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EFFECT OF GAS TEMPERATURE GRADIENTS AND
RADIANT HEAT TRANSMISSION ON KINETIC MODEL
BEHAVIOR.

New Jersey Institute of Technology, D.Eng.Sc.,
1974
Engineering, chemical

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EFFECT OF GAS TEMPERATURE GRADIENTS
AND RADIANT HEAT TRANSMISSION ON
KINETIC MODEL BEHAVIOR

by

RICHARD W. J. ROBERTSON

A DISSERTATION

PRESENTED IN PARTIAL FULFILLMENT OF

THE REQUIREMENTS FOR THE DEGREE

OF

DOCTOR OF ENGINEERING SCIENCE IN CHEMICAL ENGINEERING

AT

NEWARK COLLEGE OF ENGINEERING

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Newark, New Jersey

1974

APPROVAL OF DISSERTATION
EFFECT OF GAS TEMPERATURE GRADIENTS AND RADIANT HEAT
TRANSMISSION OF KINETIC MODEL BEHAVIOR

BY

RICHARD W. J. ROBERTSON

FOR

DEPARTMENT OF CHEMICAL ENGINEERING

NEWARK COLLEGE OF ENGINEERING

BY

FACULTY COMMITTEE

APPROVED: _____, CHAIRMAN

NEWARK, NEW JERSEY

MAY, 1974

ABSTRACT

EFFECT OF GAS TEMPERATURE GRADIENTS AND RADIANT HEAT TRANSMISSION ON KINETIC MODEL BEHAVIOR

by

Richard W. J. Robertson

Satisfactory methods to predict radiant heat transmission in enclosures containing a radiating gas at uniform temperature are available. These methods have been traditionally used in solutions of kinetic models.

Kinetic models are strongly temperature dependent with a difference of 10°K able to double the reaction rate. In the present investigation, calculation techniques which make allowance for the non-uniformity of gas temperatures in an enclosure are applied to the kinetic models. The furnace problem considers only the radiation section with the assumption that detailed knowledge of combustion and fluid flow pattern within the enclosure is available.

If the gas space in the enclosure and the bounding walls are divided into zones, a zone being taken small enough so that it may be considered isothermal, then for steady-state operation one can write an energy balance on each zone. For any specific problem, every term in these equations with the

exception of the net wall fluxes may be written as a function of unknown temperatures only; furthermore the number of equations is exactly equal to the number of unknown temperatures and wall fluxes so that a solution is possible, though exceedingly difficult due to the existing non-linearities.

The net wall fluxes are calculated by the kinetic model, the flux at any point being a function of the overall heat transfer coefficient, the extent of reaction, and the temperature of the reacting gases, each of which in turn is a complex function of reaction gas composition and velocity.

The chief problem of this investigation was one of evaluating the emission from both a gas zone and a surface zone and the radiant interchange between all zones, making due allowance for absorption along every path from one zone to another.

The primary result of this dissertation has been the application of radiant dominant heat transmissions in enclosures (which make allowances for temperature non-uniformity in gas mass) to a pyrolysis reactor. The result of this reactor-furnace hybrid model is the ability to determine optimum tube placement, furnace size, and fuel consumption, while accounting for the effect of carbon

deposition in the reactor.

The methods developed in this dissertation were instrumented on an IBM 370-15 computer. This machine made it possible to make parametric studies which predict the effect of changing furnace and reactor variables.

The high severity steam cracking furnace results in the greatest production per pound of fuel consumed. A yield of 73% represents maximum fuel economy. However, the associated problems of coke formation and high tube metal temperature must first be overcome before these yields can be realized.

Acknowledgements

The author wishes to take this opportunity to express his gratitude to all the individuals whose cooperation enabled him to produce this dissertation.

He wants to thank his advisor, Dr. E. C. Roche for his contribution of advice, exhortation, time and effort on the author's behalf.

The author's thanks are also due to the staff of the N.C.E. Computer Center.

The author includes a special thanks to his wife, Linda, for her assistance throughout the period of the writing of this dissertation and for her many hours of typing! He also wishes to thank his sons, Donald and David, for their good behavior while the thesis was being written and typed.

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Chapter ISUMMARY

An increased understanding of the basic principles underlying heat transfer processes has forced a realization of the importance of radiation as the dominant mode of heat transfer in high-temperature industrial furnaces. It is, therefore, desirable to be able to predict rates of radiant dominant heat transmission with confidence for both design and performance calculations. Methods which predict the net interchange between a radiating gas at a uniform temperature (a one gas zone furnace) with the walls forming the enclosure are available in the literature.

For many industrial furnaces, however, it is not permissible to assign a uniform temperature to the radiating gas, particularly when the distribution of heat flux within the enclosure as well as the over-all performance is desired. When endothermic fluid phase reactions take place within the process fluid of the reactor a detailed knowledge of the local temperature gradient on the tube wall becomes important in that it affects the extent of reaction. The relatively large deviation from the true temperature profile produced by assuming one zone furnace

results in solutions which, though valid, are poor in engineering application. In the present investigation, therefore, the work of applying calculational techniques for predicting radiant dominant transmission has been continued, with the specific aim of making allowance for the non-uniformity of gas temperature in a fixed reactor. It was decided to limit the scope of the project by focusing attention on the radiation section of the fired heater problem and assuming that a description of the other phenomena necessary to the formulation, namely fuel-air combustion and internal flow patterns are available for use.

If the gas space in the enclosure and the bounding walls are divided up into zones, a zone being taken small enough so that it may be considered isothermal, then for steady-state operation it is possible to write an energy balance for each zone. For a gas zone the sum of the radiant energy received from all zones in the system (both gas and surface) plus the net convection to it from adjacent gas or surface elements plus the net enthalpy flux (chemical and sensible) to it due to bulk flow must equal the radiant energy originating within the gas zone. Similarly, for a surface, the sum of the radiant energy

received from all zones (gas and surface) plus the net convection to it must equal the emission from the surface plus the net flux through the surface. Every term in these equations with the exception of the net wall fluxes may be written as a function of unknown temperatures only and the number of equations is exactly equal to the number of unknown temperatures and wall fluxes. A solution of a set of these non-linear equations, once written for each zone in the enclosure, would yield the desired distribution of temperature and energy flux throughout the system.

One problem of this investigation, therefore, was one of evaluating the emission from either a gas zone or a surface zone and the radiant interchange between any two of these zones, making due allowance for absorption along every path from one zone to another and for partial diffuