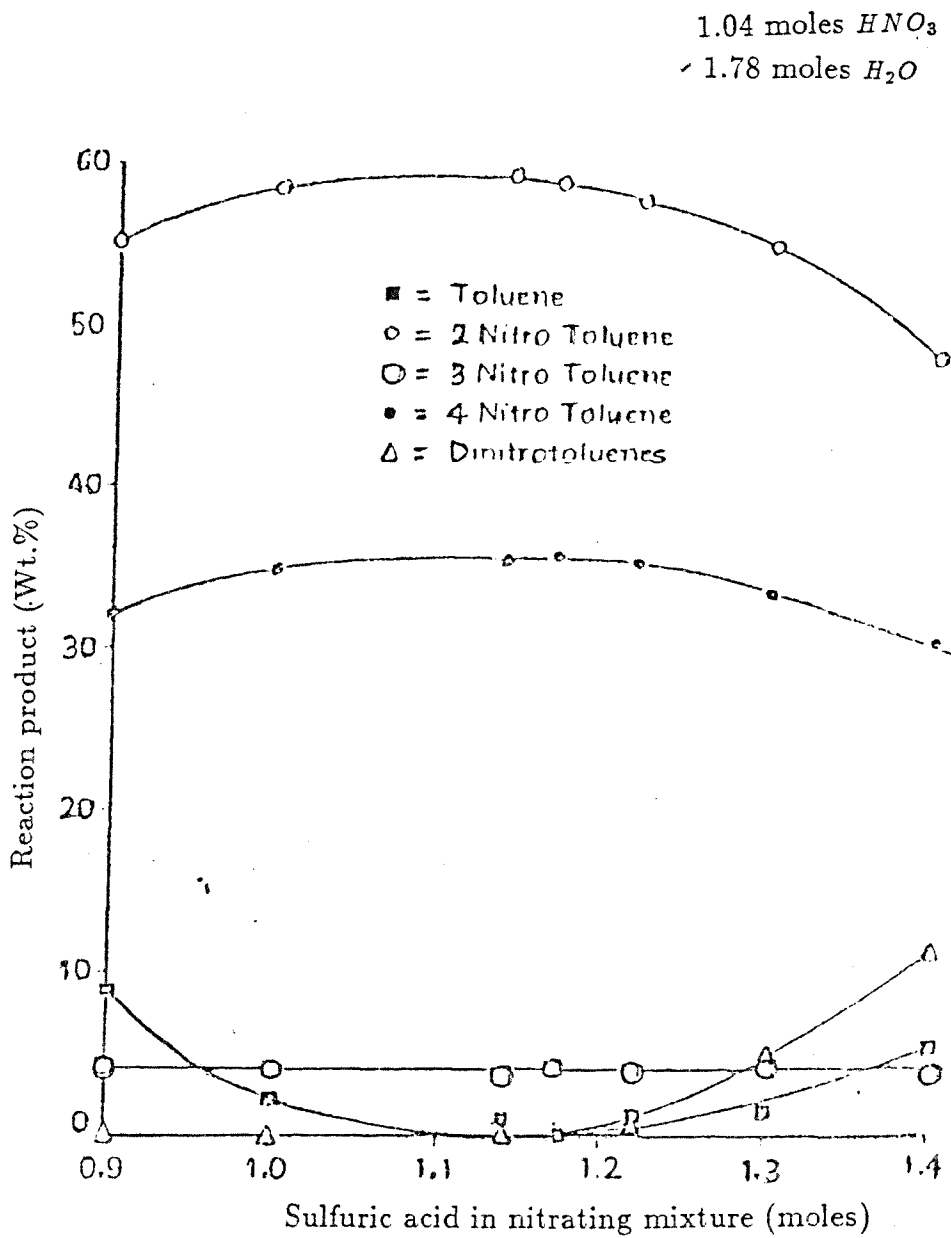


Figure: 4

Reaction product composition vs. Sulfuric acid content
of nitrating mixture

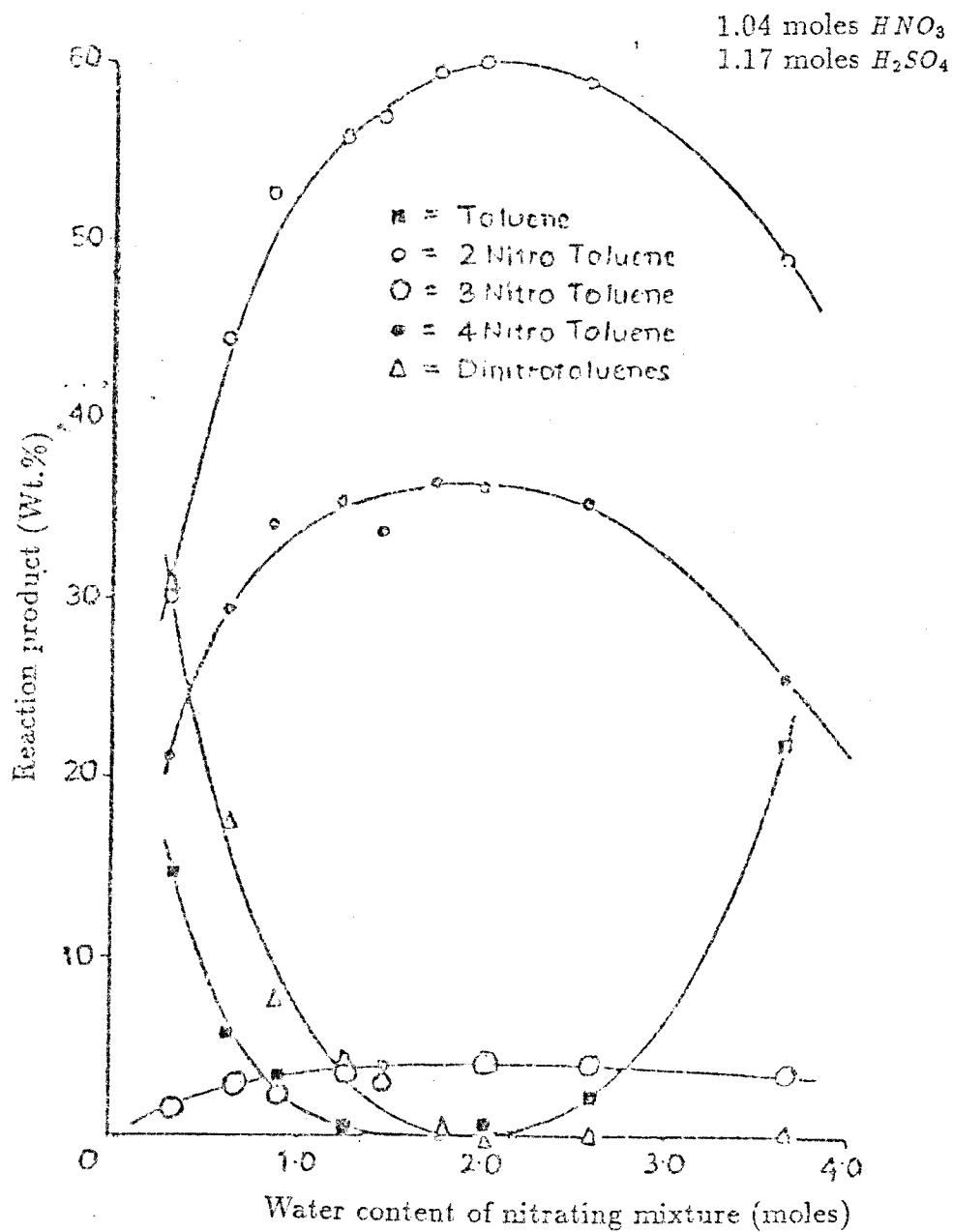


Figure: 5
Reaction product composition vs. Water content
of nitrating mixture

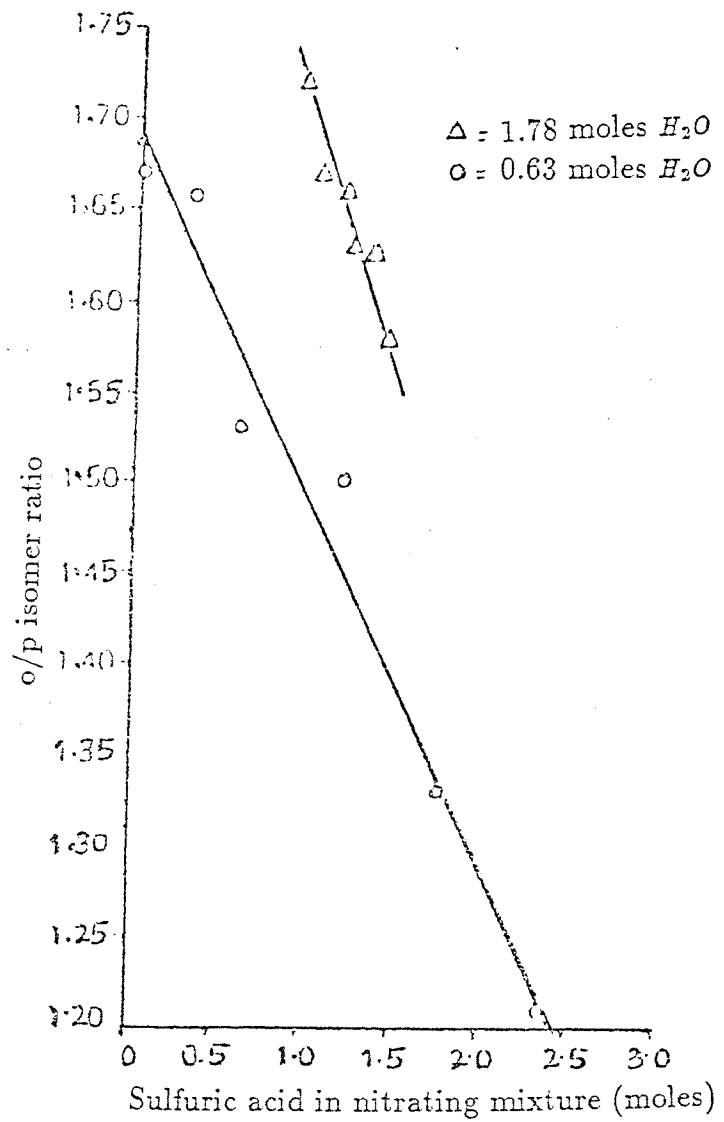


Figure: 6

o/p isomer ratio vs. sulfuric acid content
of nitrating mixture

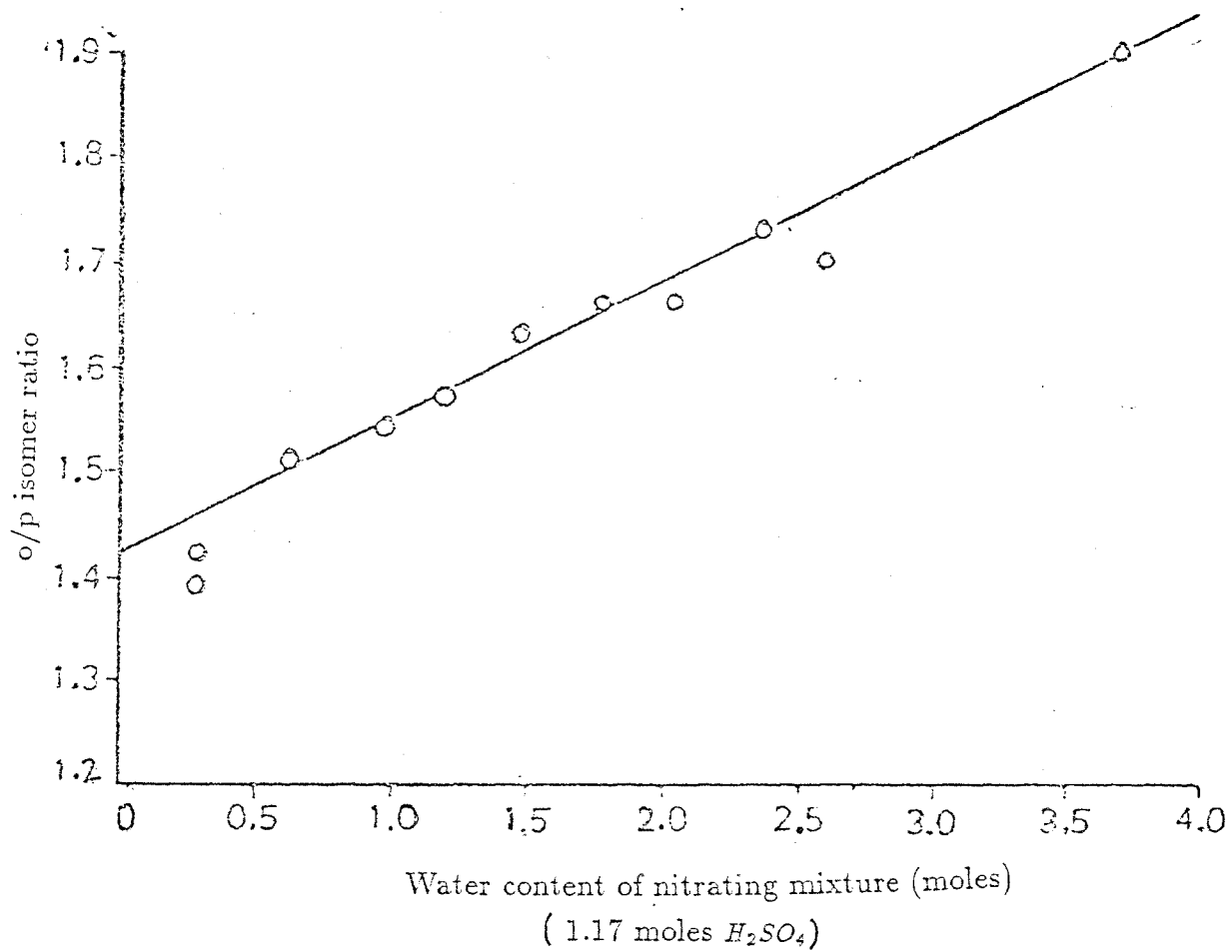


Figure: 7

o/p isomer ratio vs. Water content of nitrating mixture
(H₂SO₄ content 1.17 moles)

CHAPTER VI

FACTORS EFFECTING THE RATE OF REACTION

Effect of agitation speed

The results of the study of the reaction rate as a function of stirrer speed, with temperature as a parameter, are shown in Figure 8. Although this work greatly extends previously published data with respect to the range of agitation speed and temperature studied, the results follows the same pattern as those reported by McKinley and White⁽¹⁵⁾, Biggs and White⁽¹⁶⁾, and Barduhn and Kobe⁽¹¹⁾. These authors claim that the lower part of the curve represents a mass transfer controlled region. After a transition period, a region is found where rate appears relatively insensitive to agitation speed. In this latter region it has been claimed previously that mass transfer resistances have been eliminated. The implication of this hypothesis is that the organic and acid solutions are mutually saturated and that, under steady state conditions, the rate of mass transfer is equal to the rate of reaction. If this is so, the reaction rate would be independent of agitation speed and would give a curve of zero slope. The present results extend well past the transition range and yet they still show a small but definite positive gradient. This naturally prompts a deeper study of the inherent assumptions.

Effect of temperature

The other parameter to effect the rate is temperature. Previous measurement of the effect of temperature on the two phase nitration of toluene has

been variously interpreted. It is claimed that the rate of mononitration increases almost double with 10 °C increase in temperature up to some extent and beyond that limit where the dinitration products being are formed. There has been general agreement that where the rate is mass transfer controlled, a low temperature coefficient is to be expected. But, there has been disagreement on the magnitude of the experimental temperature coefficient and on whether it is to be regarded as high or low. Such a variation would be consistent with the fact that any mass transfer resistance will tend to become more prominent as the temperature is raised.

Since the temperature effect on mass transfer coefficient is very much less than that of chemical reactions, the validity must be questioned of using an overall temperature coefficient as a criterion of mass transfer control in such a system. Not only will temperature influence these resistances, it will also affect the distribution coefficients of the reactants between the phases, and hence the concentration of each phases, and also the concentration of the nitrating species. There are insufficient data available on the aqueous nitric acid-sulfuric acid system to allow calculations of nitronium ion concentration.

It can be readily seen that the effect of temperature on the nitration of toluene is very complex and cannot be used as evidence of kinetic control or mass transfer control of the reaction.

Effect of space time

Previous workers used space time as a test for a simple kinetic model, by operating it with a fixed feed rate, fixed agitation rate and at a constant temper-

ature. The results were analyzed on the assumption that the following kinetic rate equation applies:

$$R = k' C_{T_A} C_{T_0}$$

The constant k' includes the distribution coefficient for toluene between the two phases, the assumption being that reaction takes place homogeneously throughout the aqueous phase or atleast at the interface. The value of k' was found to vary with space time and this was taken as evidence for mass transfer control.

Previously, it was assumed that all the nitric acid would be present in the aqueous phase. As was shown earlier, a little but considerable quantities of nitric acid were found in the organic phase. This extraction of nitric acid into the organic phase effectively reduces the amount available for reaction and so decreases the rate of reaction. This was observed by McKinley and White⁽¹⁵⁾ and by Barduhn and Kobe⁽¹¹⁾. Thus it can only be concluded that the above equation is not the true rate equation, or that the measured rate includes a contribution from mass transfer.

Effect of phase inversion

A convenient criterion for the existance of a mass transfer resistance which has not been widely used in the past is the effect of phase inversion. This leads to change in both interfacial area per unit volume and mass transfer coefficients. The difference in the degree of conversion provides conclusive proof for the presence of a mass transfer resistance and a need for a rate model which takes

this in to account. It is also abundantly clear that the failure to eliminate the mass transfer resistance in the early work was not a function of scale and that the effect is likely to be of importance in industrial reactors, certainly with nitrating acid containing 30 mole % H_2SO_4 .

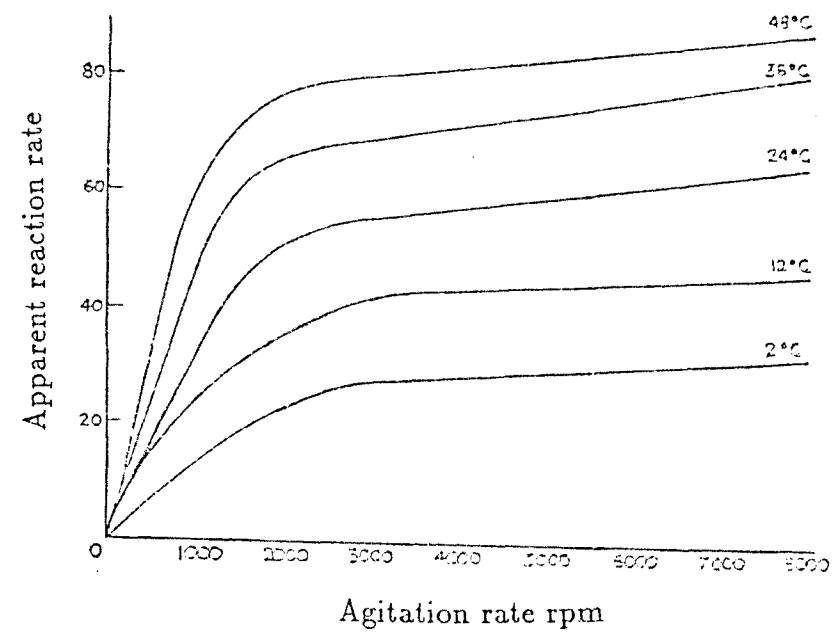


Figure: 8
Apparent reaction rate as a function of agitation
and temperature

CHAPTER VII

MONONITRATION PRODUCTS

o-Nitrotoluene is used in the synthesis of intermediates for azo dyes, sulfur dyes, rubber chemicals and agricultural chemicals. Typical intermediates are *o*-toluidine, *o*-nitrobenzaldehyde, 2-nitro-4-chlorotoluene, 2-nitro-6-chlorotoluene, 2-amino-4-chlorotoluene, and 2-amino-6-chlorotoluene. *p*-Nitrotoluene is used principally in the production of intermediates for azo dyes and sulfur dyes. Typical intermediates are *p*-toluidine, *p*-nitrobenzaldehyde, and 4-nitro-2-chlorotoluene. *m*-Nitrotoluene has no known major uses, hence it is an undesirable byproduct, and should be avoided in the selective operation of the reaction step in the mononitrotoluene synthesis.

Physical properties

o-Nitrotoluene is a clear yellow liquid. It is infinitely soluble in benzene, diethyl ether and ethanol. It is soluble in most organic solvent and only slightly soluble in water. The electron-acceptor action of the nitro group in *o*-nitrotoluene confers increased reactivity on the methyl group, thus the methyl group is easily oxidized. The physical properties of *o*-nitrotoluene are listed in Table 1.

m-Nitrotoluene is a clear yellow liquid. It is infinitely soluble in ethanol, benzene and diethyl ether. It is soluble in most organic solvent and only sparingly soluble in water. *m*-Nitrotoluene does not have an active methyl group as do the ortho and para isomers. The physical properties of *m*-nitrotoluene are listed in Table 1.

p-Nitrotoluene crystallized in colorless rhombic crystals. It is only slightly soluble in water, moderately soluble in methanol and ethanol. It is readily soluble in acetone, benzene and diethyl ether. The physical properties of o-nitrotoluene are listed in Table 1.

Table: 1

The physical properties of Mononitrotoluenes (MNT)

Properties	o-NT	m-NT	p-NT
B.P. °C	222	233	238
M.P. °C	9.5	16	52
Density gm/cc	1.163	1.157	1.104
Viscosity cP (15 °C)	0.0262	0.0178	0.0120
H _i KJ/Kg	344	364	366

Analytical and test methods

o-Nitrotoluene can be analyzed for purity and isomer content by IR spectroscopy with an accuracy of 1%. p-Nitrotoluene content can be estimated by the decomposition of the isometric toluene diazonium chlorides since the ortho and meta isomers decompose more rapidly than the para isomer. A colorimetric method for determining the contents of the various isomers is based upon the color which forms when the mononitrotoluenes are dissolved in sulfuric acid. From the absorption of the sulfuric acid solution at 436 and 305 nm, the ortho and para isomer content can be determined, and the meta isomer can be obtained by difference. However, this and other colorimetric methods are subject to possible interferences from other aromatic nitro compounds.

A titrametric method, which is based on the reduction of the nitro groups with titanium(III) sulfate or chloride, can be used to determine mononitrotoluenes. Chromatographic methods, eg. gas chromatography or higher pressure liquid chromatography, are well-suited for the determination of mononitrotoluenes as well as its individual isomers. Freezing points are used commonly as indicators of purity of the various isomers.

Health and safety consideration

The toxic effects of mononitrotoluenes as well as its individual isomers are similar to but less pronounced than those of nitrobenzene. The maximum allowable concentration for mononitrotoluenes is 5 ppm (30 mg/m³). Mononitrotoluenes may be absorbed through the skin and respiratory tract. The mononitrotoluenes represent moderate fire hazards when exposed to heat or flame. Impervious protective clothing should be worn in the area where risk of splash exists. Ordinary work clothes should be removed immediately, and the skin should be washed thoroughly with soap and warm water. In case of high vapor concentration, full facemasks with organic-vapor canisters or air supplied respirators should be used. Clean work clothing should be worn daily, and showering after each shift should be made mandatory.

CHAPTER VIII

PROGRAM DISCRIPTION

The objective of the computer program is to simulate a rigorous multicomponent batch distillation column. The computer model was originally developed by R. Springer for petroleum crude analysis. It has been being modified and made usable for nitrotoluene system. The source code is attached herewith shown in Appendix A.

The input data for the program was calculated by various approximation methods since there is limited data available in the literature for the nitrotoluenes. A plant material balance is done according to the 1000 lbs of MNT production per batch. In the calculation of vapor enthalpy of dinitrotoluene, the enthalpy of vaporization was calculated by Carruth and Kobayashi equation. The vapor pressure and the liquid molar volume for all nitrotoluenes are calculated by the Lee-Kesler method.

As discussed earlier, we are using two batch distillation columns for the whole separation process. The first column is used to remove the unreacted toluene and the trace amount of water. The second column is used for the recovery of the isomers formed in the mononitration of toluene with the dinitration products left in the still pot. The computer model was used to evaluate both separations. The input and output for both the cases are shown in the Appendix B and C respectively. Summarized in the following table is the results of the simulated batch separation.

Column 1

	Feed charged in lbmoles	Feed remaining in still, lbmole
Water	0.002	0.0
Toluene	1.316	0.8E-10
o-NT	9.486	0.3785
m-NT	0.643	0.1327
p-NT	5.865	1.930
DNT	0.002	0.002

Column 2

	Feed charged in lbmoles	Feed remaining in still, lbmole
o-NT	9.486	0.147E
m-NT	0.643	0.250E
p-NT	5.865	0.9362
DNT	0.002	0.002

CHAPTER IX

RECOMMENDATIONS

A subsidiary objective of the work described was to obtain an insight into scale-up criteria for a batch nitrator operating under industrial conditions. The rate controlling mechanism is still not completely known. Previous studies of the reaction mechanism were done by avoiding the mass transfer effect. Presently in the literature is evidence to prove that the mass transfer effect can not be completely neglected. Thus, it is very important to study the rate of diffusion taking place during the reaction. A knowledge of diffusional resistances associated with the toluene nitration will help in an understanding the of mechanism.

Other important criteria of the process is control of isomers distribution. One of the most desirable isomer is para MNT which has a wide use in the dyes industry. Some measure of control over the isomer distribution resulting from the mixed acid nitration of toluene is possible but only under severe constraints and far from the conditions normally employed for efficient mononitration. It is very important to have a nitrating agent which can maximize the desired product and can improve our control on the isomer distribution of MNT. The effects that are observable appear to be best explained by mass transfer influences. Although alternative methods of nitration do offer greater latitude in the determination of the isometric content, none can be accomplished with the convenience, speed, and low cost of the mixed acid, nitrating agent.

In summary, it is highly recommended to extend the study of this process to combine the reaction, crude MNT wash, and the separation sections of the

total process, and evaluate the process conditions of reaction to maximize the ortho-para isomers of MNT.

APPENDICES

- (A) Source Program.
- (B) Input and Output for the first column.
- (C) Input and Output for the second column.

Appendix: A

Source Program

BATCH DISTILLATION COMPUTER PROGRAM

AUTHOR - RONALD D. SPRINGER (MAY,1985)
MASTERS THESIS AT NEW JERSEY INSTITUTE OF TECHNOLOGY

REVISED BY: NITIN K. SHAH
NJIT, NEWARK, NJ
21 SEPTEMBER, 1989

THIS VERSION IS IN DOUBLE PRECISION

INTERNAL SUBROUTINES:

MAIN - CONTROLS ALL CALCULATIONS
CPU - CALCULATES AND PRINTS CPU TIME (OPTIONAL)
INPUT - READS INPUT
CDATA - CURVE FITS THERMODYNAMIC DATA
REGRSS - PERFORMS LINEAR REGRESSION FOR THERMODYNAMIC COEFFICIENTS
CNSTNT - CALCULATES CONSTANTS
CONVRT - CALCULATES MOLE, WEIGHT, AND LIQUID VOLUME
STEADY - MAIN ROUTINE FOR STEADY-STATE TOTAL-REFLUX CALCULATIONS
INITAL - INITIALIZES STEADY-STATE TOTAL-REFLUX CALCULATION
BUBBLE - CONVERGES BUBBLE POINT TEMPERATURE
MATSOL - SOLVES STEADY-STATE TOTAL-REFLUX MATRIX
MATINV - INVERTS MATRIX USING JERSYLIB ROUTINE
SETUP - SETS-UP STEADY-STATE TOTAL-REFLUX MATRIX
THERMO - CALCULATES THERMODYNAMIC DATA
CONVRG - CHECKS CONVERGENCE AND DETERMINES NEW VALUES FOR STDY-STE
HTBAL - CALCULATES FLOWS FOR STEADY-STATE TOTAL-REFLUX
SPRINT - PRINTS STEADY-STATE TOTAL-REFLUX RESULTS
UNSTDY - MAIN ROUTINE FOR UNSTEADY-STATE BATCH DISTILLATION CALCS
MAXBON - CALCULATES NORMAL BOILING POINT USING MAXWELL-BONNELL
FUNCT - CALCULATES DX/DT FOR LSODE
JACOB - CALCULATES JACOBIAN FOR LSODE
UPRINT - PRINTS UNSTEADY-STATE BATCH DISTILLATION RESULTS
LSODE - LIVERMORE SOLVER FOR ORDINARY DIFFERENTIAL EQUATIONS

EXTERNAL SUBROUTINES:

KSIMEQ - JERSYLIB ROUTINE FOR INVERTING A MATRIX
READ,WRITE - READS DATA FROM AND WRITES DATA TO FILES
WIPE - SETS VARIABLES TO ZERO
SETCPU,GETCPU - USED FOR CPU TIME (OPTIONAL)
EXIT - EXITS PROGRAM (OPTIONAL)

COMMON BLOCKS

FILE:

IIN - READ FILE
IOUT - WRITE FILE

PROP:

CNBP(50) - COMPONENT NORMAL BOILING POINT, DEGF
CMW(50) - COMPONENT MOLECULAR WEIGHT, LB/LBMOLE
CDEN(50) - COMPONENT LIQUID DENSITY AT 60 DEGF, LB/GAL
TF(8) - TEMPERATURE DATA POINTS, DEGF
CVP(50,8) - COMPONENT VAPOR PRESSURE DATA, MMHG
CHV(50,8) - COMPONENT VAPOR ENTHALPY DATA, KBTU/LBMOLE
CHL(50,8) - COMPONENT LIQUID ENTHALPY DATA, KBTU/LBMOLE
CVM(50,8) - COMPONENT LIQUID MOLAR VOLUME DATA, GAL/LBMOLE
COEFVP(50,4) - COMPONENT VAPOR PRESSURE COEFFICIENTS
- $\text{LN}(\text{VP}) = A + B/T + C/T^{**2} + D/T^{**3}$, T=DEGR

C COEFHV(50,4) - COMPONENT VAPOR ENTHALPY COEFFICIENTS
 C - $HV = A + B*T + C*T**2 + D*T**3$, T=DEGR
 C COEFHL(50,4) - COMPONENT LIQUID ENTHALPY COEFFICIENTS
 C - $HL = A + B*T + C*T**2 + D*T**3$, T=DEGR
 C COEFVM(50,4) - COMPONENT LIQUID MOLAR VOLUME COEFFICIENTS
 C - $VM = A + B*T + C*T**2 + D*T**3$, T=DEGR
 C
 C DATAIN:
 C FR - FEED CHARGE READ
 C ZR(50) - FEED COMPOSITION READ
 C EMR - MURPHREE EFFICIENCY READ
 C PCOND - CONDENSER PRESSURE, MMHG
 C DPCOND - CONDENSER PRESSURE DROP, MMHG
 C DPTRAY - STAGE PRESSURE DROP, MMHG
 C GCOND - CONDENSER VOLUME HOLDUP, GALLON
 C GTRAY - STAGE VOLUME HOLDUP, GALLON
 C QTRAY - STAGE HEAT DUTY, KBTU/HR
 C TTIMES - TOTAL TIME SAVE, HOURS
 C IFR - FEED UNITS READ, 1=MOLE, 2=WEIGHT, 3=VOLUME
 C
 C DATA:
 C F - FEED CHARGE, LBMOLE
 C Z(50) - FEED COMPOSITION, MOLE FRACTION
 C P(40) - STAGE PRESSURE, MMHG
 C G(40) - STAGE VOLUME HOLDUP, GALLON
 C Q(40) - STAGE HEAT DUTY, KBTU/HR
 C EM(40,50) - MURPHREE EFFICIENCY
 C FC - CONVRT VARIABLE, TOTAL
 C ZC(50) - CONVRT VARIABLE, COMPOSITION
 C CF(6) - MOLE, WEIGHT, VOLUME TOTALS AND PERCENTS
 C CZ(50,6) - MOLE, WEIGHT, VOLUME COMPOSITIONS AND PERCENTS
 C RR - MOLAR REFLUX RATIO
 C DR - LIQUID DISTILLATE RATE, LBMOLE/HR
 C FCUT - FEED CUT CHARGE, LBMOLE
 C ZCUT(50) - FEED CUT COMPOSITION, MOLE FRACTION
 C TCUT(15) - TEMPERATURE CUT POINTS, DEGF
 C DMAX - MAXIMUM PERCENT CHANGE (50.0)
 C TOL - CONVERGENCE PERCENT TOLERANCE (0.001)
 C NAME(50,3) - COMPONENT NAME
 C MAXIT - MAXIMUM ITERATIONS (15)
 C N - NUMBER OF COMPONENTS, 2 TO 50
 C M - NUMBER OF STAGES INCLUDING CONDENSER AND REBOILER, 2 TO 40
 C M1 - M - 1
 C IC - CONVRT VARIABLE, UNITS
 C INITL - NUMBER OF INITIALIZATION IMPROVEMENTS
 C IPRNT - PRINT LEVEL, 0=MINIMUM, 1=CUT COMPOSITIONS, 2=STAGE
 C - COMPOSITIONS, 3=INTERMEDIATE, 4=DEBUG
 C
 C REGR:
 C X(8) - REGRESSION INDEPENDENT VARIABLE
 C Y(8) - REGRESSION DEPENDENT VARIABLE
 C C(4,8) - REGRESSION MATRIX
 C D(4) - REGRESSION RIGHT-HAND SIDE
 C COEF(4) - REGRESSION COEFFICIENTS
 C
 C SCALC:
 C T(40) - STAGE TEMPERATURE, DEGF
 C AL(40) - STAGE LIQUID RATE, LBMOLE/HR
 C V(40) - STAGE VAPOR RATE, LBMOLE/HR
 C U(40) - STAGE MOLAR HOLDUP, LBMOLE

C X(40,50) - STAGE LIQUID COMPOSITION, MOLE FRACTION
 C Y(40,50) - STAGE VAPOR COMPOSITION, MOLE FRACTION
 C DT(40) - STAGE DELTA T
 C DL(40) - HTBAL VARIABLE
 C DV(40) - HTBAL VARIABLE
 C DU(40) - STAGE DELTA U
 C DX(40,50) - STAGE DELTA X
 C SUMDX(40) - STAGE SUM DELTA X
 C AK(50) - COMPONENT EQUILIBRIUM CONSTANT, VP/P
 C HV(50) - COMPONENT VAPOR ENTHALPY, KBTU/LBMOLE
 C HL(50) - COMPONENT LIQUID ENTHALPY, KBTU/LBMOLE
 C VM(50) - COMPONENT LIQUID MOLAR VOLUME, GAL/LBMOLE
 C DKDT(50) - AK TEMPERATURE DERIVATIVE
 C DHVDT(50) - HV TEMPERATURE DERIVATIVE
 C DHLDT(50) - HL TEMPERATURE DERIVATIVE
 C DVMDT(50) - VM TEMPERATURE DERIVATIVE
 C SCALE - CONVERGENCE SCALING FACTOR
 C CONV - CONVERGENCE INDICATOR FACTOR
 C ICONV - CONVERGENCE INDICATOR, 0=CONVERGED
 C ITER - ITERATION NUMBER
 C
 C MATRIX:
 C A(52,52) - A MATRIX
 C B(52,52) - B AND B INVERSE MATRIX
 C C(52,52) - C MATRIX
 C D(52) - D MATRIX
 C DM(52) - D MATRIX FOR M STAGE
 C AHOLD(52,52) - A MATRIX SAVE
 C CHOLD(52,52) - C MATRIX SAVE
 C DHOLD(52) - D MATRIX SAVE
 C ILAST - FILE MARKER
 C I1 - MATRIX CONSTANT
 C I2 - MATRIX CONSTANT
 C
 C CLSODE:
 C XT(2000) - LSODE DEPENDENT VARIABLE, X
 C RWORK(26022) - LSODE REAL WORK ARRAY
 C IWORK(2020) - LSODE INTEGER WORK ARRAY
 C
 C UCALC:
 C SAK(40) - STAGE SUM AK*X
 C SHV(40) - STAGE SUM HV*Y
 C SHL(40) - STAGE SUM HL*X
 C SVM(40) - STAGE SUM VM*X
 C SDKDT(40) - STAGE SUM DKDT*X
 C SDHLD(40) - STAGE SUM DHLDT*X
 C SDVMDT(40) - STAGE SUM DVMDT*X
 C SAKY1(40) - STAGE SUM AK*Y(J+1)
 C SAKX1(40) - STAGE SUM AK*X(J-1)
 C SAKY(40) - STAGE SUM AK*Y
 C SHLY1(40) - STAGE SUM HL*Y(J+1)
 C SHLX1(40) - STAGE SUM HL*X(J-1)
 C SHLY(40) - STAGE SUM HL*Y
 C SVMY1(40) - STAGE SUM VM*Y(J+1)
 C SVMX1(40) - STAGE SUM VM*X(J-1)
 C SVMY(40) - STAGE SUM VM*Y
 C AKS(40,50) - AK SAVE
 C DTD(40) - STAGE TEMPERATURE TIME DERIVATIVE
 C DUD(40) - STAGE HOLDUP TIME DERIVATIVE
 C DHDT(40) - STAGE LIQUID ENTHALPY TIME DERIVATIVE

C
C SUBROUTINE VARIABLES:
C I - COMPONENT INDICATOR
C J - STAGE INDICATOR
C K - LOOP VARIABLE
C L - ARGUMENT VARIABLE
C ZZ(20) - INPUT REPRINT
C NOPER - OPERATING STEP NUMBER
C NT - NUMBER CPU CALLS
C NDUM - CPU DUMMY VARIABLE
C TIME - TOTAL CPU TIME
C DTIME - DELTA CPU TIME
C STIME - START CPU TIME
C II - INPUT COMPONENT NUMBER
C DEV - CDATA PERCENT DEVIATION
C SUM - SUMMATION VARIABLE
C JJ - STAGE INDICATOR
C UU - INITAL HOLDUP VARIABLE
C DTI - DELTA BUBBLE POINT TEMPERATURE
C TOLB - BUBBLE POINT CONVERGENCE TOLERANCE
C ERROR - CONVERGENCE ERROR
C SUMKX - BUBBLE POINT SUM AK*X
C SUMDKX - BUBBLE POINT SUM DKDT*X
C K1 - MATSOL LOOP VARIABLE
C K2 - MATSOL LOOP VARIABLE
C K3 - MATSOL LOOP VARIABLE
C IFILE - READ AND WRITE FILE NUMBER
C BB - KSIMEQ MATRIX
C IN - KSIMEQ MATRIX DIMENSION
C IER - KSIMEQ SINGULAR MATRIX INDICATOR
C TR1 - THERMO TEMPERATURE, DEGR
C TR2 - TR1**2
C TR3 - TR1**3
C TR4 - TR1**4
C DELX - DELTA X
C XNEW - NEW X
C XSUM - SUM X
C XTOL - X CONVERGENCE TOLERANCE
C YSUM - SUM Y
C MF - LODE METHOD FLAG
C LIW - LODE IWORK LENGTH
C LRW - LODE RWORK LENGTH
C NEQ - LODE NUMBER OF ORDINARY DIFFERENTIAL EQUATIONS
C ATOL - LODE ABSOLUTE ERROR TOLERANCE
C IOPT - LODE OPTIONAL INPUT FLAG
C ITOL - LODE ERROR INDICATOR
C RTOL - LODE RELATIVE ERROR TOLERANCE
C TIME - LODE INDEPENDENT VARIABLE, TIME, HOURS
C TOUT - LODE FIRST TIME
C ITASK - LODE TASK INDEX
C ISTATE - LODE STATE INDEX
C ITC - CUT NUMBER
C TTIME - TOTAL TIME, HOURS
C TIMCUT - CUT TIME, HOURS
C SG - SPECIFIC GRAVITY OF DISTILLATE
C TF - OVERHEAD TEMPERATURE, DEGF
C PMMHG - DISTILLATE PRESSURE, MMHG
C TNBP - OVERHEAD NORMAL BOILING POINT
C TNBP12 - OVERHEAD NORMAL BOILING POINT (K=12)
C A - MAXBON VARIABLE

```

C      F      - MAXBON VARIABLE
C      TR     - MAXBON VARIABLE
C      WK     - MAXBON VARIABLE
C      PATM   - MAXBON VARIABLE
C      PLOG   - MAXBON VARIABLE
C      THIRD  - MAXBON VARIABLE
C      DXDT   - X COMPOSITION TIME DERIVATIVE
C      ML     - JACOBIAN HALF-BANDWIDTH
C      MU     - JACOBIAN HALF-BANDWIDTH
C      PD     - JACOBIAN MATRIX
C      NROWPD - JACOBIAN MATRIX DIMENSION
C
C      MAIN ROUTINE CONTROLS ALL CALCULATIONS
C      IMPLICIT REAL*8(A-H,O-Z)
C      COMMON /FILE/
C      1 IIN,          IOUT
C      REAL ZZ(20)
C
C      SET READ AND WRITE FILES
C
C      IIN = 5
C      IOUT = 6
C
C      PRINT INPUT
C
C      REWIND IIN
C      1 READ(IIN,2,END=4) ZZ
C      WRITE(IOUT,3) ZZ
C      GO TO 1
C      2 FORMAT(20A4)
C      3 FORMAT(1X,20A4)
C      4 REWIND IIN
C      CALL CPU
C
C      READ INPUT, CALCULATE THERMODYNAMIC DATA AND CONSTANTS
C
C      NOPER = 0
C      10 CALL INPUT ( NOPER, &99 )
C      IF( NOPER .EQ. 0 ) CALL CDATA
C      CALL CNSTNT(NOPER)
C      CALL CPU
C
C      CALCULATE STEADY-STATE TOTAL REFLUX
C
C      CALL STEADY(&99)
C      CALL CPU
C
C      CALCULATE UNSTEADY-STATE BATCH DISTILLATION
C
C      CALL UNSTDY(&99)
C      CALL CPU
C
C      NEXT OPERATING STEP
C
C      NOPER = NOPER + 1
C      GO TO 10
C
C      TERMINATING
C
C      99 WRITE(IOUT,900)

```



```

CALL CONVRT(1)
CALL CPU
WRITE(IOUT,910)
CALL EXIT
STOP
C
900 FORMAT(1H1/20X,'F E E D   C H A R G E   (REMAINING IN STILL)')
910 FORMAT(/' BATCH TERMINATING')
END
SUBROUTINE CPU
C
C   CALCULATES AND PRINTS LAPSED CPU TIME IN SECONDS
C
COMMON /FILE/  IIN,  IOUT
DATA NT/-1/
C
C   NT = NT + 1
C   IF( NT .NE. 0 ) GO TO 10
C
C   FIRST CALL ... NT = 1
C
C   STIME = SECNDS (0.0)
C
C   LAPSED CPU TIME ... NT > 1
C
10 DTIME = SECNDS (STIME)
WRITE (IOUT,900) DTIME, NT
RETURN
C
900 FORMAT(//' ( LAPSED CPU TIME = ',F8.2, ' SEC', 5X,
1         '   ENTRY COUNT = ', I4, ' )' )
C
END
SUBROUTINE INPUT(NOPER,*)
C   READS INPUT
C   IMPLICIT REAL*8(A-H,O-Z)
COMMON /FILE/
1 IIN,          IOUT
COMMON /PROP/
1 CNBP(50),    CMW(50),    CDEN(50),    TF(8),
2 CVP(50,8),  CHV(50,8),  CHL(50,8),  CVM(50,8),
3 COEFVP(50,4), COEFHV(50,4), COEFHL(50,4), COEFVM(50,4)
COMMON /DATAIN/
1 FR,          ZR(50),    EMR,          PCOND,    DPCOND,    DPTRAY,
2 GCOND,       GTRAY,    QTRAY,    TTIMES,   IFR
COMMON /DATA/
1 F,          Z(50),    P(40),    G(40),    Q(40),    EM(40,50),
2 FC,         ZC(50),  CF(6),    CZ(50,6), RR,          DR,
3 FCUT,       ZCUT(50), TCUT(15),  DMAX,    TOL,     NAME(50,3),
4 MAXIT,      N,        M,        M1, IC,   INITL,   IPRNT
C
C   IF( NOPER .NE. 0 ) GO TO 10
C
C   ZERO COMMON BLOCKS
C
CALL WIPE ( CNBP(1), 2362 )
CALL WIPE ( FR, 59 )
IFR = 0
CALL WIPE ( F, 2598 )

```

```

CALL IWIPE ( NAME(1,1), 157)
C
C
C
READ INPUT
READ(IIN,930) N
READ(IIN,900) (II,(NAME(II,K),K=1,3),CNBP(II),CMW(II),CDEN(II),
1 I=1,N)
READ(IIN,910) (TF(K),K=1,8)
READ(IIN,920) (II,(CVP(II,K),K=1,8),I=1,N)
READ(IIN,920) (II,(CHV(II,K),K=1,8),I=1,N)
READ(IIN,920) (II,(CHL(II,K),K=1,8),I=1,N)
READ(IIN,920) (II,(CVM(II,K),K=1,8),I=1,N)
READ(IIN,950) IFR, FR
READ(IIN,950) (II,ZR(II),I=1,N)
10 READ(IIN,930,END=99) M
READ(IIN,940) GCOND, GTRAY, QTRAY, EMR
READ(IIN,940) PCOND, DPCOND, DPTRAY, RR, DR
DO 20 K=1,15
20 TCUT(K)=0.0
READ(IIN,960) (TCUT(K),K=1,5)
READ(IIN,970) TOL, DMAX, MAXIT, INITL, IPRNT
RETURN
C
99 RETURN 1
C
900 FORMAT(10X,I2,3A4,3G12.1)
910 FORMAT(9X,8G9.1)
920 FORMAT(7X,I2,8G9.1)
930 FORMAT(12X,I6)
940 FORMAT(12X,5G12.1)
950 FORMAT(10X,I2,G12.1)
960 FORMAT(12X,5G12.0)
970 FORMAT(12X,2G12.1,3I6)
END
SUBROUTINE CDATA
C
CURVE FITS THERMODYNAMIC DATA
IMPLICIT REAL*8(A-H,O-Z)
COMMON /FILE/
1 IIN, IOUT
COMMON /PROP/
1 CNBP(50), CMW(50), CDEN(50), TF(8),
2 CVP(50,8), CHV(50,8), CHL(50,8), CVM(50,8),
3 COEFVFP(50,4), COEFHV(50,4), COEFHL(50,4), COEFVM(50,4)
COMMON /DATA/
1 F, Z(50), P(40), G(40), Q(40), EM(40,50),
2 FC, ZC(50), CF(6), CZ(50,6), RR, DR,
3 FCUT, ZCUT(50), TCUT(15), DMAX, TOL, NAME(50,3),
4 MAXIT, N, M, M1, IC, INITL, IPRNT
COMMON /REGR/
1 X(8), Y(8), C(4,8), D(4), COEF(4)
C
C
C
PRINT COMPONENTS AND PROPERTIES
WRITE(IOUT,900)
WRITE(IOUT,905) (I,(NAME(I,K),K=1,3),CNBP(I),CMW(I),CDEN(I),I=1,N)
C
C
C
CURVE FIT VAPOR PRESSURE
WRITE(IOUT,910)
DO 5 K=1,8

```

```

      X(K) = 1.0D0 / ( TF(K) + 459.67D0 )
5  CONTINUE
      CALL REGRSS(1)
      DO 40 I=1,N
      DO 10 K=1,8
      Y(K) = DLOG( CVP(I,K) )
10  CONTINUE
      CALL REGRSS(2)
      DO 20 K=1,4
      COEFVP(I,K) = COEF(K)
20  CONTINUE
      WRITE(IOUT,950) I, (NAME(I,K),K=1,3)
      DO 30 K=1,8
      Y(K) = DEXP( Y(K) )
      DEV = 100.0D0 * ( Y(K) - CVP(I,K) ) / CVP(I,K)
      WRITE(IOUT,960) TF(K), CVP(I,K), Y(K), DEV
30  CONTINUE
40  CONTINUE

C
C      CURVE FIT VAPOR ENTHALPY
C

      WRITE(IOUT,920)
      DO 45 K=1,8
      X(K) = TF(K) + 459.67D0
45  CONTINUE
      CALL REGRSS(1)
      DO 80 I=1,N
      DO 50 K=1,8
      Y(K) = CHV(I,K)
50  CONTINUE
      CALL REGRSS(2)
      DO 60 K=1,4
      COEFHV(I,K) = COEF(K)
60  CONTINUE
      WRITE(IOUT,950) I, (NAME(I,K),K=1,3)
      DO 70 K=1,8
      DEV = 100.0D0 * ( Y(K) - CHV(I,K) ) / CHV(I,K)
      WRITE(IOUT,960) TF(K), CHV(I,K), Y(K), DEV
70  CONTINUE
80  CONTINUE

C
C      CURVE FIT LIQUID ENTHALPY
C

      WRITE(IOUT,930)
      DO 120 I=1,N
      DO 90 K=1,8
      Y(K) = CHL(I,K)
90  CONTINUE
      CALL REGRSS(2)
      DO 100 K=1,4
      COEFHL(I,K) = COEF(K)
100 CONTINUE
      WRITE(IOUT,950) I, (NAME(I,K),K=1,3)
      DO 110 K=1,8
      DEV = 100.0D0 * ( Y(K) - CHL(I,K) ) / CHL(I,K)
      WRITE(IOUT,960) TF(K), CHL(I,K), Y(K), DEV
110 CONTINUE
120 CONTINUE

C
C      CURVE FIT MOLAR VOLUME

```

```

C
  WRITE(IOUT,940)
  DO 160 I=1,N
  DO 130 K=1,8
  Y(K) = CVM(I,K)
130 CONTINUE
  CALL REGRSS(2)
  DO 140 K=1,4
  COEFVM(I,K) = COEF(K)
140 CONTINUE
  COEFVM(I,1)=1.0
  COEFVM(I,2)=0.0
  COEFVM(I,3)=0.0
  COEFVM(I,4)=0.0
  WRITE(IOUT,950) I, (NAME(I,K),K=1,3)
  DO 150 K=1,8
  DEV = 100.0D0 * ( Y(K) - CVM(I,K) ) / CVM(I,K)
  WRITE(IOUT,960) TF(K), CVM(I,K), Y(K), DEV
150 CONTINUE
160 CONTINUE

C
C   PRINT CURVE FIT COEFFICIENTS
C
  WRITE(IOUT,970)
  DO 170 I=1,N
  WRITE(IOUT,1010) I, (NAME(I,K),K=1,3), (COEFVP(I,K),K=1,4)
170 CONTINUE
  WRITE(IOUT,980)
  DO 180 I=1,N
  WRITE(IOUT,1010) I, (NAME(I,K),K=1,3), (COEFHV(I,K),K=1,4)
180 CONTINUE
  WRITE(IOUT,990)
  DO 190 I=1,N
  WRITE(IOUT,1010) I, (NAME(I,K),K=1,3), (COEFHL(I,K),K=1,4)
190 CONTINUE
  WRITE(IOUT,1000)
  DO 200 I=1,N
  WRITE(IOUT,1010) I, (NAME(I,K),K=1,3), (COEFVM(I,K),K=1,4)
200 CONTINUE
  RETURN

C
900 FORMAT(1H1/20X,'C O M P O N E N T   P R O P E R T I E S'
  1 // '   NO NAME                               NBP           MOLE WT       DENSITY'//)
905 FORMAT(I6,2X,3A4,3G12.4)
910 FORMAT(1H1/' VAPOR PRESSURE DATA')
920 FORMAT(1H1/' VAPOR ENTHALPY DATA')
930 FORMAT(1H1/' LIQUID ENTHALPY DATA')
940 FORMAT(1H1/' MOLAR VOLUME DATA')
950 FORMAT(/I6,2X,3A4
  1 /6X,'   TEMP           EXP           CALC           %DEV')
960 FORMAT(6X,4G12.4)
970 FORMAT(1H1/' VAPOR PRESSURE COEFFICIENTS'//)
980 FORMAT(/' VAPOR ENTHALPY COEFFICIENTS'//)
990 FORMAT(/' LIQUID ENTHALPY COEFFICIENTS'//)
1000 FORMAT(/' MOLAR VOLUME COEFFICIENTS'//)
1010 FORMAT(I6,2X,3A4,4G13.5)
  END
  SUBROUTINE REGRSS (L)
C   PERFORMS LINEAR REGRESSION FOR THERMODYNAMIC COEFFICIENTS
  IMPLICIT REAL*8(A-H,O-Z)

```

```

COMMON /FILE/
1 IIN, IOUT
COMMON /REGR/
1 X(8), Y(8), C(4,8), D(4), COEF(4)
C
C
C DIMENSION BB(16), LHOLD(4), MHOLD(4)
C
C GO TO (10,40), L
C
C SETUP AND INVERT MATRIX
C
C GENERATE THE COEFFICIENT MATRIX
C
10 CALL WIPE ( C(1,1), 32 )
DO 20 I=1,8
C(1,2) = C(1,2) + X(I)
C(1,3) = C(1,3) + X(I)**2
C(1,4) = C(1,4) + X(I)**3
C(2,4) = C(2,4) + X(I)**4
C(3,4) = C(3,4) + X(I)**5
C(4,4) = C(4,4) + X(I)**6
20 CONTINUE
C(1,1) = 7.0D0
C(2,1) = C(1,2)
C(2,2) = C(1,3)
C(2,3) = C(1,4)
C(3,1) = C(1,3)
C(3,2) = C(1,4)
C(3,3) = C(2,4)
C(4,1) = C(1,4)
C(4,2) = C(2,4)
C(4,3) = C(3,4)
C
C ISIZE = 4
K = 0
DO 31 J=1, ISIZE
DO 30 I=1, ISIZE
K=K+1
BB(K) = C(I,J)
30 CONTINUE
31 CONTINUE
CALL MINV (BB, ISIZE, DET, LHOLD, MHOLD )
IF ( DET .EQ. 0.0D0 ) WRITE(IOUT,900)
K = 0
DO 39 J=1, ISIZE
DO 38 I=1, ISIZE
K=K+1
C(I,J) = BB(K)
C
C 38 CONTINUE
39 CONTINUE
C
C RETURN
C
C CALCULATE COEFFICIENTS, RETURN CALCULATED VALUES
C
40 CALL WIPE ( D(1), 8 )
DO 50 I=1,8
D(1) = D(1) + Y(I)

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D(2) = D(2) + Y(I) * X(I)
D(3) = D(3) + Y(I) * X(I)**2
D(4) = D(4) + Y(I) * X(I)**3
50 CONTINUE
COEF(1)=0.0D0
COEF(2)=0.0D0
COEF(3)=0.0D0
COEF(4)=0.0D0
DO 60 I=1,4
DO 60 J=1,4
COEF(I) = COEF(I) + C(I,J) * D(J)
60 CONTINUE
DO 70 I=1,8
Y(I) = COEF(1) + COEF(2)*X(I) + COEF(3)*X(I)**2 + COEF(4)*X(I)**3
70 CONTINUE
RETURN

C
900 FORMAT(/' SINGULAR MATRIX')
C
END
SUBROUTINE CNSTNT(NOPER)
CALCULATES CONSTANTS
C
IMPLICIT REAL*8(A-H,O-Z)
COMMON /FILE/
1 IIN, IOUT
COMMON /DATAIN/
1 FR, ZR(50), EMR, PCOND, DPCOND, DPTRAY,
2 GCOND, GTRAY, QTRAY, TTIMES, IFR
COMMON /DATA/
1 F, Z(50), P(40), G(40), Q(40), EM(40,50),
2 FC, ZC(50), CF(6), CZ(50,6), RR, DR,
3 FCUT, ZCUT(50), TCUT(15), DMAX, TOL, NAME(50,3),
4 MAXIT, N, M, ML, IC, INITL, IPRNT

C
C CALCULATE FIXED DISTILLATION VARIABLES
C
M1 = M - 1
P(1) = PCOND
G(1) = GCOND
Q(1) = 0.0D0
DO 10 J = 2,M
IF( J .EQ. 2 ) P(J) = P(J-1) + DPCOND
IF( J .NE. 2 ) P(J) = P(J-1) + DPTRAY
IF( J .NE. M ) G(J) = GTRAY
IF( J .EQ. M ) G(J) = 0.0D0
IF( J .NE. M ) Q(J) = QTRAY
IF( J .EQ. M ) Q(J) = 0.0D0
10 CONTINUE
DO 20 J = 1,M
DO 20 I = 1,N
EM(J,I) = EMR
IF( (J.EQ.1) .OR. (J.EQ.M) ) EM(J,I) = 1.0D0
20 CONTINUE

C
C CONVERT AND PRINT FEED CHARGE
C
IF( NOPER .NE. 0 ) GO TO 40
TTIMES = 0.0D0
IC = IFR
FC = FR

```

```

DO 30 I=1,N
ZC(I) = ZR(I)
30 CONTINUE
40 WRITE(IOUT,900)
CALL CONVRT(1)
F = FC
FCUT = FC
IF( NOPER .EQ. 0 ) FR = FC
DO 50 I=1,N
Z(I) = ZC(I)
ZCUT(I) = ZC(I)
IF( NOPER .EQ. 0 ) ZR(I) = ZC(I)
50 CONTINUE
RETURN

C
900 FORMAT(1H1/20X,'F E E D   C H A R G E')
END
SUBROUTINE CONVRT(L)
C
CALCULATES MOLE, WEIGHT, AND LIQUID VOLUME
IMPLICIT REAL*8(A-H,O-Z)
COMMON /FILE/
1 IIN, IOUT
COMMON /PROP/
1 CNBP(50), CMW(50), CDEN(50), TF(8),
2 CVP(50,8), CHV(50,8), CHL(50,8), CVM(50,8),
3 COEFVP(50,4), COEFHV(50,4), COEFHL(50,4), COEFVM(50,4)
COMMON /DATA/
1 F, Z(50), P(40), G(40), Q(40), EM(40,50),
2 FC, ZC(50), CF(6), CZ(50,6), RR, DR,
3 FCUT, ZCUT(50), TCUT(15), DMAX, TOL, NAME(50,3),
4 MAXIT, N, M, M1, IC, INITL, IPRNT

C
C
C
NORMALIZE INPUT

CALL WIPE ( CF(1), 306 )
SUM = 0.0
DO 10 I=1,N
SUM = SUM + ZC(I)
10 CONTINUE
DO 20 I=1,N
ZC(I) = FC * ZC(I) / SUM
20 CONTINUE

C
C
C
CONVERT INPUT

GO TO (30,50,70), IC

C
C
C
MOLE INPUT

30 DO 40 I=1,N
CZ(I,1) = ZC(I)
CZ(I,3) = CZ(I,1) * CMW(I)
CZ(I,5) = CZ(I,3) / CDEN(I)
40 CONTINUE
GO TO 90

C
C
C
WEIGHT INPUT

50 DO 60 I=1,N
CZ(I,3) = ZC(I)

```

```

      CZ(I,1) = CZ(I,3) / CMW(I)
      CZ(I,5) = CZ(I,3) / CDEN(I)
60  CONTINUE
      GO TO 90
C
C   VOLUME INPUT
C
70  DO 80 I=1,N
      CZ(I,5) = ZC(I)
      CZ(I,3) = CZ(I,5) * CDEN(I)
      CZ(I,1) = CZ(I,3) / CMW(I)
80  CONTINUE
      GO TO 90
C
C   CALCULATE PERCENTS AND TOTALS
C
90  DO 100 I=1,N
      CF(1) = CF(1) + CZ(I,1)
      CF(3) = CF(3) + CZ(I,3)
      CF(5) = CF(5) + CZ(I,5)
100 CONTINUE
      DO 110 I=1,N
      CZ(I,2) = 100.0D0 * CZ(I,1) / CF(1)
      CZ(I,4) = 100.0D0 * CZ(I,3) / CF(3)
      CZ(I,6) = 100.0D0 * CZ(I,5) / CF(5)
      CF(2) = CF(2) + CZ(I,2)
      CF(4) = CF(4) + CZ(I,4)
      CF(6) = CF(6) + CZ(I,6)
110 CONTINUE
C
C   RETURN MOLE
C
      FC = CF(1)
      DO 120 I=1,N
      ZC(I) = CZ(I,1) / CF(1)
120 CONTINUE
C
C   PRINT
C
      IF( L .EQ. 3 ) RETURN
      WRITE(IOUT,900)
      IF( (L.EQ.1) .OR. (IPRNT.GE.1) )
1  WRITE(IOUT,910) (I,(NAME(I,K),K=1,3),(CZ(I,K),K=1,6),I=1,N)
      WRITE(IOUT,920) (CF(K),K=1,6)
      RETURN
C
900 FORMAT(/'      NO NAME          LBMOLES      MOLE %      POUNDS
1  WEIGHT %      GALLONS      VOLUME %'/)
910 FORMAT(I6,2X,3A4,6G12.4)
920 FORMAT(/8X,'TOTAL',7X,6G12.4)
      END
      SUBROUTINE STEADY(*)
C   MAIN ROUTINE FOR STEADY-STATE TOTAL-REFLUX CALCULATION
      IMPLICIT REAL*8(A-H,O-Z)
      COMMON /FILE/
1  IIN,          IOUT
      COMMON /DATA/
1  F,           Z(50),      P(40),      G(40),      Q(40),      EM(40,50),
2  FC,          ZC(50),     CF(6),      CZ(50,6),  RR,         DR,
3  FCUT,        ZCUT(50),   TCUT(15),  DMAX,      TOL,        NAME(50,3),

```



```

4 MAXIT,      N,      M,      M1, IC,  INITL,  IPRNT
COMMON /SCALC/
1 T(40),      AL(40),  V(40),   U(40),   X(40,50), Y(40,50),
2 DT(40),      DL(40),  DV(40),  DU(40),  DX(40,50), SUMDX(40),
3 AK(50),      HV(50),  HL(50),  VM(50),  DKDT(50), DHVDT(50),
4 DHLDT(50),  DVMDT(50), SCALE,  CONV,   ICONV,   ITER

C
C   INITIALIZE
C
C   CALL WIPE ( T(1), 6760 )
C   CALL INITAL
C   CALL WIPE( DT(1), 2600 )
C   ITER = 0

C
C   SCALE = 0.0
C   CONV = 0.0
C   ICONV = 0

C
C   CALL SPRINT
C
C   CONVERGENCE LOOP
C
10 ITER = ITER + 1
    CALL MATSOL(&99)
    CALL CONVRG
    IF( ICONV .EQ. 0 ) CALL HTBAL
    CALL SPRINT
    IF( (ICONV.NE.0) .AND. (ITER.LT.MAXIT) ) GO TO 10
    IF( ICONV .NE. 0 ) GO TO 90
    RETURN

C
C   NON-CONVERGENCE
C
90 WRITE(IOUT,900) ITER
99 RETURN 1

C
900 FORMAT('/' STEADY-STATE TOTAL REFLUX CALCULATIONS DID NOT CONVERGE
1IN',I3,' ITERATIONS')
END
SUBROUTINE INITAL
INITIALIZES STEADY-STATE TOTAL-REFLUX CALCULATION
IMPLICIT REAL*8(A-H,O-Z)
COMMON /DATA/
1 F,          Z(50),    P(40),    G(40),    Q(40),    EM(40,50),
2 FC,         ZC(50),   CF(6),    CZ(50,6), RR,      DR,
3 FCUT,       ZCUT(50), TCUT(15), DMAX,     TOL,     NAME(50,3),
4 MAXIT,      N,      M,      M1, IC,  INITL,  IPRNT
COMMON /SCALC/
1 T(40),      AL(40),  V(40),   U(40),   X(40,50), Y(40,50),
2 DT(40),      DL(40),  DV(40),  DU(40),  DX(40,50), SUMDX(40),
3 AK(50),      HV(50),  HL(50),  VM(50),  DKDT(50), DHVDT(50),
4 DHLDT(50),  DVMDT(50), SCALE,  CONV,   ICONV,   ITER

C
C   INITL = INITL + 1
C
C   ZERO OUT THE X ARRAY
C   DO 5 J=1,M
C   DO 5 I=1,N
5 X(J,I)=0.0D0
C

```

```

C     ESTIMATE U
C
C     ASSUME THAT THE COLUMN HAS A TEMPERATURE OF 60 f AND
C     EVALUATE THE LIQUID MOLAR VOLUME (GALLONS/LB-MOLE) TO
C     ESTIMATE THE MOLAR INVENTORY ON EACH STAGE.
C
      J = 1
      T(J) = 60.0D0
      CALL THERMO(J,4)
      DU(1) = 0.0D0
      DO 10 I=1,N
      DU(1) = DU(1) + Z(I) * VM(I)
C
C     F = FEED MOLES
C     G = VOLUMETRIC HOLDUP IN GALLONS
C     U = MOLAR HOLDUP, LB-MOLES
C
      10 CONTINUE
      U(M) = F
      DO 20 J=1,M1
      U(J) = G(J) / DU(1)
      U(M) = U(M) - U(J)
      20 CONTINUE
C
C     IMPROVE INITIALIZATION
C
      DO 110 K=1,INITL
C
C     INITIALIZE X
C
C     ALGORITHM ASSUMES THAT THE FEED IS ORDERED BY INCREASING
C     BOILING POINT.  START BY PLACING THE LIGHTEST COMPONENT
C     ON THE TOP STAGE (#1 - CONDENSER) AND PROCEED DOWN THE
C     COLUMN.  WHEN COMPONENT IS EXHAUSTER USE THE NEXT HIGHER
C     BOILER.
C
      IF( K .NE. 1 ) CALL WIPE ( X(1,1), 2000 )
C
C     AK IS A DUMMY VARIABLE HERE (NOT K-VALUES) AND CONTAINS
C     THE MOLES OF EACH SPECIES IN THE CHARGE TO THE STILL.
C
      DO 30 I=1,N
      AK(I) = F * Z(I)
      30 CONTINUE
      I = 1
      DO 60 J=1,M
      UU = U(J)
      40 IF( AK(I) .GT. UU ) GO TO 50
      X(J,I) = AK(I)
      UU = UU - AK(I)
      I = I + 1
      IF( I .GT. N ) GO TO 60
      GO TO 40
      50 X(J,I) = UU
      AK(I) = AK(I) - UU
      60 CONTINUE
      DO 70 J=1,M
      DO 70 I=1,N
      X(J,I) = X(J,I) / U(J)
      70 CONTINUE

```

```

C
C   INITIALIZE T
C
C   IF( K .EQ. 1 ) T(M) = 300.0D0
C   CALL BUBBLE(M,2)
C
C   BUBBLE POINTS ARE ACCOMPLISHED FROM THE BOTTOM OF THE COLUMN
C   TO TH TOP (M = REBOLIER/STILL-POT, 1 = CONDENSER)
C
C   DO 80 JJ=1,M1
C   J = M1 - JJ + 1
C   IF( K .EQ. 1 ) T(J) = T(J+1)
C   CALL BUBBLE(J,2)
80 CONTINUE
C
C   INITIALIZE U
C
C   REEVALUATE THE LIQUID MOLAR VOLUME SINCE WE NOW HAVE
C   A COMPOSITION X'S AND TEMPERATURES T'S.
C
C   DO 90 J=1,M
C   CALL THERMO(J,4)
C   DU(J) = 0.0D0
C   DO 90 I=1,N
C   DU(J) = DU(J) + X(J,I) * VM(I)
90 CONTINUE
C   U(M) = F
C   DO 100 J=1,M1
C   U(J) = G(J) / DU(J)
C   U(M) = U(M) - U(J)
100 CONTINUE
C
C   110 CONTINUE
C
C   RETURN
C   END
C
C   SUBROUTINE BUBBLE(J,L)
C   CONVERGES BUBBLE POINT TEMPERATURE
C   IMPLICIT REAL*8(A-H,O-Z)
C   COMMON /FILE/
C   1 IIN,          IOUT
C   COMMON /DATA/
C   1 F,           Z(50),      P(40),      G(40),      Q(40),      EM(40,50),
C   2 FC,          ZC(50),     CF(6),       CZ(50,6),  RR,         DR,
C   3 FCUT,        ZCUT(50),   TCUT(15),   DMAX,      TOL,        NAME(50,3),
C   4 MAXIT,       N,          M,          M1, IC,     INITL,      IPRNT
C   COMMON /SCALC/
C   1 T(40),       AL(40),     V(40),     U(40),     X(40,50),  Y(40,50),
C   2 DT(40),      DL(40),     DV(40),    DU(40),    DX(40,50), SUMDX(40),
C   3 AK(50),      HV(50),     HL(50),    VM(50),    DKDT(50),  DHVDT(50),
C   4 DHLDT(50),  DVMDT(50),  SCALE,    CONV,     ICONV,     ITER
C
C   CONVERGE T
C
C   SUMX = 0.0
C   DO 2 I=1,N
C   2 SUMX= SUMX + X(J,I)
C   DO 4 I=1,N
C   4 X(J,I) = X(J,I)/SUMX

```

C

```
TOLB = TOL * TOL
ITER = 0
10 ITER = ITER + 1
CALL THERMO(J,1)
SUMKX = 0.0D0
SUMDKX = 0.0D0
DO 20 I=1,N
SUMKX = SUMKX + EM(J,I) * X(J,I) * AK(I)
IF( J .NE. M ) SUMKX = SUMKX + ( 1.0D0 - EM(J,I) ) * Y(J+1,I)
SUMDKX = SUMDKX + EM(J,I) * X(J,I) * DKDT(I)
20 CONTINUE
DTI = ( 1.0D0 - SUMKX ) / SUMDKX
ICONV = 0
SCALE = 1.0D0
CONV = 1.0D0
ERROR = DABS(DTI)
IF( ERROR .LT. TOLB ) GO TO 30
SCALE = DMIN1( SCALE, DMAX/ERROR )
CONV = DMIN1( CONV, TOLB/ERROR )
ICONV = 1
30 T(J) = T(J) + SCALE * DTI
IF( (ICONV.NE.0) .AND. (ITER.LT.MAXIT) ) GO TO 10
```

C

```
IF( ICONV .NE. 0 ) WRITE(IOUT,900) J, ITER, SCALE, CONV, T(J), DTI
```

C

```
CALCULATE Y
```

C

```
IF( L .EQ. 2 ) RETURN
CALL THERMO(J,1)
SUM = 0.0D0
DO 40 I=1,N
Y(J,I) = EM(J,I) * X(J,I) * AK(I)
IF( J .NE. M ) Y(J,I) = Y(J,I) + ( 1.0D0 - EM(J,I) ) * Y(J+1,I)
SUM = SUM + Y(J,I)
40 CONTINUE
DO 50 I=1,N
Y(J,I) = Y(J,I) / SUM
50 CONTINUE
RETURN
```

C

```
900 FORMAT(' STAGE =',I3,' ITER =',I3,' SCALE =',G12.4,'CONV =',
1 G12.4,'T =',G12.4,'DT =',G12.4)
END
SUBROUTINE MATSOL(*)
```

C

```
SOLVES STEADY-STATE TOTAL-REFLUX MATRIX
```

C

```
IMPLICIT REAL*8(A-H,O-Z)
COMMON /FILE/
1 IIN, IOUT
COMMON /DATA/
1 F, Z(50), P(40), G(40), Q(40), EM(40,50),
2 FC, ZC(50), CF(6), CZ(50,6), RR, DR,
3 FCUT, ZCUT(50), TCUT(15), DMAX, TOL, NAME(50,3),
4 MAXIT, N, M, M1, IC, INITL, IPRNT
COMMON /SCALC/
1 T(40), AL(40), V(40), U(40), X(40,50), Y(40,50),
2 DT(40), DL(40), DV(40), DU(40), DX(40,50), SUMDX(40),
3 AK(50), HV(50), HL(50), VM(50), DKDT(50), DHVDT(50),
```

```

4 DHLDT(50), DVMDT(50), SCALE, CONV, ICONV, ITER
COMMON /MATRIX/
1 A(52,52), B(52,52), C(52,52), D(52), DM(52),
2 AHOLD(52,52), CHOLD(52,52), DHOLD(52), ILAST, I1, I2
DIMENSION CSAVE(52,52,40), DSAVE(52,40)
DATA IFILE/'1 '/

C
C
C
C CALCULATE MATRIX CONSTANTS
C N = NUMBER OF COMONENTS
C M = NUMBER OF STAGES
C
I1 = N + 1
I2 = N + 2

C
C
C SETUP AND REDUCE MATRIX

DO 70 J = 1,M
CALL SETUP(J)
IF( J .EQ. 1 ) GO TO 20
IF( J .EQ. M ) GO TO 40

C
C
C A-HOLD IS ELIMINATED VIA A SUBSTRACTION
C DM = DM - AHOLD * DHOLD
C A = A - AHOLD * CHOLD
C
DO 10 K1 = 1,I2
DO 10 K2 = 1,I2
DM(K1) = DM(K1) - AHOLD(K1,K2) * DHOLD(K2)
DO 10 K3 = 1,I2
A(K1,K2) = A(K1,K2) - AHOLD(K1,K3) * CHOLD(K3,K2)
10 CONTINUE

C
C
C AHOLD = A
C DHOLD = BINV * D
C CHOLD = BINV * C
C SAVE CHOLD, DHOLD
C
C
C PUT A MATRIX INTO A-HOLD,
C PREMULTIPLY C BY B-INVERSE AND SAVE IN C-HOLD,
C PREMULTIPLY D BY D-INVERSE AND SAVE IN D-HOLD
C
20 CALL WIPE( AHOLD(1,1), 5460 )
DO 30 K1 = 1,I2
DO 30 K2 = 1,I2
AHOLD(K1,K2) = A(K1,K2)
DHOLD(K1) = DHOLD(K1) + B(K1,K2) * D(K2)
DO 30 K3 = 1,I2
CHOLD(K1,K2) = CHOLD(K1,K2) + B(K1,K3) * C(K3,K2)
30 CONTINUE
DO 34 K1 = 1,I2
DO 32 K2 = 1,I2
CSAVE(K1,K2,J) = CHOLD(K1,K2)
32 CONTINUE
DSAVE(K1,J) = DHOLD(K1)
34 CONTINUE
GO TO 70

C
C
C DM = DM - AHOLD * DHOLD
C B = B - AHOLD * CHOLD

```

```

C
40 DO 50 K1 = 1,I2
   DO 50 K2 = 1,I2
   DM(K1) = DM(K1) - AHOLD(K1,K2) * DHOLD(K2)
   DO 50 K3 = 1,I2
   B(K1,K2) = B(K1,K2) - AHOLD(K1,K3) * CHOLD(K3,K2)
50 CONTINUE
C
C   INVERT B
C
C   CALL MATINV (&99)
C
C   D = BINV * DM
C
C   CALL WIPE ( D(1), 52 )
   DO 60 K1 = 1,I2
   DO 60 K2 = 1,I2
   D(K1) = D(K1) + B(K1,K2) * DM(K2)
60 CONTINUE
70 CONTINUE
C
C   SOLUTION
C   DHOLD = DHOLD - CHOLD * D
C
C   DO 120 JJ = 1,M
   J = M - JJ + 1
   IF( J .EQ. M ) GO TO 100
C
C   DO 74 K1 = 1,I2
   DO 72 K2 = 1,I2
   CHOLD(K1,K2) = CSAVE(K1,K2,J)
72 CONTINUE
   DHOLD(K1) = DSAVE(K1,J)
74 CONTINUE
C
C   DO 80 K1 = 1,I2
   DO 80 K2 = 1,I2
   DHOLD(K1) = DHOLD(K1) - CHOLD(K1,K2) * D(K2)
80 CONTINUE
   DO 90 K1 = 1,I2
   D(K1) = DHOLD(K1)
90 CONTINUE
C
100 DO 110 I = 1,N
   DX(J,I) = D(I)
110 CONTINUE
   DT(J) = D(I1)
   DU(J) = D(I2)
120 CONTINUE
c
c   write (6,130) iter
c 130 format('1',4x,'iter = ', i5 /
c     1      5x, 'stage',5x,'temp dt',5x,'inventory')
c   write (6,140) (i,dt(i),du(i),i=1,m)
c 140 format(i8,2f14.2)
c
c   write (6,150)
c 150 format('1',4x,'stage',5x,'comps 1-5 dxs')
c   do 170 j=1,m
c   write (6,160) j,(dx(j,i),i=1,n)

```

```

c 160 format(i5,5(lx,d11.4))
c 170 continue
c
      RETURN
C
C      SINGULAR MATRIX
C
      99 WRITE(IOUT,900)
      RETURN 1
C
      900 FORMAT(/' SINGULAR MATRIX')
      END
      SUBROUTINE MATINV (*)
C
C      INVERTS MATRIX USING IBM-SSP ROUTINE 'MINV'
C
      IMPLICIT REAL*8(A-H,O-Z)
      COMMON /MATRIX/
      1 A(52,52), B(52,52), C(52,52), D(52), DM(52),
      2 AHOLD(52,52), CHOLD(52,52), DHOLD(52), ILAST, I1, I2
      COMMON /CLNODE/
      1 XT(2000), RWORK(26022), IWORK(2020)
C
      DIMENSION BB(2704), LHOLD(52), MHOLD(52)
C
      DATA IN/52/
C
      SETUP MATRIX FOR MINV
C
      CALL WIPE ( BB(1), 2704)
C
      MOVE MATRIX INTO 'BB'
C
      K=0
      DO 11 I=1,I2
      DO 10 J=1,I2
      K=K+1
      BB(K) = B(I,J)
      10 CONTINUE
      11 CONTINUE
C
      INVERT MATRIX USING MINV
C
      CALL MINV ( BB, I2, DET, LHOLD, MHOLD )
      IF (DET .EQ. 0.0D0) RETURN 1
C
      MOVE INVERSE INTO 'B'
C
      K=0
      DO 21 I=1,I2
      DO 20 J=1,I2
      K=K+1
      B(I,J) = BB(K)
      20 CONTINUE
      21 CONTINUE
C
      END
      SUBROUTINE SETUP(J)
C
      SETS-UP STEADY-STATE TOTAL-REFLUX MATRIX
      IMPLICIT REAL*8(A-H,O-Z)

```

```

COMMON /DATA/
1 F,          Z(50),      P(40),      G(40),      Q(40),      EM(40,50),
2 FC,        ZC(50),     CF(6),     CZ(50,6),  RR,         DR,
3 FCUT,      ZCUT(50),   TCUT(15), DMAX,      TOL,        NAME(50,3),
4 MAXIT,     N,          M,         M1, IC,    INITL,      IPRNT
COMMON /SCALC/
1 T(40),     AL(40),     V(40),     U(40),     X(40,50),  Y(40,50),
2 DT(40),    DL(40),     DV(40),    DU(40),    DX(40,50), SUMDX(40),
3 AK(50),    HV(50),     HL(50),    VM(50),    DKDT(50),  DHVDT(50),
4 DHLDT(50), DVMDT(50), SCALE,     CONV,      ICONV,     ITER
COMMON /MATRIX/
1 A(52,52),  B(52,52),  C(52,52),  D(52),     DM(52),
2 AHOLD(52,52), CHOLD(52,52), DHOLD(52),  ILAST,  I1,  I2
C
C   CALL WIPE ( A(1,1), 8164 )
C   DO 16 K1=1,52
C   DO 12 K2=1,52
C   A(K2,K1)=0.0D0
C   B(K2,K1)=0.0D0
C   C(K2,K1)=0.0D0
12 CONTINUE
C   D(K1)=0.0D0
16 CONTINUE
C
C   A MATRIX
C
C   IF( J .EQ. M ) GO TO 20
C   DO 10 I=1,N
C   A(I,I) = U(J)
C   A(I,I2) = X(J,I)
10 CONTINUE
C   A(I2,I2) = 1.0D0
C
C   B AND D MATRIX
C
C   THERMO(J,1) OBTAINS K-VALUES AND THE TEMP. DERIVATIVES FOR STAGE J
C   THERMO(J,4) OBTAINS LIQUID MOLAR VOL. AND THE TEMP. DERIVATIVES
C   FOR STAGE J
C
20 CALL THERMO(J,1)
C   IF( J .NE. M ) CALL THERMO(J,4)
C   DO 40 I=1,N
C   B(I1,I) = EM(J,I) * AK(I) + ( 1.0D0 - EM(J,I) )
C   B(I1,I1) = B(I1,I1) + EM(J,I) * DKDT(I) * X(J,I)
C   IF( J .EQ. M ) GO TO 30
C   B(I,I) = 1.0D0
C   B(I2,I) = U(J) * VM(I)
C   B(I2,I1) = B(I2,I1) + U(J) * X(J,I) * DVMDT(I)
C   B(I2,I2) = B(I2,I2) + X(J,I) * VM(I)
C   D(I) = -X(J,I)
C   D(I1) = D(I1) - ( EM(J,I) * AK(I) + ( 1.0D0 - EM(J,I) ) ) * X(J,I)
C   D(I2) = D(I2) - U(J) * X(J,I) * VM(I)
C   GO TO 40
30 B(I,I) = U(J)
C   B(I,I2) = X(J,I)
40 CONTINUE
C   IF( J .EQ. M ) B(I2,I2) = 1.0D0
C   IF( J .EQ. M ) RETURN
C   D(I1) = D(I1) + 1.0D0
C   D(I2) = D(I2) + G(J)

```



```

C
C
C      INVERT B MATRIX
C
C      DO 50 I=1,N
C      B(I2,I) = (B(I1,I)*B(I2,I1)-B(I2,I)*B(I1,I1))/(B(I1,I1)*B(I2,I2))
C      B(I1,I) = -B(I1,I) / B(I1,I1)
50  CONTINUE
C      B(I2,I1) = -B(I2,I1) / ( B(I1,I1) * B(I2,I2) )
C      B(I1,I1) = 1.0D0 / B(I1,I1)
C      B(I2,I2) = 1.0D0 / B(I2,I2)
C
C
C      C AND D MATRIX
C
C      THERMO(J+1,1) OBTAINS K-VALUES AND THE TEMP. DERIVATIVES FOR STAGE J+1
C
C      CALL THERMO(J+1,1)
C      DO 60 I=1,N
C      C(I,I) = -( EM(J+1,I) * AK(I) + ( 1.0D0 - EM(J+1,I) ) )
C      C(I,I1) = -EM(J+1,I) * DKDT(I) * X(J+1,I)
C      D(I) = D(I) + ( EM(J+1,I) * AK(I) + (1.0D0-EM(J+1,I)) ) * X(J+1,I)
60  CONTINUE
C      IF( J .NE. 1 ) RETURN
C
C
C      DM MATRIX
C
C      CALL WIPE ( DM(1), 52 )
C      DO 62 K1=1,52
62  DM(K1)=0.0D0
C      THERMO(M,1) OBTAINS K-VALUES AND THE TEMP. DERIVATIVES FOR STAGE M
C
C      CALL THERMO(M,1)
C      DO 70 I=1,N
C      DM(I) = F * Z(I)
C      DM(I1) = DM(I1) - ( EM(M,I) * AK(I) + ( 1.0D0-EM(M,I) ) ) * X(M,I)
C      DO 70 JJ = 1,M
C      DM(I) = DM(I) - U(JJ) * X(JJ,I)
70  CONTINUE
C      DO 80 JJ = 1,M
C      DM(I2) = DM(I2) - U(JJ)
80  CONTINUE
C      DM(I1) = DM(I1) + 1.0D0
C      DM(I2) = DM(I2) + F
C      RETURN
C      END
C
C      SUBROUTINE THERMO(J,L)
C      CALCULATES THERMODYNAMIC DATA
C      IMPLICIT REAL*8(A-H,O-Z)
C      COMMON /PROP/
C      1 CNBP(50),      CMW(50),      CDEN(50),      TF(8),
C      2 CVP(50,8),      CHV(50,8),      CHL(50,8),      CVM(50,8),
C      3 COEFVP(50,4), COEFHV(50,4), COEFHL(50,4), COEFVM(50,4)
C      COMMON /DATA/
C      1 F,              Z(50),      P(40),      G(40),      Q(40),      EM(40,50),
C      2 FC,              ZC(50),      CF(6),      CZ(50,6),  RR,        DR,
C      3 FCUT,           ZCUT(50),  TCUT(15),  DMAX,      TOL,        NAME(50,3),
C      4 MAXIT,          N,          M,          M1, IC,    INITL,      IPRNT
C      COMMON /SCALC/
C      1 T(40),          AL(40),      V(40),      U(40),      X(40,50),  Y(40,50),
C      2 DT(40),         DL(40),      DV(40),      DU(40),      DX(40,50), SUMDX(40),

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```

3 AK(50),      HV(50),      HL(50),      VM(50),      DKDT(50),      DHVDT(50),
4 DHLDT(50),  DVMDT(50),  SCALE,      CONV,        ICONV,         ITER
C
  TR1 = T(J) + 459.67D0
  TR2 = TR1 * TR1
  TR3 = TR2 * TR1
  TR4 = TR3 * TR1
  GO TO (1,2,3,4), L
C
C
C
  K-VALUE
C
1 DO 10 I=1,N
  AK(I) =COEFVP(I,1)+COEFVP(I,2)/TR1+COEFVP(I,3)/TR2+COEFVP(I,4)/TR3
  AK(I) = DEXP(AK(I)) / P(J)
  DKDT(I) = -COEFVP(I,2)/TR2-2.0D0*COEFVP(I,3)/TR3-3.0D0*COEFVP(I,4)
1      /TR4
  DKDT(I) = DKDT(I) * AK(I)
10 CONTINUE
  RETURN
C
C
C
  VAPOR ENTHALPY
C
2 DO 20 I=1,N
  HV(I) =COEFHV(I,1)+COEFHV(I,2)*TR1+COEFHV(I,3)*TR2+COEFHV(I,4)*TR3
  DHVDT(I) = COEFHV(I,2)+2.0D0*COEFHV(I,3)*TR1+3.0D0*COEFHV(I,4)*TR2
20 CONTINUE
  RETURN
C
C
C
  LIQUID ENTHALPY
C
3 DO 30 I=1,N
  HL(I) =COEFHL(I,1)+COEFHL(I,2)*TR1+COEFHL(I,3)*TR2+COEFHL(I,4)*TR3
  DHLDT(I) = COEFHL(I,2)+2.0D0*COEFHL(I,3)*TR1+3.0D0*COEFHL(I,4)*TR2
30 CONTINUE
  RETURN
C
C
C
  MOLAR VOLUME
C
4 DO 40 I=1,N
  VM(I) =COEFVM(I,1)+COEFVM(I,2)*TR1+COEFVM(I,3)*TR2+COEFVM(I,4)*TR3
  DVMDT(I) = COEFVM(I,2)+2.0D0*COEFVM(I,3)*TR1+3.0D0*COEFVM(I,4)*TR2
40 CONTINUE
  RETURN
  END
C
  SUBROUTINE CONVRG
C
  CHECKS CONVERGENCE AND DETERMINES NEW VALUES FOR STEADY-STATE
  IMPLICIT REAL*8(A-H,O-Z)
  COMMON /DATA/
1 F,          Z(50),      P(40),      G(40),      Q(40),      EM(40,50),
2 FC,         ZC(50),    CF(6),      CZ(50,6),  RR,         DR,
3 FCUT,       ZCUT(50),  TCUT(15),  DMAX,      TOL,        NAME(50,3),
4 MAXIT,      N,         M,         M1, IC,     INITL,      IPRNT
  COMMON /SCALC/
1 T(40),      AL(40),      V(40),      U(40),      X(40,50),  Y(40,50),
2 DT(40),     DL(40),      DV(40),     DU(40),     DX(40,50),  SUMDX(40),
3 AK(50),     HV(50),      HL(50),     VM(50),     DKDT(50),  DHVDT(50),
4 DHLDT(50), DVMDT(50),  SCALE,     CONV,       ICONV,      ITER
C
C
  CALCULATE SCALE

```

```

C
  ICONV = 0
  SCALE = 1.0D0
  CONV = 1.0D0
  DO 20 J=1,M
    ERROR = DABS(DT(J))
    IF( ERROR .LT. TOL ) GO TO 10
    SCALE = DMIN1( SCALE, DMAX/ERROR )
    CONV = DMIN1( CONV, TOL/ERROR )
    ICONV = ICONV + 1
10  ERROR = 100.0D0 * DABS( DU(J)/U(J) )
    IF( ERROR .LT. TOL ) GO TO 20
    SCALE = DMIN1( SCALE, DMAX/ERROR )
    CONV = DMIN1( CONV, TOL/ERROR )
    ICONV = ICONV + 1
20  CONTINUE

C
C   CALCULATE NEW T AND U
C
  DO 30 J=1,M
    T(J) = T(J) + SCALE * DT(J)
    U(J) = U(J) + SCALE * DU(J)
30  CONTINUE

C
C   CALCULATE SUMDX
C
  DO 40 J=1,M
    SUMDX(J) = 0.0D0
    DO 40 I=1,N
      SUMDX(J) = SUMDX(J) + DABS(DX(J,I))
40  CONTINUE

C
C   CHECK X CONVERGENCE
C
  RTOL = 0.01D0 * TOL
  ATOL = RTOL * RTOL
  DO 50 J=1,M
    DO 50 I=1,N
      ERROR = DABS( DX(J,I) )
      XTOL = RTOL * DABS( X(J,I) ) + ATOL
      IF( ERROR .GT. XTOL ) ICONV = ICONV + 1
50  CONTINUE

C
C   CALCULATE NEW X
C
  DO 100 J=1,M
    XSUM = 0.0D0
    DO 80 I=1,N
      DELX = SCALE * DX(J,I)
      XNEW = X(J,I) + DELX
      IF( XNEW .GE. 0.0D0 ) GO TO 70
      IF( X(J,I) .EQ. 0.0D0 ) GO TO 60
      IF( DELX/X(J,I) .LT. -30.0D0 ) GO TO 60
      XNEW = X(J,I) * DEXP( DELX / X(J,I) )
      GO TO 70
60  XNEW = 0.0D0
70  X(J,I) = XNEW
    XSUM = XSUM + X(J,I)
80  CONTINUE
    DO 90 I=1,N

```

```

X(J,I) = X(J,I) / XSUM
90 CONTINUE
100 CONTINUE
RETURN
END

C
SUBROUTINE HTBAL
C CALCULATES FLOWS FOR STEADY-STATE TOTAL-REFLUX
IMPLICIT REAL*8(A-H,O-Z)
COMMON /DATA/
1 F, Z(50), P(40), G(40), Q(40), EM(40,50),
2 FC, ZC(50), CF(6), CZ(50,6), RR, DR,
3 FCUT, ZCUT(50), TCUT(15), DMAX, TOL, NAME(50,3),
4 MAXIT, N, M, M1, IC, INITL, IPRNT
COMMON /SCALC/
1 T(40), AL(40), V(40), U(40), X(40,50), Y(40,50),
2 DT(40), DL(40), DV(40), DU(40), DX(40,50), SUMDX(40),
3 AK(50), HV(50), HL(50), VM(50), DKDT(50), DHVDT(50),
4 DHLDT(50), DVMDT(50), SCALE, CONV, ICONV, ITER

C
C CALCULATE Y
C
DO 30 J=1,M
CALL THERMO(J,1)
YSUM = 0.0D0
DO 10 I=1,N
Y(J,I) = ( EM(J,I) * AK(I) + ( 1.0D0 - EM(J,I) ) ) * X(J,I)
YSUM = YSUM + Y(J,I)
10 CONTINUE
DO 20 I=1,N
Y(J,I) = Y(J,I) / YSUM
20 CONTINUE
30 CONTINUE

C
C CALCULATE HV AND HL
C
DO 40 J=1,M
CALL THERMO(J,2)
CALL THERMO(J,3)
DV(J) = 0.0D0
DL(J) = 0.0D0
DO 40 I=1,N
DV(J) = DV(J) + Y(J,I) * HV(I)
DL(J) = DL(J) + X(J,I) * HL(I)
40 CONTINUE

C
C CALCULATE V, L, Q1, AND QM
C
DO 80 J=1,M
IF( J .EQ. 1 ) GO TO 50
IF( J .EQ. M ) GO TO 70
GO TO 60

C
C CONDENSER
C
50 V(J) = 0.0D0
AL(J) = RR * DR + DR
Q(J) = AL(J) * ( DL(J) - DV(J+1) )
GO TO 80

C

```

```

C     STAGES
C
60  V(J) = AL(J-1)
    AL(J) = ( AL(J-1) * ( DV(J)-DL(J-1) ) - Q(J) ) / ( DV(J+1)-DL(J) )
    GO TO 80
C
C     REBOILER
C
70  V(J) = AL(J-1)
    AL(J) = 0.0D0
    Q(J) = AL(J-1) * ( DV(J) - DL(J-1) )
80  CONTINUE
C
C     CALCULATE GM
C
    CALL THERMO(M,4)
    SUM = 0.0D0
    DO 90 I=1,N
    SUM = SUM + X(M,I) * VM(I)
90  CONTINUE
    G(M) = U(M) * SUM
    RETURN
    END
C
C     SUBROUTINE SPRINT
C     PRINTS STEADY-STATE TOTAL-REFLUX RESULTS
C     IMPLICIT REAL*8(A-H,O-Z)
C     COMMON /FILE/
1   IIN,          IOUT
    COMMON /DATA/
1   F,           Z(50),      P(40),      G(40),      Q(40),      EM(40,50),
2   FC,          ZC(50),     CF(6),      CZ(50,6),   RR,         DR,
3   FCUT,        ZCUT(50),   TCUT(15),   DMAX,       TOL,        NAME(50,3),
4   MAXIT,       N,          M,          M1, IC,     INITL,      IPRNT
    COMMON /SCALC/
1   T(40),       AL(40),     V(40),     U(40),     X(40,50),   Y(40,50),
2   DT(40),     DL(40),     DV(40),    DU(40),    DX(40,50),  SUMDX(40),
3   AK(50),     HV(50),     HL(50),    VM(50),    DKDT(50),   DHVDT(50),
4   DHLDT(50),  DVMDT(50),  SCALE,     CONV,      ICONV,      ITER
C
    IF( (ICONV.NE.0) .AND. (IPRNT.LE.2) ) RETURN
C
C     PRINT STEADY STATE PROFILE
C
    WRITE(IOUT,900) ITER
    WRITE(IOUT,910) (J,DT(J),T(J),V(J),AL(J),DU(J),U(J),G(J),Q(J),
1   P(J),SUMDX(J),J=1,M)
    WRITE(IOUT,920) SCALE, CONV, ICONV
C
    IF( (ICONV.NE.0) .OR. (IPRNT.LE.1) ) RETURN
C
C     PRINT X
C
    WRITE(IOUT,930)
    WRITE(IOUT,1000) (I,I=1,N)
    WRITE(IOUT,1010) ((NAME(I,K),K=1,3),I=1,N)
    DO 10 J=1,M
    WRITE(IOUT,1020) J, (X(J,I),I=1,N)
10  CONTINUE
C

```

```

C      PRINT DX
C
      WRITE(IOUT,940)
      WRITE(IOUT,1000) (I,I=1,N)
      WRITE(IOUT,1010) ((NAME(I,K),K=1,3),I=1,N)
      DO 20 J=1,M
      WRITE(IOUT,1020) J, (DX(J,I),I=1,N)
20 CONTINUE
C
C      PRINT Y
C
      WRITE(IOUT,950)
      WRITE(IOUT,1000) (I,I=1,N)
      WRITE(IOUT,1010) ((NAME(I,K),K=1,3),I=1,N)
      DO 30 J=1,M
      WRITE(IOUT,1020) J, (Y(J,I),I=1,N)
30 CONTINUE
C
C      PRINT EM
C
      WRITE(IOUT,960)
      WRITE(IOUT,1000) (I,I=1,N)
      WRITE(IOUT,1010) ((NAME(I,K),K=1,3),I=1,N)
      DO 40 J=1,M
      WRITE(IOUT,1020) J, (EM(J,I),I=1,N)
40 CONTINUE
      RETURN
C
900 FORMAT(1H1/40X,'ITERATION NUMBER',I6
1 //40X,'S T E A D Y - S T A T E   P R O F I L E'
2 //' STAGE   DEL TEMP   TEMPERATURE   VAPOR RATE LIQUID RATE   DEL HO
3LDUP MOL HOLDUP VOL HOLDUP   HEAT DUTY   PRESSURE   SUMDX'/)
910 FORMAT(I6,10G12.4)
920 FORMAT('/' SCALE           CONV           ICONV'
1 //2G12.4,I6)
930 FORMAT(1H1/40X,'L I Q U I D   C O M P O S I T I O N')
940 FORMAT( //40X,'D E L   L I Q U I D   C O M P')
950 FORMAT(1H1/40X,'V A P O R   C O M P O S I T I O N')
960 FORMAT( //40X,'M U R P H R E E   E F F I C I E N C Y')
1000 FORMAT(/6X,10(I4,8X),4X
1 //6X,10(I4,8X),4X
2 //6X,10(I4,8X),4X
3 //6X,10(I4,8X),4X
4 //6X,10(I4,8X),4X )
1010 FORMAT(' STAGE',3X,30A4,1X
1 // 9X,30A4,1X
2 // 9X,30A4,1X
3 // 9X,30A4,1X
4 // 9X,30A4,1X )
1020 FORMAT(I6,10G12.4,4X
1 //6X,10G12.4,4X
2 //6X,10G12.4,4X
3 //6X,10G12.4,4X
4 //6X,10G12.4,4X )
      END
      SUBROUTINE UNSTDY(*)
C      MAIN ROUTINE FOR UNSTEADY-STATE BATCH DISTILLATION CALCULATIONS
      IMPLICIT REAL*8(A-H,O-Z)
      COMMON /FILE/
1 IIN, IOUT

```

```

COMMON /DATAIN/
1 FR,          ZR(50),      EMR,          PCOND,      DPCOND,      DPTRAY,
2 GCOND,      GTRAY,      QTRAY,      TTIMES,      IFR
COMMON /DATA/
1 F,          Z(50),      P(40),      G(40),      Q(40),      EM(40,50),
2 FC,          ZC(50),      CF(6),      CZ(50,6),  RR,          DR,
3 FCUT,      ZCUT(50),      TCUT(15),  DMAX,      TOL,        NAME(50,3),
4 MAXIT,      N,          M,          M1, IC,      INITL,      IPRNT
COMMON /SCALC/
1 T(40),      AL(40),      V(40),      U(40),      X(40,50),  Y(40,50),
2 DT(40),      DL(40),      DV(40),      DU(40),      DX(40,50),  SUMDX(40),
3 AK(50),      HV(50),      HL(50),      VM(50),      DKDT(50),  DHVDT(50),
4 DHLDT(50),  DVMDT(50),  SCALE,      CONV,      ICONV,      ITER
COMMON /CLCODE/
1 XT(2000),   RWORK(26022),  IWORK(2020)
EXTERNAL FUNCT, JACOB
DATA LRW/26022/, LIW/2020/, IOPT/0/, ITASK/2/, ITOL/1/, MF/24/
C
CALL WIPE ( XT(1), 28022 )
CALL IWIPE ( IWORK(1), 2020 )
C
INITIALIZE VARIABLES FOR FIRST CALL TO LODE
C
ISTATE = 1
IWORK(1) = 1
IWORK(2) = 1
NEQ = N * M
RTOL = 0.01D0 * TOL
ATOL = RTOL * RTOL
TIME = 0.0D0
TOUT = 1.0D0 / 60.0D0
DO 10 J=1,M
DO 10 I=1,N
L = M * ( I - 1 ) + J
XT(L) = X(J,I)
10 CONTINUE
ITC = 0
TIMCUT = 0.0D0
C
CALL LODE
C
20 CALL LODE( FUNCT, NEQ, XT, TIME, TOUT, ITOL, RTOL, ATOL, ITASK,
1          ISTATE, IOPT, RWORK, LRW, IWORK, LIW, JACOB, MF)
IF( ISTATE .LT. 0 ) GO TO 30
IF( U(M)/F .LT. 0.05D0 ) GO TO 30
IF( ITC .EQ. 0 ) GO TO 30
IF( T(2) .GE. TCUT(ITC) ) GO TO 30
GO TO 20
C
PRINT TIME AND OVERHEAD TEMPERATURE
C
30 TTIME = TTIMES + TIME
TIMCUT = TIME - TIMCUT
IC = 1
FC = DR
DO 40 I=1,N
ZC(I) = X(1,I)
40 CONTINUE
CALL CONVRT(3)
SG = CF(3) / CF(5) / 8.345D0 / 0.999D0

```

```

PMMHG = P(1)
TF = T(2)
CALL MAXBON( PMMHG, TF, SG, TNBP, TNBP12 )
WRITE(IOUT,900) TTIME, TIME, TIMCUT, RWORK(11), T(2), TNBP, TNBP12
C
C PRINT INSTANTANEOUS DISTILLATE
C
IC = 1
FC = DR
DO 50 I=1,N
ZC(I) = X(1,I)
50 CONTINUE
WRITE(IOUT,910)
CALL CONVRT(2)
C
C PRINT CUT DISTILLATE
C
IC = 1
FC = FCUT
DO 60 J=1,M
FC = FC - U(J)
60 CONTINUE
DO 70 I=1,N
ZC(I) = FCUT * ZCUT(I)
DO 70 J=1,M
ZC(I) = ZC(I) - U(J) * X(J,I)
70 CONTINUE
WRITE(IOUT,920)
CALL CONVRT(2)
C
C PRINT CUMULATIVE DISTILLATE
C
IC = 1
FC = F
DO 80 J=1,M
FC = FC - U(J)
80 CONTINUE
DO 90 I=1,N
ZC(I) = F * Z(I)
DO 90 J=1,M
ZC(I) = ZC(I) - U(J) * X(J,I)
90 CONTINUE
WRITE(IOUT,930)
CALL CONVRT(2)
C
C PRINT TOTAL DISTILLATE
C
IC = 1
FC = FR
DO 100 J=1,M
FC = FC - U(J)
100 CONTINUE
DO 110 I=1,N
ZC(I) = FR * ZR(I)
DO 110 J=1,M
ZC(I) = ZC(I) - U(J) * X(J,I)
110 CONTINUE
WRITE(IOUT,940)
CALL CONVRT(2)
C

```



```

C   ADDITIONAL PRINTS
C
WRITE(IOOUT,950) IWORK(11), IWORK(12), IWORK(13)
IF( IPRNT .LE. 3 ) GO TO 120
K1 = IWORK(17) - NEQ + 1
K2 = IWORK(17)
WRITE(IOOUT,960) (RWORK(K),K=K1,K2)
120 CALL UPRINT(TIME)
C
C   CHECK FOR ERRORS OR LIMITS
C
IF( ISTATE .LT. 0 ) GO TO 210
IF( U(M)/F .LT. 0.05D0 ) GO TO 170
ITC = ITC + 1
IF( ITC .GT. 15 ) GO TO 170
IF( TCUT(ITC) .EQ. 0.0D0 ) GO TO 170
C
C   INITIALIZE FOR NEXT CUT
C
TIMCUT = 0.0D0
IF( ITC .EQ. 1 ) GO TO 20
TIMCUT = TIME
FCUT = 0.0D0
DO 130 J=1,M
FCUT = FCUT + U(J)
130 CONTINUE
DO 140 I=1,N
ZCUT(I) = 0.0D0
DO 140 J=1,M
ZCUT(I) = ZCUT(I) + U(J) * X(J,I)
140 CONTINUE
SUM = 0.0D0
DO 150 I=1,N
SUM = SUM + ZCUT(I)
150 CONTINUE
DO 160 I=1,N
ZCUT(I) = ZCUT(I) / SUM
160 CONTINUE
GO TO 20
C
C   CALCULATE FEED CHARGE FOR NEXT OPERATING STEP
C
170 TTIMES = TTIME
IC = 1
FC = 0.0D0
DO 180 J=1,M
FC = FC + U(J)
180 CONTINUE
DO 200 I=1,N
ZC(I) = 0.0D0
DO 190 J=1,M
ZC(I) = ZC(I) + U(J) * X(J,I)
190 CONTINUE
IF( ZC(I)/FC .LT. 1.0D-12 ) ZC(I) = 0.0D0
200 CONTINUE
RETURN
C
C   ERROR RETURN
C
210 WRITE(IOOUT,970) ISTATE

```

RETURN 1

C

```
900 FORMAT(1H1/10X,'TOTAL TIME, HOURS      ',G12.4
1      /10X,'CUMULATIVE TIME, HOURS',G12.4
2      /10X,'CUT TIME, HOURS              ',G12.4
3      /10X,'TIME STEP, HOURS             ',G12.4
4      //10X,'OVERHEAD TEMPERATURE      ',G12.4
5      /10X,'AT 760 MM HG                 ',G12.4
6      /10X,'K = 12                        ',G12.4)
910 FORMAT(//20X,'INSTANTANEOUS DISTILLATE DRAOFF PER HOUR')
920 FORMAT(//20X,'CUT DISTILLATE DRAOFF')
930 FORMAT(//20X,'CUMULATIVE DISTILLATE DRAOFF')
940 FORMAT(//20X,'TOTAL DISTILLATE DRAOFF')
950 FORMAT(//10X,'NUMBER OF STEPS          ',I6
1      /10X,'NUMBER OF FUNCTION CALLS',I6
2      /10X,'NUMBER OF JACOBIAN CALLS',I6)
960 FORMAT(10G12.4)
970 FORMAT(/' LODE ERROR, ISTATE =',I6)
END
```

C

```
SUBROUTINE MAXBON( PMMHG, TF, SG, TNBP, TNBP12 )
CALCULATES NORMAL BOILING POINT USING MAXWELL-BONNELL
IMPLICIT REAL*8(A-H,O-Z)
```

C

```
THIRD = 1.0D0 / 3.0D0
PATM = PMMHG / 760.0D0
TR = TF + 459.67D0
PLOG = DLOG10(PATM)
IF( PMMHG .LT. 2.0D0 )
1 A = (4.741D0-PLOG) / (2876.663D0-43.0D0*PLOG) - 0.0002867D0
IF( (PMMHG.GE.2.0D0) .AND. (PMMHG.LE.760.0D0) )
1 A = (3.877D0-PLOG) / (2387.262D0-95.76D0*PLOG) - 0.0002867D0
IF( PMMHG .GT. 760.0D0 )
1 A = (4.326D0-PLOG) / (2666.376D0-36.0D0*PLOG) - 0.0002867D0
TNBP = 748.1D0*A / ( 1.0D0/TR - 0.0002867D0 + 0.2145D0*A )
TNBP12 = TNBP - 459.67D0
WK = TNBP**THIRD / SG
F = -1.0D0 + 0.005D0 * ( TNBP - 459.67D0 )
IF( F .LT. 0.0D0 ) F = 0.0D0
IF( F .GT. 1.0D0 ) F = 1.0D0
TNBP = TNBP + 2.5D0 * ( WK - 12.0D0 ) * PLOG * F - 459.67D0
RETURN
END
```

C

```
SUBROUTINE FUNCT( NEQ, TIME, XT, DXDT )
CALCULATES DX/DT FOR LODE
IMPLICIT REAL*8(A-H,O-Z)
COMMON /DATA/
1 F,          Z(50),      P(40),        G(40),        Q(40),        EM(40,50),
2 FC,        ZC(50),     CF(6),         CZ(50,6),    RR,           DR,
3 FCUT,      ZCUT(50),   TCUT(15),     DMAX,         TOL,          NAME(50,3),
4 MAXIT,     N,          M,            M1, IC,       INITL,        IPRNT
COMMON /SCALC/
1 T(40),     AL(40),     V(40),        U(40),        X(40,50),     Y(40,50),
2 DT(40),    DL(40),     DV(40),       DU(40),       DX(40,50),    SUMDX(40),
3 AK(50),    HV(50),     HL(50),       VM(50),       DKDT(50),     DHVDT(50),
4 DHLDT(50), DVMDT(50), SCALE,         CONV,         ICONV,        ITER
COMMON /UCALC/
1 SAK(40),   SHV(40),   SHL(40),   SVM(40),   SDKDT(40),   SDHLDT(40),
2 SDVMDT(40), SAKY1(40), SAKX1(40), SAKY(40),   SHLY1(40),   SHLX1(40),
3 SHLY(40),  SVMY1(40), SVMX1(40), SVMY(40),   AKS(40,50),
4 DTD(40),  DUDT(40), DHDT(40)
```

```

DIMENSION XT(NEQ), DXDT(NEQ)
C
CALL WIPE ( SAK(1), 2640 )
C
NORMALIZE X
C
DO 30 J=1,M
XSUM = 0.0D0
DO 10 I=1,N
L = M * ( I - 1 ) + J
X(J,I) = XT(L)
XSUM = XSUM + X(J,I)
10 CONTINUE
DO 20 I=1,N
X(J,I) = X(J,I) / XSUM
20 CONTINUE
30 CONTINUE
C
CALCULATE T, Y, AND AK
C
DO 40 JJ=1,M
J = M - JJ + 1
CALL BUBBLE(J,1)
DO 40 I=1,N
AKS(J,I) = AK(I)
SAK(J) = SAK(J) + X(J,I) * AK(I)
SDKDT(J) = SDKDT(J) + X(J,I) * DKDT(I)
SAKY(J) = SAKY(J) + Y(J,I) * AK(I)
IF( J .NE. M ) SAKY1(J) = SAKY1(J) + Y(J+1,I) * AK(I)
IF( J .NE. 1 ) SAKX1(J) = SAKX1(J) + X(J-1,I) * AK(I)
40 CONTINUE
C
CALCULATE HV, HL, AND VM
C
DO 50 J=1,M
CALL THERMO(J,2)
CALL THERMO(J,3)
CALL THERMO(J,4)
DO 50 I=1,N
SHV(J) = SHV(J) + Y(J,I) * HV(I)
SHL(J) = SHL(J) + X(J,I) * HL(I)
SVM(J) = SVM(J) + X(J,I) * VM(I)
SDHLDT(J) = SDHLDT(J) + X(J,I) * DHLDT(I)
SDVMDT(J) = SDVMDT(J) + X(J,I) * DVMDT(I)
SHLY(J) = SHLY(J) + Y(J,I) * HL(I)
SVMY(J) = SVMY(J) + Y(J,I) * VM(I)
IF( J .NE. M ) SHLY1(J) = SHLY1(J) + Y(J+1,I) * HL(I)
IF( J .NE. 1 ) SHLX1(J) = SHLX1(J) + X(J-1,I) * HL(I)
IF( J .NE. M ) SVMY1(J) = SVMY1(J) + Y(J+1,I) * VM(I)
IF( J .NE. 1 ) SVMX1(J) = SVMX1(J) + X(J-1,I) * VM(I)
50 CONTINUE
C
CALCULATE U, V, L, Q1, QM, GM, AND DXDT
C
U(M) = F
DO 120 J=1,M
IF( J .EQ. 1 ) GO TO 60
IF( J .EQ. M ) GO TO 100
GO TO 80
C

```

```

C      CONDENSER
C
60  U(J) = G(J) / SVM(J)
    U(M) = U(M) - U(J)
    AL(J) = RR * DR
    V(J+1) = (AL(J)+DR)/(1.0D0-SDVMDT(J)/SDKDT(J)/SVM(J)
1   *(SAKY1(J)-SAK(J))+(SVMY1(J)-SVM(J))/SVM(J)
    Q(J) = -SDHLDT(J)/SDKDT(J)*V(J+1)*(SAKY1(J)-SAK(J))
1   +V(J+1)*(SHLY1(J)-SHV(J+1))
    DO 70 I=1,N
    DX(J,I) = V(J+1)*(Y(J+1,I)-X(J,I)) / U(J)
70  CONTINUE
    GO TO 120

C
C      STAGES
C
80  U(J) = G(J) / SVM(J)
    U(M) = U(M) - U(J)
    V(J+1) = (-SDHLDT(J)/SDKDT(J)*(AL(J-1)*(SAKX1(J)-SAK(J))
1   -V(J)*(SAKY(J)-SAK(J)))+AL(J-1)*(SHLX1(J)-SHL(J-1))
2   -V(J)*(SHLY(J)-SHV(J))-Q(J))/(SDHLDT(J)/SDKDT(J)
3   *(SAKY1(J)-SAK(J))+SHV(J+1)-SHLY1(J))
    AL(J) = V(J+1)+AL(J-1)-V(J)-SDVMDT(J)/SDKDT(J)/SVM(J)
1   *(V(J+1)*(SAKY1(J)-SAK(J))+AL(J-1)*(SAKX1(J)-SAK(J))
2   -V(J)*(SAKY(J)-SAK(J)))+(V(J+1)*(SVMY1(J)-SVM(J))
3   +AL(J-1)*(SVMX1(J)-SVM(J))-V(J)*(SVMY(J)-SVM(J)))/SVM(J)
    DO 90 I=1,N
    DX(J,I) = ( V(J+1)*(Y(J+1,I)-X(J,I)) + AL(J-1)*(X(J-1,I)-X(J,I))
1   - V(J)*(Y(J,I)-X(J,I)) ) / U(J)
90  CONTINUE
    GO TO 120

C
C      REBOILER
C
100 U(J) = U(J) - DR * TIME
    G(J) = U(J) * SVM(J)
    Q(J) = -SDHLDT(J)/SDKDT(J)*(AL(J-1)*(SAKX1(J)-SAK(J))
1   -V(J)*(SAKY(J)-SAK(J)))+AL(J-1)*(SHLX1(J)-SHL(J-1))
2   -V(J)*(SHLY(J)-SHV(J))
    DO 110 I=1,N
    DX(J,I) = ( AL(J-1)*(X(J-1,I)-X(J,I)) - V(J)*(Y(J,I)-X(J,I)) )
1   / U(J)
110 CONTINUE
120 CONTINUE

C
C      RETURN DXDT
C
    DO 130 J=1,M
    DO 130 I=1,N
    L = M * ( I - 1 ) + J
    DXDT(L) = DX(J,I)
130 CONTINUE
    RETURN
    END
SUBROUTINE JACOB( NEQ, TIME, XT, ML, MU, PD, NROWPD )
C  CALCULATES JACOBIAN FOR LSODE
    IMPLICIT REAL*8(A-H,O-Z)
    COMMON /DATA/
1   F,          Z(50),      P(40),      G(40),      Q(40),      EM(40,50),
2   FC,         ZC(50),     CF(6),      CZ(50,6),  RR,          DR,

```

```

3 FCUT,          ZCUT(50),  TCUT(15),  DMAX,    TOL,      NAME(50,3),
4 MAXIT,        N,          M,        M1, IC,   INITL,    IPRNT
COMMON /SCALC/
1 T(40),        AL(40),     V(40),    U(40),    X(40,50), Y(40,50),
2 DT(40),        DL(40),     DV(40),    DU(40),    DX(40,50), SUMDX(40),
3 AK(50),        HV(50),     HL(50),    VM(50),    DKDT(50), DHVDT(50),
4 DHLDT(50),    DVMDT(50), SCALE,    CONV,     ICONV,    ITER
COMMON /UCALC/
1 SAK(40),      SHV(40),     SHL(40),   SVM(40),   SDKDT(40), SDHLDT(40),
2 SDVMDT(40),  SAKY1(40),   SAKX1(40), SAKY(40), SHLY1(40), SHLX1(40),
3 SHLY(40),    SVMY1(40), SVMX1(40), SVMY(40), AKS(40,50),
4 DTDT(40),    DUDT(40),  DHDT(40)
DIMENSION XT(NEQ), PD(NROWPD,NEQ)
C
C   CALCULATE JACOBIAN
C
DO 70 J=1,M
IF( J .EQ. 1 ) GO TO 10
IF( J .EQ. M ) GO TO 50
GO TO 30
C
C   CONDENSER
C
10 DO 20 I=1,N
L = M * ( I - 1 ) + J
PD(2,L) = - V(J+1) / U(J)
PD(1,L+1) = V(J+1) * EM(J+1,I) * AKS(J+1,I) / U(J)
20 CONTINUE
GO TO 70
C
C   STAGES
C
30 DO 40 I=1,N
L = M * ( I - 1 ) + J
PD(3,L-1) = AL(J-1) / U(J)
PD(2,L) = -(V(J+1)+AL(J-1)+V(J)*(EM(J,I)*AKS(J,I)-1.0D0)) / U(J)
PD(1,L+1) = (V(J+1)*EM(J+1,I)*AKS(J+1,I)-V(J)*(1.0D0-EM(J,I))
1          *EM(J+1,I)*AKS(J+1,I)) / U(J)
40 CONTINUE
GO TO 70
C
C   REBOILER
C
50 DO 60 I=1,N
L = M * ( I - 1 ) + J
PD(3,L-1) = AL(J-1) / U(J)
PD(2,L) = -(AL(J-1)+V(J)*(EM(J,I)*AKS(J,I)-1.0D0)) / U(J)
60 CONTINUE
70 CONTINUE
RETURN
END
SUBROUTINE UPRINT(TIME)
C   PRINTS UNSTEADY-STATE BATCH DISTILLATION RESULTS
IMPLICIT REAL*8(A-H,O-Z)
COMMON /FILE/
1 IIN,          IOUT
COMMON /DATA/
1 F,           Z(50),     P(40),     G(40),     Q(40),     EM(40,50),
2 FC,          ZC(50),    CF(6),     CZ(50,6),  RR,        DR,
3 FCUT,        ZCUT(50),   TCUT(15),  DMAX,     TOL,       NAME(50,3),

```

```

4 MAXIT,      N,          M,          M1, IC,    INITL,    IPRNT
COMMON /SCALC/
1 T(40),      AL(40),     V(40),     U(40),     X(40,50),  Y(40,50),
2 DT(40),     DL(40),     DV(40),     DU(40),     DX(40,50),  SUMDX(40),
3 AK(50),     HV(50),     HL(50),     VM(50),     DKDT(50),  DHVDT(50),
4 DHLDT(50),  DVMDT(50),  SCALE,     CONV,      ICONV,     ITER
COMMON /UCALC/
1 SAK(40),    SHV(40),    SHL(40),    SVM(40),    SDKDT(40),  SDHLDT(40),
2 SDVMDT(40), SAKY1(40),  SAKX1(40),  SAKY(40),  SHLY1(40),  SHLX1(40),
3 SHLY(40),   SVMY1(40),  SVMX1(40),  SVMY(40),  AKS(40,50),
4 DTD(40),    DUDT(40),   DHDT(40)

C
C   PRINT UNSTEADY STATE PROFILE
C
C   WRITE(IOUT,900) TIME, DR
C   WRITE(IOUT,910) (J,T(J),V(J),AL(J),U(J),G(J),Q(J),P(J),J=1,M)
C
C   IF( IPRNT .LE. 1 ) RETURN
C
C   PRINT X
C
C   WRITE(IOUT,920)
C   WRITE(IOUT,1000) (I,I=1,N)
C   WRITE(IOUT,1010) ((NAME(I,K),K=1,3),I=1,N)
C   DO 10 J=1,M
C   WRITE(IOUT,1020) J, (X(J,I),I=1,N)
10 CONTINUE
C
C   PRINT DXDT
C
C   WRITE(IOUT,930)
C   WRITE(IOUT,1000) (I,I=1,N)
C   WRITE(IOUT,1010) ((NAME(I,K),K=1,3),I=1,N)
C   DO 20 J=1,M
C   WRITE(IOUT,1020) J, (DX(J,I),I=1,N)
20 CONTINUE
C
C   PRINT Y
C
C   WRITE(IOUT,940)
C   WRITE(IOUT,1000) (I,I=1,N)
C   WRITE(IOUT,1010) ((NAME(I,K),K=1,3),I=1,N)
C   DO 30 J=1,M
C   WRITE(IOUT,1020) J, (Y(J,I),I=1,N)
30 CONTINUE
C
C   IF( IPRNT .LE. 2 ) RETURN
C
C   PRINT THERMODYNAMIC DATA
C
C   CALL WIPE ( DTD(1), 120 )
C   IF( IPRNT .LE. 3 ) GO TO 40
C   WRITE(IOUT,950)
C   WRITE(IOUT,1000) (I,I=1,N)
C   WRITE(IOUT,1010) ((NAME(I,K),K=1,3),I=1,N)
40 DO 60 J=1,M
C   CALL THERMO(J,1)
C   CALL THERMO(J,2)
C   CALL THERMO(J,3)
C   CALL THERMO(J,4)

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IF( IPRNT .LE. 3 ) GO TO 50
WRITE(IOUT,1020) J, (AK(I),I=1,N)
WRITE(IOUT,1020) J, (DKDT(I),I=1,N)
WRITE(IOUT,1020) J, (HV(I),I=1,N)
WRITE(IOUT,1020) J, (DHVDT(I),I=1,N)
WRITE(IOUT,1020) J, (HL(I),I=1,N)
WRITE(IOUT,1020) J, (DHLDT(I),I=1,N)
WRITE(IOUT,1020) J, (VM(I),I=1,N)
WRITE(IOUT,1020) J, (DVMDT(I),I=1,N)
50 DO 60 I=1,N
   DTDT(J) = DTDT(J) + DX(J,I) * AK(I)
   DUDT(J) = DUDT(J) + DX(J,I) * VM(I)
   DHDT(J) = DHDT(J) + DX(J,I) * HL(I)
60 CONTINUE
C
C   PRINT DERIVATIVES
C
   DO 70 J=1,M
   DTDT(J) = -DTDT(J) / SDKDT(J)
   DUDT(J) = -U(J) / SVM(J) * ( SDVMDT(J) * DTDT(J) + DUDT(J) )
   DHDT(J) = SDHLDT(J) * DTDT(J) + DHDT(J)
70 CONTINUE
   DUDT(M) = -DR
   DO 80 J=1,M1
   DUDT(M) = DUDT(M) - DUDT(J)
80 CONTINUE
   WRITE(IOUT,960)
   WRITE(IOUT,970) (J,DTDT(J),DUDT(J),DHDT(J),SAK(J),SHV(J),SHL(J),
1     SVM(J),SDKDT(J),SDHLDT(J),SDVMDT(J),J=1,M)
   WRITE(IOUT,980)
   WRITE(IOUT,990) (J,SAKY1(J),SAKX1(J),SAKY(J),SHLY1(J),SHLX1(J),
1     SHLY(J),SVMY1(J),SVMX1(J),SVMY(J),J=1,M)
   RETURN
C
900 FORMAT(1H1/40X,'TIME, HOURS',G12.4
1     //40X,'DISTILLATE RATE',G12.4
2     //40X,'UNSTEADY - STATE PROFILE'
3     //' STAGE TEMPERATURE VAPOR RATE LIQUID RATE MOL HOLDUP VOL HO
4     LDUP HEAT DUTY PRESSURE'//)
910 FORMAT(I6,7G12.4)
920 FORMAT(1H1/40X,'LIQUID COMPOSITION')
930 FORMAT( //40X,'DX / DT')
940 FORMAT(1H1/40X,'VAPOR COMPOSITION')
950 FORMAT(1H1/40X,'THERMODYNAMIC DATA')
960 FORMAT(1H1/40X,'DERIVATIVES'
1     //' STAGE DTDT DUDT DHDT SAK SHV
2     SHL SVM SDKDT SDHLDT SDVMDT'//)
970 FORMAT(I6,10G12.4)
980 FORMAT(
1     //' STAGE SAKY1 SAKX1 SAKY SHLY1 SHLX1
2     SHLY SVMY1 SVMX1 SVMY'//)
990 FORMAT(I6,9G12.4)
1000 FORMAT(/6X,10(I4,8X),4X
1     /6X,10(I4,8X),4X
2     /6X,10(I4,8X),4X
3     /6X,10(I4,8X),4X
4     /6X,10(I4,8X),4X )
1010 FORMAT(' STAGE',3X,30A4,1X
1     / 9X,30A4,1X
2     / 9X,30A4,1X

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3      /      9X,30A4,1X
4      /      9X,30A4,1X )
1020 FORMAT(I6,10G12.4,4X
1      /6X,10G12.4,4X
2      /6X,10G12.4,4X
3      /6X,10G12.4,4X
4      /6X,10G12.4,4X )
END
SUBROUTINE LODE (F, NEQ, Y, T, TOUT, ITOL, RTOL, ATOL, ITASK,
1          ISTATE, IOPT, RWORK, LRW, IWORK, LIW, JAC, MF)
EXTERNAL F, JAC
INTEGER NEQ, ITOL, ITASK, ISTATE, IOPT, LRW, IWORK, LIW, MF
DOUBLE PRECISION Y, T, TOUT, RTOL, ATOL, RWORK
DIMENSION NEQ(1), Y(1), RTOL(1), ATOL(1), RWORK(LRW), IWORK(LIW)
C-----LS00007
C THIS IS THE SEPTEMBER 23, 1980 VERSION OF LS00008
C LODE.. LIVERMORE SOLVER FOR ORDINARY DIFFERENTIAL EQUATIONS. LS00009
C THIS VERSION IS IN DOUBLE PRECISION. LS00010
C LS00011
C LODE SOLVES THE INITIAL VALUE PROBLEM FOR STIFF OR NONSTIFF LS00012
C SYSTEMS OF FIRST ORDER ODE-S, LS00013
C  $DY/DT = F(T, Y)$  , OR, IN COMPONENT FORM, LS00014
C  $DY(I)/DT = F(I) = F(I, T, Y(1), Y(2), \dots, Y(NEQ))$  (I = 1, \dots, NEQ). LS00015
C LODE IS A PACKAGE BASED ON THE GEAR AND GEARB PACKAGES, AND ON THE LS00016
C OCTOBER 23, 1978 VERSION OF THE TENTATIVE ODEPACK USER INTERFACE LS00017
C STANDARD, WITH MINOR MODIFICATIONS. LS00018
C AUTHOR AND CONTACT.. ALAN C. HINDMARSH, LS00019
C MATHEMATICS AND STATISTICS SECTION, L-300 LS00020
C LAWRENCE LIVERMORE LABORATORY LS00021
C LIVERMORE, CA 94550. LS00022
C-----LS00023
C SUMMARY OF USAGE. LS00024
C LS00025
C COMMUNICATION BETWEEN THE USER AND THE LODE PACKAGE, FOR NORMAL LS00026
C SITUATIONS, IS SUMMARIZED BELOW. SEE THE FULL DESCRIPTION FOR LS00027
C DETAILS, INCLUDING OPTIONAL COMMUNICATION, NONSTANDARD OPTIONS, LS00028
C AND INSTRUCTIONS FOR SPECIAL SITUATIONS. SEE ALSO THE EXAMPLE LS00029
C PROBLEM (WITH PROGRAM AND OUTPUT) FOLLOWING THIS SUMMARY. LS00030
C LS00031
C A. FIRST PROVIDE A SUBROUTINE OF THE FORM.. LS00032
C SUBROUTINE F (NEQ, T, Y, YDOT) LS00033
C DIMENSION Y(NEQ), YDOT(NEQ) LS00034
C WHICH SUPPLIES THE VECTOR FUNCTION F BY LOADING YDOT(I) WITH F(I). LS00035
C LS00036
C B. NEXT DETERMINE (OR GUESS) WHETHER OR NOT THE PROBLEM IS STIFF. LS00037
C STIFFNESS OCCURS WHEN THE JACOBIAN MATRIX DF/DY HAS AN EIGENVALUE LS00038
C WHOSE REAL PART IS NEGATIVE AND LARGE IN MAGNITUDE, COMPARED TO THE LS00039
C RECIPROCAL OF THE T SPAN OF INTEREST. IF THE PROBLEM IS NONSTIFF, LS00040
C USE A METHOD FLAG MF = 10. IF IT IS STIFF, THERE ARE FOUR STANDARD LS00041
C CHOICES FOR MF, AND LODE REQUIRES THE JACOBIAN MATRIX IN SOME FORM. LS00042
C THIS MATRIX IS REGARDED EITHER AS FULL (MF = 21 OR 22), LS00043
C OR BANDED (MF = 24 OR 25). IN THE BANDED CASE, LODE REQUIRES TWO LS00044
C HALF-BANDWIDTH PARAMETERS ML AND MU. THESE ARE, RESPECTIVELY, THE LS00045
C WIDTHS OF THE LOWER AND UPPER PARTS OF THE BAND, EXCLUDING THE MAIN LS00046
C DIAGONAL. THUS THE BAND CONSISTS OF THE LOCATIONS (I,J) WITH LS00047
C I-ML .LE. J .LE. I+MU, AND THE FULL BANDWIDTH IS ML+MU+1. LS00048
C LS00049
C C. IF THE PROBLEM IS STIFF, YOU ARE ENCOURAGED TO SUPPLY THE JACOBIAN LS00050
C DIRECTLY (MF = 21 OR 24), BUT IF THIS IS NOT FEASIBLE, LODE WILL LS00051
C COMPUTE IT INTERNALLY BY DIFFERENCE QUOTIENTS (MF = 22 OR 25). LS00052

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C IF YOU ARE SUPPLYING THE JACOBIAN, PROVIDE A SUBROUTINE OF THE FORM.. LS0005
C     SUBROUTINE JAC (NEQ, T, Y, ML, MU, PD, NROWPD) LS0005
C     DIMENSION Y(NEQ), PD(NROWPD,NEQ) LS0005
C WHICH SUPPLIES DF/DY BY LOADING PD AS FOLLOWS.. LS0005
C     FOR A FULL JACOBIAN (MF = 21), LOAD PD(I,J) WITH DF(I)/DY(J), LS0005
C THE PARTIAL DERIVATIVE OF F(I) WITH RESPECT TO Y(J). (IGNORE THE LS0005
C ML AND MU ARGUMENTS IN THIS CASE.) LS0005
C     FOR A BANDED JACOBIAN (MF = 24), LOAD PD(I-J+MU+1,J) WITH LS0006
C DF(I)/DY(J), I.E. LOAD THE DIAGONAL LINES OF DF/DY INTO THE ROWS OF LS0006
C PD FROM THE TOP DOWN. LS0006
C     IN EITHER CASE, ONLY NONZERO ELEMENTS NEED BE LOADED. LS0006
C LS0006
C D. WRITE A MAIN PROGRAM WHICH CALLS SUBROUTINE LSODE ONCE FOR LS0006
C EACH POINT AT WHICH ANSWERS ARE DESIRED. THIS SHOULD ALSO PROVIDE LS0006
C FOR POSSIBLE USE OF LOGICAL UNIT 6 FOR OUTPUT OF ERROR MESSAGES LS0006
C BY LSODE. ON THE FIRST CALL TO LSODE, SUPPLY ARGUMENTS AS FOLLOWS.. LS0006
C F = NAME OF SUBROUTINE FOR RIGHT-HAND SIDE VECTOR F. LS0006
C     THIS NAME MUST BE DECLARED EXTERNAL IN CALLING PROGRAM. LS0007
C NEQ = NUMBER OF FIRST ORDER ODE-S. LS0007
C Y = ARRAY OF INITIAL VALUES, OF LENGTH NEQ. LS0007
C T = THE INITIAL VALUE OF THE INDEPENDENT VARIABLE. LS0007
C TOUT = FIRST POINT WHERE OUTPUT IS DESIRED (.NE. T). LS0007
C ITOL = 1 OR 2 ACCORDING AS ATOL (BELOW) IS A SCALAR OR ARRAY. LS0007
C RTOL = RELATIVE TOLERANCE PARAMETER (SCALAR). LS0007
C ATOL = ABSOLUTE TOLERANCE PARAMETER (SCALAR OR ARRAY). LS0007
C     THE LOCAL ERROR IN Y(I) WILL BE CONTROLLED SO AS TO BE LS0007
C     ROUGHLY LESS THAN RTOL*ABS(Y(I)) + ATOL IF ITOL = 1, LS0007
C     OR RTOL*ABS(Y(I)) + ATOL(I) IF ITOL = 2. USE RTOL = 0.0 LS0008
C     FOR PURE ABSOLUTE ERROR CONTROL, ATOL (OR ATOL(I)) = 0.0 LS0008
C     FOR PURE RELATIVE. CAUTION.. ACTUAL (GLOBAL) ERRORS LS0008
C     MAY EXCEED THESE TOLERANCES, SO CHOOSE THEM CONSERVATIVELY. LS0008
C ITASK = 1 FOR NORMAL COMPUTATION OF OUTPUT VALUES OF Y AT T = TOUT. LS0008
C ISTATE = INTEGER FLAG (INPUT AND OUTPUT). SET ISTATE = 1. LS0008
C IOPT = 0 TO INDICATE NO OPTIONAL INPUTS USED. LS0008
C RWORK = REAL WORK ARRAY OF LENGTH AT LEAST.. LS0008
C     20 + 16*NEQ FOR MF = 10, LS0008
C     22 + 9*NEQ + NEQ**2 FOR MF = 21 OR 22, LS0008
C     22 + 10*NEQ + (2*ML + MU)*NEQ FOR MF = 24 OR 25. LS0009
C LRW = DECLARED LENGTH OF RWORK (IN USER-S DIMENSION). LS0009
C IWORK = INTEGER WORK ARRAY OF LENGTH AT LEAST.. LS0009
C     20 FOR MF = 10, LS0009
C     20 + NEQ FOR MF = 21, 22, 24, OR 25. LS0009
C     IF MF = 24 OR 25, INPUT IN IWORK(1),IWORK(2) THE LOWER LS0009
C     AND UPPER HALF-BANDWIDTHS ML,MU. LS0009
C LIW = DECLARED LENGTH OF IWORK (IN USER-S DIMENSION). LS0009
C JAC = NAME OF SUBROUTINE FOR JACOBIAN MATRIX (MF = 21 OR 24). LS0009
C     IF USED, THIS NAME MUST BE DECLARED EXTERNAL IN CALLING LS0009
C     PROGRAM. IF NOT USED, PASS A DUMMY NAME. LS0010
C MF = METHOD FLAG. STANDARD VALUES ARE.. LS0010
C     10 FOR NONSTIFF (ADAMS) METHOD, NO JACOBIAN USED. LS0010
C     21 FOR STIFF (BDF) METHOD, USER-SUPPLIED FULL JACOBIAN. LS0010
C     22 FOR STIFF METHOD, INTERNALLY GENERATED FULL JACOBIAN. LS0010
C     24 FOR STIFF METHOD, USER-SUPPLIED BANDED JACOBIAN. LS0010
C     25 FOR STIFF METHOD, INTERNALLY GENERATED BANDED JACOBIAN. LS0010
C LS0010
C E. THE OUTPUT FROM THE FIRST CALL (OR ANY CALL) IS.. LS0010
C     Y = ARRAY OF COMPUTED VALUES OF Y(T) VECTOR. LS0010
C     T = CORRESPONDING VALUE OF INDEPENDENT VARIABLE (NORMALLY TOUT). LS0010
C ISTATE = 2 IF LSODE WAS SUCCESSFUL, NEGATIVE OTHERWISE. LS0010
C     -1 MEANS EXCESS WORK DONE ON THIS CALL (PERHAPS WRONG MF). LS0010

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C 80 WRITE(3,90)ISTATE LS00177
C 90 FORMAT(///22H ERROR HALT.. ISTATE =,I3) LS00177
C STOP LS00177
C END LS00177
C LS00177
C SUBROUTINE FEX (NEQ, T, Y, YDOT) LS00178
C DOUBLE PRECISION T, Y, YDOT LS00179
C DIMENSION Y(3), YDOT(3) LS00180
C YDOT(1) = -.04D0*Y(1) + 1.D4*Y(2)*Y(3) LS00181
C YDOT(3) = 3.D7*Y(2)*Y(2) LS00182
C YDOT(2) = -YDOT(1) - YDOT(3) LS00183
C RETURN LS00184
C END LS00185
C LS00186
C SUBROUTINE JEX (NEQ, T, Y, ML, MU, PD, NRPD) LS00187
C DOUBLE PRECISION PD, T, Y LS00188
C DIMENSION Y(3), PD(NRPD,3) LS00189
C PD(1,1) = -.04D0 LS00190
C PD(1,2) = 1.D4*Y(3) LS00191
C PD(1,3) = 1.D4*Y(2) LS00192
C PD(2,1) = .04D0 LS00193
C PD(2,3) = -PD(1,3) LS00194
C PD(3,2) = 6.D7*Y(2) LS00195
C PD(2,2) = -PD(1,2) - PD(3,2) LS00196
C RETURN LS00197
C END LS00198
C LS00199
C THE OUTPUT OF THIS PROGRAM (ON A CDC-7600 IN SINGLE PRECISION) LS00200
C IS AS FOLLOWS.. LS00201
C LS00202
C AT T = 4.0000E-01 Y = 9.851726E-01 3.386406E-05 1.479357E-02 LS00203
C AT T = 4.0000E+00 Y = 9.055142E-01 2.240418E-05 9.446344E-02 LS00204
C AT T = 4.0000E+01 Y = 7.158050E-01 9.184616E-06 2.841858E-01 LS00205
C AT T = 4.0000E+02 Y = 4.504846E-01 3.222434E-06 5.495122E-01 LS00206
C AT T = 4.0000E+03 Y = 1.831701E-01 8.940379E-07 8.168290E-01 LS00207
C AT T = 4.0000E+04 Y = 3.897016E-02 1.621193E-07 9.610297E-01 LS00208
C AT T = 4.0000E+05 Y = 4.935213E-03 1.983756E-08 9.950648E-01 LS00209
C AT T = 4.0000E+06 Y = 5.159269E-04 2.064759E-09 9.994841E-01 LS00210
C AT T = 4.0000E+07 Y = 5.306413E-05 2.122677E-10 9.999469E-01 LS00211
C AT T = 4.0000E+08 Y = 5.494529E-06 2.197824E-11 9.999945E-01 LS00212
C AT T = 4.0000E+09 Y = 5.129458E-07 2.051784E-12 9.999995E-01 LS00213
C AT T = 4.0000E+10 Y = -7.170592E-08 -2.868236E-13 1.000000E+00 LS00214
C LS00215
C NO. STEPS = 330 NO. F-S = 405 NO. J-S = 69 LS00216
C ----- LS00217
C FULL DESCRIPTION OF USER INTERFACE TO LSNODE. LS00218
C LS00219
C THE USER INTERFACE TO LSNODE CONSISTS OF THE FOLLOWING PARTS. LS00220
C LS00221
C I. THE CALL SEQUENCE TO SUBROUTINE LSNODE, WHICH IS A DRIVER LS00222
C ROUTINE FOR THE SOLVER. THIS INCLUDES DESCRIPTIONS OF BOTH LS00223
C THE CALL SEQUENCE ARGUMENTS AND OF USER-SUPPLIED ROUTINES. LS00224
C FOLLOWING THESE DESCRIPTIONS IS A DESCRIPTION OF LS00225
C OPTIONAL INPUTS AVAILABLE THROUGH THE CALL SEQUENCE, AND THEN LS00226
C A DESCRIPTION OF OPTIONAL OUTPUTS (IN THE WORK ARRAYS). LS00227
C LS00228
C II. DESCRIPTIONS OF OTHER ROUTINES IN THE LSNODE PACKAGE THAT MAY BE LS00229
C (OPTIONALLY) CALLED BY THE USER. THESE PROVIDE THE ABILITY TO LS00230
C ALTER ERROR MESSAGE HANDLING, SAVE AND RESTORE THE INTERNAL LS00231
C COMMON, AND OBTAIN SPECIFIED DERIVATIVES OF THE SOLUTION Y(T). LS00232

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C		LS00233
C	III. DESCRIPTIONS OF COMMON BLOCKS TO BE DECLARED IN OVERLAY	LS00234
C	OR SIMILAR ENVIRONMENTS, OR TO BE SAVED WHEN DOING AN INTERRUPT	LS00235
C	OF THE PROBLEM AND CONTINUED SOLUTION LATER.	LS00236
C		LS00237
C	IV. DESCRIPTION OF TWO SUBROUTINES IN THE LSODE PACKAGE, EITHER OF	LS00238
C	WHICH THE USER MAY REPLACE WITH HIS OWN VERSION, IF DESIRED.	LS00239
C	THESE RELATE TO THE MEASUREMENT OF ERRORS.	LS00240
C		LS00241
C	-----	LS00242
C	PART I. CALL SEQUENCE.	LS00243
C		LS00244
C	THE CALL SEQUENCE PARAMETERS USED FOR INPUT ONLY ARE	LS00245
C	F, NEQ, TOUT, ITOL, RTOL, ATOL, ITASK, IOPT, LRW, LIW, JAC, MF,	LS00246
C	AND THOSE USED FOR BOTH INPUT AND OUTPUT ARE	LS00247
C	Y, T, ISTATE.	LS00248
C	THE WORK ARRAYS RWORK AND IWORK ARE ALSO USED FOR CONDITIONAL AND	LS00249
C	OPTIONAL INPUTS AND OPTIONAL OUTPUTS. (THE TERM OUTPUT HERE REFERS	LS00250
C	TO THE RETURN FROM SUBROUTINE LSODE TO THE USER-S CALLING PROGRAM.)	LS00251
C		LS00252
C	THE LEGALITY OF INPUT PARAMETERS WILL BE THOROUGHLY CHECKED ON THE	LS00253
C	INITIAL CALL FOR THE PROBLEM, BUT NOT CHECKED THEREAFTER UNLESS A	LS00254
C	CHANGE IN INPUT PARAMETERS IS FLAGGED BY ISTATE = 3 ON INPUT.	LS00255
C		LS00256
C	THE DESCRIPTIONS OF THE CALL ARGUMENTS ARE AS FOLLOWS.	LS00257
C		LS00258
C	F = THE NAME OF THE USER-SUPPLIED SUBROUTINE DEFINING THE	LS00259
C	ODE SYSTEM. THE SYSTEM MUST BE PUT IN THE FIRST-ORDER	LS00260
C	FORM $DY/DT = F(T,Y)$, WHERE F IS A VECTOR-VALUED FUNCTION	LS00261
C	OF THE SCALAR T AND THE VECTOR Y. SUBROUTINE F IS TO	LS00262
C	COMPUTE THE FUNCTION F. IT IS TO HAVE THE FORM	LS00263
C	SUBROUTINE F (NEQ, T, Y, YDOT)	LS00264
C	DIMENSION Y(1), YDOT(1)	LS00265
C	WHERE NEQ, T, AND Y ARE INPUT, AND THE ARRAY YDOT = F(T,Y)	LS00266
C	IS OUTPUT. Y AND YDOT ARE ARRAYS OF LENGTH NEQ.	LS00267
C	(IN THE DIMENSION STATEMENT ABOVE, 1 IS A DUMMY	LS00268
C	DIMENSION.. IT CAN BE REPLACED BY ANY VALUE.)	LS00269
C	SUBROUTINE F SHOULD NOT ALTER Y(1),...,Y(NEQ).	LS00270
C	F MUST BE DECLARED EXTERNAL IN THE CALLING PROGRAM.	LS00271
C		LS00272
C	SUBROUTINE F MAY ACCESS USER-DEFINED QUANTITIES IN	LS00273
C	NEQ(2),... AND Y(NEQ(1)+1),... IF NEQ IS AN ARRAY	LS00274
C	(DIMENSIONED IN F) AND Y HAS LENGTH EXCEEDING NEQ(1).	LS00275
C	SEE THE DESCRIPTIONS OF NEQ AND Y BELOW.	LS00276
C		LS00277
C	NEQ = THE SIZE OF THE ODE SYSTEM (NUMBER OF FIRST ORDER	LS00278
C	ORDINARY DIFFERENTIAL EQUATIONS). USED ONLY FOR INPUT.	LS00279
C	NEQ MAY BE DECREASED, BUT NOT INCREASED, DURING THE PROBLEM.	LS00280
C	IF NEQ IS DECREASED (WITH ISTATE = 3 ON INPUT), THE	LS00281
C	REMAINING COMPONENTS OF Y SHOULD BE LEFT UNDISTURBED, IF	LS00282
C	THESE ARE TO BE ACCESSED IN F AND/OR JAC.	LS00283
C		LS00284
C	NORMALLY, NEQ IS A SCALAR, AND IT IS GENERALLY REFERRED TO	LS00285
C	AS A SCALAR IN THIS USER INTERFACE DESCRIPTION. HOWEVER,	LS00286
C	NEQ MAY BE AN ARRAY, WITH NEQ(1) SET TO THE SYSTEM SIZE.	LS00287
C	(THE LSODE PACKAGE ACCESSES ONLY NEQ(1).) IN EITHER CASE,	LS00288
C	THIS PARAMETER IS PASSED AS THE NEQ ARGUMENT IN ALL CALLS	LS00289
C	TO F AND JAC. HENCE, IF IT IS AN ARRAY, LOCATIONS	LS00290
C	NEQ(2),... MAY BE USED TO STORE OTHER INTEGER DATA AND PASS	LS00291
C	IT TO F AND/OR JAC. SUBROUTINES F AND/OR JAC MUST INCLUDE	LS00292

C NEQ IN A DIMENSION STATEMENT IN THAT CASE. LS0029
 C LS0029
 C Y = A REAL ARRAY FOR THE VECTOR OF DEPENDENT VARIABLES, OF LS0029
 C LENGTH NEQ OR MORE. USED FOR BOTH INPUT AND OUTPUT ON THE LS0029
 C FIRST CALL (ISTATE = 1), AND ONLY FOR OUTPUT ON OTHER CALLS. LS0029
 C ON THE FIRST CALL, Y MUST CONTAIN THE VECTOR OF INITIAL LS0029
 C VALUES. ON OUTPUT, Y CONTAINS THE COMPUTED SOLUTION VECTOR, LS0029
 C EVALUATED AT T. IF DESIRED, THE Y ARRAY MAY BE USED LS0030
 C FOR OTHER PURPOSES BETWEEN CALLS TO THE SOLVER. LS0030
 C LS0030
 C THIS ARRAY IS PASSED AS THE Y ARGUMENT IN ALL CALLS TO LS0030
 C F AND JAC. HENCE ITS LENGTH MAY EXCEED NEQ, AND LOCATIONS LS0030
 C Y(NEQ+1),... MAY BE USED TO STORE OTHER REAL DATA AND LS0030
 C PASS IT TO F AND/OR JAC. (THE LSODE PACKAGE ACCESSES ONLY LS0030
 C Y(1),...,Y(NEQ).) LS0030
 C LS0030
 C T = THE INDEPENDENT VARIABLE. ON INPUT, T IS USED ONLY ON THE LS0030
 C FIRST CALL, AS THE INITIAL POINT OF THE INTEGRATION. LS0031
 C ON OUTPUT, AFTER EACH CALL, T IS THE VALUE AT WHICH A LS0031
 C COMPUTED SOLUTION Y IS EVALUATED (USUALLY THE SAME AS TOUT). LS0031
 C ON AN ERROR RETURN, T IS THE FARTHEST POINT REACHED. LS0031
 C LS0031
 C TOUT = THE NEXT VALUE OF T AT WHICH A COMPUTED SOLUTION IS DESIRED. LS0031
 C USED ONLY FOR INPUT. LS0031
 C LS0031
 C WHEN STARTING THE PROBLEM (ISTATE = 1), TOUT MAY BE EQUAL LS0031
 C TO T FOR ONE CALL, THEN SHOULD .NE. T FOR THE NEXT CALL. LS0031
 C FOR THE INITIAL T, AN INPUT VALUE OF TOUT .NE. T IS USED LS0032
 C IN ORDER TO DETERMINE THE DIRECTION OF THE INTEGRATION LS0032
 C (I.E. THE ALGEBRAIC SIGN OF THE STEP SIZES) AND THE ROUGH LS0032
 C SCALE OF THE PROBLEM. INTEGRATION IN EITHER DIRECTION LS0032
 C (FORWARD OR BACKWARD IN T) IS PERMITTED. LS0032
 C LS0032
 C IF ITASK = 2 OR 5 (ONE-STEP MODES), TOUT IS IGNORED AFTER LS0032
 C THE FIRST CALL (I.E. THE FIRST CALL WITH TOUT .NE. T). LS0032
 C OTHERWISE, TOUT IS REQUIRED ON EVERY CALL. LS0032
 C LS0032
 C IF ITASK = 1, 3, OR 4, THE VALUES OF TOUT NEED NOT BE LS0033
 C MONOTONE, BUT A VALUE OF TOUT WHICH BACKS UP IS LIMITED LS0033
 C TO THE CURRENT INTERNAL T INTERVAL, WHOSE ENDPOINTS ARE LS0033
 C TCUR - HU AND TCUR (SEE OPTIONAL OUTPUTS, BELOW, FOR LS0033
 C TCUR AND HU). LS0033
 C LS0033
 C ITOL = AN INDICATOR FOR THE TYPE OF ERROR CONTROL. SEE LS0033
 C DESCRIPTION BELOW UNDER ATOL. USED ONLY FOR INPUT. LS0033
 C LS0033
 C RTOL = A RELATIVE ERROR TOLERANCE PARAMETER, EITHER A SCALAR OR LS0033
 C AN ARRAY OF LENGTH NEQ. SEE DESCRIPTION BELOW UNDER ATOL. LS0034
 C INPUT ONLY. LS0034
 C LS0034
 C ATOL = AN ABSOLUTE ERROR TOLERANCE PARAMETER, EITHER A SCALAR OR LS0034
 C AN ARRAY OF LENGTH NEQ. INPUT ONLY. LS0034
 C LS0034
 C THE INPUT PARAMETERS ITOL, RTOL, AND ATOL DETERMINE LS0034
 C THE ERROR CONTROL PERFORMED BY THE SOLVER. THE SOLVER WILL LS0034
 C CONTROL THE VECTOR E = (E(I)) OF ESTIMATED LOCAL ERRORS LS0034
 C IN Y, ACCORDING TO AN INEQUALITY OF THE FORM LS0034
 C
$$\text{RMS-NORM OF } (E(I)/\text{EWT}(I)) \leq 1,$$
 C WHERE
$$\text{EWT}(I) = \text{RTOL}(I)*\text{ABS}(Y(I)) + \text{ATOL}(I),$$
 C AND THE RMS-NORM (ROOT-MEAN-SQUARE NORM) HERE IS LS0035
 C LS0035

C RMS-NORM(V) = SQRT(SUM V(I)**2 / NEQ). HERE EWT = (EWT(I)) LS00353
 C IS A VECTOR OF WEIGHTS WHICH MUST ALWAYS BE POSITIVE, AND LS00354
 C THE VALUES OF RTOL AND ATOL SHOULD ALL BE NON-NEGATIVE. LS00355
 C THE FOLLOWING TABLE GIVES THE TYPES (SCALAR/ARRAY) OF LS00356
 C RTOL AND ATOL, AND THE CORRESPONDING FORM OF EWT(I). LS00357
 C LS00358
 C

ITOL	RTOL	ATOL	EWT(I)
1	SCALAR	SCALAR	RTOL*ABS(Y(I)) + ATOL
2	SCALAR	ARRAY	RTOL*ABS(Y(I)) + ATOL(I)
3	ARRAY	SCALAR	RTOL(I)*ABS(Y(I)) + ATOL
4	ARRAY	ARRAY	RTOL(I)*ABS(Y(I)) + ATOL(I)

C LS00359
 C LS00360
 C LS00361
 C LS00362
 C LS00363
 C LS00364
 C WHEN EITHER OF THESE PARAMETERS IS A SCALAR, IT NEED NOT LS00365
 C BE DIMENSIONED IN THE USER-S CALLING PROGRAM. LS00366
 C LS00367
 C IF NONE OF THE ABOVE CHOICES (WITH ITOL, RTOL, AND ATOL LS00368
 C FIXED THROUGHOUT THE PROBLEM) IS SUITABLE, MORE GENERAL LS00369
 C ERROR CONTROLS CAN BE OBTAINED BY SUBSTITUTING LS00370
 C USER-SUPPLIED ROUTINES FOR THE SETTING OF EWT AND/OR FOR LS00371
 C THE NORM CALCULATION. SEE PART IV BELOW. LS00372
 C LS00373
 C IF GLOBAL ERRORS ARE TO BE ESTIMATED BY MAKING A REPEATED LS00374
 C RUN ON THE SAME PROBLEM WITH SMALLER TOLERANCES, THEN ALL LS00375
 C COMPONENTS OF RTOL AND ATOL (I.E. OF EWT) SHOULD BE SCALED LS00376
 C DOWN UNIFORMLY. LS00377
 C LS00378
 C

C ITASK = AN INDEX SPECIFYING THE TASK TO BE PERFORMED. LS00379
 C INPUT ONLY. ITASK HAS THE FOLLOWING VALUES AND MEANINGS. LS00380
 C 1 MEANS NORMAL COMPUTATION OF OUTPUT VALUES OF Y(T) AT LS00381
 C T = TOUT (BY OVERSHOOTING AND INTERPOLATING). LS00382
 C 2 MEANS TAKE ONE STEP ONLY AND RETURN. LS00383
 C 3 MEANS STOP AT THE FIRST INTERNAL MESH POINT AT OR LS00384
 C BEYOND T = TOUT AND RETURN. LS00385
 C 4 MEANS NORMAL COMPUTATION OF OUTPUT VALUES OF Y(T) AT LS00386
 C T = TOUT BUT WITHOUT OVERSHOOTING T = TCRIT. LS00387
 C TCRIT MUST BE INPUT AS RWORK(1). TCRIT MAY BE EQUAL TO LS00388
 C OR BEYOND TOUT, BUT NOT BEHIND IT IN THE DIRECTION OF LS00389
 C INTEGRATION. THIS OPTION IS USEFUL IF THE PROBLEM LS00390
 C HAS A SINGULARITY AT OR BEYOND T = TCRIT. LS00391
 C 5 MEANS TAKE ONE STEP, WITHOUT PASSING TCRIT, AND RETURN. LS00392
 C TCRIT MUST BE INPUT AS RWORK(1). LS00393
 C LS00394
 C

C NOTE.. IF ITASK = 4 OR 5 AND THE SOLVER REACHES TCRIT LS00395
 C (WITHIN ROUND OFF), IT WILL RETURN T = TCRIT (EXACTLY) LS00396
 C INDICATE THIS (UNLESS ITASK = 4 AND TOUT COMES BEFORE TCRIT, LS00397
 C IN WHICH CASE ANSWERS AT T = TOUT ARE RETURNED FIRST). LS00398
 C LS00399
 C

C ISTATE = AN INDEX USED FOR INPUT AND OUTPUT TO SPECIFY THE LS00400
 C THE STATE OF THE CALCULATION. LS00401
 C LS00402
 C ON INPUT, THE VALUES OF ISTATE ARE AS FOLLOWS. LS00403
 C 1 MEANS THIS IS THE FIRST CALL FOR THE PROBLEM LS00404
 C (INITIALIZATIONS WILL BE DONE). SEE NOTE BELOW. LS00405
 C 2 MEANS THIS IS NOT THE FIRST CALL, AND THE CALCULATION LS00406
 C IS TO CONTINUE NORMALLY, WITH NO CHANGE IN ANY INPUT LS00407
 C PARAMETERS EXCEPT POSSIBLY TOUT AND ITASK. LS00408
 C (IF ITOL, RTOL, AND/OR ATOL ARE CHANGED BETWEEN CALLS LS00409
 C WITH ISTATE = 2, THE NEW VALUES WILL BE USED BUT NOT LS00410
 C TESTED FOR LEGALITY.) LS00411
 C 3 MEANS THIS IS NOT THE FIRST CALL, AND THE LS00412

C CALCULATION IS TO CONTINUE NORMALLY, BUT WITH LS0041
 C A CHANGE IN INPUT PARAMETERS OTHER THAN LS0041
 C TOUT AND ITASK. CHANGES ARE ALLOWED IN LS0041
 C NEQ, ITOL, RTOL, ATOL, IOPT, MF, ML, MU, AND ANY OF THE LS0041
 C OPTIONAL INPUTS EXCEPT H0. LS0041
 C (SEE IWORK DESCRIPTION FOR ML AND MU.) LS0041
 C NOTE.. A PRELIMINARY CALL WITH TOUT = T IS NOT COUNTED LS0041
 C AS A FIRST CALL HERE, AS NO INITIALIZATION OR CHECKING OF LS0042
 C INPUT IS DONE. (SUCH A CALL IS SOMETIMES USEFUL FOR THE LS0042
 C PURPOSE OF OUTPUTTING THE INITIAL CONDITIONS.) LS0042
 C THUS THE FIRST CALL FOR WHICH TOUT .NE. T REQUIRES LS0042
 C ISTATE = 1 ON INPUT. LS0042
 C ON OUTPUT, ISTATE HAS THE FOLLOWING VALUES AND MEANINGS. LS0042
 C 1 MEANS NOTHING WAS DONE, AS TOUT WAS EQUAL TO T WITH LS0042
 C ISTATE = 1 ON INPUT. (HOWEVER, AN INTERNAL COUNTER WAS LS0042
 C SET TO DETECT AND PREVENT REPEATED CALLS OF THIS TYPE.) LS0042
 C 2 MEANS THE INTEGRATION WAS PERFORMED SUCCESSFULLY. LS0043
 C -1 MEANS AN EXCESSIVE AMOUNT OF WORK (MORE THAN MXSTEP LS0043
 C STEPS) WAS DONE ON THIS CALL, BEFORE COMPLETING THE LS0043
 C REQUESTED TASK, BUT THE INTEGRATION WAS OTHERWISE LS0043
 C SUCCESSFUL AS FAR AS T. (MXSTEP IS AN OPTIONAL INPUT LS0043
 C AND IS NORMALLY 500.) TO CONTINUE, THE USER MAY LS0043
 C SIMPLY RESET ISTATE TO A VALUE .GT. 1 AND CALL AGAIN LS0043
 C (THE EXCESS WORK STEP COUNTER WILL BE RESET TO 0). LS0043
 C IN ADDITION, THE USER MAY INCREASE MXSTEP TO AVOID LS0043
 C THIS ERROR RETURN (SEE BELOW ON OPTIONAL INPUTS). LS0043
 C -2 MEANS TOO MUCH ACCURACY WAS REQUESTED FOR THE PRECISION LS0044
 C OF THE MACHINE BEING USED. THIS WAS DETECTED BEFORE LS0044
 C COMPLETING THE REQUESTED TASK, BUT THE INTEGRATION LS0044
 C WAS SUCCESSFUL AS FAR AS T. TO CONTINUE, THE TOLERANCE LS0044
 C PARAMETERS MUST BE RESET, AND ISTATE MUST BE SET LS0044
 C TO 3. THE OPTIONAL OUTPUT TOLSF MAY BE USED FOR THIS LS0044
 C PURPOSE. (NOTE.. IF THIS CONDITION IS DETECTED BEFORE LS0044
 C TAKING ANY STEPS, THEN AN ILLEGAL INPUT RETURN LS0044
 C (ISTATE = -3) OCCURS INSTEAD.) LS0044
 C -3 MEANS ILLEGAL INPUT WAS DETECTED, BEFORE TAKING ANY LS0044
 C INTEGRATION STEPS. SEE WRITTEN MESSAGE FOR DETAILS. LS0045
 C NOTE.. IF THE SOLVER DETECTS AN INFINITE LOOP OF CALLS LS0045
 C TO THE SOLVER WITH ILLEGAL INPUT, IT WILL CAUSE LS0045
 C THE RUN TO STOP. LS0045
 C -4 MEANS THERE WERE REPEATED ERROR TEST FAILURES ON LS0045
 C ONE ATTEMPTED STEP, BEFORE COMPLETING THE REQUESTED LS0045
 C TASK, BUT THE INTEGRATION WAS SUCCESSFUL AS FAR AS T. LS0045
 C THE PROBLEM MAY HAVE A SINGULARITY, OR THE INPUT LS0045
 C MAY BE INAPPROPRIATE. LS0045
 C -5 MEANS THERE WERE REPEATED CONVERGENCE TEST FAILURES ON LS0045
 C ONE ATTEMPTED STEP, BEFORE COMPLETING THE REQUESTED LS0046
 C TASK, BUT THE INTEGRATION WAS SUCCESSFUL AS FAR AS T. LS0046
 C THIS MAY BE CAUSED BY AN INACCURATE JACOBIAN MATRIX, LS0046
 C IF ONE IS BEING USED. LS0046
 C -6 MEANS EWT(I) BECAME ZERO FOR SOME I DURING THE LS0046
 C INTEGRATION. PURE RELATIVE ERROR CONTROL (ATOL(I)=0.0) LS0046
 C WAS REQUESTED ON A VARIABLE WHICH HAS NOW VANISHED. LS0046
 C THE INTEGRATION WAS SUCCESSFUL AS FAR AS T. LS0046
 C NOTE.. SINCE THE NORMAL OUTPUT VALUE OF ISTATE IS 2, LS0046
 C IT DOES NOT NEED TO BE RESET FOR NORMAL CONTINUATION. LS0047
 C ALSO, SINCE A NEGATIVE INPUT VALUE OF ISTATE WILL BE LS0047
 C REGARDED AS ILLEGAL, A NEGATIVE OUTPUT VALUE REQUIRES THE LS0047

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C          USER TO CHANGE IT, AND POSSIBLY OTHER INPUTS, BEFORE          LS0047
C          CALLING THE SOLVER AGAIN.                                       LS0047
C          LS0047
C IOPT    = AN INTEGER FLAG TO SPECIFY WHETHER OR NOT ANY OPTIONAL        LS0047
C          INPUTS ARE BEING USED ON THIS CALL.  INPUT ONLY.               LS0047
C          THE OPTIONAL INPUTS ARE LISTED SEPARATELY BELOW.               LS0047
C          IOPT = 0 MEANS NO OPTIONAL INPUTS ARE BEING USED.              LS0047
C          DEFAULT VALUES WILL BE USED IN ALL CASES.                      LS0048
C          IOPT = 1 MEANS ONE OR MORE OPTIONAL INPUTS ARE BEING USED.     LS0048
C          LS0048
C RWORK   = A REAL WORKING ARRAY (DOUBLE PRECISION).                      LS0048
C          THE LENGTH OF RWORK MUST BE AT LEAST                            LS0048
C          20 + NYH*(MAXORD + 1) + 3*NEQ + LWM    WHERE                    LS0048
C          NYH    = THE INITIAL VALUE OF NEQ,                              LS0048
C          MAXORD = 12 (IF METH = 1) OR 5 (IF METH = 2) (UNLESS A        LS0048
C          SMALLER VALUE IS GIVEN AS AN OPTIONAL INPUT),                  LS0048
C          LWM    = 0    IF MITER = 0,                                     LS0048
C          LWM    = NEQ**2 + 2    IF MITER IS 1 OR 2,                    LS0049
C          LWM    = NEQ + 2    IF MITER = 3, AND                         LS0049
C          LWM    = (2*ML+MU+1)*NEQ + 2 IF MITER IS 4 OR 5.              LS0049
C          (SEE THE MF DESCRIPTION FOR METH AND MITER.)                   LS0049
C          THUS IF MAXORD HAS ITS DEFAULT VALUE AND NEQ IS CONSTANT,      LS0049
C          THIS LENGTH IS..                                               LS0049
C          20 + 16*NEQ    FOR MF = 10,                                  LS0049
C          22 + 16*NEQ + NEQ**2    FOR MF = 11 OR 12,                  LS0049
C          22 + 17*NEQ    FOR MF = 13,                                  LS0049
C          22 + 17*NEQ + (2*ML+MU)*NEQ    FOR MF = 14 OR 15,          LS0049
C          20 + 9*NEQ    FOR MF = 20,                                  LS0049
C          22 + 9*NEQ + NEQ**2    FOR MF = 21 OR 22,                  LS0050
C          22 + 10*NEQ    FOR MF = 23,                                  LS0050
C          22 + 10*NEQ + (2*ML+MU)*NEQ    FOR MF = 24 OR 25.          LS0050
C          THE FIRST 20 WORDS OF RWORK ARE RESERVED FOR CONDITIONAL        LS0050
C          AND OPTIONAL INPUTS AND OPTIONAL OUTPUTS.                      LS0050
C          LS0050
C          THE FOLLOWING WORD IN RWORK IS A CONDITIONAL INPUT..           LS0050
C          RWORK(1) = TCRIT = CRITICAL VALUE OF T WHICH THE SOLVER        LS0050
C          IS NOT TO OVERSHOOT.  REQUIRED IF ITASK IS                       LS0050
C          4 OR 5, AND IGNORED OTHERWISE.  (SEE ITASK.)                  LS0050
C          LS0050
C LRW     = THE LENGTH OF THE ARRAY RWORK, AS DECLARED BY THE USER.     LS0051
C          (THIS WILL BE CHECKED BY THE SOLVER.)                          LS0051
C          LS0051
C IWORK   = AN INTEGER WORK ARRAY.  THE LENGTH OF IWORK MUST BE AT LEAST LS0051
C          20    IF MITER = 0 OR 3 (MF = 10, 13, 20, 23), OR            LS0051
C          20 + NEQ OTHERWISE (MF = 11, 12, 14, 15, 21, 22, 24, 25).    LS0051
C          THE FIRST FEW WORDS OF IWORK ARE USED FOR CONDITIONAL AND      LS0051
C          OPTIONAL INPUTS AND OPTIONAL OUTPUTS.                          LS0051
C          LS0051
C          THE FOLLOWING 2 WORDS IN IWORK ARE CONDITIONAL INPUTS..        LS0052
C          IWORK(1) = ML    THESE ARE THE LOWER AND UPPER                LS0052
C          IWORK(2) = MU    HALF-BANDWIDTHS, RESPECTIVELY, OF THE        LS0052
C          BANDED JACOBIAN, EXCLUDING THE MAIN DIAGONAL.                 LS0052
C          THE BAND IS DEFINED BY THE MATRIX LOCATIONS                    LS0052
C          (I,J) WITH I-ML .LE. J .LE. I+MU.  ML AND MU                  LS0052
C          MUST SATISFY 0 .LE. ML,MU .LE. NEQ-1.                        LS0052
C          THESE ARE REQUIRED IF MITER IS 4 OR 5, AND                      LS0052
C          IGNORED OTHERWISE.  ML AND MU MAY IN FACT BE                  LS0052
C          THE BAND PARAMETERS FOR A MATRIX TO WHICH                     LS0052
C          DF/DY IS ONLY APPROXIMATELY EQUAL.                            LS0053
C          LS0053

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C LIW = THE LENGTH OF THE ARRAY IWORK, AS DECLARED BY THE USER. LS0053
C (THIS WILL BE CHECKED BY THE SOLVER.) LS0053
C LS0053
C NOTE.. THE WORK ARRAYS MUST NOT BE ALTERED BETWEEN CALLS TO LSCODE LS0053
C FOR THE SAME PROBLEM, EXCEPT POSSIBLY FOR THE CONDITIONAL AND LS0053
C OPTIONAL INPUTS, AND EXCEPT FOR THE LAST 3*NEQ WORDS OF RWORK. LS0053
C THE LATTER SPACE IS USED FOR INTERNAL SCRATCH SPACE, AND SO IS LS0053
C AVAILABLE FOR USE BY THE USER OUTSIDE LSCODE BETWEEN CALLS, IF LS0053
C DESIRED (BUT NOT FOR USE BY F OR JAC). LS0054
C LS0054
C JAC = THE NAME OF THE USER-SUPPLIED ROUTINE (MITER = 1 OR 4) TO LS0054
C COMPUTE THE JACOBIAN MATRIX, DF/DY, AS A FUNCTION OF LS0054
C THE SCALAR T AND THE VECTOR Y. IT IS TO HAVE THE FORM LS0054
C SUBROUTINE JAC (NEQ, T, Y, ML, MU, PD, NROWPD) LS0054
C DIMENSION Y(1), PD(NROWPD,1) LS0054
C WHERE NEQ, T, Y, ML, MU, AND NROWPD ARE INPUT AND THE ARRAY LS0054
C PD IS TO BE LOADED WITH PARTIAL DERIVATIVES (ELEMENTS OF LS0054
C THE JACOBIAN MATRIX) ON OUTPUT. PD MUST BE GIVEN A FIRST LS0054
C DIMENSION OF NROWPD. T AND Y HAVE THE SAME MEANING AS IN LS0055
C SUBROUTINE F. (IN THE DIMENSION STATEMENT ABOVE, 1 IS A LS0055
C DUMMY DIMENSION.. IT CAN BE REPLACED BY ANY VALUE.) LS0055
C IN THE FULL MATRIX CASE (MITER = 1), ML AND MU ARE LS0055
C IGNORED, AND THE JACOBIAN IS TO BE LOADED INTO PD IN LS0055
C COLUMNWISE MANNER, WITH DF(I)/DY(J) LOADED INTO PD(I,J). LS0055
C IN THE BAND MATRIX CASE (MITER = 4), THE ELEMENTS LS0055
C WITHIN THE BAND ARE TO BE LOADED INTO PD IN COLUMNWISE LS0055
C MANNER, WITH DIAGONAL LINES OF DF/DY LOADED INTO THE ROWS LS0055
C OF PD. THUS DF(I)/DY(J) IS TO BE LOADED INTO PD(I-J+MU+1,J). LS0055
C ML AND MU ARE THE HALF-BANDWIDTH PARAMETERS (SEE IWORK). LS0056
C THE LOCATIONS IN PD IN THE TWO TRIANGULAR AREAS WHICH LS0056
C CORRESPOND TO NONEXISTENT MATRIX ELEMENTS CAN BE IGNORED LS0056
C OR LOADED ARBITRARILY, AS THEY ARE OVERWRITTEN BY LSCODE. LS0056
C JAC NEED NOT PROVIDE DF/DY EXACTLY. A CRUDE LS0056
C APPROXIMATION (POSSIBLY WITH A SMALLER BANDWIDTH) WILL DO. LS0056
C IN EITHER CASE, PD IS PRESET TO ZERO BY THE SOLVER, LS0056
C SO THAT ONLY THE NONZERO ELEMENTS NEED BE LOADED BY JAC. LS0056
C EACH CALL TO JAC IS PRECEDED BY A CALL TO F WITH THE SAME LS0056
C ARGUMENTS NEQ, T, AND Y. THUS TO GAIN SOME EFFICIENCY, LS0056
C INTERMEDIATE QUANTITIES SHARED BY BOTH CALCULATIONS MAY BE LS0057
C SAVED IN A USER COMMON BLOCK BY F AND NOT RECOMPUTED BY JAC, LS0057
C IF DESIRED. ALSO, JAC MAY ALTER THE Y ARRAY, IF DESIRED. LS0057
C JAC MUST BE DECLARED EXTERNAL IN THE CALLING PROGRAM. LS0057
C SUBROUTINE JAC MAY ACCESS USER-DEFINED QUANTITIES IN LS0057
C NEQ(2),... AND Y(NEQ(1)+1),... IF NEQ IS AN ARRAY LS0057
C (DIMENSIONED IN JAC) AND Y HAS LENGTH EXCEEDING NEQ(1). LS0057
C SEE THE DESCRIPTIONS OF NEQ AND Y ABOVE. LS0057
C LS0057
C MF = THE METHOD FLAG. USED ONLY FOR INPUT. THE LEGAL VALUES OF LS0057
C MF ARE 10, 11, 12, 13, 14, 15, 20, 21, 22, 23, 24, AND 25. LS0058
C MF HAS DECIMAL DIGITS METH AND MITER.. MF = 10*METH + MITER. LS0058
C METH INDICATES THE BASIC LINEAR MULTISTEP METHOD.. LS0058
C METH = 1 MEANS THE IMPLICIT ADAMS METHOD. LS0058
C METH = 2 MEANS THE METHOD BASED ON BACKWARD LS0058
C DIFFERENTIATION FORMULAS (BDF-S). LS0058
C MITER INDICATES THE CORRECTOR ITERATION METHOD.. LS0058
C MITER = 0 MEANS FUNCTIONAL ITERATION (NO JACOBIAN MATRIX LS0058
C IS INVOLVED). LS0058
C MITER = 1 MEANS CHORD ITERATION WITH A USER-SUPPLIED LS0058
C FULL (NEQ BY NEQ) JACOBIAN. LS0059
C MITER = 2 MEANS CHORD ITERATION WITH AN INTERNALLY LS0059

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C          GENERATED (DIFFERENCE QUOTIENT) FULL JACOBIAN          LS0059
C          (USING NEQ EXTRA CALLS TO F PER DF/DY VALUE).          LS0059
C          MITER = 3 MEANS CHORD ITERATION WITH AN INTERNALLY      LS0059
C          GENERATED DIAGONAL JACOBIAN APPROXIMATION.            LS0059
C          (USING 1 EXTRA CALL TO F PER DF/DY EVALUATION).        LS0059
C          MITER = 4 MEANS CHORD ITERATION WITH A USER-SUPPLIED   LS0059
C          BANDED JACOBIAN.                                        LS0059
C          MITER = 5 MEANS CHORD ITERATION WITH AN INTERNALLY      LS0059
C          GENERATED BANDED JACOBIAN (USING ML+MU+1 EXTRA         LS0060
C          CALLS TO F PER DF/DY EVALUATION).                       LS0060
C          IF MITER = 1 OR 4, THE USER MUST SUPPLY A SUBROUTINE   LS0060
C          (THE NAME IS ARBITRARY) AS DESCRIBED ABOVE UNDER JAC.  LS0060
C          FOR OTHER VALUES OF MITER, A DUMMY ARGUMENT CAN BE    LS0060
C          -----LS0060
C OPTIONAL INPUTS.                                               LS0060
C                                                                 LS0060
C THE FOLLOWING IS A LIST OF THE OPTIONAL INPUTS PROVIDED FOR IN  LS0060
C CALL SEQUENCE. (SEE ALSO PART II.) FOR EACH SUCH INPUT VARIABLE, LS0060
C THIS TABLE LISTS ITS NAME AS USED IN THIS DOCUMENTATION, ITS   LS0061
C LOCATION IN THE CALL SEQUENCE, ITS MEANING, AND THE DEFAULT     LS0061
C VALUE. THE USE OF ANY OF THESE INPUTS REQUIRES IOPT = 1, AND IN  LS0061
C THAT CASE ALL OF THESE INPUTS ARE EXAMINED. A VALUE OF ZERO FOR  LS0061
C ANY OF THESE OPTIONAL INPUTS WILL CAUSE THE DEFAULT VALUE TO BE  LS0061
C USED. THUS TO USE A SUBSET OF THE OPTIONAL INPUTS, SIMPLY PRE-  LS0061
C LOAD LOCATIONS 5 TO 10 IN RWORK AND IWORK TO 0.0 AND 0 RESPECTIVELY, AND  LS0061
C THEN SET THOSE OF INTEREST TO NONZERO VALUES.                  LS0061
C                                                                 LS0061
C NAME      LOCATION      MEANING AND DEFAULT VALUE              LS0061
C                                                                 LS0062
C H0        RWORK(5)      THE STEP SIZE TO BE ATTEMPTED ON THE FIRST STEP.  LS0062
C                                     THE DEFAULT VALUE IS DETERMINED BY THE SOLVER.  LS0062
C                                                                 LS0062
C HMAX      RWORK(6)      THE MAXIMUM ABSOLUTE STEP SIZE ALLOWED.  LS0062
C                                     THE DEFAULT VALUE IS INFINITE.                LS0062
C                                                                 LS0062
C HMIN      RWORK(7)      THE MINIMUM ABSOLUTE STEP SIZE ALLOWED.  LS0062
C                                     THE DEFAULT VALUE IS 0. (THIS LOWER BOUND IS NOT  LS0062
C                                     ENFORCED ON THE FINAL STEP BEFORE REACHING TCRIT  LS0062
C                                     WHEN ITASK = 4 OR 5.)                          LS0063
C                                                                 LS0063
C MAXORD    IWORK(5)      THE MAXIMUM ORDER TO BE ALLOWED. THE DEFAULT  LS0063
C                                     VALUE IS 12 IF METH = 1, AND 5 IF METH = 2.     LS0063
C                                     IF MAXORD EXCEEDS THE DEFAULT VALUE, IT WILL   LS0063
C                                     BE REDUCED TO THE DEFAULT VALUE.              LS0063
C                                     IF MAXORD IS CHANGED DURING THE PROBLEM, IT MAY  LS0063
C                                     CAUSE THE CURRENT ORDER TO BE REDUCED.         LS0063
C                                                                 LS0063
C MXSTEP    IWORK(6)      MAXIMUM NUMBER OF (INTERNALLY DEFINED) STEPS  LS0063
C                                     ALLOWED DURING ONE CALL TO THE SOLVER.        LS0064
C                                     THE DEFAULT VALUE IS 500.                       LS0064
C                                                                 LS0064
C MXHNIL    IWORK(7)      MAXIMUM NUMBER OF MESSAGES PRINTED (PER PROBLEM)  LS0064
C                                     WARNING THAT T + H = T ON A STEP (H = STEP SIZE).  LS0064
C                                     THIS MUST BE POSITIVE TO RESULT IN A NON-DEFAULT  LS0064
C                                     VALUE. THE DEFAULT VALUE IS 10.                LS0064
C          -----LS0064
C OPTIONAL OUTPUTS.                                               LS0064
C                                                                 LS0064
C AS OPTIONAL ADDITIONAL OUTPUT FROM LSODE, THE VARIABLES LISTED  LS0065
C BELOW ARE QUANTITIES RELATED TO THE PERFORMANCE OF LSODE       LS0065

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C WHICH ARE AVAILABLE TO THE USER. THESE ARE COMMUNICATED BY WAY OF LS00652
 C THE WORK ARRAYS, BUT ALSO HAVE INTERNAL MNEMONIC NAMES AS SHOWN. LS00653
 C EXCEPT WHERE STATED OTHERWISE, ALL OF THESE OUTPUTS ARE DEFINED LS00654
 C ON ANY SUCCESSFUL RETURN FROM LSCODE, AND ON ANY RETURN WITH LS00655
 C ISTATE = -1, -2, -4, -5, OR -6. ON AN ILLEGAL INPUT RETURN LS00656
 C (ISTATE = -3), THEY WILL BE UNCHANGED FROM THEIR EXISTING VALUES LS00657
 C (IF ANY), EXCEPT POSSIBLY FOR TOLSF, LENRW, AND LENIW. LS00658
 C ON ANY ERROR RETURN, OUTPUTS RELEVANT TO THE ERROR WILL BE DEFINED, LS00659
 C AS NOTED BELOW. LS00660
 C LS00661
 C NAME LOCATION MEANING LS00662
 C LS00663
 C HU RWORK(11) THE STEP SIZE IN T LAST USED (SUCCESSFULLY). LS00664
 C LS00665
 C HCUR RWORK(12) THE STEP SIZE TO BE ATTEMPTED ON THE NEXT STEP. LS00666
 C LS00667
 C TCUR RWORK(13) THE CURRENT VALUE OF THE INDEPENDENT VARIABLE LS00668
 C WHICH THE SOLVER HAS ACTUALLY REACHED, I.E. THE LS00669
 C CURRENT INTERNAL MESH POINT IN T. ON OUTPUT, TCUR LS00670
 C WILL ALWAYS BE AT LEAST AS FAR AS THE ARGUMENT LS00671
 C T, BUT MAY BE FARTHER (IF INTERPOLATION WAS DONE). LS00672
 C LS00673
 C TOLSF RWORK(14) A TOLERANCE SCALE FACTOR, GREATER THAN 1.0, LS00674
 C COMPUTED WHEN A REQUEST FOR TOO MUCH ACCURACY WAS LS00675
 C DETECTED (ISTATE = -3 IF DETECTED AT THE START OF LS00676
 C THE PROBLEM, ISTATE = -2 OTHERWISE). IF ITOL IS LS00677
 C LEFT UNALTERED BUT RTOL AND ATOL ARE UNIFORMLY LS00678
 C SCALED UP BY A FACTOR OF TOLSF FOR THE NEXT CALL, LS00679
 C THEN THE SOLVER IS DEEMED LIKELY TO SUCCEED. LS00680
 C (THE USER MAY ALSO IGNORE TOLSF AND ALTER THE LS00681
 C TOLERANCE PARAMETERS IN ANY OTHER WAY APPROPRIATE.) LS00682
 C LS00683
 C NST IWORK(11) THE NUMBER OF STEPS TAKEN FOR THE PROBLEM SO FAR. LS00684
 C LS00685
 C NFE IWORK(12) THE NUMBER OF F EVALUATIONS FOR THE PROBLEM SO FAR. LS00686
 C LS00687
 C NJE IWORK(13) THE NUMBER OF JACOBIAN EVALUATIONS (AND OF MATRIX LS00688
 C LU DECOMPOSITIONS) FOR THE PROBLEM SO FAR. LS00689
 C LS00690
 C NQU IWORK(14) THE METHOD ORDER LAST USED (SUCCESSFULLY). LS00691
 C LS00692
 C NQCUR IWORK(15) THE ORDER TO BE ATTEMPTED ON THE NEXT STEP. LS00693
 C LS00694
 C IMXER IWORK(16) THE INDEX OF THE COMPONENT OF LARGEST MAGNITUDE IN LS00695
 C THE WEIGHTED LOCAL ERROR VECTOR (E(I)/EWT(I)), LS00696
 C ON AN ERROR RETURN WITH ISTATE = -4 OR -5. LS00697
 C LS00698
 C LENRW IWORK(17) THE LENGTH OF RWORK ACTUALLY REQUIRED. LS00699
 C THIS IS DEFINED ON NORMAL RETURNS AND ON AN ILLEGAL LS00700
 C INPUT RETURN FOR INSUFFICIENT STORAGE. LS00701
 C LS00702
 C LENIW IWORK(18) THE LENGTH OF IWORK ACTUALLY REQUIRED. LS00703
 C THIS IS DEFINED ON NORMAL RETURNS AND ON AN ILLEGAL LS00704
 C INPUT RETURN FOR INSUFFICIENT STORAGE. LS00705
 C LS00706
 C THE FOLLOWING TWO ARRAYS ARE SEGMENTS OF THE RWORK ARRAY WHICH LS00707
 C MAY ALSO BE OF INTEREST TO THE USER AS OPTIONAL OUTPUTS. LS00708
 C FOR EACH ARRAY, THE TABLE BELOW GIVES ITS INTERNAL NAME, LS00709
 C ITS BASE ADDRESS IN RWORK, AND ITS DESCRIPTION. LS00710
 C LS00711

C NAME	BASE ADDRESS	DESCRIPTION	LS00710
C YH	21	THE NORDSIECK HISTORY ARRAY, OF SIZE NYH BY (NQCUR + 1), WHERE NYH IS THE INITIAL VALUE OF NEQ. FOR J = 0,1,...,NQCUR, COLUMN J+1 OF YH CONTAINS HCUR**J/FACTORIAL(J) TIMES THE J-TH DERIVATIVE OF THE INTERPOLATING POLYNOMIAL CURRENTLY REPRESENTING THE SOLUTION, EVALUATED AT T = TCUR.	LS00714 LS00715 LS00716 LS00717 LS00718 LS00719 LS00720 LS00721
C ACOR	LENRW-NEQ+1	ARRAY OF SIZE NEQ USED FOR THE ACCUMULATED CORRECTIONS ON EACH STEP, SCALED ON OUTPUT TO REPRESENT THE ESTIMATED LOCAL ERROR IN Y ON THE LAST STEP. THIS IS THE VECTOR E IN THE DESCRIPTION OF THE ERROR CONTROL. IT IS DEFINED ONLY ON A SUCCESSFUL RETURN FROM LCODE.	LS00722 LS00723 LS00724 LS00725 LS00726 LS00727 LS00728
-----LS00729			
C PART II. OTHER ROUTINES CALLABLE. LS00730			
C THE FOLLOWING ARE OPTIONAL CALLS WHICH THE USER MAY MAKE TO LS00731			
C GAIN ADDITIONAL CAPABILITIES IN CONJUNCTION WITH LCODE. LS00732			
C (THE ROUTINES XSETUN AND XSETF ARE DESIGNED TO CONFORM TO THE LS00733			
C SLATEC ERROR HANDLING PACKAGE.) LS00734			
C LS00735			
C LS00736			
C FORM OF CALL FUNCTION LS00737			
C CALL XSETUN(LUN) SET THE LOGICAL UNIT NUMBER, LUN, FOR LS00738			
C OUTPUT OF MESSAGES FROM LCODE, IF LS00739			
C THE DEFAULT IS NOT DESIRED. LS00740			
C THE DEFAULT VALUE OF LUN IS 6. LS00741			
C CALL XSETF(MFLAG) SET A FLAG TO CONTROL THE PRINTING OF LS00742			
C MESSAGES BY LCODE. LS00743			
C MFLAG = 0 MEANS DO NOT PRINT. (DANGER.. LS00744			
C THIS RISKS LOSING VALUABLE INFORMATION.) LS00745			
C MFLAG = 1 MEANS PRINT (THE DEFAULT). LS00746			
C LS00747			
C LS00748			
C EITHER OF THE ABOVE CALLS MAY BE MADE AT LS00749			
C ANY TIME AND WILL TAKE EFFECT IMMEDIATELY. LS00750			
C LS00751			
C CALL SVCOM (RSAV, ISAV) STORE IN RSAV AND ISAV THE CONTENTS LS00752			
C OF THE INTERNAL COMMON BLOCKS USED BY LS00753			
C LCODE (SEE PART III BELOW). LS00754			
C RSAV MUST BE A REAL ARRAY OF LENGTH 218 LS00755			
C OR MORE, AND ISAVE MUST BE AN INTEGER LS00756			
C ARRAY OF LENGTH 35 OR MORE. LS00757			
C LS00758			
C CALL RSCOM (RSAV, ISAV) RESTORE, FROM RSAV AND ISAV, THE CONTENTS LS00759			
C OF THE INTERNAL COMMON BLOCKS USED BY LS00760			
C LCODE. PRESUMES A PRIOR CALL TO SVCOM LS00761			
C WITH THE SAME ARGUMENTS. LS00762			
C LS00763			
C SVCOM AND RSCOM ARE USEFUL IF LS00764			
C INTERRUPTING A RUN AND RESTARTING LS00765			
C LATER, OR ALTERNATING BETWEEN TWO OR LS00766			
C MORE PROBLEMS SOLVED WITH LCODE. LS00767			
C LS00768			
C CALL INTDY(,,,,) PROVIDE DERIVATIVES OF Y, OF VARIOUS LS00769			
C (SEE BELOW) ORDERS, AT A SPECIFIED POINT T, IF LS00770			
C DESIRED. IT MAY BE CALLED ONLY AFTER LS00771			

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C                                     A SUCCESSFUL RETURN FROM LODE.          LS00772
C                                     LS00773
C THE DETAILED INSTRUCTIONS FOR USING INTDY ARE AS FOLLOWS.          LS00774
C THE FORM OF THE CALL IS..          LS00775
C                                     LS00776
C CALL INTDY (T, K, RWORK(21), NYH, DKY, IFLAG)          LS00777
C                                     LS00778
C THE INPUT PARAMETERS ARE..          LS00779
C                                     LS00780
C T      = VALUE OF INDEPENDENT VARIABLE WHERE ANSWERS ARE DESIRED  LS00781
C          (NORMALLY THE SAME AS THE T LAST RETURNED BY LODE).      LS00782
C          FOR VALID RESULTS, T MUST LIE BETWEEN TCUR - HU AND TCUR. LS00783
C          (SEE OPTIONAL OUTPUTS FOR TCUR AND HU.)                   LS00784
C K      = INTEGER ORDER OF THE DERIVATIVE DESIRED. K MUST SATISFY LS00785
C          0 .LE. K .LE. NQCUR, WHERE NQCUR IS THE CURRENT ORDER    LS00786
C          (SEE OPTIONAL OUTPUTS). THE CAPABILITY CORRESPONDING     LS00787
C          TO K = 0, I.E. COMPUTING Y(T), IS ALREADY PROVIDED       LS00788
C          BY LODE DIRECTLY. SINCE NQCUR .GE. 1, THE FIRST         LS00789
C          DERIVATIVE DY/DT IS ALWAYS AVAILABLE WITH INTDY.        LS00790
C RWORK(21) = THE BASE ADDRESS OF THE HISTORY ARRAY YH.            LS00791
C NYH      = COLUMN LENGTH OF YH, EQUAL TO THE INITIAL VALUE OF NEQ. LS00792
C                                     LS00793
C THE OUTPUT PARAMETERS ARE..          LS00794
C                                     LS00795
C DKY      = A REAL ARRAY OF LENGTH NEQ CONTAINING THE COMPUTED VALUE LS00796
C            OF THE K-TH DERIVATIVE OF Y(T).                        LS00797
C IFLAG    = INTEGER FLAG, RETURNED AS 0 IF K AND T WERE LEGAL,     LS00798
C            -1 IF K WAS ILLEGAL, AND -2 IF T WAS ILLEGAL.         LS00799
C            ON AN ERROR RETURN, A MESSAGE IS ALSO WRITTEN.        LS00800
C-----LS00801
C PART III. COMMON BLOCKS.          LS00802
C                                     LS00803
C IF LODE IS TO BE USED IN AN OVERLAY SITUATION, THE USER          LS00804
C MUST DECLARE, IN THE PRIMARY OVERLAY, THE VARIABLES IN..        LS00805
C (1) THE CALL SEQUENCE TO LODE,          LS00806
C (2) THE TWO INTERNAL COMMON BLOCKS     LS00807
C /LS0001/ OF LENGTH 251 (218 DOUBLE PRECISION WORDS          LS00808
C          FOLLOWED BY 33 INTEGER WORDS),          LS00809
C /EH0001/ OF LENGTH 2 (INTEGER WORDS).          LS00810
C                                     LS00811
C IF LODE IS USED ON A SYSTEM IN WHICH THE CONTENTS OF INTERNAL    LS00812
C COMMON BLOCKS ARE NOT PRESERVED BETWEEN CALLS, THE USER SHOULD  LS00813
C DECLARE THE ABOVE TWO COMMON BLOCKS IN HIS MAIN PROGRAM TO INSURE LS00814
C THAT THEIR CONTENTS ARE PRESERVED.          LS00815
C                                     LS00816
C IF THE SOLUTION OF A GIVEN PROBLEM BY LODE IS TO BE INTERRUPTED  LS00817
C AND THEN LATER CONTINUED, SUCH AS WHEN RESTARTING AN INTERRUPTED RUN LS00818
C OR ALTERNATING BETWEEN TWO OR MORE PROBLEMS, THE USER SHOULD SAVE, LS00819
C FOLLOWING THE RETURN FROM THE LAST LODE CALL PRIOR TO THE        LS00820
C INTERRUPTION, THE CONTENTS OF THE CALL SEQUENCE VARIABLES AND THE LS00821
C INTERNAL COMMON BLOCKS, AND LATER RESTORE THESE VALUES BEFORE THE LS00822
C NEXT LODE CALL FOR THAT PROBLEM. TO SAVE AND RESTORE THE COMMON  LS00823
C BLOCKS, USE SUBROUTINES SVCOM AND RSCOM (SEE PART II ABOVE).     LS00824
C                                     LS00825
C-----LS00826
C PART IV. OPTIONALLY REPLACEABLE SOLVER ROUTINES.          LS00827
C                                     LS00828
C BELOW ARE DESCRIPTIONS OF TWO ROUTINES IN THE LODE PACKAGE WHICH  LS00829
C RELATE TO THE MEASUREMENT OF ERRORS. EITHER ROUTINE CAN BE      LS00830
C REPLACED BY A USER-SUPPLIED VERSION, IF DESIRED. HOWEVER, SINCE SUCH LS00831

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C A REPLACEMENT MAY HAVE A MAJOR IMPACT ON PERFORMANCE, IT SHOULD BE LS0083
C DONE ONLY WHEN ABSOLUTELY NECESSARY, AND ONLY WITH GREAT CAUTION. LS0083
C (NOTE.. THE MEANS BY WHICH THE PACKAGE VERSION OF A ROUTINE IS LS0083
C SUPERSEDED BY THE USER-S VERSION MAY BE SYSTEM-DEPENDENT.) LS0083
C LS0083
C (A) EWSET. LS0083
C THE FOLLOWING SUBROUTINE IS CALLED JUST BEFORE EACH INTERNAL LS0083
C INTEGRATION STEP, AND SETS THE ARRAY OF ERROR WEIGHTS, EWT, AS LS0083
C DESCRIBED UNDER ITOL/RTOL/ATOL ABOVE.. LS0084
C SUBROUTINE EWSET (NEQ, ITOL, RTOL, ATOL, YCUR, EWT) LS0084
C WHERE NEQ, ITOL, RTOL, AND ATOL ARE AS IN THE LSODE CALL SEQUENCE, LS0084
C YCUR CONTAINS THE CURRENT DEPENDENT VARIABLE VECTOR, AND LS0084
C EWT IS THE ARRAY OF WEIGHTS SET BY EWSET. LS0084
C LS0084
C IF THE USER SUPPLIES THIS SUBROUTINE, IT MUST RETURN IN EWT(I) LS0084
C (I = 1,...,NEQ) A POSITIVE QUANTITY SUITABLE FOR COMPARING ERRORS LS0084
C IN Y(I) TO. THE EWT ARRAY RETURNED BY EWSET IS PASSED TO THE LS0085
C VNORM ROUTINE (SEE BELOW), AND ALSO USED BY LSODE IN THE COMPUTATION LS0085
C OF THE OPTIONAL OUTPUT IMXER, THE DIAGONAL JACOBIAN APPROXIMATION, LS0085
C AND THE INCREMENTS FOR DIFFERENCE QUOTIENT JACOBIANS. LS0085
C LS0085
C IN THE USER-SUPPLIED VERSION OF EWSET, IT MAY BE DESIRABLE TO USE LS0085
C THE CURRENT VALUES OF DERIVATIVES OF Y. DERIVATIVES UP TO ORDER NQ LS0085
C ARE AVAILABLE FROM THE HISTORY ARRAY YH, DESCRIBED ABOVE UNDER LS0085
C OPTIONAL OUTPUTS. IN EWSET, YH IS IDENTICAL TO THE YCUR ARRAY, LS0085
C EXTENDED TO NQ + 1 COLUMNS WITH A COLUMN LENGTH OF NYH AND SCALE LS0085
C FACTORS OF H**J/FACTORIAL(J). ON THE FIRST CALL FOR THE PROBLEM, LS0086
C GIVEN BY NST = 0, NQ IS 1 AND H IS TEMPORARILY SET TO 1.0. LS0086
C THE QUANTITIES NQ, NYH, H, AND NST CAN BE OBTAINED BY INCLUDING LS0086
C IN EWSET THE STATEMENTS.. LS0086
C DOUBLE PRECISION H, RLS LS0086
C COMMON /LS0001/ RLS(218),ILS(33) LS0086
C NQ = ILS(29) LS0086
C NYH = ILS(14) LS0086
C NST = ILS(30) LS0086
C H = RLS(213) LS0086
C THUS, FOR EXAMPLE, THE CURRENT VALUE OF DY/DT CAN BE OBTAINED AS LS0087
C YCUR(NYH+I)/H (I=1,...,NEQ) (AND THE DIVISION BY H IS LS0087
C UNNECESSARY WHEN NST = 0). LS0087
C LS0087
C (B) VNORM. LS0087
C THE FOLLOWING IS A REAL FUNCTION ROUTINE WHICH COMPUTES THE WEIGHTED LS0087
C ROOT-MEAN-SQUARE NORM OF A VECTOR V.. LS0087
C D = VNORM (N, V, W) LS0087
C WHERE.. LS0087
C N = THE LENGTH OF THE VECTOR, LS0087
C V = REAL ARRAY OF LENGTH N CONTAINING THE VECTOR, LS0088
C W = REAL ARRAY OF LENGTH N CONTAINING WEIGHTS, LS0088
C D = SQRT((1/N) * SUM(V(I)/W(I))**2). LS0088
C VNORM IS CALLED WITH N = NEQ AND A WEIGHT VECTOR OF W = EWT, LS0088
C AS SET BY SUBROUTINE EWSET. LS0088
C LS0088
C IF THE USER SUPPLIES THIS FUNCTION, IT SHOULD RETURN A NON-NEGATIVE LS0088
C VALUE OF VNORM SUITABLE FOR USE IN THE ERROR CONTROL IN LSODE. LS0088
C THE WEIGHT ARRAY W MAY BE USED AS NEEDED, BUT SHOULD NOT BE ALTERED. LS0088
C FOR EXAMPLE, A USER-SUPPLIED VNORM ROUTINE MIGHT.. LS0088
C -SUBSTITUTE A MAX-NORM OF (V(I)/W(I)) FOR THE RMS-NORM, OR LS0089
C -IGNORE SOME COMPONENTS OF V IN THE NORM, WITH THE EFFECT OF LS0089
C SUPPRESSING THE ERROR CONTROL ON THOSE COMPONENTS OF Y. LS0089
C-----LS0089

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C-----LS0089
C OTHER ROUTINES IN THE LSODE PACKAGE. LS0089
C LS0089
C IN ADDITION TO SUBROUTINE LSODE, THE LSODE PACKAGE INCLUDES THE LS0089
C FOLLOWING SUBROUTINES AND FUNCTION ROUTINES.. LS0089
C INTDY COMPUTES AN INTERPOLATED VALUE OF THE Y VECTOR AT T = TOUT. LS0089
C STODE IS THE CORE INTEGRATOR, WHICH DOES ONE STEP OF THE LS0090
C INTEGRATION AND THE ASSOCIATED ERROR CONTROL. LS0090
C CFODE SETS ALL METHOD COEFFICIENTS AND TEST CONSTANTS. LS0090
C PREPJ COMPUTES AND PREPROCESSES THE JACOBIAN MATRIX J = DF/DY LS0090
C AND THE NEWTON ITERATION MATRIX P = I - H*L0*J. LS0090
C SOLSY MANAGES SOLUTION OF LINEAR SYSTEM IN CHORD ITERATION. LS0090
C EWSET SETS THE ERROR WEIGHT VECTOR EWT BEFORE EACH STEP. LS0090
C VNORM COMPUTES THE WEIGHTED R.M.S. NORM OF A VECTOR. LS0090
C SVCOM AND RSCOM ARE USER-CALLABLE ROUTINES TO SAVE AND RESTORE, LS0090
C RESPECTIVELY, THE CONTENTS OF THE INTERNAL COMMON BLOCKS. LS0090
C DGEFA AND DGESL ARE ROUTINES FROM LINPACK FOR SOLVING FULL LS0091
C SYSTEMS OF LINEAR ALGEBRAIC EQUATIONS. LS0091
C DGBFA AND DGBSL ARE ROUTINES FROM LINPACK FOR SOLVING BANDED LS0091
C LINEAR SYSTEMS. LS0091
C DAXPY, DSCAL, IDAMAX, AND DDOT ARE BASIC LINEAR ALGEBRA MODULES LS0091
C (BLAS) USED BY THE ABOVE LINPACK ROUTINES. LS0091
C DIMACH COMPUTES THE UNIT ROUND-OFF IN A MACHINE-INDEPENDENT MANNER. LS0091
C XERRWV, XSETUN, AND XSETF HANDLE THE PRINTING OF ALL ERROR LS0091
C MESSAGES AND WARNINGS. XERRWV IS MACHINE-DEPENDENT. LS0091
C NOTE.. VNORM, IDAMAX, DDOT, AND DIMACH ARE FUNCTION ROUTINES. LS0091
C ALL THE OTHERS ARE SUBROUTINES. LS0092
C LS0092
C THE INTRINSIC AND EXTERNAL ROUTINES USED BY LSODE ARE.. LS0092
C DABS, DMAX1, DMIN1, DFLOAT, MAX0, MIN0, MOD, DSIGN, DSQRT, AND WRITE. LS0092
C LS0092
C A BLOCK DATA SUBPROGRAM IS ALSO INCLUDED WITH THE PACKAGE, LS0092
C FOR LOADING SOME OF THE VARIABLES IN INTERNAL COMMON. LS0092
C LS0092
C-----LS0092
EXTERNAL PREPJ, SOLSY LS0092
INTEGER I, I1, I2, IER, IFLAG, ILLIN, IMXER, INIT, IOWNS, LS0093
1 JSTART, KFLAG, KGO, L, LACOR, LENIW, LENRW, LENWM, LEWT, LFO, LS0093
2 LIWM, LSAVF, LWM, LYH, MAXORD, METH, MITER, ML, MORD, MU, LS0093
3 MXHNIL, MXHNLO, MXSTEP, MXSTP0, N, NFE, NHNIL, NJE, NQ, NQU, LS0093
4 NSLAST, NST, NTREP, NYH LS0093
DOUBLE PRECISION TRET, ROWNS, ELO, H, HMIN, HMXI, HU, TN, UROUND, LS0093
1 ATOLI, AYI, BIG, EWTI, H0, HMAX, HMX, RH, RTOLI, TCRIT, TDIST, LS0093
2 TNEXT, TOL, TOLSF, TP, SIZE, SUM, W0, DIMACH, VNORM LS0093
DIMENSION MORD(2) LS0093
LOGICAL IHIT LS0093
C-----LS0094
C THE FOLLOWING INTERNAL COMMON BLOCK CONTAINS LS0094
C (A) VARIABLES WHICH ARE LOCAL TO ANY SUBROUTINE BUT WHOSE VALUES MUST LS0094
C BE PRESERVED BETWEEN CALLS TO THE ROUTINE (OWN VARIABLES), AND LS0094
C (B) VARIABLES WHICH ARE COMMUNICATED BETWEEN SUBROUTINES. LS0094
C THE STRUCTURE OF THE BLOCK IS AS FOLLOWS.. ALL REAL VARIABLES ARE LS0094
C LISTED FIRST, FOLLOWED BY ALL INTEGERS. WITHIN EACH TYPE, THE LS0094
C VARIABLES ARE GROUPED WITH THOSE LOCAL TO SUBROUTINE LSODE FIRST, LS0094
C THEN THOSE LOCAL TO SUBROUTINE STODE, AND FINALLY THOSE USED LS0094
C FOR COMMUNICATION. THE BLOCK IS DECLARED IN SUBROUTINES LS0094
C LSODE, INTDY, STODE, PREPJ, AND SOLSY. GROUPS OF VARIABLES ARE LS0094
C REPLACED BY DUMMY ARRAYS IN THE COMMON DECLARATIONS IN ROUTINES LS0094
C WHERE THOSE VARIABLES ARE NOT USED. LS0094
C-----LS0095

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COMMON /LS0001/ TRET, ROWNS(210),
1  ELO, H, HMIN, HMXI, HU, TN, UROUND,
2  ILLIN, INIT, LYH, LEWT, LACOR, LSAVF, LWM, LIWM,
3  MXSTEP, MXHNIL, NHNIL, NTREP, NSLAST, NYH, IOWNS(6),
4  IER, JSTART, KFLAG, L, METH, MITER, MAXORD, N, NQ, NST, NFE,
5  NJE, NQU

C
DATA MORD(1),MORD(2)/12,5/, MXSTP0/500/, MXHNLO/10/

C-----
C BLOCK A.
C THIS CODE BLOCK IS EXECUTED ON EVERY CALL.
C IT TESTS ISTATE AND ITASK FOR LEGALITY AND BRANCHES APPROPRIATELY.
C IF ISTATE .GT. 1 BUT THE FLAG INIT SHOWS THAT INITIALIZATION HAS
C NOT YET BEEN DONE, AN ERROR RETURN OCCURS.
C IF ISTATE = 1 AND TOUT = T, JUMP TO BLOCK G AND RETURN IMMEDIATELY.
C-----
IF (ISTATE .LT. 1 .OR. ISTATE .GT. 3) GO TO 601
IF (ITASK .LT. 1 .OR. ITASK .GT. 5) GO TO 602
IF (ISTATE .EQ. 1) GO TO 10
IF (INIT .EQ. 0) GO TO 603
IF (ISTATE .EQ. 2) GO TO 200
GO TO 20
10  INIT = 0
IF (TOUT .EQ. T) GO TO 430
20  NTREP = 0

C-----
C BLOCK B.
C THE NEXT CODE BLOCK IS EXECUTED FOR THE INITIAL CALL (ISTATE = 1),
C OR FOR A CONTINUATION CALL WITH PARAMETER CHANGES (ISTATE = 3).
C IT CONTAINS CHECKING OF ALL INPUTS AND VARIOUS INITIALIZATIONS.
C
C FIRST CHECK LEGALITY OF THE NON-OPTIONAL INPUTS NEQ, ITOL, IOPT,
C MF, ML, AND MU.
C-----
IF (NEQ(1) .LE. 0) GO TO 604
IF (ISTATE .EQ. 1) GO TO 25
IF (NEQ(1) .GT. N) GO TO 605
25  N = NEQ(1)
IF (ITOL .LT. 1 .OR. ITOL .GT. 4) GO TO 606
IF (IOPT .LT. 0 .OR. IOPT .GT. 1) GO TO 607
METH = MF/10
MITER = MF - 10*METH
IF (METH .LT. 1 .OR. METH .GT. 2) GO TO 608
IF (MITER .LT. 0 .OR. MITER .GT. 5) GO TO 608
IF (MITER .LE. 3) GO TO 30
ML = IWORK(1)
MU = IWORK(2)
IF (ML .LT. 0 .OR. ML .GE. N) GO TO 609
IF (MU .LT. 0 .OR. MU .GE. N) GO TO 610
30  CONTINUE
C NEXT PROCESS AND CHECK THE OPTIONAL INPUTS. -----
IF (IOPT .EQ. 1) GO TO 40
MAXORD = MORD(METH)
MXSTEP = MXSTP0
MXHNIL = MXHNLO
IF (ISTATE .EQ. 1) H0 = 0.0D0
HMXI = 0.0D0
HMIN = 0.0D0
GO TO 60
40  MAXORD = IWORK(5)

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IF (MAXORD .LT. 0) GO TO 611
IF (MAXORD .EQ. 0) MAXORD = 100
MAXORD = MIN0(MAXORD,MORD(METH))
MXSTEP = IWORK(6)
IF (MXSTEP .LT. 0) GO TO 612
IF (MXSTEP .EQ. 0) MXSTEP = MXSTP0
MXHNIL = IWORK(7)
IF (MXHNIL .LT. 0) GO TO 613
IF (MXHNIL .EQ. 0) MXHNIL = MXHNLO
IF (ISTATE .NE. 1) GO TO 50
H0 = RWORK(5)
IF ((TOUT - T)*H0 .LT. 0.0D0) GO TO 614
50 HMAX = RWORK(6)
IF (HMAX .LT. 0.0D0) GO TO 615
HMXI = 0.0D0
IF (HMAX .GT. 0.0D0) HMXI = 1.0D0/HMAX
HMIN = RWORK(7)
IF (HMIN .LT. 0.0D0) GO TO 616
C-----
C SET WORK ARRAY POINTERS AND CHECK LENGTHS LRW AND LIW.
C POINTERS TO SEGMENTS OF RWORK AND IWORK ARE NAMED BY PREFIXING L TO
C THE NAME OF THE SEGMENT. E.G., THE SEGMENT YH STARTS AT RWORK(LYH).
C SEGMENTS OF RWORK (IN ORDER) ARE DENOTED YH, WM, EWT, SAVF, ACOR.
C-----
60 LYH = 21
IF (ISTATE .EQ. 1) NYH = N
LWM = LYH + (MAXORD + 1)*NYH
IF (MITER .EQ. 0) LENWM = 0
IF (MITER .EQ. 1 .OR. MITER .EQ. 2) LENWM = N*N + 2
IF (MITER .EQ. 3) LENWM = N + 2
IF (MITER .GE. 4) LENWM = (2*ML + MU + 1)*N + 2
LEWT = LWM + LENWM
LSAVF = LEWT + N
LACOR = LSAVF + N
LENRW = LACOR + N - 1
IWORK(17) = LENRW
LIWM = 1
LENIW = 20 + N
IF (MITER .EQ. 0 .OR. MITER .EQ. 3) LENIW = 20
IWORK(18) = LENIW
IF (LENRW .GT. LRW) GO TO 617
IF (LENIW .GT. LIW) GO TO 618
C CHECK RTOL AND ATOL FOR LEGALITY. -----
RTOLI = RTOL(1)
ATOLI = ATOL(1)
DO 70 I = 1,N
IF (ITOL .GE. 3) RTOLI = RTOL(I)
IF (ITOL .EQ. 2 .OR. ITOL .EQ. 4) ATOLI = ATOL(I)
IF (RTOLI .LT. 0.0D0) GO TO 619
IF (ATOLI .LT. 0.0D0) GO TO 620
70 CONTINUE
IF (ISTATE .EQ. 1) GO TO 100
C IF ISTATE = 3, SET FLAG TO SIGNAL PARAMETER CHANGES TO STODE. -----
JSTART = -1
IF (NQ .LE. MAXORD) GO TO 90
C MAXORD WAS REDUCED BELOW NQ. COPY YH(*,MAXORD+2) INTO SAVF. -----
DO 80 I = 1,N
80 RWORK(I+LSAVF-1) = RWORK(I+LWM-1)
C RELOAD WM(1) = RWORK(LWM), SINCE LWM MAY HAVE CHANGED. -----
90 RWORK(LWM) = DSQRT(UROUND)

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      IF (N .EQ. NYH) GO TO 200
C NEQ WAS REDUCED. ZERO PART OF YH TO AVOID UNDEFINED REFERENCES. -----LS0107
      I1 = LYH + L*NYH
      I2 = LYH + (MAXORD + 1)*NYH - 1
      IF (I1 .GT. I2) GO TO 200
      DO 95 I = I1,I2
95      RWORK(I) = 0.0D0
      GO TO 200
C-----LS0108
C BLOCK C.
C THE NEXT BLOCK IS FOR THE INITIAL CALL ONLY (ISTATE = 1).
C IT CONTAINS ALL REMAINING INITIALIZATIONS, THE INITIAL CALL TO F,
C AND THE CALCULATION OF THE INITIAL STEP SIZE.
C-----LS0108
100  UROUND = DLMACH(4)
      TN = T
      IF (ITASK .NE. 4 .AND. ITASK .NE. 5) GO TO 110
      TCRIT = RWORK(1)
      IF ((TCRIT - TOUT)*(TOUT - T) .LT. 0.0D0) GO TO 625
      IF (H0 .NE. 0.0D0 .AND. (T + H0 - TCRIT)*H0 .GT. 0.0D0)
1      H0 = TCRIT - T
110  JSTART = 0
      RWORK(LWM) = DSQRT(UROUND)
      NHNIL = 0
      NST = 0
      NJE = 0
      NSLAST = 0
      HU = 0.0D0
      NQU = 0
C INITIAL CALL TO F. (LF0 POINTS TO YH(*,2). -----LS01099
      LF0 = LYH + NYH
      CALL F (NEQ, T, Y, RWORK(LF0))
      NFE = 1
C LOAD THE INITIAL VALUE VECTOR IN YH. -----LS01103
      DO 115 I = 1,N
115  RWORK(I+LYH-1) = Y(I)
C LOAD THE ERROR WEIGHT VECTOR EWT. (H IS TEMPORARILY SET TO 1.0.) ----LS01106
      NQ = 1
      H = 1.0D0
      CALL EWSET (N, ITOL, RTOL, ATOL, RWORK(LYH), RWORK(LEWT))
      DO 120 I = 1,N
          IF (RWORK(I+LEWT-1) .LE. 0.0D0) GO TO 621
120  CONTINUE
C-----LS01113
C THE CODING BELOW COMPUTES THE STEP SIZE, H0, TO BE ATTEMPTED ON THE
C FIRST STEP, UNLESS THE USER HAS SUPPLIED A VALUE FOR THIS.
C FIRST CHECK THAT TOUT - T DIFFERS SIGNIFICANTLY FROM ZERO.
C A SCALAR TOLERANCE QUANTITY TOL IS COMPUTED, AS MAX(RTOL(I))
C IF THIS IS POSITIVE, OR MAX(ATOL(I)/ABS(Y(I))) OTHERWISE, ADJUSTED
C SO AS TO BE BETWEEN 100*UROUND AND 1.0E-3.
C THEN THE COMPUTED VALUE H0 IS GIVEN BY..
C
C      H0**2 = TOL / ( W0**-2 + (1/NEQ) * SUM ( F(I)/YWT(I) )**2 )
C
C WHERE  W0      = MAX ( ABS(T), ABS(TOUT) ),
C         F(I)   = I-TH COMPONENT OF INITIAL VALUE OF F,
C         YWT(I) = EWT(I)/TOL (A WEIGHT FOR Y(I)).
C THE SIGN OF H0 IS INFERRED FROM THE INITIAL VALUES OF TOUT AND T.
C-----LS01128
      IF (H0 .NE. 0.0D0) GO TO 180

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      TDIST = DABS(TOUT - T)
      W0 = DMAX1(DABS(T),DABS(TOUT))
      IF (TDIST .LT. 2.0D0*UROUND*W0) GO TO 622
      TOL = RTOL(1)
      IF (ITOL .LE. 2) GO TO 140
      DO 130 I = 1,N
130     TOL = DMAX1(TOL,RTOL(I))
140     IF (TOL .GT. 0.0D0) GO TO 160
      ATOLI = ATOL(1)
      DO 150 I = 1,N
          IF (ITOL .EQ. 2 .OR. ITOL .EQ. 4) ATOLI = ATOL(I)
          AYI = DABS(Y(I))
          IF (AYI .NE. 0.0D0) TOL = DMAX1(TOL,ATOLI/AYI)
150     CONTINUE
160     TOL = DMAX1(TOL,100.0D0*UROUND)
      TOL = DMIN1(TOL,0.001D0)
      SUM = VNORM (N, RWORK(LF0), RWORK(LEWT))
      SUM = 1.0D0/(TOL*W0*W0) + TOL*SUM**2
      H0 = 1.0D0/DSQRT(SUM)
      H0 = DMIN1(H0,TDIST)
      H0 = DSIGN(H0,TOUT-T)
C ADJUST H0 IF NECESSARY TO MEET HMAX BOUND. -----
180     RH = DABS(H0)*HMXI
      IF (RH .GT. 1.0D0) H0 = H0/RH
C LOAD H WITH H0 AND SCALE YH(*,2) BY H0. -----
      H = H0
      DO 190 I = 1,N
190     RWORK(I+LF0-1) = H0*RWORK(I+LF0-1)
      GO TO 270
C-----
C BLOCK D.
C THE NEXT CODE BLOCK IS FOR CONTINUATION CALLS ONLY (ISTATE = 2 OR 3)
C AND IS TO CHECK STOP CONDITIONS BEFORE TAKING A STEP.
C-----
200     NSLAST = NST
      GO TO (210, 250, 220, 230, 240), ITASK
210     IF ((TN - TOUT)*H .LT. 0.0D0) GO TO 250
      CALL INTDY (TOUT, 0, RWORK(LYH), NYH, Y, IFLAG)
      IF (IFLAG .NE. 0) GO TO 627
      T = TOUT
      GO TO 420
220     TP = TN - HU*(1.0D0 + 100.0D0*UROUND)
      IF ((TP - TOUT)*H .GT. 0.0D0) GO TO 623
      IF ((TN - TOUT)*H .LT. 0.0D0) GO TO 250
      GO TO 400
230     TCRIT = RWORK(1)
      IF ((TN - TCRIT)*H .GT. 0.0D0) GO TO 624
      IF ((TCRIT - TOUT)*H .LT. 0.0D0) GO TO 625
      IF ((TN - TOUT)*H .LT. 0.0D0) GO TO 245
      CALL INTDY (TOUT, 0, RWORK(LYH), NYH, Y, IFLAG)
      IF (IFLAG .NE. 0) GO TO 627
      T = TOUT
      GO TO 420
240     TCRIT = RWORK(1)
      IF ((TN - TCRIT)*H .GT. 0.0D0) GO TO 624
245     HMX = DABS(TN) + DABS(H)
      IHIT = DABS(TN - TCRIT) .LE. 100.0D0*UROUND*HMX
      IF (IHIT) GO TO 400
      TNEXT = TN + H*(1.0D0 + 4.0D0*UROUND)
      IF ((TNEXT - TCRIT)*H .LE. 0.0D0) GO TO 250

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      H = (TCRIT - TN)*(1.0D0 - 4.0D0*UROUND)
      IF (ISTATE .EQ. 2) JSTART = -2
C-----
C BLOCK E.
C THE NEXT BLOCK IS NORMALLY EXECUTED FOR ALL CALLS AND CONTAINS
C THE CALL TO THE ONE-STEP CORE INTEGRATOR STODE.
C
C THIS IS A LOOPING POINT FOR THE INTEGRATION STEPS.
C
C FIRST CHECK FOR TOO MANY STEPS BEING TAKEN, UPDATE EWT (IF NOT AT
C START OF PROBLEM), CHECK FOR TOO MUCH ACCURACY BEING REQUESTED, AND
C CHECK FOR H BELOW THE ROUNDOFF LEVEL IN T.
C-----
250  CONTINUE
      IF ((NST-NSLAST) .GE. MXSTEP) GO TO 500
      CALL EWSET (N, ITOL, RTOL, ATOL, RWORK(LYH), RWORK(LEWT))
      DO 260 I = 1,N
          IF (RWORK(I+LEWT-1) .LE. 0.0D0) GO TO 510
260  CONTINUE
270  TOLSF = UROUND*VNORM (N, RWORK(LYH), RWORK(LEWT))
      IF (TOLSF .LE. 1.0D0) GO TO 280
      TOLSF = TOLSF*2.0D0
      IF (NST .EQ. 0) GO TO 626
      GO TO 520
280  IF ((TN + H) .NE. TN) GO TO 290
      NHNIL = NHNIL + 1
      IF (NHNIL .GT. MXHNIL) GO TO 290
      CALL XERRWV(50HLSODE-- WARNING..INTERNAL T (=R1) AND H (=R2) ARE,
1    50, 101, 1, 0, 0, 0, 0, 0.0D0, 0.0D0)
      CALL XERRWV(
1    60H      SUCH THAT IN THE MACHINE, T + H = T ON THE NEXT STEP ,
1    60, 101, 1, 0, 0, 0, 0, 0.0D0, 0.0D0)
      CALL XERRWV(50H      (H = STEP SIZE). SOLVER WILL CONTINUE ANYWAY,
1    50, 101, 1, 0, 0, 0, 2, TN, H)
      IF (NHNIL .LT. MXHNIL) GO TO 290
      CALL XERRWV(50HLSODE-- ABOVE WARNING HAS BEEN ISSUED I1 TIMES. ,
1    50, 102, 1, 0, 0, 0, 0, 0.0D0, 0.0D0)
      CALL XERRWV(50H      IT WILL NOT BE ISSUED AGAIN FOR THIS PROBLEM,
1    50, 102, 1, 1, MXHNIL, 0, 0, 0.0D0, 0.0D0)
290  CONTINUE
C-----
C      CALL STODE(NEQ,Y,YH,NYH,YH,EWT,SAVF,ACOR,WM,IWM,F,JAC,PREPJ,SOLSY)
C-----
      CALL STODE (NEQ, Y, RWORK(LYH), NYH, RWORK(LYH), RWORK(LEWT),
1    RWORK(LSAVF), RWORK(LACOR), RWORK(LWM), IWORK(LIWM),
2    F, JAC, PREPJ, SOLSY)
      KGO = 1 - KFLAG
      GO TO (300, 530, 540), KGO
C-----
C BLOCK F.
C THE FOLLOWING BLOCK HANDLES THE CASE OF A SUCCESSFUL RETURN FROM THE
C CORE INTEGRATOR (KFLAG = 0). TEST FOR STOP CONDITIONS.
C-----
300  INIT = 1
      GO TO (310, 400, 330, 340, 350), ITASK
C ITASK = 1. IF TOUT HAS BEEN REACHED, INTERPOLATE. -----
310  IF ((TN - TOUT)*H .LT. 0.0D0) GO TO 250
      CALL INTDY (TOUT, 0, RWORK(LYH), NYH, Y, IFLAG)
      T = TOUT
      GO TO 420

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C ITASK = 3.  JUMP TO EXIT IF TOUT WAS REACHED. -----LS0125
  330 IF ((TN - TOUT)*H .GE. 0.0D0) GO TO 400          LS0125
      GO TO 250                                       LS0125
C ITASK = 4.  SEE IF TOUT OR TCRTIT WAS REACHED.  ADJUST H IF NECESSARY. LS0125
  340 IF ((TN - TOUT)*H .LT. 0.0D0) GO TO 345        LS0125
      CALL INTDY (TOUT, 0, RWORK(LYH), NYH, Y, IFLAG) LS0125
      T = TOUT                                       LS0125
      GO TO 420                                       LS0125
  345 HMX = DABS(TN) + DABS(H)                        LS0125
      IHIT = DABS(TN - TCRTIT) .LE. 100.0D0*UROUND*HMX LS0125
      IF (IHIT) GO TO 400                            LS0126
      TNEXT = TN + H*(1.0D0 + 4.0D0*UROUND)          LS0126
      IF ((TNEXT - TCRTIT)*H .LE. 0.0D0) GO TO 250  LS0126
      H = (TCRTIT - TN)*(1.0D0 - 4.0D0*UROUND)      LS0126
      JSTART = -2                                     LS0126
      GO TO 250                                       LS0126
C ITASK = 5.  SEE IF TCRTIT WAS REACHED AND JUMP TO EXIT. -----LS0126
  350 HMX = DABS(TN) + DABS(H)                        LS0126
      IHIT = DABS(TN - TCRTIT) .LE. 100.0D0*UROUND*HMX LS0126
C -----LS0126
C BLOCK G.                                           LS0127
C THE FOLLOWING BLOCK HANDLES ALL SUCCESSFUL RETURNS FROM LODE. LS0127
C IF ITASK .NE. 1, Y IS LOADED FROM YH AND T IS SET ACCORDINGLY. LS0127
C ISTATE IS SET TO 2, THE ILLEGAL INPUT COUNTER IS ZEROED, AND THE LS0127
C OPTIONAL OUTPUTS ARE LOADED INTO THE WORK ARRAYS BEFORE RETURNING. LS0127
C IF ISTATE = 1 AND TOUT = T, THERE IS A RETURN WITH NO ACTION TAKEN, LS0127
C EXCEPT THAT IF THIS HAS HAPPENED REPEATEDLY, THE RUN IS TERMINATED. LS0127
C -----LS0127
  400 DO 410 I = 1,N                                 LS0127
      410 Y(I) = RWORK(I+LYH-1)                       LS0127
          T = TN                                       LS0128
          IF (ITASK .NE. 4 .AND. ITASK .NE. 5) GO TO 420 LS0128
          IF (IHIT) T = TCRTIT                         LS0128
  420 ISTATE = 2                                       LS0128
      ILLIN = 0                                         LS0128
      RWORK(11) = HU                                    LS0128
      RWORK(12) = H                                    LS0128
      RWORK(13) = TN                                    LS0128
      IWORK(11) = NST                                   LS0128
      IWORK(12) = NFE                                   LS0128
      IWORK(13) = NJE                                   LS0129
      IWORK(14) = NQU                                   LS0129
      IWORK(15) = NQ                                    LS0129
      RETURN                                           LS0129
C -----LS0129
  430 NTREP = NTREP + 1                                 LS0129
      IF (NTREP .LT. 5) RETURN                          LS0129
      CALL XERRWV(                                       LS0129
  1 60HLSODE-- REPEATED CALLS WITH ISTATE = 1 AND TOUT = T (=R1) ,LS0129
  1 60, 301, 1, 0, 0, 0, 1, T, 0.0D0)                LS0129
      GO TO 800                                         LS0130
C -----LS0130
C BLOCK H.                                           LS0130
C THE FOLLOWING BLOCK HANDLES ALL UNSUCCESSFUL RETURNS OTHER THAN LS0130
C THOSE FOR ILLEGAL INPUT.  FIRST THE ERROR MESSAGE ROUTINE IS CALLED. LS0130
C IF THERE WAS AN ERROR TEST OR CONVERGENCE TEST FAILURE, IMXER IS SET. LS0130
C THEN Y IS LOADED FROM YHIS, T IS SET TO TN, AND THE ILLEGAL INPUT LS0130
C COUNTER ILLIN IS SET TO 0.  THE OPTIONAL OUTPUTS ARE LOADED INTO LS0130
C THE WORK ARRAYS BEFORE RETURNING.                  LS0130
C -----LS0130

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C THE MAXIMUM NUMBER OF STEPS WAS TAKEN BEFORE REACHING TOUT. -----LS0131
500 CALL XERRWV(50HLSODE-- AT CURRENT T (=R1), MXSTEP (=I1) STEPS ,LS0131
    1 50, 201, 1, 0, 0, 0, 0, 0.0D0, 0.0D0) ,LS0131
    CALL XERRWV(50H TAKEN ON THIS CALL BEFORE REACHING TOUT ,LS0131
    1 50, 201, 1, 1, MXSTEP, 0, 1, TN, 0.0D0) ,LS0131
    ISTATE = -1 ,LS0131
    GO TO 580 ,LS0131
C EWT(I) .LE. 0.0 FOR SOME I (NOT AT START OF PROBLEM). -----LS0131
510 EWTI = RWORK(LEWT+I-1) ,LS0131
    CALL XERRWV(50HLSODE-- AT T (=R1), EWT(I1) HAS BECOME R2 .LE. 0., ,LS0131
    1 50, 202, 1, 1, I, 0, 2, TN, EWTI) ,LS0132
    ISTATE = -6 ,LS0132
    GO TO 580 ,LS0132
C TOO MUCH ACCURACY REQUESTED FOR MACHINE PRECISION. -----LS0132
520 CALL XERRWV(50HLSODE-- AT T (=R1), TOO MUCH ACCURACY REQUESTED ,LS0132
    1 50, 203, 1, 0, 0, 0, 0, 0.0D0, 0.0D0) ,LS0132
    CALL XERRWV(50H FOR PRECISION OF MACHINE.. SEE TOLSF (=R2) ,LS0132
    1 50, 203, 1, 0, 0, 0, 2, TN, TOLSF) ,LS0132
    RWORK(14) = TOLSF ,LS0132
    ISTATE = -2 ,LS0132
    GO TO 580 ,LS0132
C KFLAG = -1. ERROR TEST FAILED REPEATEDLY OR WITH ABS(H) = HMIN. -----LS0133
530 CALL XERRWV(50HLSODE-- AT T(=R1) AND STEP SIZE H(=R2), THE ERROR, ,LS0133
    1 50, 204, 1, 0, 0, 0, 0, 0.0D0, 0.0D0) ,LS0133
    CALL XERRWV(50H TEST FAILED REPEATEDLY OR WITH ABS(H) = HMIN, ,LS0133
    1 50, 204, 1, 0, 0, 0, 2, TN, H) ,LS0133
    ISTATE = -4 ,LS0133
    GO TO 560 ,LS0133
C KFLAG = -2. CONVERGENCE FAILED REPEATEDLY OR WITH ABS(H) = HMIN. -----LS0133
540 CALL XERRWV(50HLSODE-- AT T (=R1) AND STEP SIZE H (=R2), THE ,LS0133
    1 50, 205, 1, 0, 0, 0, 0, 0.0D0, 0.0D0) ,LS0134
    CALL XERRWV(50H CORRECTOR CONVERGENCE FAILED REPEATEDLY ,LS0134
    1 50, 205, 1, 0, 0, 0, 0, 0.0D0, 0.0D0) ,LS0134
    CALL XERRWV(30H OR WITH ABS(H) = HMIN , ,LS0134
    1 30, 205, 1, 0, 0, 0, 2, TN, H) ,LS0134
    ISTATE = -5 ,LS0134
C COMPUTE IMXER IF RELEVANT. -----LS0134
560 BIG = 0.0D0 ,LS0134
    IMXER = 1 ,LS0134
    DO 570 I = 1,N ,LS0134
        SIZE = DABS(RWORK(I+LACOR-1)/RWORK(I+LEWT-1)) ,LS0135
        IF (BIG .GE. SIZE) GO TO 570 ,LS0135
        BIG = SIZE ,LS0135
        IMXER = I ,LS0135
570 CONTINUE ,LS0135
    IWORK(16) = IMXER ,LS0135
C SET Y VECTOR, T, ILLIN, AND OPTIONAL OUTPUTS. -----LS0135
580 DO 590 I = 1,N ,LS0135
590 Y(I) = RWORK(I+LYH-1) ,LS0135
    T = TN ,LS0135
    ILLIN = 0 ,LS0136
    RWORK(11) = HU ,LS0136
    RWORK(12) = H ,LS0136
    RWORK(13) = TN ,LS0136
    IWORK(11) = NST ,LS0136
    IWORK(12) = NFE ,LS0136
    IWORK(13) = NJE ,LS0136
    IWORK(14) = NQU ,LS0136
    IWORK(15) = NQ ,LS0136
    RETURN ,LS0136

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C-----LS0137
C BLOCK I. LS0137
C THE FOLLOWING BLOCK HANDLES ALL ERROR RETURNS DUE TO ILLEGAL INPUT LS0137
C (ISTATE = -3), AS DETECTED BEFORE CALLING THE CORE INTEGRATOR. LS0137
C FIRST THE ERROR MESSAGE ROUTINE IS CALLED. THEN IF THERE HAVE BEEN LS0137
C 5 CONSECUTIVE SUCH RETURNS JUST BEFORE THIS CALL TO THE SOLVER, LS0137
C THE RUN IS HALTED. LS0137
C-----LS0137
601 CALL XERRWV(30HLSODE-- ISTATE (=I1) ILLEGAL , LS0137
1 30, 1, 1, 1, ISTATE, 0, 0, 0.0D0, 0.0D0) LS0137
GO TO 700 LS0138
602 CALL XERRWV(30HLSODE-- ITASK (=I1) ILLEGAL , LS0138
1 30, 2, 1, 1, ITASK, 0, 0, 0.0D0, 0.0D0) LS0138
GO TO 700 LS0138
603 CALL XERRWV(50HLSODE-- ISTATE .GT. 1 BUT LSODE NOT INITIALIZED ,LS0138
1 50, 3, 1, 0, 0, 0, 0, 0.0D0, 0.0D0) LS0138
GO TO 700 LS0138
604 CALL XERRWV(30HLSODE-- NEQ (=I1) .LT. 0 , LS0138
1 30, 4, 1, 1, NEQ(1), 0, 0, 0.0D0, 0.0D0) LS0138
GO TO 700 LS0138
605 CALL XERRWV(50HLSODE-- ISTATE = 3 AND NEQ INCREASED (I1 TO I2) ,LS0139
1 50, 5, 1, 2, N, NEQ(1), 0, 0.0D0, 0.0D0) LS0139
GO TO 700 LS0139
606 CALL XERRWV(30HLSODE-- ITOL (=I1) ILLEGAL , LS0139
1 30, 6, 1, 1, ITOL, 0, 0, 0.0D0, 0.0D0) LS0139
GO TO 700 LS0139
607 CALL XERRWV(30HLSODE-- IOPT (=I1) ILLEGAL , LS0139
1 30, 7, 1, 1, IOPT, 0, 0, 0.0D0, 0.0D0) LS0139
GO TO 700 LS0139
608 CALL XERRWV(30HLSODE-- MF (=I1) ILLEGAL , LS0139
1 30, 8, 1, 1, MF, 0, 0, 0.0D0, 0.0D0) LS0140
GO TO 700 LS0140
609 CALL XERRWV(50HLSODE-- ML (=I1) ILLEGAL.. .LT.0 OR .GE.NEQ (=I2),LS0140
1 50, 9, 1, 2, ML, NEQ(1), 0, 0.0D0, 0.0D0) LS0140
GO TO 700 LS0140
610 CALL XERRWV(50HLSODE-- MU (=I1) ILLEGAL.. .LT.0 OR .GE.NEQ (=I2),LS0140
1 50, 10, 1, 2, MU, NEQ(1), 0, 0.0D0, 0.0D0) LS0140
GO TO 700 LS0140
611 CALL XERRWV(30HLSODE-- MAXORD (=I1) .LT. 0 , LS0140
1 30, 11, 1, 1, MAXORD, 0, 0, 0.0D0, 0.0D0) LS0140
GO TO 700 LS0141
612 CALL XERRWV(30HLSODE-- MXSTEP (=I1) .LT. 0 , LS0141
1 30, 12, 1, 1, MXSTEP, 0, 0, 0.0D0, 0.0D0) LS0141
GO TO 700 LS0141
613 CALL XERRWV(30HLSODE-- MXHNIL (=I1) .LT. 0 , LS0141
1 30, 13, 1, 1, MXHNIL, 0, 0, 0.0D0, 0.0D0) LS0141
GO TO 700 LS0141
614 CALL XERRWV(40HLSODE-- TOUT (=R1) BEHIND T (=R2) , LS0141
1 40, 14, 1, 0, 0, 0, 2, TOUT, T) LS0141
CALL XERRWV(50H INTEGRATION DIRECTION IS GIVEN BY H0 (=R1) ,LS0141
1 50, 14, 1, 0, 0, 0, 1, H0, 0.0D0) LS0141
GO TO 700 LS0142
615 CALL XERRWV(30HLSODE-- HMAX (=R1) .LT. 0.0 , LS0142
1 30, 15, 1, 0, 0, 0, 1, HMAX, 0.0D0) LS0142
GO TO 700 LS0142
616 CALL XERRWV(30HLSODE-- HMIN (=R1) .LT. 0.0 , LS0142
1 30, 16, 1, 0, 0, 0, 1, HMIN, 0.0D0) LS0142
GO TO 700 LS0142
617 CALL XERRWV( LS0142
1 60HLSODE-- RWORK LENGTH NEEDED, LENRW (=I1), EXCEEDS LRW (=I2),LS0142

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1 60, 17, 1, 2, LENRW, LRW, 0, 0.0D0, 0.0D0) LS0143
GO TO 700 LS0143
618 CALL XERRWV( LS0143
1 60HLSODE-- IWORK LENGTH NEEDED, LENIW (=I1), EXCEEDS LIW (=I2), LS0143
1 60, 18, 1, 2, LENIW, LIW, 0, 0.0D0, 0.0D0) LS0143
GO TO 700 LS0143
619 CALL XERRWV(40HLSODE-- RTOL(I1) IS R1 .LT. 0.0 LS0143
1 40, 19, 1, 1, I, 0, 1, RTOLI, 0.0D0) , LS0143
GO TO 700 LS0143
620 CALL XERRWV(40HLSODE-- ATOL(I1) IS R1 .LT. 0.0 LS0143
1 40, 20, 1, 1, I, 0, 1, ATOLI, 0.0D0) , LS0144
GO TO 700 LS0144
621 EWTI = RWORK(LEWT+I-1) LS0144
CALL XERRWV(40HLSODE-- EWT(I1) IS R1 .LE. 0.0 , LS0144
1 40, 21, 1, 1, I, 0, 1, EWTI, 0.0D0) LS0144
GO TO 700 LS0144
622 CALL XERRWV( LS0144
1 60HLSODE-- TOUT (=R1) TOO CLOSE TO T(=R2) TO START INTEGRATION, LS0144
1 60, 22, 1, 0, 0, 0, 2, TOUT, T) LS0144
GO TO 700 LS0144
623 CALL XERRWV( LS0145
1 60HLSODE-- ITASK = I1 AND TOUT (=R1) BEHIND TCUR - HU (= R2) , LS0145
1 60, 23, 1, 1, ITASK, 0, 2, TOUT, TP) LS0145
GO TO 700 LS0145
624 CALL XERRWV( LS0145
1 60HLSODE-- ITASK = 4 OR 5 AND TCRIT (=R1) BEHIND TCUR (=R2) , LS0145
1 60, 24, 1, 0, 0, 0, 2, TCRIT, TN) LS0145
GO TO 700 LS0145
625 CALL XERRWV( LS0145
1 60HLSODE-- ITASK = 4 OR 5 AND TCRIT (=R1) BEHIND TOUT (=R2) , LS0145
1 60, 25, 1, 0, 0, 0, 2, TCRIT, TOUT) LS0146
GO TO 700 LS0146
626 CALL XERRWV(50HLSODE-- AT START OF PROBLEM, TOO MUCH ACCURACY , LS0146
1 50, 26, 1, 0, 0, 0, 0, 0.0D0, 0.0D0) LS0146
CALL XERRWV( LS0146
1 60H REQUESTED FOR PRECISION OF MACHINE.. SEE TOLSF (=R1) , LS0146
1 60, 26, 1, 0, 0, 0, 1, TOLSF, 0.0D0) LS0146
RWORK(14) = TOLSF LS0146
GO TO 700 LS0146
627 CALL XERRWV(50HLSODE-- TROUBLE FROM INTDY. ITASK = I1, TOUT = R1, LS0146
1 50, 27, 1, 1, ITASK, 0, 1, TOUT, 0.0D0) LS0147
C LS0147
700 IF (ILLIN .EQ. 5) GO TO 710 LS0147
ILLIN = ILLIN + 1 LS0147
ISTATE = -3 LS0147
RETURN LS0147
710 CALL XERRWV(50HLSODE-- REPEATED OCCURRENCES OF ILLEGAL INPUT , LS0147
1 50, 302, 1, 0, 0, 0, 0, 0.0D0, 0.0D0) LS0147
C LS0147
800 CALL XERRWV(50HLSODE-- RUN ABORTED.. APPARENT INFINITE LOOP , LS0147
1 50, 303, 2, 0, 0, 0, 0, 0.0D0, 0.0D0) LS0148
RETURN LS0148
C----- END OF SUBROUTINE LODE ----- LS0148
END LS0148
SUBROUTINE INTDY (T, K, YH, NYH, DKY, IFLAG) LS0148
INTEGER K, NYH, IFLAG, I, IC, IER, IOWND, IOWNS, J, JB, JB2, LS0148
1 JJ, JJ1, JP1, JSTART, KFLAG, L, MAXORD, METH, MITER, N, NFE, LS0148
2 NJE, NQ, NQU, NST LS0148
DOUBLE PRECISION T, YH, DKY, LS0148
1 ROWND, ROWNS, ELO, H, HMIN, HMXI, HU, TN, UROUND, LS0148

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2   C, R, S, TP
   DIMENSION YH(NYH,1), DKY(1)
   COMMON /LS0001/ ROWND, ROWNS(210),
1   EL0, H, HMIN, HMXI, HU, TN, UROUND, IOWND(14), IOWNS(6),
4   IER, JSTART, KFLAG, L, METH, MITER, MAXORD, N, NQ, NST, NFE,
5   NJE, NQU
C-----LS0149
C INTDY COMPUTES INTERPOLATED VALUES OF THE K-TH DERIVATIVE OF THE
C DEPENDENT VARIABLE VECTOR Y, AND STORES IT IN DKY.
C THIS ROUTINE IS CALLED BY LSODE WITH K = 0 AND T = TOUT, BUT MAY
C ALSO BE CALLED BY THE USER FOR ANY K UP TO THE CURRENT ORDER.
C (SEE DETAILED INSTRUCTIONS IN LSODE USAGE DOCUMENTATION.)
C-----LS0150
C THE COMPUTED VALUES IN DKY ARE GOTTEN BY INTERPOLATION USING THE
C NORDSIECK HISTORY ARRAY YH. THIS ARRAY CORRESPONDS UNIQUELY TO A
C VECTOR-VALUED POLYNOMIAL OF DEGREE NQCUR OR LESS, AND DKY IS SET
C TO THE K-TH DERIVATIVE OF THIS POLYNOMIAL AT T.
C THE FORMULA FOR DKY IS..
C
C      Q
C   DKY(I) = SUM C(J,K) * (T - TN)**(J-K) * H**(-J) * YH(I,J+1)
C             J=K
C WHERE C(J,K) = J*(J-1)*...*(J-K+1), Q = NQCUR, TN = TCUR, H = HCUR.
C THE QUANTITIES NQ = NQCUR, L = NQ+1, N = NEQ, TN, AND H ARE
C COMMUNICATED BY COMMON. THE ABOVE SUM IS DONE IN REVERSE ORDER.
C IFLAG IS RETURNED NEGATIVE IF EITHER K OR T IS OUT OF BOUNDS.
C-----LS0151
      IFLAG = 0
      IF (K .LT. 0 .OR. K .GT. NQ) GO TO 80
      TP = TN - HU*(1.0D0 + 100.0D0*UROUND)
      IF ((T-TP)*(T-TN) .GT. 0.0D0) GO TO 90
C
      S = (T - TN)/H
      IC = 1
      IF (K .EQ. 0) GO TO 15
      JJ1 = L - K
      DO 10 JJ = JJ1,NQ
10      IC = IC*JJ
15      C = DFLOAT(IC)
      DO 20 I = 1,N
20      DKY(I) = C*YH(I,L)
      IF (K .EQ. NQ) GO TO 55
      JB2 = NQ - K
      DO 50 JB = 1,JB2
          J = NQ - JB
          JPl = J + 1
          IC = 1
          IF (K .EQ. 0) GO TO 35
          JJ1 = JPl - K
          DO 30 JJ = JJ1,J
30      IC = IC*JJ
35      C = DFLOAT(IC)
      DO 40 I = 1,N
40      DKY(I) = C*YH(I,JPl) + S*DKY(I)
50      CONTINUE
      IF (K .EQ. 0) RETURN
55      R = H**(-K)
      DO 60 I = 1,N
60      DKY(I) = R*DKY(I)
      RETURN
C

```

```

80 CALL XERRWV(30HINTDY-- K (=I1) ILLEGAL , LS01550
1 30, 51, 1, 1, K, 0, 0, 0.0D0, 0.0D0) LS01551
IFLAG = -1 LS01552
RETURN LS01553
90 CALL XERRWV(30HINTDY-- T (=R1) ILLEGAL , LS01554
1 30, 52, 1, 0, 0, 0, 1, T, 0.0D0) LS01555
CALL XERRWV( LS01556
1 60H T NOT IN INTERVAL TCUR - HU (= R1) TO TCUR (=R2) ,LS01557
1 60, 52, 1, 0, 0, 0, 2, TP, TN) LS01558
IFLAG = -2 LS01559
RETURN LS01560
C----- END OF SUBROUTINE INTDY -----LS01561
END LS01562
SUBROUTINE STODE (NEQ, Y, YH, NYH, YH1, EWT, SAVF, ACOR, LS01563
1 WM, IWM, F, JAC, PJAC, SLVS) LS01564
EXTERNAL F, JAC, PJAC, SLVS LS01565
INTEGER NEQ, NYH, IWM, I, I1, IALTH, IER, IOWND, IREDO, IRET, LS01566
1 IPUP, J, JB, JSTART, KFLAG, L, LMAX, M, MAXORD, MEO, METH, LS01567
2 MITER, N, NCF, NEWQ, NFE, NJE, NQ, NQNYH, NQU, NST, NSTEPJ LS01568
DOUBLE PRECISION Y, YH, YH1, EWT, SAVF, ACOR, WM, LS01569
1 ROWND, CONIT, CRATE, EL, ELCO, HOLD, RC, RMAX, TESCO, LS01570
2 EL0, H, HMIN, HMXI, HU, TN, UROUND, LS01571
3 DCON, DDN, DEL, DELP, DSM, DUP, EXDN, EXSM, EXUP, LS01572
4 R, RH, RHDN, RHSM, RHUP, TOLD, VNORM LS01573
DIMENSION NEQ(1), Y(1), YH(NYH,1), YH1(1), EWT(1), SAVF(1), LS01574
1 ACOR(1), WM(1), IWM(1) LS01575
COMMON /LS0001/ ROWND, CONIT, CRATE, EL(13), ELCO(13,12), LS01576
1 HOLD, RC, RMAX, TESCO(3,12), LS01577
2 EL0, H, HMIN, HMXI, HU, TN, UROUND, IOWND(14), LS01578
3 IALTH, IPUP, LMAX, MEO, NQNYH, NSTEPJ, LS01579
4 IER, JSTART, KFLAG, L, METH, MITER, MAXORD, N, NQ, NST, NFE, LS01580
5 NJE, NQU LS01581
C-----LS01582
C STODE PERFORMS ONE STEP OF THE INTEGRATION OF AN INITIAL VALUE LS01583
C PROBLEM FOR A SYSTEM OF ORDINARY DIFFERENTIAL EQUATIONS. LS01584
C NOTE.. STODE IS INDEPENDENT OF THE VALUE OF THE ITERATION METHOD LS01585
C INDICATOR MITER, WHEN THIS IS .NE. 0, AND HENCE IS INDEPENDENT LS01586
C OF THE TYPE OF CHORD METHOD USED, OR THE JACOBIAN STRUCTURE. LS01587
C COMMUNICATION WITH STODE IS DONE WITH THE FOLLOWING VARIABLES.. LS01588
C LS01589
C NEQ = INTEGER ARRAY CONTAINING PROBLEM SIZE IN NEQ(1), AND LS01590
C PASSED AS THE NEQ ARGUMENT IN ALL CALLS TO F AND JAC. LS01591
C Y = AN ARRAY OF LENGTH .GE. N USED AS THE Y ARGUMENT IN LS01592
C ALL CALLS TO F AND JAC. LS01593
C YH = AN NYH BY LMAX ARRAY CONTAINING THE DEPENDENT VARIABLES LS01594
C AND THEIR APPROXIMATE SCALED DERIVATIVES, WHERE LS01595
C LMAX = MAXORD + 1. YH(I,J+1) CONTAINS THE APPROXIMATE LS01596
C J-TH DERIVATIVE OF Y(I), SCALED BY H**J/FACTORIAL(J) LS01597
C (J = 0,1,...,NQ). ON ENTRY FOR THE FIRST STEP, THE FIRST LS01598
C TWO COLUMNS OF YH MUST BE SET FROM THE INITIAL VALUES. LS01599
C NYH = A CONSTANT INTEGER .GE. N, THE FIRST DIMENSION OF YH. LS01600
C YH1 = A ONE-DIMENSIONAL ARRAY OCCUPYING THE SAME SPACE AS YH. LS01601
C EWT = AN ARRAY OF N ELEMENTS WITH WHICH THE ESTIMATED LOCAL LS01602
C ERRORS IN YH ARE COMPARED. LS01603
C SAVF = AN ARRAY OF WORKING STORAGE, OF LENGTH N. LS01604
C ALSO USED FOR INPUT OF YH(*,MAXORD+2) WHEN JSTART = -1 LS01605
C AND MAXORD .LT. THE CURRENT ORDER NQ. LS01606
C ACOR = A WORK ARRAY OF LENGTH N, USED FOR THE ACCUMULATED LS01607
C CORRECTIONS. ON A SUCCESSFUL RETURN, ACOR(I) CONTAINS LS01608
C THE ESTIMATED ONE-STEP LOCAL ERROR IN Y(I). LS01609

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HOLD = H	LS0167
MEO = METH	LS0167
NSTEPJ = 0	LS0167
IRET = 3	LS0167
GO TO 140	LS0167
C-----	LS0167
C THE FOLLOWING BLOCK HANDLES PRELIMINARIES NEEDED WHEN JSTART = -1.	LS0167
C IPUP IS SET TO MITER TO FORCE A MATRIX UPDATE.	LS0167
C IF AN ORDER INCREASE IS ABOUT TO BE CONSIDERED (IALTH = 1),	LS0167
C IALTH IS RESET TO 2 TO POSTPONE CONSIDERATION ONE MORE STEP.	LS0167
C IF THE CALLER HAS CHANGED METH, CFODE IS CALLED TO RESET	LS0168
C THE COEFFICIENTS OF THE METHOD.	LS0168
C IF THE CALLER HAS CHANGED MAXORD TO A VALUE LESS THAN THE CURRENT	LS0168
C ORDER NQ, NQ IS REDUCED TO MAXORD, AND A NEW H CHOSEN ACCORDINGLY.	LS0168
C IF H IS TO BE CHANGED, YH MUST BE RESCALED.	LS0168
C IF H OR METH IS BEING CHANGED, IALTH IS RESET TO L = NQ + 1	LS0168
C TO PREVENT FURTHER CHANGES IN H FOR THAT MANY STEPS.	LS0168
C-----	LS0168
100 IPUP = MITER	LS0168
LMAX = MAXORD + 1	LS0168
IF (IALTH .EQ. 1) IALTH = 2	LS0169
IF (METH .EQ. MEO) GO TO 110	LS0169
CALL CFODE (METH, ELCO, TESCO)	LS0169
MEO = METH	LS0169
IF (NQ .GT. MAXORD) GO TO 120	LS0169
IALTH = L	LS0169
IRET = 1	LS0169
GO TO 150	LS0169
110 IF (NQ .LE. MAXORD) GO TO 160	LS0169
120 NQ = MAXORD	LS0169
L = LMAX	LS0170
DO 125 I = 1, L	LS0170
125 EL(I) = ELCO(I, NQ)	LS0170
NQNYH = NQ*NYH	LS0170
RC = RC*EL(1)/ELO	LS0170
ELO = EL(1)	LS0170
CONIT = 0.5D0/DFLOAT(NQ+2)	LS0170
DDN = VNORM (N, SAVF, EWT)/TESCO(1, L)	LS0170
EXDN = 1.0D0/DFLOAT(L)	LS0170
RHDN = 1.0D0/(1.3D0*DDN**EXDN + 0.0000013D0)	LS0170
RH = DMIN1(RHDN, 1.0D0)	LS0171
IREDO = 3	LS0171
IF (H .EQ. HOLD) GO TO 170	LS0171
RH = DMIN1(RH, DABS(H/HOLD))	LS0171
H = HOLD	LS0171
GO TO 175	LS0171
C-----	LS0171
C CFODE IS CALLED TO GET ALL THE INTEGRATION COEFFICIENTS FOR THE	LS0171
C CURRENT METH. THEN THE EL VECTOR AND RELATED CONSTANTS ARE RESET	LS0171
C WHENEVER THE ORDER NQ IS CHANGED, OR AT THE START OF THE PROBLEM.	LS0171
C-----	LS0172
140 CALL CFODE (METH, ELCO, TESCO)	LS0172
150 DO 155 I = 1, L	LS0172
155 EL(I) = ELCO(I, NQ)	LS0172
NQNYH = NQ*NYH	LS0172
RC = RC*EL(1)/ELO	LS0172
ELO = EL(1)	LS0172
CONIT = 0.5D0/DFLOAT(NQ+2)	LS0172
GO TO (160, 170, 200), IRET	LS0172
C-----	LS0172

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C
      DO 30 J = KP1, N
      T = A(L,J)
      IF (L .EQ. K) GO TO 20
      A(L,J) = A(K,J)
      A(K,J) = T
20      CONTINUE
      CALL DAXPY(N-K,T,A(K+1,K),1,A(K+1,J),1)
30      CONTINUE
      GO TO 50
40      CONTINUE
      INFO = K
50      CONTINUE
60      CONTINUE
70      CONTINUE
      IPVT(N) = N
      IF (A(N,N) .EQ. 0.0D0) INFO = N
      RETURN
      END
      SUBROUTINE DGESL(A,LDA,N,IPVT,B,JOB)
      INTEGER LDA,N,IPVT(1),JOB
      DOUBLE PRECISION A(LDA,1),B(1)
C
C     DGESL SOLVES THE DOUBLE PRECISION SYSTEM
C     A * X = B OR TRANS(A) * X = B
C     USING THE FACTORS COMPUTED BY DGEKO OR DGEFA.
C
C     ON ENTRY
C
C     A      DOUBLE PRECISION(LDA, N)
C           THE OUTPUT FROM DGEKO OR DGEFA.
C
C     LDA   INTEGER
C           THE LEADING DIMENSION OF THE ARRAY A .
C
C     N     INTEGER
C           THE ORDER OF THE MATRIX A .
C
C     IPVT  INTEGER(N)
C           THE PIVOT VECTOR FROM DGEKO OR DGEFA.
C
C     B     DOUBLE PRECISION(N)
C           THE RIGHT HAND SIDE VECTOR.
C
C     JOB   INTEGER
C           = 0         TO SOLVE A*X = B ,
C           = NONZERO   TO SOLVE TRANS(A)*X = B WHERE
C                   TRANS(A) IS THE TRANSPOSE.
C
C     ON RETURN
C
C     B     THE SOLUTION VECTOR X .
C
C     ERROR CONDITION
C
C     A DIVISION BY ZERO WILL OCCUR IF THE INPUT FACTOR CONTAINS A
C     ZERO ON THE DIAGONAL.  TECHNICALLY THIS INDICATES SINGULARITY
C     BUT IT IS OFTEN CAUSED BY IMPROPER ARGUMENTS OR IMPROPER
C     SETTING OF LDA . IT WILL NOT OCCUR IF THE SUBROUTINES ARE
C     CALLED CORRECTLY AND IF DGEKO HAS SET RCOND .GT. 0.0

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CALL PJAC (NEQ, Y, YH, NYH, EWT, ACOR, SAVF, WM, IWM, F, JAC)      LS01790
IF (IER .NE. 0) GO TO 430      LS01791
250 DO 260 I = 1,N      LS01792
260   ACOR(I) = 0.0D0      LS01793
270 IF (MITER .NE. 0) GO TO 350      LS01794
C-----LS01795
C IN THE CASE OF FUNCTIONAL ITERATION, UPDATE Y DIRECTLY FROM      LS01796
C THE RESULT OF THE LAST FUNCTION EVALUATION.      LS01797
C-----LS01798
DO 290 I = 1,N      LS01799
   SAVF(I) = H*SAVF(I) - YH(I,2)      LS01800
290   Y(I) = SAVF(I) - ACOR(I)      LS01801
   DEL = VNORM (N, Y, EWT)      LS01802
DO 300 I = 1,N      LS01803
   Y(I) = YH(I,1) + EL(1)*SAVF(I)      LS01804
300   ACOR(I) = SAVF(I)      LS01805
   GO TO 400      LS01806
C-----LS01807
C IN THE CASE OF THE CHORD METHOD, COMPUTE THE CORRECTOR ERROR,      LS01808
C AND SOLVE THE LINEAR SYSTEM WITH THAT AS RIGHT-HAND SIDE AND      LS01809
C P AS COEFFICIENT MATRIX.      LS01810
C-----LS01811
350 DO 360 I = 1,N      LS01812
360   Y(I) = H*SAVF(I) - (YH(I,2) + ACOR(I))      LS01813
   CALL SLVS (WM, IWM, Y, SAVF)      LS01814
   IF (IER .NE. 0) GO TO 410      LS01815
   DEL = VNORM (N, Y, EWT)      LS01816
DO 380 I = 1,N      LS01817
   ACOR(I) = ACOR(I) + Y(I)      LS01818
380   Y(I) = YH(I,1) + EL(1)*ACOR(I)      LS01819
C-----LS01820
C TEST FOR CONVERGENCE. IF M.GT.0, AN ESTIMATE OF THE CONVERGENCE      LS01821
C RATE CONSTANT IS STORED IN CRATE, AND THIS IS USED IN THE TEST.      LS01822
C-----LS01823
400 IF (M .NE. 0) CRATE = DMAX1(0.2D0*CRATE,DEL/DELP)      LS01824
   DCON = DEL*DMIN1(1.0D0,1.5D0*CRATE)/(TESCO(2,NQ)*CONIT)      LS01825
   IF (DCON .LE. 1.0D0) GO TO 450      LS01826
   M = M + 1      LS01827
   IF (M .EQ. 3) GO TO 410      LS01828
   IF (M .GE. 2 .AND. DEL .GT. 2.0D0*DELP) GO TO 410      LS01829
   DELP = DEL      LS01830
   CALL F (NEQ, TN, Y, SAVF)      LS01831
   NFE = NFE + 1      LS01832
   GO TO 270      LS01833
C-----LS01834
C THE CORRECTOR ITERATION FAILED TO CONVERGE IN 3 TRIES.      LS01835
C IF MITER .NE. 0 AND THE JACOBIAN IS OUT OF DATE, PJAC IS CALLED FOR      LS01836
C THE NEXT TRY. OTHERWISE THE YH ARRAY IS RETRACTED TO ITS VALUES      LS01837
C BEFORE PREDICTION, AND H IS REDUCED, IF POSSIBLE. IF H CANNOT BE      LS01838
C REDUCED OR 10 FAILURES HAVE OCCURRED, EXIT WITH KFLAG = -2.      LS01839
C-----LS01840
410 IF (IPUP .EQ. 0) GO TO 430      LS01841
   IPUP = MITER      LS01842
   GO TO 220      LS01843
430 TN = TOLD      LS01844
   NCF = NCF + 1      LS01845
   RMAX = 2.0D0      LS01846
   I1 = NQNYH + 1      LS01847
DO 445 JB = 1,NQ      LS01848
   I1 = I1 - NYH      LS01849

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DO 440 I = 11,NQNYH
440   YH1(I) = YH1(I) - YH1(I+NYH)
445   CONTINUE
      IF (DABS(H) .LE. HMIN*1.00001D0) GO TO 670
      IF (NCF .EQ. 10) GO TO 670
      RH = 0.25D0
      IPUP = MITER
      IREDO = 1
      GO TO 170
C-----
C THE CORRECTOR HAS CONVERGED.  IPUP IS SET TO -1 IF MITER .NE. 0,
C TO SIGNAL THAT THE JACOBIAN INVOLVED MAY NEED UPDATING LATER.
C THE LOCAL ERROR TEST IS MADE AND CONTROL PASSES TO STATEMENT 500
C IF IT FAILS.
C-----
450   IF (MITER .NE. 0) IPUP = -1
      IF (M .EQ. 0) DSM = DEL/TESCO(2,NQ)
      IF (M .GT. 0) DSM = VNORM (N, ACOR, EWT)/TESCO(2,NQ)
      IF (DSM .GT. 1.0D0) GO TO 500
C-----
C AFTER A SUCCESSFUL STEP, UPDATE THE YH ARRAY.
C CONSIDER CHANGING H IF IALTH = 1.  OTHERWISE DECREASE IALTH BY 1.
C IF IALTH IS THEN 1 AND NQ .LT. MAXORD, THEN ACOR IS SAVED FOR
C USE IN A POSSIBLE ORDER INCREASE ON THE NEXT STEP.
C IF A CHANGE IN H IS CONSIDERED, AN INCREASE OR DECREASE IN ORDER
C BY ONE IS CONSIDERED ALSO.  A CHANGE IN H IS MADE ONLY IF IT IS BY A
C FACTOR OF AT LEAST 1.1.  IF NOT, IALTH IS SET TO 3 TO PREVENT
C TESTING FOR THAT MANY STEPS.
C-----
      KFLAG = 0
      IREDO = 0
      NST = NST + 1
      HU = H
      NQU = NQ
      DO 470 J = 1,L
        DO 470 I = 1,N
470   YH(I,J) = YH(I,J) + EL(J)*ACOR(I)
      IALTH = IALTH - 1
      IF (IALTH .EQ. 0) GO TO 520
      IF (IALTH .GT. 1) GO TO 690
      IF (L .EQ. LMAX) GO TO 690
      DO 490 I = 1,N
490   YH(I,LMAX) = ACOR(I)
      GO TO 690
C-----
C THE ERROR TEST FAILED.  KFLAG KEEPS TRACK OF MULTIPLE FAILURES.
C RESTORE TN AND THE YH ARRAY TO THEIR PREVIOUS VALUES, AND PREPARE
C TO TRY THE STEP AGAIN.  COMPUTE THE OPTIMUM STEP SIZE FOR THIS OR
C ONE LOWER ORDER.  AFTER 2 OR MORE FAILURES, H IS FORCED TO DECREASE
C BY A FACTOR OF 0.2 OR LESS.
C-----
500   KFLAG = KFLAG - 1
      TN = TOLD
      I1 = NQNYH + 1
      DO 515 JB = 1,NQ
        I1 = I1 - NYH
      DO 510 I = 11,NQNYH
510   YH1(I) = YH1(I) - YH1(I+NYH)
515   CONTINUE
      RMAX = 2.0D0

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IF (DABS(H) .LE. HMIN*1.00001D0) GO TO 660
IF (KFLAG .LE. -3) GO TO 640
IREDO = 2
RHUP = 0.0D0
GO TO 540
C-----
C REGARDLESS OF THE SUCCESS OR FAILURE OF THE STEP, FACTORS
C RHDN, RHSM, AND RHUP ARE COMPUTED, BY WHICH H COULD BE MULTIPLIED
C AT ORDER NQ - 1, ORDER NQ, OR ORDER NQ + 1, RESPECTIVELY.
C IN THE CASE OF FAILURE, RHUP = 0.0 TO AVOID AN ORDER INCREASE.
C THE LARGEST OF THESE IS DETERMINED AND THE NEW ORDER CHOSEN
C ACCORDINGLY. IF THE ORDER IS TO BE INCREASED, WE COMPUTE ONE
C ADDITIONAL SCALED DERIVATIVE.
C-----
520 RHUP = 0.0D0
IF (L .EQ. LMAX) GO TO 540
DO 530 I = 1,N
530 SAVF(I) = ACOR(I) - YH(I,LMAX)
DUP = VNORM (N, SAVF, EWT)/TESCO(3,NQ)
EXUP = 1.0D0/DFLOAT(L+1)
RHUP = 1.0D0/(1.4D0*DUP**EXUP + 0.0000014D0)
540 EXSM = 1.0D0/DFLOAT(L)
RHSM = 1.0D0/(1.2D0*DSM**EXSM + 0.0000012D0)
RHDN = 0.0D0
IF (NQ .EQ. 1) GO TO 560
DDN = VNORM (N, YH(1,L), EWT)/TESCO(1,NQ)
EXDN = 1.0D0/DFLOAT(NQ)
RHDN = 1.0D0/(1.3D0*DDN**EXDN + 0.0000013D0)
560 IF (RHSM .GE. RHUP) GO TO 570
IF (RHUP .GT. RHDN) GO TO 590
GO TO 580
570 IF (RHSM .LT. RHDN) GO TO 580
NEWQ = NQ
RH = RHSM
GO TO 620
580 NEWQ = NQ - 1
RH = RHDN
IF (KFLAG .LT. 0 .AND. RH .GT. 1.0D0) RH = 1.0D0
GO TO 620
590 NEWQ = L
RH = RHUP
IF (RH .LT. 1.1D0) GO TO 610
R = EL(L)/DFLOAT(L)
DO 600 I = 1,N
600 YH(I,NEWQ+1) = ACOR(I)*R
GO TO 630
610 IALTH = 3
GO TO 690
620 IF ((KFLAG .EQ. 0) .AND. (RH .LT. 1.1D0)) GO TO 610
IF (KFLAG .LE. -2) RH = DMIN1(RH,0.2D0)
C-----
C IF THERE IS A CHANGE OF ORDER, RESET NQ, L, AND THE COEFFICIENTS.
C IN ANY CASE H IS RESET ACCORDING TO RH AND THE YH ARRAY IS RESCALED.
C THEN EXIT FROM 680 IF THE STEP WAS OK, OR REDO THE STEP OTHERWISE.
C-----
IF (NEWQ .EQ. NQ) GO TO 170
630 NQ = NEWQ
L = NQ + 1
IRET = 2
GO TO 150

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C-----LS0197
C CONTROL REACHES THIS SECTION IF 3 OR MORE FAILURES HAVE OCCURED. LS0197
C IF 10 FAILURES HAVE OCCURRED, EXIT WITH KFLAG = -1. LS0197
C IT IS ASSUMED THAT THE DERIVATIVES THAT HAVE ACCUMULATED IN THE LS0197
C YH ARRAY HAVE ERRORS OF THE WRONG ORDER. HENCE THE FIRST LS0197
C DERIVATIVE IS RECOMPUTED, AND THE ORDER IS SET TO 1. THEN LS0197
C H IS REDUCED BY A FACTOR OF 10, AND THE STEP IS RETRIED, LS0197
C UNTIL IT SUCCEEDS OR H REACHES HMIN. LS0197
C-----LS0197
640 IF (KFLAG .EQ. -10) GO TO 660 LS0197
    RH = 0.1D0 LS0198
    RH = DMAX1(HMIN/DABS(H),RH) LS0198
    H = H*RH LS0198
    DO 645 I = 1,N LS0198
645   Y(I) = YH(I,1) LS0198
    CALL F (NEQ, TN, Y, SAVF) LS0198
    NFE = NFE + 1 LS0198
    DO 650 I = 1,N LS0198
650   YH(I,2) = H*SAVF(I) LS0198
    IPUP = MITER LS0198
    IALTH = 5 LS0199
    IF (NQ .EQ. 1) GO TO 200 LS0199
    NQ = 1 LS0199
    L = 2 LS0199
    IRET = 3 LS0199
    GO TO 150 LS0199
C-----LS01996
C ALL RETURNS ARE MADE THROUGH THIS SECTION. H IS SAVED IN HOLD LS01997
C TO ALLOW THE CALLER TO CHANGE H ON THE NEXT STEP. LS01998
C-----LS01999
660 KFLAG = -1 LS02000
    GO TO 700 LS02001
670 KFLAG = -2 LS02002
    GO TO 700 LS02003
680 RMAX = 10.0D0 LS02004
690 R = 1.0D0/TESCO(2,NQU) LS02005
    DO 695 I = 1,N LS02006
695   ACOR(I) = ACOR(I)*R LS02007
700 HOLD = H LS02008
    JSTART = 1 LS02009
    RETURN LS02010
C----- END OF SUBROUTINE STODE -----LS02011
    END LS02012
    SUBROUTINE CFODE (METH, ELCO, TESCO) LS02013
    INTEGER METH, I, IB, NQ, NQM1, NQP1 LS02014
    DOUBLE PRECISION ELCO, TESCO, AGAMQ, FNQ, FNQM1, PC, PINT, RAGQ, LS02015
1   RQFAC, RQ1FAC, TSIGN, XPIN LS02016
    DIMENSION ELCO(13,12), TESCO(3,12) LS02017
C-----LS02018
C CFODE IS CALLED BY THE INTEGRATOR ROUTINE TO SET COEFFICIENTS LS02019
C NEEDED THERE. THE COEFFICIENTS FOR THE CURRENT METHOD, AS LS02020
C GIVEN BY THE VALUE OF METH, ARE SET FOR ALL ORDERS AND SAVED. LS02021
C THE MAXIMUM ORDER ASSUMED HERE IS 12 IF METH = 1 AND 5 IF METH = 2. LS02022
C (A SMALLER VALUE OF THE MAXIMUM ORDER IS ALSO ALLOWED.) LS02023
C CFODE IS CALLED ONCE AT THE BEGINNING OF THE PROBLEM, LS02024
C AND IS NOT CALLED AGAIN UNLESS AND UNTIL METH IS CHANGED. LS02025
C LS02026
C THE ELCO ARRAY CONTAINS THE BASIC METHOD COEFFICIENTS. LS02027
C THE COEFFICIENTS EL(I), 1 .LE. I .LE. NQ+1, FOR THE METHOD OF LS02028
C ORDER NQ ARE STORED IN ELCO(I,NQ). THEY ARE GIVEN BY A GENETRATING LS02029

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C POLYNOMIAL, I.E.,
C L(X) = EL(1) + EL(2)*X + ... + EL(NQ+1)*X**NQ.
C FOR THE IMPLICIT ADAMS METHODS, L(X) IS GIVEN BY
C DL/DX = (X+1)*(X+2)*...*(X+NQ-1)/FACTORIAL(NQ-1), L(-1) = 0.
C FOR THE BDF METHODS, L(X) IS GIVEN BY
C L(X) = (X+1)*(X+2)*...*(X+NQ)/K,
C WHERE K = FACTORIAL(NQ)*(1 + 1/2 + ... + 1/NQ).
C
C THE TESCO ARRAY CONTAINS TEST CONSTANTS USED FOR THE
C LOCAL ERROR TEST AND THE SELECTION OF STEP SIZE AND/OR ORDER.
C AT ORDER NQ, TESCO(K,NQ) IS USED FOR THE SELECTION OF STEP
C SIZE AT ORDER NQ - 1 IF K = 1, AT ORDER NQ IF K = 2, AND AT ORDER
C NQ + 1 IF K = 3.
C-----
      DIMENSION PC(12)
C
      GO TO (100, 200), METH
C
100  ELCO(1,1) = 1.0D0
      ELCO(2,1) = 1.0D0
      TESCO(1,1) = 0.0D0
      TESCO(2,1) = 2.0D0
      TESCO(1,2) = 1.0D0
      TESCO(3,12) = 0.0D0
      PC(1) = 1.0D0
      RQFAC = 1.0D0
      DO 140 NQ = 2,12
C-----
C THE PC ARRAY WILL CONTAIN THE COEFFICIENTS OF THE POLYNOMIAL
C P(X) = (X+1)*(X+2)*...*(X+NQ-1).
C INITIALLY, P(X) = 1.
C-----
      RQ1FAC = RQFAC
      RQFAC = RQFAC/DFLOAT(NQ)
      NQM1 = NQ - 1
      FNQM1 = DFLOAT(NQM1)
      NQP1 = NQ + 1
C FORM COEFFICIENTS OF P(X)*(X+NQ-1).
      PC(NQ) = 0.0D0
      DO 110 IB = 1,NQM1
        I = NQP1 - IB
110   PC(I) = PC(I-1) + FNQM1*PC(I)
      PC(1) = FNQM1*PC(1)
C COMPUTE INTEGRAL, -1 TO 0, OF P(X) AND X*P(X).
      PINT = PC(1)
      XPIN = PC(1)/2.0D0
      TSIGN = 1.0D0
      DO 120 I = 2,NQ
        TSIGN = -TSIGN
        PINT = PINT + TSIGN*PC(I)/DFLOAT(I)
120   XPIN = XPIN + TSIGN*PC(I)/DFLOAT(I+1)
C STORE COEFFICIENTS IN ELCO AND TESCO.
      ELCO(1,NQ) = PINT*RQ1FAC
      ELCO(2,NQ) = 1.0D0
      DO 130 I = 2,NQ
130   ELCO(I+1,NQ) = RQ1FAC*PC(I)/DFLOAT(I)
      AGAMQ = RQFAC*XPIN
      RAGQ = 1.0D0/AGAMQ
      TESCO(2,NQ) = RAGQ
      IF (NQ .LT. 12) TESCO(1,NQP1) = RAGQ*RQFAC/DFLOAT(NQP1)

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          TESCO(3,NQM1) = RAGQ
140      CONTINUE
          RETURN
C
200      PC(1) = 1.0D0
          RQ1FAC = 1.0D0
          DO 230 NQ = 1,5
C-----LS02097
C THE PC ARRAY WILL CONTAIN THE COEFFICIENTS OF THE POLYNOMIAL
C P(X) = (X+1)*(X+2)*...*(X+NQ).
C INITIALLY, P(X) = 1.
C-----LS02098
          FNQ = DFLOAT(NQ)
          NQP1 = NQ + 1
C FORM COEFFICIENTS OF P(X)*(X+NQ).
          PC(NQP1) = 0.0D0
          DO 210 IB = 1,NQ
            I = NQ + 2 - IB
210      PC(I) = PC(I-1) + FNQ*PC(I)
          PC(1) = FNQ*PC(1)
C STORE COEFFICIENTS IN ELCO AND TESCO.
          DO 220 I = 1,NQP1
220      ELCO(I,NQ) = PC(I)/PC(2)
          ELCO(2,NQ) = 1.0D0
          TESCO(1,NQ) = RQ1FAC
          TESCO(2,NQ) = DFLOAT(NQP1)/ELCO(1,NQ)
          TESCO(3,NQ) = DFLOAT(NQ+2)/ELCO(1,NQ)
          RQ1FAC = RQ1FAC/FNQ
230      CONTINUE
          RETURN
C-----LS02100
          END OF SUBROUTINE CFODE
          END
          SUBROUTINE PREPJ (NEQ, Y, YH, NYH, EWT, FTEM, SAVF, WM, IWM,
1          F, JAC)
          EXTERNAL F, JAC
          INTEGER NEQ, NYH, IWM, I, I1, I2, IER, II, IOWND, IOWNS, J, J1,
1          JJ, JSTART, KFLAG, L, LENP, MAXORD, MBA, MBAND, MEB1, MEBAND,
2          METH, MITER, ML, ML3, MU, N, NFE, NJE, NQ, NQU, NST
          DOUBLE PRECISION Y, YH, EWT, FTEM, SAVF, WM,
1          ROWND, ROWNS, EL0, H, HMIN, HMXI, HU, TN, UROUND,
2          CON, DI, FAC, HLO, R, R0, SRUR, YI, YJ, YJJ, VNORM
          DIMENSION NEQ(1), Y(1), YH(NYH,1), EWT(1), FTEM(1), SAVF(1),
1          WM(1), IWM(1)
          COMMON /LS0001/ ROWND, ROWNS(210),
1          EL0, H, HMIN, HMXI, HU, TN, UROUND, IOWND(14), IOWNS(6),
4          IER, JSTART, KFLAG, L, METH, MITER, MAXORD, N, NQ, NST, NFE,
5          NJE, NQU
C-----LS02101
C PREPJ IS CALLED BY STODE TO COMPUTE AND PROCESS THE MATRIX
C P = I - H*EL(1)*J , WHERE J IS AN APPROXIMATION TO THE JACOBIAN.
C HERE J IS COMPUTED BY THE USER-SUPPLIED ROUTINE JAC IF
C MITER = 1 OR 4, OR BY FINITE DIFFERENCING IF MITER = 2, 3, OR 5.
C IF MITER = 3, A DIAGONAL APPROXIMATION TO J IS USED.
C J IS STORED IN WM AND REPLACED BY P. IF MITER .NE. 3, P IS THEN
C SUBJECTED TO LU DECOMPOSITION IN PREPARATION FOR LATER SOLUTION
C OF LINEAR SYSTEMS WITH P AS COEFFICIENT MATRIX. THIS IS DONE
C BY DGEFA IF MITER = 1 OR 2, AND BY DGBFA IF MITER = 4 OR 5.
C
C IN ADDITION TO VARIABLES DESCRIBED PREVIOUSLY, COMMUNICATION
C WITH PREPJ USES THE FOLLOWING..

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C	Y	= ARRAY CONTAINING PREDICTED VALUES ON ENTRY.	LS02150
C	FTEM	= WORK ARRAY OF LENGTH N (ACOR IN STODE).	LS02151
C	SAVF	= ARRAY CONTAINING F EVALUATED AT PREDICTED Y.	LS02152
C	WM	= REAL WORK SPACE FOR MATRICES. ON OUTPUT IT CONTAINS THE	LS02153
C		INVERSE DIAGONAL MATRIX IF MITER = 3 AND THE LU DECOMPOSITION	LS02154
C		OF P IF MITER IS 1, 2, 4, OR 5.	LS02155
C		STORAGE OF MATRIX ELEMENTS STARTS AT WM(3).	LS02156
C		WM ALSO CONTAINS THE FOLLOWING MATRIX-RELATED DATA..	LS02157
C		WM(1) = SQRT(UROUND), USED IN NUMERICAL JACOBIAN INCREMENTS.	LS02158
C		WM(2) = H*ELO, SAVED FOR LATER USE IF MITER = 3.	LS02159
C	IWM	= INTEGER WORK SPACE CONTAINING PIVOT INFORMATION, STARTING AT	LS02160
C		IWM(21), IF MITER IS 1, 2, 4, OR 5. IWM ALSO CONTAINS THE	LS02161
C		BAND PARAMETERS ML = IWM(1) AND MU = IWM(2) IF MITER IS 4 OR 5.	LS02162
C	ELO	= EL(1) (INPUT).	LS02163
C	IER	= OUTPUT ERROR FLAG, = 0 IF NO TROUBLE, .NE. 0 IF	LS02164
C		P MATRIX FOUND TO BE SINGULAR.	LS02165
C		THIS ROUTINE ALSO USES THE COMMON VARIABLES ELO, H, TN, UROUND,	LS02166
C		MITER, N, NFE, AND NJE.	LS02167
C		-----	LS02168
		NJE = NJE + 1	LS02169
		HLO = H*ELO	LS02170
		GO TO (100, 200, 300, 400, 500), MITER	LS02171
C	IF	MITER = 1, CALL JAC AND MULTIPLY BY SCALAR. -----	LS02172
100		LENP = N*N	LS02173
		DO 110 I = 1,LENP	LS02174
110		WM(I+2) = 0.0D0	LS02175
		CALL JAC (NEQ, TN, Y, 0, 0, WM(3), N)	LS02176
		CON = -HLO	LS02177
		DO 120 I = 1,LENP	LS02178
120		WM(I+2) = WM(I+2)*CON	LS02179
		GO TO 240	LS02180
C	IF	MITER = 2, MAKE N CALLS TO F TO APPROXIMATE J. -----	LS02181
200		FAC = VNORM (N, SAVF, EWT)	LS02182
		R0 = 1000.0D0*DABS(H)*UROUND*DFLOAT(N)*FAC	LS02183
		IF (R0 .EQ. 0.0D0) R0 = 1.0D0	LS02184
		SRUR = WM(1)	LS02185
		J1 = 2	LS02186
		DO 230 J = 1,N	LS02187
		YJ = Y(J)	LS02188
		R = DMAX1(SRUR*DABS(YJ),R0*EWT(J))	LS02189
		Y(J) = Y(J) + R	LS02190
		FAC = -HLO/R	LS02191
		CALL F (NEQ, TN, Y, FTEM)	LS02192
		DO 220 I = 1,N	LS02193
220		WM(I+J1) = (FTEM(I) - SAVF(I))*FAC	LS02194
		Y(J) = YJ	LS02195
		J1 = J1 + N	LS02196
230		CONTINUE	LS02197
		NFE = NFE + N	LS02198
C	ADD	IDENTITY MATRIX. -----	LS02199
240		J = 3	LS02200
		DO 250 I = 1,N	LS02201
		WM(J) = WM(J) + 1.0D0	LS02202
250		J = J + (N + 1)	LS02203
C	DO	LU DECOMPOSITION ON P. -----	LS02204
		CALL DGEFA (WM(3), N, N, IWM(21), IER)	LS02205
		RETURN	LS02206
C	IF	MITER = 3, CONSTRUCT A DIAGONAL APPROXIMATION TO J AND P. -----	LS02207
300		WM(2) = HLO	LS02208
		IER = 0	LS02209

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R = EL0*0.1D0
DO 310 I = 1,N
310 Y(I) = Y(I) + R*(H*SAVF(I) - YH(I,2))
CALL F (NEQ, TN, Y, WM(3))
NFE = NFE + 1
DO 320 I = 1,N
R0 = H*SAVF(I) - YH(I,2)
DI = 0.1D0*R0 - H*(WM(I+2) - SAVF(I))
WM(I+2) = 1.0D0
IF (DABS(R0) .LT. UROUND*EWT(I)) GO TO 320
IF (DABS(DI) .EQ. 0.0D0) GO TO 330
WM(I+2) = 0.1D0*R0/DI
320 CONTINUE
RETURN
330 IER = -1
RETURN
C IF MITER = 4, CALL JAC AND MULTIPLY BY SCALAR. -----
400 ML = IWM(1)
MU = IWM(2)
ML3 = ML + 3
MBAND = ML + MU + 1
NEBAND = MBAND + ML
LENP = MEBAND*N
DO 410 I = 1,LENP
410 WM(I+2) = 0.0D0
CALL JAC (NEQ, TN, Y, ML, MU, WM(ML3), MEBAND)
CON = -HL0
DO 420 I = 1,LENP
420 WM(I+2) = WM(I+2)*CON
GO TO 570
C IF MITER = 5, MAKE MBAND CALLS TO F TO APPROXIMATE J. -----
500 ML = IWM(1)
MU = IWM(2)
MBAND = ML + MU + 1
MBA = MIN0(MBAND,N)
MEBAND = MBAND + ML
MEB1 = MEBAND - 1
SRUR = WM(1)
FAC = VNORM (N, SAVF, EWT)
R0 = 1000.0D0*DABS(H)*UROUND*DFLOAT(N)*FAC
IF (R0 .EQ. 0.0D0) R0 = 1.0D0
DO 560 J = 1,MBA
DO 530 I = J,N,MBAND
YI = Y(I)
R = DMAX1(SRUR*DABS(YI),R0*EWT(I))
530 Y(I) = Y(I) + R
CALL F (NEQ, TN, Y, FTEM)
DO 550 JJ = J,N,MBAND
Y(JJ) = YH(JJ,1)
YJJ = Y(JJ)
R = DMAX1(SRUR*DABS(YJJ),R0*EWT(JJ))
FAC = -HL0/R
I1 = MAX0(JJ-MU,1)
I2 = MIN0(JJ+ML,N)
II = JJ*MEB1 - ML + 2
DO 540 I = I1,I2
540 WM(II+I) = (FTEM(I) - SAVF(I))*FAC
550 CONTINUE
560 CONTINUE
NFE = NFE + MBA

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C ADD IDENTITY MATRIX. -----LS02270
570  II = MBAND + 2                LS02271
    DO 580 I = 1,N                LS02272
        WM(II) = WM(II) + 1.0D0   LS02273
580  II = II + MEBAND             LS02274
C DO LU DECOMPOSITION OF P. -----LS02275
    CALL DGBFA (WM(3), MEBAND, N, ML, MU, IWM(21), IER)   LS02276
    RETURN                        LS02277
C----- END OF SUBROUTINE PREPJ -----LS02278
    END                            LS02279
    SUBROUTINE SOLSY (WM, IWM, X, TEM)   LS02280
    INTEGER IWM, I, IER, IOWND, IOWNS, JSTART, KFLAG, L, MAXORD,
1    MEBAND, METH, MITER, ML, MU, N, NFE, NJE, NQ, NQU, NST   LS02282
    DOUBLE PRECISION WM, X, TEM,       LS02283
1    ROWND, ROWNS, EL0, H, HMIN, HMXI, HU, TN, UROUND,       LS02284
2    DI, HL0, PHL0, R                 LS02285
    DIMENSION WM(1), IWM(1), X(1), TEM(1)   LS02286
    COMMON /LS0001/ ROWND, ROWNS(210),     LS02287
1    EL0, H, HMIN, HMXI, HU, TN, UROUND, IOWND(14), IOWNS(6), LS02288
4    IER, JSTART, KFLAG, L, METH, MITER, MAXORD, N, NQ, NST, NFE, LS02289
5    NJE, NQU                          LS02290
C-----LS02291
C THIS ROUTINE MANAGES THE SOLUTION OF THE LINEAR SYSTEM ARISING FROM LS02292
C A CHORD ITERATION. IT IS CALLED BY STODE IF MITER .NE. 0.   LS02293
C IF MITER IS 1 OR 2, IT CALLS DGESL TO ACCOMPLISH THIS.     LS02294
C IF MITER = 3 IT UPDATES THE COEFFICIENT H*EL0 IN THE DIAGONAL LS02295
C MATRIX, AND THEN COMPUTES THE SOLUTION.                    LS02296
C IF MITER IS 4 OR 5, IT CALLS DGBSL.                        LS02297
C COMMUNICATION WITH SOLSY USES THE FOLLOWING VARIABLES..   LS02298
C WM = REAL WORK SPACE CONTAINING THE INVERSE DIAGONAL MATRIX IF MITER LS02299
C IS 3 AND THE LU DECOMPOSITION OF THE MATRIX OTHERWISE.    LS02300
C STORAGE OF MATRIX ELEMENTS STARTS AT WM(3).              LS02301
C WM ALSO CONTAINS THE FOLLOWING MATRIX-RELATED DATA..    LS02302
C WM(1) = SQRT(UROUND) (NOT USED HERE),                    LS02303
C WM(2) = HL0, THE PREVIOUS VALUE OF H*EL0, USED IF MITER = 3. LS02304
C IWM = INTEGER WORK SPACE CONTAINING PIVOT INFORMATION, STARTING AT LS02305
C IWM(21), IF MITER IS 1, 2, 4, OR 5. IWM ALSO CONTAINS THE LS02306
C BAND PARAMETERS ML = IWM(1) AND MU = IWM(2) IF MITER IS 4 OR 5. LS02307
C X = THE RIGHT-HAND SIDE VECTOR ON INPUT, AND THE SOLUTION VECTOR LS02308
C ON OUTPUT, OF LENGTH N.                                  LS02309
C TEM = VECTOR OF WORK SPACE OF LENGTH N, NOT USED IN THIS VERSION. LS02310
C IER = OUTPUT FLAG (IN COMMON). IER = 0 IF NO TROUBLE OCCURRED. LS02311
C IER = -1 IF A SINGULAR MATRIX AROSE WITH MITER = 3.      LS02312
C THIS ROUTINE ALSO USES THE COMMON VARIABLES EL0, H, MITER, AND N. LS02313
C-----LS02314
    IER = 0                LS02315
    GO TO (100, 100, 300, 400, 400), MITER   LS02316
100  CALL DGESL (WM(3), N, N, IWM(21), X, 0) LS02317
    RETURN                    LS02318
C                               LS02319
300  PHL0 = WM(2)           LS02320
    HL0 = H*EL0            LS02321
    WM(2) = HL0            LS02322
    IF (HL0 .EQ. PHL0) GO TO 330             LS02323
    R = HL0/PHL0           LS02324
    DO 320 I = 1,N         LS02325
        DI = 1.0D0 - R*(1.0D0 - 1.0D0/WM(I+2)) LS02326
        IF (DABS(DI) .EQ. 0.0D0) GO TO 390   LS02327
320  WM(I+2) = 1.0D0/DI   LS02328
330  DO 340 I = 1,N       LS02329

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340   X(I) = WM(I+2)*X(I)                                LS02330
      RETURN                                             LS02331
390   IER = -1                                           LS02332
      RETURN                                             LS02333
C                                           LS02334
400   ML = IWM(1)                                         LS02335
      MU = IWM(2)                                         LS02336
      MEBAND = 2*ML + MU + 1                             LS02337
      CALL DGBSL (WM(3), MEBAND, N, ML, MU, IWM(21), X, 0) LS02338
      RETURN                                             LS02339
C----- END OF SUBROUTINE SOLSY -----LS02340
      END                                               LS02341
      SUBROUTINE EWSET (N, ITOL, RTOL, ATOL, YCUR, EWT)   LS02342
C-----LS02343
C THIS SUBROUTINE SETS THE ERROR WEIGHT VECTOR EWT ACCORDING TO LS02344
C EWT(I) = RTOL(I)*DABS(YCUR(I)) + ATOL(I), I = 1,...,N, LS02345
C WITH THE SUBSCRIPT ON RTOL AND/OR ATOL POSSIBLY REPLACED BY I ABOVE, LS02346
C DEPENDING ON THE VALUE OF ITOL.                     LS02347
C-----LS02348
      INTEGER N, ITOL, I                                  LS02349
      DOUBLE PRECISION RTOL, ATOL, YCUR, EWT, ATOLI, RTOLI LS02350
      DIMENSION RTOL(1), ATOL(1), YCUR(N), EWT(N)       LS02351
      RTOLI = RTOL(1)                                    LS02352
      ATOLI = ATOL(1)                                    LS02353
      DO 10 I = 1,N                                      LS02354
          IF (ITOL .GE. 3) RTOLI = RTOL(I)               LS02355
          IF (ITOL .EQ. 2 .OR. ITOL .EQ. 4) ATOLI = ATOL(I) LS02356
          EWT(I) = RTOLI*DABS(YCUR(I)) + ATOLI           LS02357
10     CONTINUE                                         LS02358
      RETURN                                             LS02359
C----- END OF SUBROUTINE EWSET -----LS02360
      END                                               LS02361
      DOUBLE PRECISION FUNCTION VNORM (N, V, W)          LS02362
C-----LS02363
C THIS FUNCTION ROUTINE COMPUTES THE WEIGHTED ROOT-MEAN-SQUARE NORM LS02364
C OF THE VECTOR OF LENGTH N CONTAINED IN THE ARRAY V, WITH WEIGHTS LS02365
C CONTAINED IN THE ARRAY W OF LENGTH N..              LS02366
C VNORM = SQRT( (1/N) * SUM( V(I)/W(I) )**2 )          LS02367
C-----LS02368
      INTEGER N, I                                        LS02369
      DOUBLE PRECISION V, W, SUM                        LS02370
      DIMENSION V(N), W(N)                              LS02371
      SUM = 0.0D0                                        LS02372
      DO 10 I = 1,N                                      LS02373
10     SUM = SUM + (V(I)/W(I))**2                       LS02374
      VNORM = DSQRT(SUM/DFLOAT(N))                     LS02375
      RETURN                                             LS02376
C----- END OF FUNCTION VNORM -----LS02377
      END                                               LS02378
      SUBROUTINE SVCOM (RSAV, ISAV)                     LS02379
C-----LS02380
C THIS ROUTINE STORES IN RSAV AND ISAV THE CONTENTS OF COMMON BLOCKS LS02381
C LS0001 AND EH0001, WHICH ARE USED INTERNALLY IN THE LSODE PACKAGE. LS02382
C                                                     LS02383
C RSAV = REAL ARRAY OF LENGTH 218 OR MORE.            LS02384
C ISAV = INTEGER ARRAY OF LENGTH 35 OR MORE.           LS02385
C-----LS02386
      INTEGER ISAV, I, IEH, ILS, LENILS, LENRLS         LS02387
      DOUBLE PRECISION RSAV, RLS                       LS02388
      DIMENSION RSAV(1), ISAV(1)                       LS02389

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COMMON /LS0001/ RLS(218), ILS(33)
COMMON /EH0001/ IEH(2)
DATA LENRLS/218/, LENILS/33/
C
DO 10 I = 1,LENRLS
10   RSAV(I) = RLS(I)
DO 20 I = 1,LENILS
20   ISAV(I) = ILS(I)
   ISAV(LLENILS+1) = IEH(1)
   ISAV(LLENILS+2) = IEH(2)
RETURN
C----- END OF SUBROUTINE SVCOM -----
END
SUBROUTINE RSCOM (RSAV, ISAV)
C-----
C THIS ROUTINE RESTORES FROM RSAV AND ISAV THE CONTENTS OF COMMON
C BLOCKS LS0001 AND EH0001, WHICH ARE USED INTERNALLY IN THE LODE
C PACKAGE. THIS PRESUMES THAT RSAV AND ISAV WERE LOADED BY MEANS
C OF SUBROUTINE SVCOM OR THE EQUIVALENT.
C-----
INTEGER ISAV, I, IEH, ILS, LENILS, LENRLS
DOUBLE PRECISION RSAV, RLS
DIMENSION RSAV(1), ISAV(1)
COMMON /LS0001/ RLS(218), ILS(33)
COMMON /EH0001/ IEH(2)
DATA LENRLS/218/, LENILS/33/
C
DO 10 I = 1,LENRLS
10   RLS(I) = RSAV(I)
DO 20 I = 1,LENILS
20   ILS(I) = ISAV(I)
   IEH(1) = ISAV(LLENILS+1)
   IEH(2) = ISAV(LLENILS+2)
RETURN
C----- END OF SUBROUTINE RSCOM -----
END
SUBROUTINE DGEFA(A,LDA,N,IPVT,INFO)
INTEGER LDA,N,IPVT(1),INFO
DOUBLE PRECISION A(LDA,1)
C
C DGEFA FACTORS A DOUBLE PRECISION MATRIX BY GAUSSIAN ELIMINATION.
C
C DGEFA IS USUALLY CALLED BY DGEFO, BUT IT CAN BE CALLED
C DIRECTLY WITH A SAVING IN TIME IF RCOND IS NOT NEEDED.
C (TIME FOR DGEFO) = (1 + 9/N)*(TIME FOR DGEFA) .
C
C ON ENTRY
C
C   A      DOUBLE PRECISION(LDA, N)
C          THE MATRIX TO BE FACTORED.
C
C   LDA    INTEGER
C          THE LEADING DIMENSION OF THE ARRAY A .
C
C   N      INTEGER
C          THE ORDER OF THE MATRIX A .
C
C ON RETURN
C
C   A      AN UPPER TRIANGULAR MATRIX AND THE MULTIPLIERS

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C		WHICH WERE USED TO OBTAIN IT.	DG00025
C		THE FACTORIZATION CAN BE WRITTEN $A = L*U$ WHERE	DG00026
C		L IS A PRODUCT OF PERMUTATION AND UNIT LOWER	DG00027
C		TRIANGULAR MATRICES AND U IS UPPER TRIANGULAR.	DG00028
C			DG00029
C	IPVT	INTEGER(N)	DG00030
C		AN INTEGER VECTOR OF PIVOT INDICES.	DG00031
C			DG00032
C	INFO	INTEGER	DG00033
C		= 0 NORMAL VALUE.	DG00034
C		= K IF $U(K,K) .EQ. 0.0$. THIS IS NOT AN ERROR	DG00035
C		CONDITION FOR THIS SUBROUTINE, BUT IT DOES	DG00036
C		INDICATE THAT DGESL OR DGED1 WILL DIVIDE BY ZERO	DG00037
C		IF CALLED. USE RCOND IN DGECCO FOR A RELIABLE	DG00038
C		INDICATION OF SINGULARITY.	DG00039
C			DG00040
C		LINPACK. THIS VERSION DATED 08/14/78 .	DG00041
C		CLEVE MOLER, UNIVERSITY OF NEW MEXICO, ARGONNE NATIONAL LAB.	DG00042
C			DG00043
C		SUBROUTINES AND FUNCTIONS	DG00044
C			DG00045
C		BLAS DAXPY,DSCAL,IDAMAX	DG00046
C			DG00047
C		INTERNAL VARIABLES	DG00048
C			DG00049
C		DOUBLE PRECISION T	DG00050
C		INTEGER IDAMAX,J,K,KP1,L,NM1	DG00051
C			DG00052
C		GAUSSIAN ELIMINATION WITH PARTIAL PIVOTING	DG00053
C			DG00054
C		INFO = 0	DG00055
C		NM1 = N - 1	DG00056
C		IF (NM1 .LT. 1) GO TO 70	DG00057
C		DO 60 K = 1, NM1	DG00058
C		KP1 = K + 1	DG00059
C			DG00060
C		FIND L = PIVOT INDEX	DG00061
C			DG00062
C		L = IDAMAX(N-K+1,A(K,K),1) + K - 1	DG00063
C		IPVT(K) = L	DG00064
C			DG00065
C		ZERO PIVOT IMPLIES THIS COLUMN ALREADY TRIANGULARIZED	DG00066
C			DG00067
C		IF (A(L,K) .EQ. 0.0D0) GO TO 40	DG00068
C			DG00069
C		INTERCHANGE IF NECESSARY	DG00070
C			DG00071
C		IF (L .EQ. K) GO TO 10	DG00072
C		T = A(L,K)	DG00073
C		A(L,K) = A(K,K)	DG00074
C		A(K,K) = T	DG00075
C	10	CONTINUE	DG00076
C			DG00077
C		COMPUTE MULTIPLIERS	DG00078
C			DG00079
C		T = -1.0D0/A(K,K)	DG00080
C		CALL DSCAL(N-K,T,A(K+1,K),1)	DG00081
C			DG00082
C		ROW ELIMINATION WITH COLUMN INDEXING	DG00083
C			DG00084

C	OR DGEFA HAS SET INFO .EQ. 0 .	DG0014
C		DG0014
C	TO COMPUTE INVERSE(A) * C WHERE C IS A MATRIX	DG0014
C	WITH P COLUMNS	DG0014
C	CALL DGEKO(A,LDA,N,IPVT,RCOND,Z)	DG0014
C	IF (RCOND IS TOO SMALL) GO TO ...	DG0015
C	DO 10 J = 1, P	DG0015
C	CALL DGESL(A,LDA,N,IPVT,C(1,J),0)	DG0015
C	10 CONTINUE	DG0015
C		DG0015
C	LINPACK. THIS VERSION DATED 08/14/78 .	DG0015
C	CLEVE MOLER, UNIVERSITY OF NEW MEXICO, ARGONNE NATIONAL LAB.	DG0015
C		DG0015
C	SUBROUTINES AND FUNCTIONS	DG0015
C		DG0015
C	BLAS DAXPY,DDOT	DG0016
C		DG0016
C	INTERNAL VARIABLES	DG0016
C		DG0016
C	DOUBLE PRECISION DDOT,T	DG0016
C	INTEGER K,KB,L,NM1	DG0016
C		DG0016
C	NM1 = N - 1	DG0016
C	IF (JOB .NE. 0) GO TO 50	DG0016
C		DG0016
C	JOB = 0 , SOLVE A * X = B	DG0017
C	FIRST SOLVE L*Y = B	DG0017
C		DG0017
C	IF (NM1 .LT. 1) GO TO 30	DG0017
C	DO 20 K = 1, NM1	DG0017
C	L = IPVT(K)	DG0017
C	T = B(L)	DG0017
C	IF (L .EQ. K) GO TO 10	DG0017
C	B(L) = B(K)	DG0017
C	B(K) = T	DG0017
C	10 CONTINUE	DG0017
C	CALL DAXPY(N-K,T,A(K+1,K),1,B(K+1),1)	DG0018
C	20 CONTINUE	DG0018
C	30 CONTINUE	DG0018
C		DG0018
C	NOW SOLVE U*X = Y	DG0018
C		DG0018
C	DO 40 KB = 1, N	DG0018
C	K = N + 1 - KB	DG0018
C	B(K) = B(K)/A(K,K)	DG0018
C	T = -B(K)	DG0018
C	CALL DAXPY(K-1,T,A(1,K),1,B(1),1)	DG0019
C	40 CONTINUE	DG0019
C	GO TO 100	DG0019
C	50 CONTINUE	DG0019
C		DG0019
C	JOB = NONZERO, SOLVE TRANS(A) * X = B	DG0019
C	FIRST SOLVE TRANS(U)*Y = B	DG0019
C		DG0019
C	DO 60 K = 1, N	DG0019
C	T = DDOT(K-1,A(1,K),1,B(1),1)	DG0020
C	B(K) = (B(K) - T)/A(K,K)	DG0020
C	60 CONTINUE	DG0020
C		DG0020
C	NOW SOLVE TRANS(L)*X = Y	DG0020
C		DG0020

C

```
IF (NM1 .LT. 1) GO TO 90
DO 80 KB = 1, NM1
  K = N - KB
  B(K) = B(K) + DDOT(N-K,A(K+1,K),1,B(K+1),1)
  L = IPVT(K)
  IF (L .EQ. K) GO TO 70
  T = B(L)
  B(L) = B(K)
  B(K) = T
70   CONTINUE
80   CONTINUE
90   CONTINUE
100  CONTINUE
RETURN
END
SUBROUTINE DGBFA(ABD,LDA,N,ML,MU,IPVT,INFO)
INTEGER LDA,N,ML,MU,IPVT(1),INFO
DOUBLE PRECISION ABD(LDA,1)

DGBFA FACTORS A DOUBLE PRECISION BAND MATRIX BY ELIMINATION.

DGBFA IS USUALLY CALLED BY DGBCO, BUT IT CAN BE CALLED
DIRECTLY WITH A SAVING IN TIME IF RCOND IS NOT NEEDED.

ON ENTRY

  ABD      DOUBLE PRECISION(LDA, N)
           CONTAINS THE MATRIX IN BAND STORAGE.  THE COLUMNS
           OF THE MATRIX ARE STORED IN THE COLUMNS OF ABD AND
           THE DIAGONALS OF THE MATRIX ARE STORED IN ROWS
           ML+1 THROUGH 2*ML+MU+1 OF ABD .
           SEE THE COMMENTS BELOW FOR DETAILS.

  LDA      INTEGER
           THE LEADING DIMENSION OF THE ARRAY ABD .
           LDA MUST BE .GE. 2*ML + MU + 1 .

  N        INTEGER
           THE ORDER OF THE ORIGINAL MATRIX.

  ML       INTEGER
           NUMBER OF DIAGONALS BELOW THE MAIN DIAGONAL.
           0 .LE. ML .LT. N .

  MU       INTEGER
           NUMBER OF DIAGONALS ABOVE THE MAIN DIAGONAL.
           0 .LE. MU .LT. N .
           MORE EFFICIENT IF ML .LE. MU .

ON RETURN

  ABD      AN UPPER TRIANGULAR MATRIX IN BAND STORAGE AND
           THE MULTIPLIERS WHICH WERE USED TO OBTAIN IT.
           THE FACTORIZATION CAN BE WRITTEN A = L*U WHERE
           L IS A PRODUCT OF PERMUTATION AND UNIT LOWER
           TRIANGULAR MATRICES AND U IS UPPER TRIANGULAR.

  IPVT     INTEGER(N)
           AN INTEGER VECTOR OF PIVOT INDICES.
```

C

DG00205
DG00206
DG00207
DG00208
DG00209
DG00210
DG00211
DG00212
DG00213
DG00214
DG00215
DG00216
DG00217
DG00218
DG00219
DG00220
DG00221
DG00222
DG00223
DG00224
DG00225
DG00226
DG00227
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DG00230
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DG00232
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DG00248
DG00249
DG00250
DG00251
DG00252
DG00253
DG00254
DG00255
DG00256
DG00257
DG00258
DG00259
DG00260
DG00261
DG00262
DG00263
DG00264

```

C          INFO      INTEGER
C          = 0      NORMAL VALUE.
C          = K      IF U(K,K) .EQ. 0.0 . THIS IS NOT AN ERROR
C                   CONDITION FOR THIS SUBROUTINE, BUT IT DOES
C                   INDICATE THAT DGBSL WILL DIVIDE BY ZERO IF
C                   CALLED. USE RCOND IN DGBCO FOR A RELIABLE
C                   INDICATION OF SINGULARITY.
C
C          BAND STORAGE
C
C          IF A IS A BAND MATRIX, THE FOLLOWING PROGRAM SEGMENT
C          WILL SET UP THE INPUT.
C
C                   ML = (BAND WIDTH BELOW THE DIAGONAL)
C                   MU = (BAND WIDTH ABOVE THE DIAGONAL)
C                   M = ML + MU + 1
C                   DO 20 J = 1, N
C                       I1 = MAX0(1, J-MU)
C                       I2 = MIN0(N, J+ML)
C                       DO 10 I = I1, I2
C                           K = I - J + M
C                           ABD(K,J) = A(I,J)
C                   10 CONTINUE
C                   20 CONTINUE
C
C          THIS USES ROWS ML+1 THROUGH 2*ML+MU+1 OF ABD .
C          IN ADDITION, THE FIRST ML ROWS IN ABD ARE USED FOR
C          ELEMENTS GENERATED DURING THE TRIANGULARIZATION.
C          THE TOTAL NUMBER OF ROWS NEEDED IN ABD IS 2*ML+MU+1 .
C          THE ML+MU BY ML+MU UPPER LEFT TRIANGLE AND THE
C          ML BY ML LOWER RIGHT TRIANGLE ARE NOT REFERENCED.
C
C          LINPACK. THIS VERSION DATED 08/14/78 .
C          CLEVE MOLER, UNIVERSITY OF NEW MEXICO, ARGONNE NATIONAL LAB.
C
C          SUBROUTINES AND FUNCTIONS
C
C          BLAS DAXPY,DSCAL,IDAMAX
C          FORTRAN MAX0,MIN0
C
C          INTERNAL VARIABLES
C
C          DOUBLE PRECISION T
C          INTEGER I, IDAMAX, IO, J, JU, JZ, JO, J1, K, KPL, L, LM, M, MM, NM1
C
C          M = ML + MU + 1
C          INFO = 0
C
C          ZERO INITIAL FILL-IN COLUMNS
C
C          JO = MU + 2
C          J1 = MIN0(N,M) - 1
C          IF (J1 .LT. JO) GO TO 30
C          DO 20 JZ = JO, J1
C              IO = M + 1 - JZ
C              DO 10 I = IO, ML
C                  ABD(I,JZ) = 0.0D0
C          10 CONTINUE
C          20 CONTINUE

```

30	CONTINUE	DG0032
	JZ = J1	DG0032
	JU = 0	DG0032
C		DG0032
C	GAUSSIAN ELIMINATION WITH PARTIAL PIVOTING	DG0032
C		DG0033
	NM1 = N - 1	DG0033
	IF (NM1 .LT. 1) GO TO 130	DG0033
	DO 120 K = 1, NM1	DG0033
	KPl = K + 1	DG0033
C		DG0033
C	ZERO NEXT FILL-IN COLUMN	DG0033
C		DG0033
	JZ = JZ + 1	DG0033
	IF (JZ .GT. N) GO TO 50	DG0033
	IF (ML .LT. 1) GO TO 50	DG0034
	DO 40 I = 1, ML	DG0034
	ABD(I,JZ) = 0.0D0	DG0034
40	CONTINUE	DG0034
50	CONTINUE	DG0034
C		DG0034
C	FIND L = PIVOT INDEX	DG0034
C		DG0034
	LM = MIN0(ML,N-K)	DG0034
	L = IDAMAX(LM+1,ABD(M,K),1) + M - 1	DG0034
	IPVT(K) = L + K - M	DG0035
C		DG0035
C	ZERO PIVOT IMPLIES THIS COLUMN ALREADY TRIANGULARIZED	DG0035
C		DG0035
	IF (ABD(L,K) .EQ. 0.0D0) GO TO 100	DG0035
C		DG0035
C	INTERCHANGE IF NECESSARY	DG0035
C		DG0035
	IF (L .EQ. M) GO TO 60	DG0035
	T = ABD(L,K)	DG0035
	ABD(L,K) = ABD(M,K)	DG0036
	ABD(M,K) = T	DG0036
60	CONTINUE	DG0036
C		DG0036
C	COMPUTE MULTIPLIERS	DG0036
C		DG0036
	T = -1.0D0/ABD(M,K)	DG0036
	CALL DSCAL(LM,T,ABD(M+1,K),1)	DG0036
C		DG0036
C	ROW ELIMINATION WITH COLUMN INDEXING	DG0036
C		DG0037
	JU = MIN0(MAX0(JU,MU+IPVT(K)),N)	DG0037
	MM = M	DG0037
	IF (JU .LT. KPl) GO TO 90	DG0037
	DO 80 J = KPl, JU	DG0037
	L = L - 1	DG0037
	MM = MM - 1	DG0037
	T = ABD(L,J)	DG0037
	IF (L .EQ. MM) GO TO 70	DG0037
	ABD(L,J) = ABD(MM,J)	DG0037
	ABD(MM,J) = T	DG0038
70	CONTINUE	DG0038
	CALL DAXPY(LM,T,ABD(M+1,K),1,ABD(MM+1,J),1)	DG0038
80	CONTINUE	DG0038
90	CONTINUE	DG0038

C	WITH P COLUMNS	DG00445
C	CALL DGBCO(ABD,LDA,N,ML,MU,IPVT,RCOND,Z)	DG00446
C	IF (RCOND IS TOO SMALL) GO TO ...	DG00447
C	DO 10 J = 1, P	DG00448
C	CALL DGBSL(ABD,LDA,N,ML,MU,IPVT,C(1,J),0)	DG00449
C	10 CONTINUE	DG00450
C		DG00451
C	LINPACK. THIS VERSION DATED 08/14/78 .	DG00452
C	CLEVE MOLER, UNIVERSITY OF NEW MEXICO, ARGONNE NATIONAL LAB.	DG00453
C		DG00454
C	SUBROUTINES AND FUNCTIONS	DG00455
C		DG00456
C	BLAS DAXPY,DDOT	DG00457
C	FORTRAN MIN0	DG00458
C		DG00459
C	INTERNAL VARIABLES	DG00460
C		DG00461
C	DOUBLE PRECISION DDOT,T	DG00462
C	INTEGER K,KB,L,LA,LB,LM,M,NM1	DG00463
C		DG00464
C	M = MU + ML + 1	DG00465
C	NM1 = N - 1	DG00466
C	IF (JOB .NE. 0) GO TO 50	DG00467
C		DG00468
C	JOB = 0 , SOLVE A * X = B	DG00469
C	FIRST SOLVE L*Y = B	DG00470
C		DG00471
C	IF (ML .EQ. 0) GO TO 30	DG00472
C	IF (NM1 .LT. 1) GO TO 30	DG00473
C	DO 20 K = 1, NM1	DG00474
C	LM = MIN0(ML,N-K)	DG00475
C	L = IPVT(K)	DG00476
C	T = B(L)	DG00477
C	IF (L .EQ. K) GO TO 10	DG00478
C	B(L) = B(K)	DG00479
C	B(K) = T	DG00480
C	10 CONTINUE	DG00481
C	CALL DAXPY(LM,T,ABD(M+1,K),1,B(K+1),1)	DG00482
C	20 CONTINUE	DG00483
C	30 CONTINUE	DG00484
C		DG00485
C	NOW SOLVE U*X = Y	DG00486
C		DG00487
C	DO 40 KB = 1, N	DG00488
C	K = N + 1 - KB	DG00489
C	B(K) = B(K)/ABD(M,K)	DG00490
C	LM = MIN0(K,M) - 1	DG00491
C	LA = M - LM	DG00492
C	LB = K - LM	DG00493
C	T = -B(K)	DG00494
C	CALL DAXPY(LM,T,ABD(LA,K),1,B(LB),1)	DG00495
C	40 CONTINUE	DG00496
C	GO TO 100	DG00497
C	50 CONTINUE	DG00498
C		DG00499
C	JOB = NONZERO, SOLVE TRANS(A) * X = B	DG00500
C	FIRST SOLVE TRANS(U)*Y = B	DG00501
C		DG00502
C	DO 60 K = 1, N	DG00503
C	LM = MIN0(K,M) - 1	DG00504

	LA = M - LM	DG00505
	LB = K - LM	DG00506
	T = DDOT(LM,ABD(LA,K),1,B(LB),1)	DG00507
	B(K) = (B(K) - T)/ABD(M,K)	DG00508
60	CONTINUE	DG00509
C		DG00510
C	NOW SOLVE TRANS(L)*X = Y	DG00511
C		DG00512
	IF (ML .EQ. 0) GO TO 90	DG00513
	IF (NML .LT. 1) GO TO 90	DG00514
	DO 80 KB = 1, NML	DG00515
	K = N - KB	DG00516
	LM = MIN0(ML,N-K)	DG00517
	B(K) = B(K) + DDOT(LM,ABD(M+1,K),1,B(K+1),1)	DG00518
	L = IPVT(K)	DG00519
	IF (L .EQ. K) GO TO 70	DG00520
	T = B(L)	DG00521
	B(L) = B(K)	DG00522
	B(K) = T	DG00523
70	CONTINUE	DG00524
80	CONTINUE	DG00525
90	CONTINUE	DG00526
100	CONTINUE	DG00527
	RETURN	DG00528
	END	DG00529
	SUBROUTINE DAXPY(N,DA,DX,INCX,DY,INCY)	DG00530
C		DG00531
C	CONSTANT TIMES A VECTOR PLUS A VECTOR.	DG00532
C	USES UNROLLED LOOPS FOR INCREMENTS EQUAL TO ONE.	DG00533
C	JACK DONGARRA, LINPACK, 3/11/78.	DG00534
C		DG00535
	DOUBLE PRECISION DX(1),DY(1),DA	DG00536
	INTEGER I,INCX,INCY,IX,IY,M,MP1,N	DG00537
C		DG00538
	IF(N.LE.0)RETURN	DG00539
	IF (DA .EQ. 0.0D0) RETURN	DG00540
	IF(INCX.EQ.1.AND.INCY.EQ.1)GO TO 20	DG00541
C		DG00542
C	CODE FOR UNEQUAL INCREMENTS OR EQUAL INCREMENTS	DG00543
C	NOT EQUAL TO 1	DG00544
C		DG00545
	IX = 1	DG00546
	IY = 1	DG00547
	IF(INCX.LT.0)IX = (-N+1)*INCX + 1	DG00548
	IF(INCY.LT.0)IY = (-N+1)*INCY + 1	DG00549
	DO 10 I = 1,N	DG00550
	DY(IY) = DY(IY) + DA*DX(IX)	DG00551
	IX = IX + INCX	DG00552
	IY = IY + INCY	DG00553
10	CONTINUE	DG00554
	RETURN	DG00555
C		DG00556
C	CODE FOR BOTH INCREMENTS EQUAL TO 1	DG00557
C		DG00558
C		DG00559
C	CLEAN-UP LOOP	DG00560
C		DG00561
20	M = MOD(N,4)	DG00562
	IF(M .EQ. 0) GO TO 40	DG00563
	DO 30 I = 1,M	DG00564

	DY(I) = DY(I) + DA*DX(I)	DG00561
30	CONTINUE	DG00560
	IF(N .LT. 4) RETURN	DG00561
40	MPl = M + 1	DG00561
	DO 50 I = MPl,N,4	DG00561
	DY(I) = DY(I) + DA*DX(I)	DG00570
	DY(I + 1) = DY(I + 1) + DA*DX(I + 1)	DG00571
	DY(I + 2) = DY(I + 2) + DA*DX(I + 2)	DG00572
	DY(I + 3) = DY(I + 3) + DA*DX(I + 3)	DG00573
50	CONTINUE	DG00574
	RETURN	DG00575
	END	DG00576
	SUBROUTINE DSCAL(N,DA,DX,INCX)	DG00577
C		DG00578
C	SCALES A VECTOR BY A CONSTANT.	DG00579
C	USES UNROLLED LOOPS FOR INCREMENT EQUAL TO ONE.	DG00580
C	JACK DONGARRA, LINPACK, 3/11/78.	DG00581
C		DG00582
	DOUBLE PRECISION DA,DX(1)	DG00583
	INTEGER I,INCX,M,MPl,N,NINCX	DG00584
C		DG00585
	IF(N.LE.0)RETURN	DG00586
	IF(INCX.EQ.1)GO TO 20	DG00587
C		DG00588
C	CODE FOR INCREMENT NOT EQUAL TO 1	DG00589
C		DG00590
	NINCX = N*INCX	DG00591
	DO 10 I = 1,NINCX,INCX	DG00592
	DX(I) = DA*DX(I)	DG00593
10	CONTINUE	DG00594
	RETURN	DG00595
C		DG00596
C	CODE FOR INCREMENT EQUAL TO 1	DG00597
C		DG00598
C		DG00599
C	CLEAN-UP LOOP	DG00600
C		DG00601
20	M = MOD(N,5)	DG00602
	IF(M .EQ. 0) GO TO 40	DG00603
	DO 30 I = 1,M	DG00604
	DX(I) = DA*DX(I)	DG00605
30	CONTINUE	DG00606
	IF(N .LT. 5) RETURN	DG00607
40	MPl = M + 1	DG00608
	DO 50 I = MPl,N,5	DG00609
	DX(I) = DA*DX(I)	DG00610
	DX(I + 1) = DA*DX(I + 1)	DG00611
	DX(I + 2) = DA*DX(I + 2)	DG00612
	DX(I + 3) = DA*DX(I + 3)	DG00613
	DX(I + 4) = DA*DX(I + 4)	DG00614
50	CONTINUE	DG00615
	RETURN	DG00616
	END	DG00617
	DOUBLE PRECISION FUNCTION DDOT(N,DX,INCX,DY,INCY)	DG00618
C		DG00619
C	FORMS THE DOT PRODUCT OF TWO VECTORS.	DG00620
C	USES UNROLLED LOOPS FOR INCREMENTS EQUAL TO ONE.	DG00621
C	JACK DONGARRA, LINPACK, 3/11/78.	DG00622
C		DG00623
C	DOUBLE PRECISION DX(1),DY(1),DTEMP	DG00624

	INTEGER I, INCX, INCY, IX, IY, M, MP1, N	DG00625
C		DG00626
	DDOT = 0.0D0	DG00627
	DTEMP = 0.0D0	DG00628
	IF(N.LE.0)RETURN	DG00629
	IF(INCX.EQ.1.AND.INCY.EQ.1)GO TO 20	DG00630
C		DG00631
C	CODE FOR UNEQUAL INCREMENTS OR EQUAL INCREMENTS	DG00632
C	NOT EQUAL TO 1	DG00633
C		DG00634
	IX = 1	DG00635
	IY = 1	DG00636
	IF(INCX.LT.0)IX = (-N+1)*INCX + 1	DG00637
	IF(INCY.LT.0)IY = (-N+1)*INCY + 1	DG00638
	DO 10 I = 1, N	DG00639
	DTEMP = DTEMP + DX(IX)*DY(IY)	DG00640
	IX = IX + INCX	DG00641
	IY = IY + INCY	DG00642
10	CONTINUE	DG00643
	DDOT = DTEMP	DG00644
	RETURN	DG00645
C		DG00646
C	CODE FOR BOTH INCREMENTS EQUAL TO 1	DG00647
C		DG00648
C		DG00649
C	CLEAN-UP LOOP	DG00650
C		DG00651
20	M = MOD(N,5)	DG00652
	IF(M .EQ. 0) GO TO 40	DG00653
	DO 30 I = 1, M	DG00654
	DTEMP = DTEMP + DX(I)*DY(I)	DG00655
30	CONTINUE	DG00656
	IF(N .LT. 5) GO TO 60	DG00657
40	MP1 = M + 1	DG00658
	DO 50 I = MP1, N, 5	DG00659
	DTEMP = DTEMP + DX(I)*DY(I) + DX(I + 1)*DY(I + 1) +	DG00660
	* DX(I + 2)*DY(I + 2) + DX(I + 3)*DY(I + 3) + DX(I + 4)*DY(I + 4)	DG00661
50	CONTINUE	DG00662
60	DDOT = DTEMP	DG00663
	RETURN	DG00664
	END	DG00665
	INTEGER FUNCTION IDAMAX(N,DX,INCX)	DG00666
C		DG00667
C	FINDS THE INDEX OF ELEMENT HAVING MAX. ABSOLUTE VALUE.	DG00668
C	JACK DONGARRA, LINPACK, 3/11/78.	DG00669
C		DG00670
	DOUBLE PRECISION DX(1), DMAX	DG00671
	INTEGER I, INCX, IX, N	DG00672
C		DG00673
	IDAMAX = 0	DG00674
	IF(N .LT. 1) RETURN	DG00675
	IDAMAX = 1	DG00676
	IF(N.EQ.1)RETURN	DG00677
	IF(INCX.EQ.1)GO TO 20	DG00678
C		DG00679
C	CODE FOR INCREMENT NOT EQUAL TO 1	DG00680
C		DG00681
	IX = 1	DG00682
	DMAX = DABS(DX(1))	DG00683
	IX = IX + INCX	DG00684

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DO 10 I = 2,N
  IF(DABS(DX(IX)).LE.DMAX) GO TO 5
  IDAMAX = I
  DMAX = DABS(DX(IX))
5  IX = IX + INCX
10 CONTINUE
RETURN

C
C      CODE FOR INCREMENT EQUAL TO 1
C
20 DMAX = DABS(DX(1))
DO 30 I = 2,N
  IF(DABS(DX(I)).LE.DMAX) GO TO 30
  IDAMAX = I
  DMAX = DABS(DX(I))
30 CONTINUE
RETURN
END
DOUBLE PRECISION FUNCTION DLMACH (IDUM)
INTEGER IDUM
C-----DLMACH003
C THIS ROUTINE COMPUTES THE UNIT ROUND-OFF OF THE MACHINE IN DOUBLE
C PRECISION. THIS IS DEFINED AS THE SMALLEST POSITIVE MACHINE NUMBER
C U SUCH THAT 1.0D0 + U .NE. 1.0D0 (IN DOUBLE PRECISION).
C-----DLMACH007
DOUBLE PRECISION U, COMP
U = 1.0D0
10 U = U*0.5D0
COMP = 1.0D0 + U
IF (COMP .NE. 1.0D0) GO TO 10
DLMACH = U*2.0D0
RETURN
C-----DLMACH015
END OF FUNCTION DLMACH -----DLMACH015
END
SUBROUTINE XERRWV (MSG, NMES, NERR, IERT, NI, I1, I2, NR, R1, R2)
INTEGER MSG, NMES, NERR, IERT, NI, I1, I2, NR,
1 I, LUN, LUNIT, MESFLG, NWDS
DOUBLE PRECISION R1, R2
DIMENSION MSG(NMES)
C-----EHP0006
C SUBROUTINES XERRWV, XSETF, AND XSETUN, AS GIVEN HERE, CONSTITUTE
C A SIMPLIFIED VERSION OF THE SLATEC ERROR HANDLING PACKAGE.
C WRITTEN BY A. C. HINDMARSH AT LLL. VERSION OF JANUARY 23, 1980.
C THIS VERSION IS IN DOUBLE PRECISION.
C
C ALL ARGUMENTS ARE INPUT ARGUMENTS.
C
C MSG      = THE MESSAGE (HOLLERITH LITERAL OR INTEGER ARRAY).
C NMES     = THE LENGTH OF MSG (NUMBER OF CHARACTERS).
C NERR     = THE ERROR NUMBER (NOT USED).
C IERT     = THE ERROR TYPE..
C           1 MEANS RECOVERABLE (CONTROL RETURNS TO CALLER).
C           2 MEANS FATAL (RUN IS ABORTED--SEE NOTE BELOW).
C NI       = NUMBER OF INTEGERS (0, 1, OR 2) TO BE PRINTED WITH MESSAGE.
C I1,I2    = INTEGERS TO BE PRINTED, DEPENDING ON NI.
C NR       = NUMBER OF REALS (0, 1, OR 2) TO BE PRINTED WITH MESSAGE.
C R1,R2    = REALS TO BE PRINTED, DEPENDING ON NI.
C
C NOTE.. THIS ROUTINE IS MACHINE-DEPENDENT AND SPECIALIZED FOR USE
C IN LIMITED CONTEXT, IN THE FOLLOWING WAYS..

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C 1. THE NUMBER OF HOLLERITH CHARACTERS STORED PER WORD IS ASSUMED      EHP0027
C   TO BE 10.                                                            EHP0028
C 2. THE VALUE OF NMES IS ASSUMED TO BE A MULTIPLE OF 10 AND AT MOST 60. EHP0029
C   (MULTI-LINE MESSAGES ARE GENERATED BY REPEATED CALLS.)            EHP0030
C 3. IF IERT = 2, CONTROL PASSES TO THE STATEMENT STOP                  EHP0031
C   TO ABORT THE RUN. THIS STATEMENT MAY BE MACHINE-DEPENDENT.         EHP0032
C 4. R1 AND R2 ARE ASSUMED TO BE IN DOUBLE PRECISION AND ARE PRINTED    EHP0033
C   IN D21.13 FORMAT.                                                  EHP0034
C 5. THE COMMON BLOCK /EH0001/ BELOW IS DATA-LOADED (A MACHINE-      EHP0035
C   DEPENDENT FEATURE) WITH DEFAULT VALUES.                            EHP0036
C   THIS BLOCK IS NEEDED FOR PROPER RETENTION OF PARAMETERS USED BY     EHP0037
C   THIS ROUTINE WHICH THE USER CAN RESET BY CALLING XSETF OR XSETUN.   EHP0038
C   THE VARIABLES IN THIS BLOCK ARE AS FOLLOWS..                       EHP0039
C     MESFLG = PRINT CONTROL FLAG..                                     EHP0040
C       1 MEANS PRINT ALL MESSAGES (THE DEFAULT).                       EHP0041
C       0 MEANS NO PRINTING.                                           EHP0042
C     LUNIT = LOGICAL UNIT NUMBER FOR MESSAGES.                         EHP0043
C       THE DEFAULT IS 6 (MACHINE-DEPENDENT).                           EHP0044
C-----EHP0045
C THE FOLLOWING ARE INSTRUCTIONS FOR INSTALLING THIS ROUTINE            EHP0046
C IN DIFFERENT MACHINE ENVIRONMENTS.                                    EHP0047
C-----EHP0048
C TO CHANGE THE DEFAULT OUTPUT UNIT, CHANGE THE DATA STATEMENT        EHP0049
C IN THE BLOCK DATA SUBPROGRAM BELOW.                                  EHP0050
C-----EHP0051
C FOR A DIFFERENT NUMBER OF CHARACTERS PER WORD, CHANGE THE            EHP0052
C STATEMENTS SETTING NWDS BELOW, AND FORMAT 10.                         EHP0053
C-----EHP0054
C FOR A DIFFERENT RUN-ABORT COMMAND, CHANGE THE STATEMENT FOLLOWING    EHP0055
C STATEMENT 100 AT THE END.                                             EHP0056
C-----EHP0057
COMMON /EH0001/ MESFLG, LUNIT                                          EHP0058
C-----EHP0059
C     IF (MESFLG .EQ. 0) GO TO 100                                       EHP0060
C GET LOGICAL UNIT NUMBER. -----EHP0061
LUN = LUNIT                                                            EHP0062
C GET NUMBER OF WORDS IN MESSAGE. -----EHP0063
NWDS = NMES/10                                                         EHP0064
NWDS = MIN0(NWDS,6)                                                    EHP0065
C WRITE THE MESSAGE. -----EHP0066
WRITE (LUN, 10) (MSG(I),I=1,NWDS)                                       EHP0067
10  FORMAT(6A10)                                                         EHP0068
   IF (NI .EQ. 1) WRITE (LUN, 20) I1                                       EHP0069
20  FORMAT(6X,23HIN ABOVE MESSAGE, I1 =,I10)                             EHP0070
   IF (NI .EQ. 2) WRITE (LUN, 30) I1,I2                                       EHP0071
30  FORMAT(6X,23HIN ABOVE MESSAGE, I1 =,I10,3X,4HI2 =,I10)             EHP0072
   IF (NR .EQ. 1) WRITE (LUN, 40) R1                                       EHP0073
40  FORMAT(6X,23HIN ABOVE MESSAGE, R1 =,D21.13)                           EHP0074
   IF (NR .EQ. 2) WRITE (LUN, 50) R1,R2                                       EHP0075
50  FORMAT(6X,15HIN ABOVE, R1 =,D21.13,3X,4HR2 =,D21.13)               EHP0076
C ABORT THE RUN IF IERT = 2. -----EHP0077
100 IF (IERT .NE. 2) RETURN                                              EHP0078
   CALL EXIT                                                            EHP0079
   STOP                                                                EHP0079
C-----EHP0080
END OF SUBROUTINE XERRWV -----EHP0080
END                                                                    EHP0081
SUBROUTINE XSETF (MFLAG)                                               EHP0082
C-----EHP0083
C THIS ROUTINE RESETS THE PRINT CONTROL FLAG MFLAG.                   EHP0084
C-----EHP0085

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      INTEGER MFLAG, MESFLG, LUNIT
      COMMON /EH0001/ MESFLG, LUNIT
C
      IF (MFLAG .EQ. 0 .OR. MFLAG .EQ. 1) MESFLG = MFLAG
      RETURN
C----- END OF SUBROUTINE XSETF -----
      END
      SUBROUTINE XSETUN (LUN)
C
C THIS ROUTINE RESETS THE LOGICAL UNIT NUMBER FOR MESSAGES.
C
      INTEGER LUN, MESFLG, LUNIT
      COMMON /EH0001/ MESFLG, LUNIT
C
      IF (LUN .GT. 0) LUNIT = LUN
      RETURN
C----- END OF SUBROUTINE XSETUN -----
      END
      BLOCK DATA
C-----
C THE FOLLOWING DATA STATEMENT LOADS VARIABLES INTO THE INTERNAL COMMON
C BLOCKS USED BY LCODE. THE VARIABLES ARE DEFINED AS FOLLOWS..
C ILLIN = COUNTER FOR THE NUMBER OF CONSECUTIVE TIMES LCODE WAS
C CALLED WITH ILLEGAL INPUT. THE RUN IS STOPPED WHEN
C ILLIN REACHES 5.
C NTREP = COUNTER FOR THE NUMBER OF CONSECUTIVE TIMES LCODE WAS
C CALLED WITH ISTATE = 1 AND TOUT = T. THE RUN IS STOPPED
C WHEN NTREP REACHES 5.
C MESFLG = FLAG TO CONTROL PRINTING OF ERROR MESSAGES. 1 MEANS PRINT,
C 0 MEANS NO PRINTING.
C LUNIT = DEFAULT VALUE OF LOGICAL UNIT NUMBER FOR PRINTING OF ERROR
C MESSAGES.
C-----
      INTEGER ILLIN, IDUMA, NTREP, IDUMB, IOWNS, ICOMM, MESFLG, LUNIT
      DOUBLE PRECISION ROWND, ROWNS, RCOMM
      COMMON /LS0001/ ROWND, ROWNS(210), RCOMM(7),
1 ILLIN, IDUMA(10), NTREP, IDUMB(2), IOWNS(6), ICOMM(13)
      COMMON /EH0001/ MESFLG, LUNIT
      DATA ILLIN/0/, NTREP/0/
      DATA MESFLG/1/, LUNIT/6/
C
C----- END OF BLOCK DATA -----
      END
      SUBROUTINE WIPE ( A, IMAX )
      IMPLICIT DOUBLE PRECISION (A-H,O-Z)
C
C WIPE ... ZEROS OUT THE ARRAY A(*)
C
      DIMENSION A(1)
      DO 10 I=1,IMAX
10 A(I) = 0.0
      RETURN
      END
C
      SUBROUTINE IWIFE ( IA, IMAX )
C
C WIPE ... ZEROS OUT THE ARRAY IA(*)
C
      DIMENSION IA(1)
      DO 10 I=1,IMAX
10 IA(I) = 0

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RETURN
END
FUNCTION ISIMEQ ( B, M, N, N1 )
IMPLICIT REAL*8(A-H,O-Z)
C
C      DEFINITION OF TERMS
C      B = MATRIX PLUS RHS
C      M = SIZE OF MATRIX, M => N
C      N = NUMBER OF EQUATIONS IN "B"
C      N1 = NUMBER OF RHS'S
C      NOTE: MATRIX AND RHS DO NOT HAVE TO BE REARRANGED
C            TO ELIMINATE VOID SPACE
C
C      REAL          B(1),          COL(200), PIVOT,          RATIO
C      INTEGER       ROW(200), PR,          PC,          ISIMEQ
C
C      PR = ROW OF PIVOT.
C      PC = COLUMN OF PIVOT.
C      PIVOT = VALUE OF THE MATRIX PIVOT.
C
C      ZERO ROW AND COL, AND SET CONTROLS.
C
C      ISIMEQ = COMPUTATION CODE
C      0      INITIAL VALUE ... NO MEANING
C      1      COMPUTATION SUCCESSFUL
C      2      ERROR ... PIVOT IS EQUAL TO 0.0
C
C      ISIMEQ = 0
C
C      DO 10 I=1,N
C      ROW(I) = 0
C      COL(I) = 0.0
10 CONTINUE
C      N2 = N + 1
C      N3 = N + N1
C
C      ITERATE LOOP.
C
C      DO 200 NN = 1,N
C
C      FIND MAXIMUM PIVOT, REGARDLESS OF SIGN.
C
C      PIVOT = 0.0
C
C      J ... COLUMN INDEX
C      I ... ROW INDEX
C
C      K+1 ... INDEX IN "B" FOR THE BEGINNING OF THE SPECIFIC
C            COLUMN BEING SEARCHED, HENCE THE INITIAL VALUE
C            OF ZERO (0)
C
C      K = 0
C
C      DO 50 J=1,N
C      IF ( COL(J) .NE. 0.0 ) GO TO 40
C      DO 40 I=1,N
C      IF ( ROW(I) .NE. 0 ) GO TO 20
C      IF ( ABS ( B(I + K) ) .LE. ABS ( PIVOT ) ) GO TO 20
C      PR = I

```

```

      PC = J
      PIVOT = B ( I + K )
C
C 20 CONTINUE
C
C      INDEX K BY THE NUMBER OF ROWS/COLUMNS IN "B" ... M
C 40 K = K + M
C 50 CONTINUE
C
C      SEE IF ERROR.
C
C      IF ( PIVOT .NE. 0.0 ) GO TO 70
C 60 ISIMEQ = 2
C      RETURN
C
C      MARK KEY ROW AND COLUMN.
C
C 70 ROW(PR) = PC
C      COL(PC) = 1.0
C      L = M*(PC-1)
C
C      ITERATE ON MATRIX AND RHS.
C
C      DO 190 I=1,N
C      IF ( I .EQ. PR .OR. B(I+L) .EQ. 0.0 ) GO TO 190
C
C      ITERATE ON MATRIX.
C
C      RATIO = - B(I+L) / PIVOT
C      K = 0
C      DO 100 J=1,N
C      B(I+K) = B(I+K) + RATIO*B(K+PR)
C
C      INDEX K BY THE NUMBER OF ROWS/COLUMNS IN "B" ... M
C 100 K = K + M
C
C      ITERATE ON RHS.
C
C      DO 120 J=N2,N3
C      B(I+K) = B(I+K) + RATIO*B(K+PR)
C      INDEX K BY THE NUMBER OF ROWS IN "B's RHS" ... M
C 120 K = K + M
C
C 190 CONTINUE
C
C 200 CONTINUE
C
C      SOLVE AND STORE ANSWERS.
C
C      K = M*N
C      DO 250 J=N2,N3
C      DO 210 I=1,N
C 210 COL(ROW(I)) = B(I+K) / B(M*ROW(I) - M + I)
C      DO 220 I=1,N
C 220 B(I+K) = COL(I)
C 250 K = K + M
C
C      ISIMEQ = 1
C      RETURN
C

```


END	MINV 00
.....	MINV 00
SUBROUTINE MINV	MINV 00
PURPOSE	MINV 00
INVERT A MATRIX	MINV 00
USAGE	MINV 00
CALL MINV(A,N,D,L,M)	MINV 01
DESCRIPTION OF PARAMETERS	MINV 01
A - INPUT MATRIX, DESTROYED IN COMPUTATION AND REPLACED BY	MINV 01
RESULTANT INVERSE.	MINV 01
N - ORDER OF MATRIX A	MINV 01
D - RESULTANT DETERMINANT	MINV 01
L - WORK VECTOR OF LENGTH N	MINV 01
M - WORK VECTOR OF LENGTH N	MINV 01
REMARKS	MINV 02
MATRIX A MUST BE A GENERAL MATRIX	MINV 02
SUBROUTINES AND FUNCTION SUBPROGRAMS REQUIRED	MINV 02
NONE	MINV 02
METHOD	MINV 02
THE STANDARD GAUSS-JORDAN METHOD IS USED. THE DETERMINANT	MINV 02
IS ALSO CALCULATED. A DETERMINANT OF ZERO INDICATES THAT	MINV 02
THE MATRIX IS SINGULAR.	MINV 02
.....	MINV 03
SUBROUTINE MINV (A,N,D,L,M)	MINV 03
DIMENSION A(1),L(1),M(1)	MINV 03
.....	MINV 03
IF A DOUBLE PRECISION VERSION OF THIS ROUTINE IS DESIRED, THE	MINV 03
C IN COLUMN 1 SHOULD BE REMOVED FROM THE DOUBLE PRECISION	MINV 03
STATEMENT WHICH FOLLOWS.	MINV 04
DOUBLE PRECISION A,D,BIGA,HOLD	MINV 04
THE C MUST ALSO BE REMOVED FROM DOUBLE PRECISION STATEMENTS	MINV 04
APPEARING IN OTHER ROUTINES USED IN CONJUNCTION WITH THIS	MINV 04
ROUTINE.	MINV 04
THE DOUBLE PRECISION VERSION OF THIS SUBROUTINE MUST ALSO	MINV 04
CONTAIN DOUBLE PRECISION FORTRAN FUNCTIONS. ABS IN STATEMENT	MINV 04
10 MUST BE CHANGED TO DABS.	MINV 05
.....	MINV 05
SEARCH FOR LARGEST ELEMENT	MINV 05
D=1.0	MINV 05
NK=-N	MINV 05
DO 80 K=1,N	MINV 05
NK=NK+N	MINV 05

	L(K)=K	MINV 0
	M(K)=K	MINV 0
	KK=NK+K	MINV 0
	BIGA=A(KK)	MINV 0
	DO 20 J=K,N	MINV 0
	IZ=N*(J-1)	MINV 0
	DO 20 I=K,N	MINV 0
	IJ=IZ+I	MINV 0
	10 IF(DABS(BIGA)- DABS(A(IJ))) 15,20,20	MINV 0
	15 BIGA=A(IJ)	MINV 0
	L(K)=I	MINV 0
	M(K)=J	MINV 0
	20 CONTINUE	MINV 0
C		MINV 0
C	INTERCHANGE ROWS	MINV 0
C		MINV 0
	J=L(K)	MINV 0
	IF(J-K) 35,35,25	MINV 0
	25 KI=K-N	MINV 0
	DO 30 I=1,N	MINV 0
	KI=KI+N	MINV 0
	HOLD=-A(KI)	MINV 0
	JI=KI-K+J	MINV 0
	A(KI)=A(JI)	MINV 0
	30 A(JI) =HOLD	MINV 0
C		MINV 0
C	INTERCHANGE COLUMNS	MINV 0
C		MINV 0
	35 I=M(K)	MINV 0
	IF(I-K) 45,45,38	MINV 0
	38 JP=N*(I-1)	MINV 0
	DO 40 J=1,N	MINV 0
	JK=NK+J	MINV 0
	JI=JP+J	MINV 0
	HOLD=-A(JK)	MINV 0
	A(JK)=A(JI)	MINV 0
	40 A(JI) =HOLD	MINV 0
C		MINV 0
C	DIVIDE COLUMN BY MINUS PIVOT (VALUE OF PIVOT ELEMENT IS	MINV 0
C	CONTAINED IN BIGA)	MINV 0
C		MINV 10
	45 IF(BIGA) 48,46,48	MINV 10
	46 D=0.0	MINV 10
	RETURN	MINV 10
	48 DO 55 I=1,N	MINV 10
	IF(I-K) 50,55,50	MINV 10
	50 IK=NK+I	MINV 10
	A(IK)=A(IK)/(-BIGA)	MINV 10
	55 CONTINUE	MINV 10
C		MINV 10
C	REDUCE MATRIX	MINV 11
C		MINV 11
	DO 65 I=1,N	MINV 11
	IK=NK+I	MINV 11
	IJ=I-N	MINV 11
	DO 65 J=1,N	MINV 11
	IJ=IJ+N	MINV 11
	IF(I-K) 60,65,60	MINV 11
	60 IF(J-K) 62,65,62	MINV 11
	62 KJ=IJ-I+K	MINV 11

	A(IJ)=A(IK)*A(KJ)+A(IJ)	MINV 12
	65 CONTINUE	MINV 12
C		MINV 12
C	DIVIDE ROW BY PIVOT	MINV 12
C		MINV 12
	KJ=K-N	MINV 12
	DO 75 J=1,N	MINV 12
	KJ=KJ+N	MINV 12
	IF(J-K) 70,75,70	MINV 12
	70 A(KJ)=A(KJ)/BIGA	MINV 12
	75 CONTINUE	MINV 13
C		MINV 13
C	PRODUCT OF PIVOTS	MINV 13
C		MINV 13
	D=D*BIGA	MINV 13
C		MINV 13
C	REPLACE PIVOT BY RECIPROCAL	MINV 13
C		MINV 13
	A(KK)=1.0/BIGA	MINV 13
	80 CONTINUE	MINV 13
C		MINV 14
C	FINAL ROW AND COLUMN INTERCHANGE	MINV 14
C		MINV 14
	K=N	MINV 14
100	K=(K-1)	MINV 14
	IF(K) 150,150,105	MINV 14
105	I=L(K)	MINV 14
	IF(I-K) 120,120,108	MINV 14
108	JQ=N*(K-1)	MINV 14
	JR=N*(I-1)	MINV 14
	DO 110 J=1,N	MINV 15
	JK=JQ+J	MINV 15
	HOLD=A(JK)	MINV 15
	JI=JR+J	MINV 15
	A(JK)=-A(JI)	MINV 15
110	A(JI) =HOLD	MINV 15
120	J=M(K)	MINV 15
	IF(J-K) 100,100,125	MINV 15
125	KI=K-N	MINV 15
	DO 130 I=1,N	MINV 15
	KI=KI+N	MINV 16
	HOLD=A(KI)	MINV 16
	JI=KI-K+J	MINV 16
	A(KI)=-A(JI)	MINV 16
130	A(JI) =HOLD	MINV 16
	GO TO 100	MINV 16
150	RETURN	MINV 16
	END	MINV 16

Appendix: B

Input and Output for the first column

COMPONENTS										
6										
COMPONENT	1	WATER	212.0	18.0	8.35					
COMPONENT	2	TOLUENE	231.2	92.14	7.24					
COMPONENT	3	o-NT	431.8	137.14	9.72					
COMPONENT	4	m-NT	451.4	137.14	9.88					
COMPONENT	5	p-NT	460.4	137.14	9.22					
COMPONENT	6	DNT	572.0	182.14	11.03					
TEMP	104.0	176.0	248.0	320.0	392.0	464.0	536.0	608.0		
VP	1 55.31	355.20	1489.	4635.4	11662.	25110.	48150.	84668.		
VP	2 56.53	280.43	957.5	2528.6	5568.8	10750.	18817.	31305.		
VP	3 0.3505	4.3187	29.43	130.90	431.9	1141.32	2556.2	5052.		
VP	4 0.2054	2.78	20.22	95.17	327.1	892.13	2048.	4127.		
VP	5 0.1926	2.549	18.306	85.466	292.29	794.98	1822.	3668.		
VP	6 0.0017	0.050	0.672	5.123	25.88	96.077	282.04	690.8		
HV	1 1.11	1.14	1.163	1.185	1.200	1.205	1.195	1.162		
HV	2 24.42	26.26	28.47	31.14	34.36	36.67	39.62	42.94		
HV	3 21.09	23.26	25.42	27.59	29.75	31.91	34.09	36.24		
HV	4 22.27	24.44	26.60	28.77	30.93	33.09	35.26	37.42		
HV	5 22.39	24.56	26.72	28.88	31.05	33.21	35.37	37.54		
HV	6 33.25	35.41	37.56	39.72	41.88	44.03	46.18	48.34		
HL	1 0.074	0.144	0.217	0.290	0.366	0.446	0.532	0.629		
HL	2 8.48	11.51	14.56	17.78	21.92	25.34	29.48	35.66		
HL	3 0.808	2.974	5.137	7.300	9.467	11.630	13.79	15.96		
HL	4 0.808	2.974	5.137	7.300	9.467	11.630	13.79	15.96		
HL	5 0.808	2.974	5.137	7.300	9.467	11.630	13.79	15.96		
HL	6 0.808	2.974	5.137	7.300	9.467	11.630	13.79	15.96		
VM	1 0.1207	0.1233	0.127	0.1321	0.1386	0.1473	0.159	0.179		
VM	2 13.02	13.64	14.38	15.23	16.34	17.90	20.49	23.13		
VM	3 20.22	20.72	21.32	22.04	22.94	24.09	25.61	27.71		
VM	4 22.63	23.17	23.81	24.60	25.57	26.81	28.44	30.69		
VM	5 23.31	23.87	24.51	25.30	26.27	27.49	29.07	31.23		
VM	6 35.22	35.82	36.81	37.37	38.37	39.58	41.07	42.95		
CHARGE	1	17.314								
COMP	1	0.002								
COMP	2	1.316								
COMP	3	9.486								
COMP	4	0.643								
COMP	5	5.865								
COMP	6	0.002								
STAGES										
7										
HOLDDUTYEM	0.6	0.2	0.0	0.7						
PRESDFRRDR	760.0	0.0	0.0	4.0			4.76			
CUTTEMPS	240.436.456	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
CONVERGENCE	0.001	50.0	15	0	1					

(LAPPED CPU TIME - 0.00 SEC ENTRY COUNT = 0)

C O M P O N E N T P R O P E R T I E S

NO	NAME	NBP	MOLE WT	DENSITY
1	WATER	212.0	18.00	8.350
2	TOLUENE	231.2	92.14	7.240
3	o-NT	431.6	137.1	9.720
4	m-NT	451.4	137.1	9.680
5	p-NT	460.4	137.1	9.220
6	DNT	572.0	182.1	11.03

VAPOR PRESSURE DATA

1 WATER				
TEMP	EXP	CALC	%DEV	
104.0	55.31	60.29	8.998	
176.0	355.2	300.2	-15.49	
248.0	1489.	1390.	-6.648	
320.0	4635.	4960.	6.998	
392.0	0.1166E+05	0.1338E+05	14.71	
464.0	0.2511E+05	0.2818E+05	12.21	
536.0	0.4815E+05	0.4841E+05	0.5428	
608.0	0.8467E+05	0.7070E+05	-16.50	
2 TOLUENE				
TEMP	EXP	CALC	%DEV	
104.0	56.53	61.26	8.362	
176.0	280.4	240.0	-14.43	
248.0	957.5	897.0	-6.324	
320.0	2529.	2688.	6.291	
392.0	5569.	6323.	13.55	
464.0	0.1075E+05	0.1200E+05	11.61	
536.0	0.1882E+05	0.1906E+05	1.290	
608.0	0.3131E+05	0.2627E+05	-16.08	
3 o-NT				
TEMP	EXP	CALC	%DEV	
104.0	0.3505	0.3763	7.372	
176.0	4.319	3.761	-12.91	
248.0	29.43	27.75	-5.723	
320.0	130.9	138.6	5.874	
392.0	431.9	484.0	12.07	
464.0	1141.	1255.	9.999	
536.0	2556.	2567.	0.4140	
608.0	5052.	4352.	-13.86	
4 m-NT				
TEMP	EXP	CALC	%DEV	
104.0	0.2054	0.2204	7.323	
176.0	2.780	2.421	-12.93	
248.0	20.22	19.13	-5.410	
320.0	95.17	100.6	5.728	
392.0	327.1	365.9	11.86	
464.0	892.1	980.0	9.847	
536.0	2048.	2056.	0.4126	
608.0	4127.	3562.	-13.68	
5 p-NT				
TEMP	EXP	CALC	%DEV	
104.0	0.1926	0.2066	7.274	
176.0	2.549	2.222	-12.84	
248.0	18.31	17.32	-5.400	
320.0	85.47	90.33	5.691	
392.0	292.3	326.8	11.80	
464.0	795.0	872.8	9.788	
536.0	1822.	1829.	0.4056	
608.0	3668.	3169.	-13.61	
6 DNT				
TEMP	EXP	CALC	%DEV	
104.0	0.1700E-02	0.1816E-02	6.806	
176.0	0.5000E-01	0.4394E-01	-12.12	
248.0	0.6720	0.6379	-5.076	
320.0	5.123	5.405	5.509	
392.0	25.88	28.74	11.03	
464.0	96.08	104.7	8.931	

536.0	282.0	282.6	0.2046
608.0	690.8	603.7	-12.61

VAPOR ENTHALPY DATA

1	WATER	EXP	CALC	%DEV
	TEMP			
	104.0	1.110	1.098	-1.038
	176.0	1.140	1.144	0.3437
	248.0	1.183	1.174	0.9771
	320.0	1.185	1.192	0.5740
	392.0	1.200	1.198	-0.1483
	464.0	1.205	1.198	-0.7794
	536.0	1.195	1.186	-0.7573
	608.0	1.162	1.171	0.7947
2	TOLUENE			
	TEMP	EXP	CALC	%DEV
	104.0	24.42	24.09	-1.343
	176.0	26.26	26.45	0.7351
	248.0	28.47	28.83	1.279
	320.0	31.14	31.29	0.4845
	392.0	34.36	33.88	-1.399
	464.0	36.67	36.66	-0.4021E-01
	536.0	39.62	39.67	0.1370
	608.0	42.94	42.99	0.1216
3	o-NT			
	TEMP	EXP	CALC	%DEV
	104.0	21.09	21.05	-0.1805
	176.0	23.26	23.28	0.7393E-01
	248.0	25.42	25.46	0.1403
	320.0	27.59	27.61	0.5493E-01
	392.0	29.75	29.74	-0.2201E-01
	464.0	31.91	31.89	-0.6780E-01
	536.0	34.09	34.06	-0.9479E-01
	608.0	36.24	36.27	0.8064E-01
4	m-NT			
	TEMP	EXP	CALC	%DEV
	104.0	22.27	22.22	-0.2181
	176.0	24.44	24.46	0.9522E-01
	248.0	26.60	26.64	0.1690
	320.0	28.77	28.79	0.6749E-01
	392.0	30.93	30.92	-0.3380E-01
	464.0	33.09	33.06	-0.9595E-01
	536.0	35.26	35.23	-0.8949E-01
	608.0	37.42	37.45	0.8829E-01
5	p-NT			
	TEMP	EXP	CALC	%DEV
	104.0	22.39	22.34	-0.2191
	176.0	24.56	24.58	0.9361E-01
	248.0	26.72	26.76	0.1634
	320.0	28.88	28.91	0.9195E-01
	392.0	31.05	31.04	-0.4762E-01
	464.0	33.21	33.17	-0.1107
	536.0	35.37	35.34	-0.7307E-01
	608.0	37.54	37.57	0.8414E-01
6	DNT			
	TEMP	EXP	CALC	%DEV
	104.0	33.25	33.09	-0.4664
	176.0	35.41	35.49	0.2198
	248.0	37.56	37.70	0.3626
	320.0	39.72	39.79	0.1776
	392.0	41.88	41.84	-0.9198E-01
	464.0	44.03	43.98	-0.2509

536.0	46.18	46.10	-0.1836
608.0	48.34	48.44	0.2051

LIQUID ENTHALPY DATA

1	WATER			
	TEMP	EXP	CALC	%DEV
	104.0	0.7400E-01	0.8005E-01	8.176
	176.0	0.1440	0.1419	-1.489
	248.0	0.2170	0.2111	-2.710
	320.0	0.2900	0.2866	-1.189
	392.0	0.3660	0.3669	0.2343
	464.0	0.4460	0.4507	1.064
	536.0	0.5320	0.5369	0.9265
	608.0	0.6290	0.6241	-0.7773
2	TOLUENE			
	TEMP	EXP	CALC	%DEV
	104.0	8.480	8.787	3.617
	176.0	11.51	11.39	-1.030
	248.0	14.56	14.37	-1.324
	320.0	17.78	17.72	-0.3125
	392.0	21.92	21.47	-2.035
	464.0	25.34	25.63	1.129
	536.0	29.48	30.19	2.415
	608.0	35.66	35.18	-1.342
3	o-NT			
	TEMP	EXP	CALC	%DEV
	104.0	0.8080	0.9626	19.13
	176.0	2.974	2.894	-2.700
	248.0	5.137	5.006	-2.540
	320.0	7.300	7.231	-0.9408
	392.0	9.467	9.499	0.3331
	464.0	11.63	11.74	0.9332
	536.0	13.79	13.88	0.6647
	608.0	15.96	15.86	-0.6370
4	m-NT			
	TEMP	EXP	CALC	%DEV
	104.0	0.8080	0.9626	19.13
	176.0	2.974	2.894	-2.700
	248.0	5.137	5.006	-2.540
	320.0	7.300	7.231	-0.9408
	392.0	9.467	9.499	0.3331
	464.0	11.63	11.74	0.9332
	536.0	13.79	13.88	0.6647
	608.0	15.96	15.86	-0.6370
5	p-NT			
	TEMP	EXP	CALC	%DEV
	104.0	0.8080	0.9626	19.13
	176.0	2.974	2.894	-2.700
	248.0	5.137	5.006	-2.540
	320.0	7.300	7.231	-0.9408
	392.0	9.467	9.499	0.3331
	464.0	11.63	11.74	0.9332
	536.0	13.79	13.88	0.6647
	608.0	15.96	15.86	-0.6370
6	DNT			
	TEMP	EXP	CALC	%DEV
	104.0	0.8080	0.9626	19.13
	176.0	2.974	2.894	-2.700
	248.0	5.137	5.006	-2.540
	320.0	7.300	7.231	-0.9408
	392.0	9.467	9.499	0.3331
	464.0	11.63	11.74	0.9332

536.0	13.79	13.88	0.6647
608.0	15.96	15.86	-0.6370

MOLAR VOLUME DATA

1	WATER			
	TEMP	EXP	CALC	%DEV
	104.0	0.1207	0.1206	-0.8606E-01
	176.0	0.1233	0.1238	0.3779
	248.0	0.1270	0.1271	0.9470E-01
	320.0	0.1321	0.1316	-0.4078
	392.0	0.1386	0.1380	-0.4392
	464.0	0.1473	0.1473	0.8270E-02
	536.0	0.1590	0.1604	0.8971
	608.0	0.1790	0.1782	-0.4268
2	TOLUENE			
	TEMP	EXP	CALC	%DEV
	104.0	13.02	15.58	19.63
	176.0	13.64	13.52	-0.8612
	248.0	14.36	12.34	-14.04
	320.0	15.23	12.58	-17.38
	392.0	16.34	14.79	-9.495
	464.0	17.90	19.50	8.958
	536.0	20.49	27.27	33.11
	608.0	43.13	38.64	-10.40
3	o-NT			
	TEMP	EXP	CALC	%DEV
	104.0	20.22	20.14	-0.4041
	176.0	20.72	20.79	0.3194
	248.0	21.32	21.38	0.2976
	320.0	22.04	22.05	0.3522E-01
	392.0	22.94	22.90	-0.1886
	464.0	24.09	24.05	-0.1742
	536.0	25.61	25.62	0.3630E-01
	608.0	27.71	27.73	0.6546E-01
4	m-NT			
	TEMP	EXP	CALC	%DEV
	104.0	22.63	22.53	-0.4435
	176.0	23.17	23.24	0.3228
	248.0	23.81	23.90	0.3576
	320.0	24.60	24.61	0.4262E-01
	392.0	25.57	25.52	-0.1933
	464.0	26.81	26.76	-0.2043
	536.0	28.44	28.44	0.1473E-01
	608.0	30.69	30.72	0.8881E-01
5	p-NT			
	TEMP	EXP	CALC	%DEV
	104.0	23.31	23.20	-0.4774
	176.0	23.87	23.94	0.3075
	248.0	24.51	24.61	0.4030
	320.0	25.30	25.32	0.9531E-01
	392.0	26.27	26.22	-0.1956
	464.0	27.49	27.42	-0.2490
	536.0	29.07	29.06	-0.2716E-01
	608.0	31.23	31.27	0.1266
6	DNT			
	TEMP	EXP	CALC	%DEV
	104.0	35.22	35.01	-0.6052
	176.0	35.82	36.03	0.5753
	248.0	36.81	36.81	0.2920E-02
	320.0	37.37	37.53	0.4257
	392.0	38.37	38.35	-0.5901E-01
	464.0	39.58	39.43	-0.3710

536.0
608.0

41.07
42.95

40.95
43.08

-0.2830
0.2944

VAPOR PRESSURE COEFFICIENTS

1	WATER	-0.57833E-02	35553.	-0.32480E+08	0.77471E+10
2	TOLUENE	-0.54543E-02	31947.	-0.28993E+08	0.69304E+10
3	o-NT	-0.47888E-02	31082.	-0.30116E+08	0.69259E+10
4	m-NT	-0.47305E-02	30963.	-0.30215E+08	0.69236E+10
5	p-NT	-0.47027E-02	30897.	-0.30040E+08	0.68983E+10
6	DNT	-0.43852E-02	30460.	-0.31977E+08	0.72171E+10

VAPOR ENTHALPY COEFFICIENTS

1	WATER	-0.42378E-03	0.34366E-02	-0.31384E-05	0.88736E-09
2	TOLUENE	-0.87834E-02	0.60517E-01	-0.45541E-04	0.24898E-07
3	o-NT	-0.13173E-02	0.45912E-01	-0.19670E-04	0.79481E-08
4	m-NT	-0.16365E-02	0.50441E-01	-0.25308E-04	0.10229E-07
5	p-NT	-0.16632E-02	0.50945E-01	-0.25994E-04	0.10527E-07
6	DNT	-0.51662E-02	0.92612E-01	-0.77881E-04	0.31505E-07

LIQUID ENTHALPY COEFFICIENTS

1	WATER	0.22154E-03	-0.70065E-03	0.18194E-05	-0.57682E-09
2	TOLUENE	0.13152E-01	-0.10146E-02	0.26743E-04	0.47385E-08
3	o-NT	0.51447E-02	-0.31719E-01	0.76809E-04	-0.31090E-07
4	m-NT	0.51447E-02	-0.31719E-01	0.76809E-04	-0.31090E-07
5	p-NT	0.51447E-02	-0.31719E-01	0.76809E-04	-0.31090E-07
6	DNT	0.51447E-02	-0.31719E-01	0.76809E-04	-0.31090E-07

MOLAR VOLUME COEFFICIENTS

1	WATER	1.0000	0.00000E+00	0.00000E+00	0.00000E+00
2	TOLUENE	1.0000	0.00000E+00	0.00000E+00	0.00000E+00
3	o-NT	1.0000	0.00000E+00	0.00000E+00	0.00000E+00
4	m-NT	1.0000	0.00000E+00	0.00000E+00	0.00000E+00
5	p-NT	1.0000	0.00000E+00	0.00000E+00	0.00000E+00
6	DNT	1.0000	0.00000E+00	0.00000E+00	0.00000E+00

F E E D C H A R G E

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.2000E-02	0.1155E-01	0.3600E-01	0.1555E-02	0.4311E-02	0.1746E-02
2	TOLUENE	1.316	7.601	121.3	5.238	16.75	6.781
3	o-NT	9.486	54.79	1301.	56.19	133.8	54.19
4	m-NT	0.6430	3.714	88.18	3.809	9.110	3.689
5	p-NT	5.865	33.87	804.3	34.74	87.24	35.32
6	DNT	0.2000E-02	0.1155E-01	0.3643	0.1574E-01	0.3303E-01	0.1337E-01
	TOTAL	17.31	100.0	2315.	100.0	247.0	100.0

(LAPPED CPU TIME - 2.20 SEC ENTRY COUNT - 1)

ITERATION NUMBER 0

STEADY - STATE PROFILE

STAGE	DEL TEMP	TEMPERATURE	VAPOR RATE	LIQUID RATE	DEL HOLDUP	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE	SUMDX
1	0.0000E+00	238.2	0.0000E+00	0.0000E+00	0.0000E+00	0.6000	0.6000	0.0000E+00	760.0	0.0000E+00
2	0.0000E+00	259.5	0.0000E+00	0.0000E+00	0.0000E+00	0.2000	0.2000	0.0000E+00	760.0	0.0000E+00
3	0.0000E+00	259.5	0.0000E+00	0.0000E+00	0.0000E+00	0.2000	0.2000	0.0000E+00	760.0	0.0000E+00
4	0.0000E+00	259.5	0.0000E+00	0.0000E+00	0.0000E+00	0.2000	0.2000	0.0000E+00	760.0	0.0000E+00
5	0.0000E+00	291.3	0.0000E+00	0.0000E+00	0.0000E+00	0.2000	0.2000	0.0000E+00	760.0	0.0000E+00
6	0.0000E+00	451.6	0.0000E+00	0.0000E+00	0.0000E+00	0.2000	0.2000	0.0000E+00	760.0	0.0000E+00
7	0.0000E+00	433.8	0.0000E+00	0.0000E+00	0.0000E+00	15.71	0.0000E+00	0.0000E+00	760.0	0.0000E+00

SCALE CONV ICONV
0.0000E+00 0.0000E+00 0

TOTAL TIME, HOURS 0.2971E-04
 CUMULATIVE TIME, HOURS 0.2971E-04
 CUT TIME, HOURS 0.2971E-04
 TIME STEP, HOURS 0.2971E-04

OVERHEAD TEMPERATURE 239.6
 AT 760 MM HG 239.8
 K = 12 239.8

INSTANTANEOUS DISTILLATE DRAFF PER HOUR

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.1026E-01	0.2156	0.1847	0.4203E-01	0.2212E-01	0.3655E-01
2	TOLUENE	4.715	99.05	434.4	98.87	60.00	99.14
3	o-NT	0.2615E-01	0.5493	3.586	0.8161	0.3689	0.6086
4	m-NT	0.1041E-02	0.2187E-01	0.1428	0.3249E-01	0.1475E-01	0.2437E-01
5	p-NT	0.7807E-02	0.1640	1.071	0.2437	0.1161	0.1919
6	DNT	0.1219E-06	0.2560E-05	0.2220E-04	0.5052E-05	0.2012E-05	0.3325E-05
TOTAL		4.760	100.0	439.4	100.0	60.52	100.0

CUT DISTILLATE DRAFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.3049E-06	0.2156	0.5488E-05	0.4203E-01	0.6572E-06	0.3655E-01
2	TOLUENE	0.1401E-03	99.05	0.1291E-01	98.87	0.1783E-02	99.14
3	o-NT	0.7757E-06	0.5484	0.1064E-03	0.8148	0.1094E-04	0.6086
4	m-NT	0.3084E-07	0.2181E-01	0.4230E-05	0.3240E-01	0.4370E-06	0.2430E-01
5	p-NT	0.2312E-06	0.1635	0.3171E-04	0.2429	0.3439E-05	0.1912
6	DNT	0.3444E-11	0.2435E-05	0.6272E-09	0.4804E-05	0.5687E-10	0.3162E-05
TOTAL		0.1414E-03	100.0	0.1306E-01	100.0	0.1798E-02	100.0

CUMULATIVE DISTILLATE DRAFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.3049E-06	0.2156	0.5488E-05	0.4203E-01	0.6572E-06	0.3655E-01
2	TOLUENE	0.1401E-03	99.05	0.1291E-01	98.87	0.1783E-02	99.14
3	o-NT	0.7757E-06	0.5484	0.1064E-03	0.8148	0.1094E-04	0.6086
4	m-NT	0.3084E-07	0.2181E-01	0.4230E-05	0.3240E-01	0.4370E-06	0.2430E-01
5	p-NT	0.2312E-06	0.1635	0.3171E-04	0.2429	0.3439E-05	0.1912
6	DNT	0.3444E-11	0.2435E-05	0.6272E-09	0.4804E-05	0.5687E-10	0.3162E-05
TOTAL		0.1414E-03	100.0	0.1306E-01	100.0	0.1798E-02	100.0

TOTAL DISTILLATE DRAFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.3049E-06	0.2156	0.5488E-05	0.4203E-01	0.6572E-06	0.3655E-01
2	TOLUENE	0.1401E-03	99.05	0.1291E-01	98.87	0.1783E-02	99.14
3	o-NT	0.7757E-06	0.5484	0.1064E-03	0.8148	0.1094E-04	0.6086
4	m-NT	0.3084E-07	0.2181E-01	0.4230E-05	0.3240E-01	0.4370E-06	0.2430E-01
5	p-NT	0.2312E-06	0.1635	0.3171E-04	0.2429	0.3439E-05	0.1912
6	DNT	0.3444E-11	0.2435E-05	0.6272E-09	0.4804E-05	0.5687E-10	0.3162E-05
TOTAL		0.1414E-03	100.0	0.1306E-01	100.0	0.1798E-02	100.0

ITERATION NUMBER 5

S T E A D Y - S T A T E P R O F I L E

STAGE	DEL TEMP	TEMPERATURE	VAPOR RATE	LIQUID RATE	DEL HOLDUP	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE	SUMDX
1	0.6865E-08	238.7	0.0000E+00	23.80	-0.2991E-16	0.6000	0.6000	-347.7	760.0	0.2722E-09
2	0.2500E-07	239.6	23.80	23.54	-0.3698E-17	0.2000	0.2000	0.0000E+00	760.0	0.7579E-09
3	0.1063E-06	242.5	23.54	22.74	0.8161E-17	0.2000	0.2000	0.0000E+00	760.0	0.1998E-08
4	0.4892E-06	252.5	22.74	20.28	-0.4441E-17	0.2000	0.2000	0.0000E+00	760.0	0.9305E-09
5	-0.9336E-06	292.5	20.28	16.56	0.4669E-18	0.2000	0.2000	0.0000E+00	760.0	0.1393E-08
6	0.8268E-07	383.7	16.56	16.19	0.4368E-17	0.2000	0.2000	0.0000E+00	760.0	0.3489E-09
7	-0.2061E-07	428.7	16.19	0.0000E+00	0.2505E-16	15.71	15.71	347.7	760.0	0.6867E-10

SCALE	CONV	ICONV
1.000	1.000	0

(L A P S E D C P U T I M E - 2.89 SEC ENTRY COUNT - 2)

NUMBER OF STEPS	1
NUMBER OF FUNCTION CALLS	5
NUMBER OF JACOBIAN CALLS	2

TIME. HOURS 0.2971E-04

DISILLATE RATE 4.760

U N S T E A D Y - S T A T E P R O F I L E

STAGE	TEMPERATURE	VAPOR RATE	LIQUID RATE	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE
1	238.7	0.0000E+00	19.04	0.6000	0.6000	-347.7	760.0
2	239.6	23.80	18.78	0.2000	0.2000	0.0000E+00	760.0
3	242.5	23.54	17.98	0.2000	0.2000	0.0000E+00	760.0
4	252.5	22.74	15.53	0.2000	0.2000	0.0000E+00	760.0
5	292.5	20.29	11.91	0.2000	0.2000	0.0000E+00	760.0
6	383.8	16.67	12.06	0.2000	0.2000	0.0000E+00	760.0
7	428.7	16.82	0.0000E+00	15.71	15.71	362.3	760.0

TOTAL TIME, HOURS 0.1388E-01
 CUMULATIVE TIME, HOURS 0.1388E-01
 CUT TIME, HOURS 0.1388E-01
 TIME STEP, HOURS 0.1138E-02

OVERHEAD TEMPERATURE 240.0
 AT 760 MM HG 240.2
 K - 12 240.2

INSTANTANEOUS DISTILLATE DRAFF PER HOUR

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.1004E-01	0.2108	0.1808	0.4109E-01	0.2163E-01	0.3574E-01
2	TOLUENE	4.712	98.98	434.1	98.78	59.96	99.06
3	o-NT	0.2878E-01	0.6047	3.947	0.8979	0.4061	0.6709
4	m-NT	0.1140E-02	0.2396E-01	0.1564	0.3557E-01	0.1615E-01	0.2669E-01
5	p-NT	0.8522E-02	0.1790	1.189	0.2659	0.1268	0.2094
6	DNT	0.1244E-06	0.2613E-05	0.2265E-04	0.5153E-05	0.2054E-05	0.3393E-05
TOTAL		4.760	100.0	439.6	100.0	60.53	100.0

CUT DISTILLATE DRAFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.1412E-03	0.2138	0.2542E-02	0.4169E-01	0.3044E-03	0.3625E-01
2	TOLUENE	0.6540E-01	99.02	6.026	98.83	0.8324	99.11
3	o-NT	0.3760E-03	0.5692	0.5156E-01	0.8455	0.5304E-02	0.6316
4	m-NT	0.1495E-04	0.2264E-01	0.2050E-02	0.3362E-01	0.2118E-03	0.2522E-01
5	p-NT	0.1120E-03	0.1696	0.1536E-01	0.2519	0.1666E-02	0.1984
6	DNT	0.1710E-08	0.2590E-05	0.3115E-06	0.5109E-05	0.2824E-07	0.3363E-05
TOTAL		0.6605E-01	100.0	6.098	100.0	0.8398	100.0

CUMULATIVE DISTILLATE DRAFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.1412E-03	0.2138	0.2542E-02	0.4169E-01	0.3044E-03	0.3625E-01
2	TOLUENE	0.6540E-01	99.02	6.026	98.83	0.8324	99.11
3	o-NT	0.3760E-03	0.5692	0.5156E-01	0.8455	0.5304E-02	0.6316
4	m-NT	0.1495E-04	0.2264E-01	0.2050E-02	0.3362E-01	0.2118E-03	0.2522E-01
5	p-NT	0.1120E-03	0.1696	0.1536E-01	0.2519	0.1666E-02	0.1984
6	DNT	0.1710E-08	0.2590E-05	0.3115E-06	0.5109E-05	0.2824E-07	0.3363E-05
TOTAL		0.6605E-01	100.0	6.098	100.0	0.8398	100.0

TOTAL DISTILLATE DRAFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.1412E-03	0.2138	0.2542E-02	0.4169E-01	0.3044E-03	0.3625E-01
2	TOLUENE	0.6540E-01	99.02	6.026	98.83	0.8324	99.11
3	o-NT	0.3760E-03	0.5692	0.5156E-01	0.8455	0.5304E-02	0.6316
4	m-NT	0.1495E-04	0.2264E-01	0.2050E-02	0.3362E-01	0.2118E-03	0.2522E-01
5	p-NT	0.1120E-03	0.1696	0.1536E-01	0.2519	0.1666E-02	0.1984
6	DNT	0.1710E-08	0.2590E-05	0.3115E-06	0.5109E-05	0.2824E-07	0.3363E-05
TOTAL		0.6605E-01	100.0	6.098	100.0	0.8398	100.0

NUMBER OF STEPS	35
NUMBER OF FUNCTION CALLS	44
NUMBER OF JACOBIAN CALLS	8

TIME, HOURS 0.1388E-01

DISTILLATE RATE 4.760

UNSTEADY - STATE PROFILE

STAGE	TEMPERATURE	VAPOR RATE	LIQUID RATE	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE
1	238.7	0.0000E+00	19.04	0.6000	0.6000	-348.3	760.0
2	240.0	23.80	18.68	0.2000	0.2000	0.0000E+00	760.0
3	244.0	23.44	17.59	0.2000	0.2000	0.0000E+00	760.0
4	258.0	22.35	14.25	0.2000	0.2000	0.0000E+00	760.0
5	319.8	19.01	11.51	0.2000	0.2000	0.0000E+00	760.0
6	407.3	16.27	11.89	0.2000	0.2000	0.0000E+00	760.0
7	429.1	16.65	0.0000E+00	15.65	15.65	359.8	760.0

TOTAL TIME, HOURS 2.492
 CUMULATIVE TIME, HOURS 2.492
 CUT TIME, HOURS 2.478
 TIME STEP, HOURS 0.3738E-01

OVERHEAD TEMPERATURE 436.3
 AT 760 MM HG 436.5
 K - 12 436.5

INSTANTANEOUS DISTILLATE DRAWOFF PER HOUR

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.7282E-10	0.1530E-08	0.1311E-08	0.2008E-09	0.1570E-09	0.2289E-09
2	TOLUENE	0.8391E-07	0.1763E-05	0.7732E-05	0.1184E-05	0.1068E-05	0.1557E-05
3	o-NT	2.704	56.81	370.8	56.81	38.15	55.64
4	m-NT	0.2248	4.723	30.83	4.723	3.185	4.644
5	p-NT	1.831	38.47	251.1	38.47	27.24	39.72
6	DNT	0.1788E-05	0.3714E-04	0.3220E-03	0.4932E-04	0.2919E-04	0.4257E-04
	TOTAL	4.760	100.0	652.8	100.0	68.57	100.0

CUT DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.1859E-02	0.1576E-01	0.3346E-01	0.2143E-02	0.4007E-02	0.2406E-02
2	TOLUENE	1.251	10.60	115.2	7.381	15.92	9.556
3	o-NT	7.769	65.86	1065.	68.25	109.6	65.81
4	m-NT	0.3478	2.949	47.70	3.055	4.927	2.958
5	p-NT	2.426	20.57	332.8	21.32	36.09	21.67
6	DNT	0.1503E-05	0.1275E-04	0.2738E-03	0.1754E-04	0.2483E-04	0.1491E-04
	TOTAL	11.80	100.0	1561.	100.0	166.5	100.0

CUMULATIVE DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.2000E-02	0.1686E-01	0.3600E-01	0.2297E-02	0.4311E-02	0.2576E-02
2	TOLUENE	1.316	11.09	121.3	7.737	16.75	10.01
3	o-NT	7.769	65.50	1065.	67.98	109.6	65.49
4	m-NT	0.3478	2.932	47.70	3.043	4.927	2.944
5	p-NT	2.426	20.46	332.8	21.23	36.09	21.56
6	DNT	0.1505E-05	0.1269E-04	0.2742E-03	0.1749E-04	0.2486E-04	0.1485E-04
	TOTAL	11.86	100.0	1567.	100.0	167.4	100.0

TOTAL DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.2000E-02	0.1686E-01	0.3600E-01	0.2297E-02	0.4311E-02	0.2576E-02
2	TOLUENE	1.316	11.09	121.3	7.737	16.75	10.01
3	o-NT	7.769	65.50	1065.	67.98	109.6	65.49
4	m-NT	0.3478	2.932	47.70	3.043	4.927	2.944
5	p-NT	2.426	20.46	332.8	21.23	36.09	21.56
6	DNT	0.1505E-05	0.1269E-04	0.2742E-03	0.1749E-04	0.2486E-04	0.1485E-04
	TOTAL	11.86	100.0	1567.	100.0	167.4	100.0

NUMBER OF STEPS	355
NUMBER OF FUNCTION CALLS	563
NUMBER OF JACOBIAN CALLS	52

TIME, HOURS 2.492

DISTILLATE RATE 4.760

UNSTEADY - STATE PROFILE

STAGE	TEMPERATURE	VAPOR RATE	LIQUID RATE	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE
1	434.3	0.0000E+00	19.04	0.6000	0.6000	-494.8	760.0
2	436.3	23.80	18.95	0.2000	0.2000	0.0000E+00	760.0
3	438.1	23.71	18.87	0.2000	0.2000	0.0000E+00	760.0
4	439.6	23.63	18.81	0.2000	0.2000	0.0000E+00	760.0
5	441.0	23.57	18.75	0.2000	0.2000	0.0000E+00	760.0
6	442.2	23.51	18.70	0.2000	0.2000	0.0000E+00	760.0
7	443.4	23.46	0.0000E+00	3.853	3.853	494.9	760.0

TOTAL TIME, HOURS 3.124
 CUMULATIVE TIME, HOURS 3.124
 CUT TIME, HOURS 0.6323
 TIME STEP, HOURS 0.8672E-02

OVERHEAD TEMPERATURE 444.4
 AT 760 MM HG 444.7
 K - 12 444.7

INSTANTANEOUS DISTILLATE DRAWOFF PER HOUR

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.5119E-12	0.1075E-10	0.9215E-11	0.1412E-11	0.1104E-11	0.1587E-11
2	TOLUENE	0.6452E-09	0.1356E-07	0.5945E-07	0.9107E-08	0.8212E-08	0.1181E-07
3	o-NT	1.364	28.66	187.1	28.66	19.25	27.67
4	m-NT	0.2842	5.970	38.97	5.970	4.026	5.788
5	p-NT	3.112	65.37	426.7	65.37	46.28	66.54
6	DNT	0.8528E-05	0.1792E-03	0.1553E-02	0.2379E-03	0.1408E-03	0.2025E-03
TOTAL		4.760	100.0	652.8	100.0	69.56	100.0

CUT DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.9240E-11	0.3070E-09	0.1663E-09	0.4029E-10	0.1992E-10	0.4565E-10
2	TOLUENE	0.1084E-07	0.3801E-06	0.9985E-06	0.2419E-06	0.1379E-06	0.3161E-06
3	o-NT	1.339	44.47	183.6	44.47	18.89	43.29
4	m-NT	0.1625	5.399	22.29	5.399	2.302	5.277
5	p-NT	1.509	50.13	206.9	50.13	22.44	51.44
6	DNT	0.1692E-05	0.5621E-04	0.3081E-03	0.7465E-04	0.2794E-04	0.6403E-04
TOTAL		3.010	100.0	412.7	100.0	43.63	100.0

CUMULATIVE DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.2000E-02	0.1345E-01	0.3600E-01	0.1818E-02	0.4311E-02	0.2043E-02
2	TOLUENE	1.316	8.849	121.3	6.124	16.75	7.937
3	o-NT	9.108	61.24	1249.	63.08	128.5	60.90
4	m-NT	0.5103	3.432	69.98	3.535	7.230	3.426
5	p-NT	3.935	26.46	539.7	27.26	58.53	27.74
6	DNT	0.3197E-05	0.2150E-04	0.5823E-03	0.2941E-04	0.5279E-04	0.2502E-04
TOTAL		14.87	100.0	1980.	100.0	211.0	100.0

TOTAL DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.2000E-02	0.1345E-01	0.3600E-01	0.1818E-02	0.4311E-02	0.2043E-02
2	TOLUENE	1.316	8.849	121.3	6.124	16.75	7.937
3	o-NT	9.108	61.24	1249.	63.08	128.5	60.90
4	m-NT	0.5103	3.432	69.98	3.535	7.230	3.426
5	p-NT	3.935	26.46	539.7	27.26	58.53	27.74
6	DNT	0.3197E-05	0.2150E-04	0.5823E-03	0.2941E-04	0.5279E-04	0.2502E-04
TOTAL		14.87	100.0	1980.	100.0	211.0	100.0

NUMBER OF STEPS	414
NUMBER OF FUNCTION CALLS	680
NUMBER OF JACOBIAN CALLS	67

TIME, HOURS 3.124

DISTILLATE RATE 4.760

UNSTEADY - STATE PROFILE

STAGE	TEMPERATURE	VAPOR RATE	LIQUID RATE	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE
1	442.4	0.0000E+00	19.04	0.6000	0.6000	-503.2	760.0
2	444.4	23.80	18.97	0.2000	0.2000	0.0000E+00	760.0
3	446.0	23.73	18.91	0.2000	0.2000	0.0000E+00	760.0
4	447.2	23.67	18.87	0.2000	0.2000	0.0000E+00	760.0
5	448.2	23.63	18.84	0.2000	0.2000	0.0000E+00	760.0
6	448.9	23.60	18.80	0.2000	0.2000	0.0000E+00	760.0
7	449.8	23.56	0.0000E+00	0.8430	0.8430	503.2	760.0

(LAPSED CPU TIME = 22.88 SEC ENTRY COUNT = 3)

F E E D C H A R G E (REMAINING IN STILL)

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	WATER	0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00	0.0000E+00
2	TOLUENE	0.8379E-10	0.3430E-08	0.7720E-08	0.2304E-08	0.1066E-08	0.2965E-08
3	o-NI	0.3785	15.49	51.90	15.49	5.340	14.85
4	m-NI	0.1327	5.432	18.20	5.430	1.880	5.228
5	p-NI	1.930	79.00	264.7	78.97	28.71	79.83
6	DNI	0.1997E-02	0.8174E-01	0.3637	0.1085	0.3297E-01	0.9170E-01
	TOTAL	2.443	100.0	335.1	100.0	35.96	100.0

(LAPPED CPU TIME = 26.05 SEC ENTRY COUNT = 4)

BATCH TERMINATING

Appendix: C

Input and Output for the second column

COMPONENTS									
COMPONENT	10-NT		431.6	137.14	9.72				
COMPONENT	2m-NT		451.4	137.14	9.68				
COMPONENT	3p-NT		460.4	137.14	9.22				
COMPONENT	4DNT		572.0	182.14	11.03				
TEMP	104.0	176.0	248.0	320.0	392.0	464.0	536.0	608.0	
VP	1 0.3505	4.3187	29.43	130.90	431.9	1141.32	2556.2	5052.	
VP	2 0.2054	2.78	20.22	95.17	327.1	892.13	2048.	4127.	
VP	3 0.1926	2.549	18.306	85.466	292.29	794.98	1822.	3668.	
VP	4 0.0017	0.050	0.672	5.123	25.88	96.077	282.04	690.8	
HV	1 21.09	23.26	25.42	27.59	29.75	31.91	34.09	36.24	
HV	2 22.27	24.44	26.60	28.77	30.93	33.09	35.26	37.42	
HV	3 22.39	24.56	26.72	28.88	31.05	33.21	35.37	37.54	
HV	4 33.25	35.41	37.56	39.72	41.88	44.03	46.18	48.34	
HL	1 0.808	2.974	5.137	7.300	9.467	11.630	13.79	15.96	
HL	2 0.808	2.974	5.137	7.300	9.467	11.630	13.79	15.96	
HL	3 0.808	2.974	5.137	7.300	9.467	11.630	13.79	15.96	
HL	4 0.808	2.974	5.137	7.300	9.467	11.630	13.79	15.96	
VM	1 20.22	20.72	21.32	22.04	22.94	24.09	25.61	27.71	
VM	2 22.63	23.17	23.81	24.60	25.57	26.81	28.44	30.69	
VM	3 23.31	23.87	24.51	25.30	26.27	27.49	29.07	31.23	
VM	4 35.22	35.82	36.81	37.37	38.37	39.58	41.07	42.95	
CHARGE	1 15.996								
COMP	1 9.486								
COMP	2 0.643								
COMP	3 5.865								
COMP	4 0.002								
STAGES	14								
HOLDDUTYEM	0.05	0.01	0.0	0.7					
PRESDFRRDR	5.0	0.0	0.0	10.0	1.5332				
CUTTEMPS	186.	199.2	205.	0.	0.				
CONVERGENCE	0.001	50.0	15	0	1				

(LAPSED CPU TIME - 0.00 SEC ENTRY COUNT - 0)

C O M P O N E N T P R O P E R T I E S

NO	NAME	NBP	MOLE WT	DENSITY
1	o-NT	431.6	137.1	9.720
2	m-NT	451.4	137.1	9.680
3	p-NT	460.4	137.1	9.220
4	DNT	572.0	182.1	11.03

VAPOR PRESSURE DATA

1	o-NT			
	TEMP	EXP	CALC	%DEV
	104.0	0.3505	0.3763	7.372
	176.0	4.319	3.761	-12.91
	248.0	29.43	27.75	-5.723
	320.0	130.9	138.6	5.874
	392.0	431.9	484.0	12.07
	464.0	1141.	1255.	9.999
	536.0	2556.	2567.	0.4140
	608.0	5052.	4352.	-13.86

2	m-NT			
	TEMP	EXP	CALC	%DEV
	104.0	0.2054	0.2204	7.323
	176.0	2.780	2.421	-12.93
	248.0	20.22	19.13	-5.410
	320.0	95.17	100.6	5.728
	392.0	327.1	365.9	11.86
	464.0	892.1	980.0	9.847
	536.0	2048.	2056.	0.4126
	608.0	4127.	3562.	-13.68

3	p-NT			
	TEMP	EXP	CALC	%DEV
	104.0	0.1926	0.2066	7.274
	176.0	2.549	2.222	-12.84
	248.0	18.31	17.32	-5.400
	320.0	85.47	90.33	5.691
	392.0	292.3	326.8	11.80
	464.0	795.0	872.8	9.788
	536.0	1822.	1829.	0.4056
	608.0	3668.	3169.	-13.61

4	DNT			
	TEMP	EXP	CALC	%DEV
	104.0	0.1700E-02	0.1816E-02	6.808
	176.0	0.5000E-01	0.4394E-01	-12.12
	248.0	0.6720	0.6379	-5.076
	320.0	5.123	5.405	5.509
	392.0	25.88	28.74	11.03
	464.0	96.08	104.7	8.931
	536.0	282.0	282.6	0.2046
	608.0	690.8	603.7	-12.61

VAPOR PRESSURE DATA

1 o-NT				
TEMP	EXP	CALC	%DEV	
104.0	0.3505	0.3783	7.372	
176.0	4.319	3.761	-12.91	
248.0	29.43	27.75	-5.723	
320.0	130.9	138.6	5.874	
392.0	431.9	484.0	12.07	
464.0	1141.	1255.	9.999	
536.0	2556.	2567.	0.4140	
608.0	5052.	4352.	-13.86	

2 m-NT				
TEMP	EXP	CALC	%DEV	
104.0	0.2054	0.2204	7.323	
176.0	2.780	2.421	-12.93	
248.0	20.22	19.13	-5.410	
320.0	95.17	100.6	5.728	
392.0	327.1	365.9	11.86	
464.0	892.1	980.0	9.847	
536.0	2048.	2056.	0.4126	
608.0	4127.	3562.	-13.68	

3 p-NT				
TEMP	EXP	CALC	%DEV	
104.0	0.1926	0.2066	7.274	
176.0	2.549	2.222	-12.84	
248.0	18.31	17.32	-5.400	
320.0	85.47	90.33	5.691	
392.0	292.3	326.8	11.80	
464.0	795.0	872.8	9.788	
536.0	1822.	1829.	0.4036	
608.0	3688.	3169.	-13.61	

4 DNT				
TEMP	EXP	CALC	%DEV	
104.0	0.1700E-02	0.1816E-02	6.806	
176.0	0.5000E-01	0.4394E-01	-12.12	
248.0	0.6720	0.6379	-5.076	
320.0	5.123	5.405	5.509	
392.0	25.88	28.74	11.03	
464.0	96.08	104.7	8.931	
536.0	282.0	282.6	0.2046	
608.0	690.8	603.7	-12.61	

VAPOR ENTHALPY DATA

1	o-NT			
	TEMP	EXP	CALC	%DEV
	104.0	21.09	21.05	-0.1805
	176.0	23.26	23.28	0.7393E-01
	248.0	25.42	25.46	0.1403
	320.0	27.59	27.61	0.5493E-01
	392.0	29.75	29.74	-0.2201E-01
	464.0	31.91	31.89	-0.6780E-01
	536.0	34.09	34.06	-0.9479E-01
	608.0	36.24	36.27	0.8064E-01
2	m-NT			
	TEMP	EXP	CALC	%DEV
	104.0	22.27	22.22	-0.2181
	176.0	24.44	24.46	0.9522E-01
	248.0	26.60	26.64	0.1690
	320.0	28.77	28.79	0.6749E-01
	392.0	30.93	30.92	-0.3380E-01
	464.0	33.09	33.06	-0.9595E-01
	536.0	35.26	35.23	-0.8949E-01
	608.0	37.42	37.45	0.8829E-01
3	p-NT			
	TEMP	EXP	CALC	%DEV
	104.0	22.39	22.34	-0.2191
	176.0	24.56	24.58	0.9361E-01
	248.0	26.72	26.76	0.1634
	320.0	28.88	28.91	0.9195E-01
	392.0	31.05	31.04	-0.4762E-01
	464.0	33.21	33.17	-0.1107
	536.0	35.37	35.34	-0.7307E-01
	608.0	37.54	37.57	0.8414E-01
4	DNT			
	TEMP	EXP	CALC	%DEV
	104.0	33.25	33.09	-0.4664
	176.0	35.41	35.49	0.2198
	248.0	37.56	37.70	0.3626
	320.0	39.72	39.79	0.1776
	392.0	41.88	41.84	-0.9198E-01
	464.0	44.03	43.92	-0.2509
	536.0	46.18	46.10	-0.1836
	608.0	48.34	48.44	0.2051

LIQUID ENTHALPY DATA

1	o-NT			
	TEMP	EXP	CALC	%DEV
	104.0	0.8080	0.9626	19.13
	176.0	2.974	2.894	-2.700
	248.0	5.137	5.006	-2.540
	320.0	7.300	7.231	-0.9408
	392.0	9.467	9.499	0.3331
	464.0	11.63	11.74	0.9332
	536.0	13.79	13.88	0.6647
	608.0	15.96	15.86	-0.6370

2	m-NT			
	TEMP	EXP	CALC	%DEV
	104.0	0.8080	0.9626	19.13
	176.0	2.974	2.894	-2.700
	248.0	5.137	5.006	-2.540
	320.0	7.300	7.231	-0.9408
	392.0	9.467	9.499	0.3331
	464.0	11.63	11.74	0.9332
	536.0	13.79	13.88	0.6647
	608.0	15.96	15.86	-0.6370

3	p-NT			
	TEMP	EXP	CALC	%DEV
	104.0	0.8080	0.9626	19.13
	176.0	2.974	2.894	-2.700
	248.0	5.137	5.006	-2.540
	320.0	7.300	7.231	-0.9408
	392.0	9.467	9.499	0.3331
	464.0	11.63	11.74	0.9332
	536.0	13.79	13.88	0.6647
	608.0	15.96	15.86	-0.6370

4	DNT			
	TEMP	EXP	CALC	%DEV
	104.0	0.8080	0.9626	19.13
	176.0	2.974	2.894	-2.700
	248.0	5.137	5.006	-2.540
	320.0	7.300	7.231	-0.9408
	392.0	9.467	9.499	0.3331
	464.0	11.63	11.74	0.9332
	536.0	13.79	13.88	0.6647
	608.0	15.96	15.86	-0.6370

MOLAR VOLUME DATA

1	o-NT			
	TEMP	EXP	CALC	%DEV
	104.0	20.22	20.14	-0.4041
	176.0	20.72	20.79	0.3194
	248.0	21.32	21.38	0.2976
	320.0	22.04	22.05	0.3522E-01
	392.0	22.94	22.90	-0.1886
	464.0	24.09	24.05	-0.1742
	536.0	25.61	25.62	0.3630E-01
	608.0	27.71	27.73	0.6546E-01

2	m-NT			
	TEMP	EXP	CALC	%DEV
	104.0	22.63	22.53	-0.4435
	176.0	23.17	23.24	0.3228
	248.0	23.81	23.90	0.3576
	320.0	24.60	24.61	0.4262E-01
	392.0	25.57	25.52	-0.1933
	464.0	26.81	26.76	-0.2043
	536.0	28.44	28.44	0.1473E-01
	608.0	30.69	30.72	0.8881E-01

3	p-NT			
	TEMP	EXP	CALC	%DEV
	104.0	23.31	23.20	-0.4774
	176.0	23.87	23.94	0.3075
	248.0	24.51	24.61	0.4030
	320.0	25.30	25.32	0.9531E-01
	392.0	26.27	26.22	-0.1956
	464.0	27.49	27.42	-0.2490
	536.0	29.07	29.06	-0.2716E-01
	608.0	31.23	31.27	0.1266

4	DNT			
	TEMP	EXP	CALC	%DEV
	104.0	35.22	35.01	-0.6052
	176.0	35.82	36.03	0.5753
	248.0	36.81	36.81	0.2920E-02
	320.0	37.37	37.53	0.4257
	392.0	38.37	38.35	-0.5901E-01
	464.0	39.58	39.43	-0.3710
	536.0	41.07	40.95	-0.2830
	608.0	42.95	43.08	0.2944

VAPOR PRESSURE COEFFICIENTS

1	o-NT	-0.47888E-02	31082.	-0.30116E+08	0.69259E-10
2	m-NT	-0.47305E-02	30963.	-0.30215E+08	0.69236E-10
3	p-NT	-0.47027E-02	30697.	-0.30040E+08	0.68983E-10
4	DNT	-0.43852E-02	30460.	-0.31977E+08	0.72171E-10

VAPOR ENTHALPY COEFFICIENTS

1	o-NT	-0.13173E-02	0.45912E-01	-0.19670E-04	0.79481E-08
2	m-NT	-0.16365E-02	0.50441E-01	-0.25308E-04	0.10229E-07
3	p-NT	-0.16832E-02	0.50945E-01	-0.25994E-04	0.10527E-07
4	DNT	-0.51662E-02	0.92612E-01	-0.77881E-04	0.31505E-07

LIQUID ENTHALPY COEFFICIENTS

1	o-NT	0.51447E-02	-0.31719E-01	0.76809E-04	-0.31090E-07
2	m-NT	0.51447E-02	-0.31719E-01	0.76809E-04	-0.31090E-07
3	p-NT	0.51447E-02	-0.31719E-01	0.76809E-04	-0.31090E-07
4	DNT	0.51447E-02	-0.31719E-01	0.76809E-04	-0.31090E-07

MOLAR VOLUME COEFFICIENTS

1	o-NT	1.0000	0.00000E+00	0.00000E+00	0.00000E-00
2	m-NT	1.0000	0.00000E+00	0.00000E+00	0.00000E-00
3	p-NT	1.0000	0.00000E+00	0.00000E+00	0.00000E-00
4	DNT	1.0000	0.00000E+00	0.00000E+00	0.00000E-00

F E E D C H A R G E

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	9.486	59.30	1301.	59.30	133.8	58.14
2	m-NT	0.6430	4.020	88.18	4.020	9.110	3.957
3	p-NT	5.865	36.67	804.3	36.66	87.24	37.89
4	DNT	0.2000E-02	0.1250E-01	0.3643	0.1661E-01	0.3303E-01	0.1435E-01
TOTAL		16.00	100.0	2194.	100.0	230.2	100.0

(LAPSED CPU TIME - 0.58 SEC ENTRY COUNT - 1)

ITERATION NUMBER 0

S T E A D Y - S T A T E P R O F I L E

STAGE	DEL TEMP	TEMPERATURE	VAPOR RATE	LIQUID RATE	DEL HOLDUP	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE	SUMDX
1	0.0000E+00	185.5	0.0000E+00	0.0000E+00	0.0000E+00	0.5000E-01	0.5000E-01	0.0000E+00	5.000	0.0000E+00
2	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
3	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
4	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
5	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
6	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
7	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
8	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
9	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
10	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
11	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
12	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
13	0.0000E+00	197.7	0.0000E+00	0.0000E+00	0.0000E+00	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.0000E+00
14	0.0000E+00	191.5	0.0000E+00	0.0000E+00	0.0000E+00	15.83	0.0000E+00	0.0000E+00	5.000	0.0000E+00

SCALE CONV ICONV
0.0000E+00 0.0000E+00 0

ITERATION NUMBER 5

S T E A D Y - S T A T E P R O F I L E

STAGE	DEL TEMP	TEMPERATURE	VAPOR RATE	LIQUID RATE	DEL HOLDUP	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE	SUMDX
1	-0.1666E-06	185.6	0.0000E+00	16.87	-0.7305E-18	0.5000E-01	0.5000E-01	-344.3	5.000	0.2798E-08
2	-0.1272E-06	185.6	16.87	16.86	-0.1160E-18	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.4419E-08
3	-0.2792E-07	185.7	16.86	16.86	0.7912E-19	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.1396E-07
4	0.1037E-06	185.8	16.86	16.85	0.2347E-18	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.8307E-08
5	0.3655E-07	185.9	16.85	16.84	0.1517E-18	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.3291E-08
6	0.8992E-08	186.0	16.84	16.83	-0.1031E-18	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.9360E-09
7	-0.6053E-10	186.2	16.83	16.81	-0.5865E-19	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.1582E-09
8	-0.9619E-09	186.5	16.81	16.79	-0.4468E-22	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.5852E-11
9	-0.3398E-09	186.8	16.79	16.76	0.2298E-18	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.1006E-10
10	-0.1091E-09	187.3	16.76	16.72	-0.1128E-18	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.1286E-10
11	-0.1101E-09	187.9	16.72	16.67	0.3036E-18	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.1604E-10
12	-0.1384E-09	188.7	16.67	16.60	0.3464E-19	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.1943E-10
13	-0.1670E-09	189.7	16.60	16.51	-0.4164E-18	0.1000E-01	0.1000E-01	0.0000E+00	5.000	0.2273E-10
14	-0.1939E-09	191.5	16.51	0.0000E+00	0.5040E-18	15.83	15.83	344.3	5.000	0.2574E-10

SCALE CONV ICONV
1.000 1.000 0

(LAPSED CPU TIME - 1.59 SEC ENTRY COUNT - 2)

TOTAL TIME, HOURS 0.3584E-04
 CUMULATIVE TIME, HOURS 0.3584E-04
 CUT TIME, HOURS 0.3584E-04
 TIME STEP, HOURS 0.3584E-04

OVERHEAD TEMPERATURE 185.6
 AT 760 MM HG 460.3
 K = 12 440.1

INSTANTANEOUS DISTILLATE DRAWOFF PER HOUR

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	1.521	99.20	208.6	99.20	21.46	99.16
2	m-NT	0.2271E-02	0.1481	0.3114	0.1481	0.3217E-01	0.1487
3	p-NT	0.1002E-01	0.6536	1.374	0.6536	0.1491	0.6888
4	DNT	0.2458E-11	0.1603E-09	0.4477E-09	0.2129E-09	0.4059E-10	0.1876E-09
TOTAL		1.533	100.0	210.3	100.0	21.64	100.0

CUT DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	0.5450E-04	99.20	0.7474E-02	99.20	0.7690E-03	99.16
2	m-NT	0.8138E-07	0.1481	0.1116E-04	0.1481	0.1153E-05	0.1487
3	p-NT	0.3592E-06	0.6537	0.4925E-04	0.6537	0.5342E-05	0.6889
4	DNT	0.2380E-13	0.4331E-07	0.4335E-11	0.5753E-07	0.3930E-12	0.5068E-07
TOTAL		0.5494E-04	100.0	0.7535E-02	100.0	0.7755E-03	100.0

CUMULATIVE DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	0.5450E-04	99.20	0.7474E-02	99.20	0.7690E-03	99.16
2	m-NT	0.8138E-07	0.1481	0.1116E-04	0.1481	0.1153E-05	0.1487
3	p-NT	0.3592E-06	0.6537	0.4925E-04	0.6537	0.5342E-05	0.6889
4	DNT	0.2380E-13	0.4331E-07	0.4335E-11	0.5753E-07	0.3930E-12	0.5068E-07
TOTAL		0.5494E-04	100.0	0.7535E-02	100.0	0.7755E-03	100.0

TOTAL DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	0.5450E-04	99.20	0.7474E-02	99.20	0.7690E-03	99.16
2	m-NT	0.8138E-07	0.1481	0.1116E-04	0.1481	0.1153E-05	0.1487
3	p-NT	0.3592E-06	0.6537	0.4925E-04	0.6537	0.5342E-05	0.6889
4	DNT	0.2380E-13	0.4331E-07	0.4335E-11	0.5753E-07	0.3930E-12	0.5068E-07
TOTAL		0.5494E-04	100.0	0.7535E-02	100.0	0.7755E-03	100.0

NUMBER OF STEPS 1
 NUMBER OF FUNCTION CALLS 4
 NUMBER OF JACOBIAN CALLS 1

TIME, HOURS 0.3584E-04

DISTILLATE RATE 1.533

UNSTEADY - STATE PROFILE

STAGE	TEMPERATURE	VAPOR RATE	LIQUID RATE	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE
1	185.6	0.0000E+00	15.33	0.5000E-01	0.5000E-01	-344.3	5.000
2	185.6	16.87	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
3	185.7	16.86	15.32	0.1000E-01	0.1000E-01	0.0000E+00	5.000
4	185.8	16.86	15.32	0.1000E-01	0.1000E-01	0.0000E+00	5.000
5	185.9	16.85	15.31	0.1000E-01	0.1000E-01	0.0000E+00	5.000
6	186.0	16.84	15.29	0.1000E-01	0.1000E-01	0.0000E+00	5.000
7	186.2	16.83	15.28	0.1000E-01	0.1000E-01	0.0000E+00	5.000
8	186.5	16.81	15.25	0.1000E-01	0.1000E-01	0.0000E+00	5.000
9	186.8	16.79	15.22	0.1000E-01	0.1000E-01	0.0000E+00	5.000
10	187.3	16.76	15.18	0.1000E-01	0.1000E-01	0.0000E+00	5.000
11	187.9	16.72	15.13	0.1000E-01	0.1000E-01	0.0000E+00	5.000
12	188.7	16.67	15.07	0.1000E-01	0.1000E-01	0.0000E+00	5.000
13	189.7	16.60	14.98	0.1000E-01	0.1000E-01	0.0000E+00	5.000
14	191.5	16.51	0.0000E+00	15.83	15.83	344.3	5.000

TOTAL TIME, HOURS 2.770
 CUMULATIVE TIME, HOURS 2.770
 CUT TIME, HOURS 2.770
 TIME STEP, HOURS 0.1456E-01

OVERHEAD TEMPERATURE 186.0
 AT 760 MM HG 460.8
 K = 12 440.5

INSTANTANEOUS DISTILLATE DRAWOFF PER HOUR

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	1.491	97.23	204.4	97.23	21.03	97.11
2	m-NT	0.7883E-02	0.5011	1.054	0.5011	0.1089	0.5026
3	p-NT	0.3473E-01	2.265	4.763	2.265	0.5166	2.385
4	DNT	0.3922E-11	0.2558E-09	0.7143E-09	0.3397E-09	0.6476E-10	0.2990E-09
TOTAL		1.533	100.0	210.3	100.0	21.66	100.0

CUT DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	4.163	98.01	570.9	98.01	58.73	97.92
2	m-NT	0.1535E-01	0.3615	2.105	0.3615	0.2175	0.3626
3	p-NT	0.6913E-01	1.628	9.480	1.628	1.028	1.714
4	DNT	-0.2781E-07	-0.6548E-06	-0.5066E-05	-0.8697E-06	-0.4593E-06	-0.7657E-06
TOTAL		4.247	100.0	582.5	100.0	59.98	100.0

CUMULATIVE DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	4.163	98.01	570.9	98.01	58.73	97.92
2	m-NT	0.1535E-01	0.3615	2.105	0.3615	0.2175	0.3626
3	p-NT	0.6913E-01	1.628	9.480	1.628	1.028	1.714
4	DNT	-0.2781E-07	-0.6548E-06	-0.5066E-05	-0.8697E-06	-0.4593E-06	-0.7657E-06
TOTAL		4.247	100.0	582.5	100.0	59.98	100.0

TOTAL DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	4.163	98.01	570.9	98.01	58.73	97.92
2	m-NT	0.1535E-01	0.3615	2.105	0.3615	0.2175	0.3626
3	p-NT	0.6913E-01	1.628	9.480	1.628	1.028	1.714
4	DNT	-0.2781E-07	-0.6548E-06	-0.5066E-05	-0.8697E-06	-0.4593E-06	-0.7657E-06
TOTAL		4.247	100.0	582.5	100.0	59.98	100.0

NUMBER OF STEPS 498
 NUMBER OF FUNCTION CALLS 909
 NUMBER OF JACOBIAN CALLS 209

TIME. HOURS 2.770

DISTILLATE RATE 1.533

U N S T E A D Y - S T A T E P R O F I L E

STAGE	TEMPERATURE	VAPOR RATE	LIQUID RATE	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE
1	185.9	0.0000E+00	15.33	0.5000E-01	0.5000E-01	-344.8	5.000
2	186.0	16.87	15.32	0.1000E-01	0.1000E-01	0.0000E+00	5.000
3	186.2	16.85	15.31	0.1000E-01	0.1000E-01	0.0000E+00	5.000
4	186.4	16.84	15.29	0.1000E-01	0.1000E-01	0.0000E+00	5.000
5	186.7	16.82	15.26	0.1000E-01	0.1000E-01	0.0000E+00	5.000
6	187.1	16.80	15.23	0.1000E-01	0.1000E-01	0.0000E+00	5.000
7	187.6	16.77	15.20	0.1000E-01	0.1000E-01	0.0000E+00	5.000
8	188.1	16.73	15.15	0.1000E-01	0.1000E-01	0.0000E+00	5.000
9	188.8	16.69	15.11	0.1000E-01	0.1000E-01	0.0000E+00	5.000
10	189.6	16.64	15.05	0.1000E-01	0.1000E-01	0.0000E+00	5.000
11	190.5	16.58	14.99	0.1000E-01	0.1000E-01	0.0000E+00	5.000
12	191.4	16.53	14.93	0.1000E-01	0.1000E-01	0.0000E+00	5.000
13	192.4	16.47	14.86	0.1000E-01	0.1000E-01	0.0000E+00	5.000
14	193.9	16.40	0.0000E+00	11.58	11.58	344.8	5.000

TOTAL TIME, HOURS 6.955
 CUMULATIVE TIME, HOURS 6.955
 CUT TIME, HOURS 4.185
 TIME STEP, HOURS 0.9802E-02

OVERHEAD TEMPERATURE 199.2
 AT 760 MM HG 475.6
 K = 12 457.3

INSTANTANEOUS DISTILLATE DRAWOFF PER HOUR

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	0.3184	20.77	43.67	20.77	4.493	20.02
2	m-NT	0.1709	11.15	23.44	11.15	2.421	10.79
3	p-NT	1.044	68.08	143.2	68.08	15.53	69.19
4	DNT	0.1587E-10	0.1035E-08	0.2890E-08	0.1374E-08	0.2620E-09	0.1168E-08
TOTAL		1.533	100.0	210.3	100.0	22.44	100.0

CUT DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	5.177	80.69	709.9	80.69	73.04	79.98
2	m-NT	0.1986	3.096	27.24	3.096	2.814	3.082
3	p-NT	1.040	16.22	142.7	16.22	15.47	16.94
4	DNT	-0.3182E-07	-0.4960E-06	-0.5796E-05	-0.6588E-06	-0.5255E-06	-0.5754E-06
TOTAL		6.416	100.0	879.9	100.0	91.33	100.0

CUMULATIVE DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	9.340	87.59	1281.	87.59	131.8	87.09
2	m-NT	0.2140	2.007	29.35	2.007	3.032	2.004
3	p-NT	1.109	10.40	152.1	10.40	16.50	10.91
4	DNT	-0.5964E-07	-0.5593E-06	-0.1086E-04	-0.7428E-06	-0.9848E-06	-0.6509E-06
TOTAL		10.66	100.0	1462.	100.0	151.3	100.0

TOTAL DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	9.340	87.59	1281.	87.59	131.8	87.09
2	m-NT	0.2140	2.007	29.35	2.007	3.032	2.004
3	p-NT	1.109	10.40	152.1	10.40	16.50	10.91
4	DNT	-0.5964E-07	-0.5593E-06	-0.1086E-04	-0.7428E-06	-0.9848E-06	-0.6509E-06
TOTAL		10.66	100.0	1462.	100.0	151.3	100.0

NUMBER OF STEPS 1286
 NUMBER OF FUNCTION CALLS 2370
 NUMBER OF JACOBIAN CALLS 564

TIME, HOURS 6.955

DISTILLATE RATE 1.533

UNSTEADY - STATE PROFILE

STAGE	TEMPERATURE	VAPOR RATE	LIQUID RATE	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE
1	198.1	0.0000E+00	15.33	0.5000E-01	0.5000E-01	-362.3	5.000
2	199.2	16.87	15.28	0.1000E-01	0.1000E-01	0.0000E+00	5.000
3	200.0	16.82	15.25	0.1000E-01	0.1000E-01	0.0000E+00	5.000
4	200.6	16.78	15.22	0.1000E-01	0.1000E-01	0.0000E+00	5.000
5	201.1	16.76	15.21	0.1000E-01	0.1000E-01	0.0000E+00	5.000
6	201.4	16.74	15.20	0.1000E-01	0.1000E-01	0.0000E+00	5.000
7	201.6	16.73	15.19	0.1000E-01	0.1000E-01	0.0000E+00	5.000
8	201.7	16.72	15.18	0.1000E-01	0.1000E-01	0.0000E+00	5.000
9	201.8	16.72	15.18	0.1000E-01	0.1000E-01	0.0000E+00	5.000
10	201.9	16.71	15.18	0.1000E-01	0.1000E-01	0.0000E+00	5.000
11	201.9	16.71	15.18	0.1000E-01	0.1000E-01	0.0000E+00	5.000
12	202.0	16.71	15.18	0.1000E-01	0.1000E-01	0.0000E+00	5.000
13	202.0	16.71	15.17	0.1000E-01	0.1000E-01	0.0000E+00	5.000
14	202.0	16.71	0.0000E+00	5.163	5.163	362.3	5.000

TOTAL TIME, HOURS 9.805
 CUMULATIVE TIME, HOURS 9.805
 CUT TIME, HOURS 2.850
 TIME STEP, HOURS 0.4317E-02

OVERHEAD TEMPERATURE 202.7
 AT 760 MM HG 479.2
 K - 12 461.7

INSTANTANEOUS DISTILLATE DRAWOFF PER HOUR

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	0.1880E-05	0.1226E-03	0.2578E-03	0.1226E-03	0.2652E-04	0.1165E-03
2	m-NT	0.6742E-01	4.398	9.246	4.398	0.9552	4.197
3	p-NT	1.466	95.60	201.0	95.60	21.80	95.80
4	DNT	0.1100E-09	0.7174E-08	0.2003E-07	0.9528E-08	0.1816E-08	0.7981E-08
TOTAL		1.533	100.0	210.3	100.0	22.76	100.0

CUT DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	0.1464	3.350	20.07	3.350	2.065	3.197
2	m-NT	0.4040	9.245	55.40	9.245	5.723	8.859
3	p-NT	3.819	87.41	523.8	87.41	56.81	87.94
4	DNT	-0.5508E-07	-0.1260E-05	-0.1003E-04	-0.1674E-05	-0.9095E-06	-0.1408E-05
TOTAL		4.370	100.0	599.3	100.0	64.60	100.0

CUMULATIVE DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	9.486	63.10	1301.	63.10	133.8	61.99
2	m-NT	0.6180	4.111	84.75	4.111	8.755	4.055
3	p-NT	4.929	32.79	675.9	32.79	73.31	33.96
4	DNT	-0.1147E-06	-0.7631E-06	-0.2089E-04	-0.1013E-05	-0.1894E-05	-0.8774E-06
TOTAL		15.03	100.0	2062.	100.0	215.9	100.0

TOTAL DISTILLATE DRAWOFF

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	9.486	63.10	1301.	63.10	133.8	61.99
2	m-NT	0.6180	4.111	84.75	4.111	8.755	4.055
3	p-NT	4.929	32.79	675.9	32.79	73.31	33.96
4	DNT	-0.1147E-06	-0.7631E-06	-0.2089E-04	-0.1013E-05	-0.1894E-05	-0.8774E-06
TOTAL		15.03	100.0	2062.	100.0	215.9	100.0

NUMBER OF STEPS 2353
 NUMBER OF FUNCTION CALLS 4378
 NUMBER OF JACOBIAN CALLS 1022

TIME, HOURS 9.805

DISTILLATE RATE 1.533

UNSTEADY - STATE PROFILE

STAGE	TEMPERATURE	VAPOR RATE	LIQUID RATE	MOL HOLDUP	VOL HOLDUP	HEAT DUTY	PRESSURE
1	202.7	0.0000E+00	15.33	0.5000E-01	0.5000E-01	-366.5	5.000
2	202.7	16.87	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
3	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
4	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
5	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
6	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
7	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
8	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
9	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
10	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
11	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
12	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
13	202.7	16.86	15.33	0.1000E-01	0.1000E-01	0.0000E+00	5.000
14	202.8	16.86	0.0000E+00	0.7932	0.7932	366.5	5.000

(LAPSED CPU TIME = 179.21 SEC

ENTRY COUNT = 3)

F E E D C H A R G E (REMAINING IN STILL)

NO	NAME	LBMOLES	MOLE %	POUNDS	WEIGHT %	GALLONS	VOLUME %
1	o-NT	0.1474E-06	0.1530E-04	0.2021E-04	0.1529E-04	0.2080E-05	0.1453E-04
2	m-NT	0.2504E-01	2.600	3.434	2.598	0.3548	2.479
3	p-NT	0.9362	97.19	128.4	97.13	13.92	97.29
4	DNT	0.2000E-02	0.2076	0.3643	0.2756	0.3303E-01	0.2308
TOTAL		0.9632	100.0	132.2	100.0	14.31	100.0

(LAPSED CPU TIME = 180.76 SEC ENTRY COUNT = 4)

BATCH TERMINATING

```
$!  
$!  
$! COMMAND FILES USED TO EXECUTE THE MAIN SOURCE CODE  
$!  
$! SUBMIT NITS.COM  
$! -----  
$!  
$ SUBMIT/NOTIFY/QUEUE=MEDIUM NITS SUB.COM  
$!  
$! NITS SUB.COM  
$! -----  
$!  
$! BATCH dISTILLATION  
$! BY NITIN ...  
$! -----  
$!  
$ ASSIGN NITS.DAT FOR005  
$ ASSIGN NITS.OUT FOR006  
$!  
$ RUN NITS.EXE  
$!  
$ EXIT
```

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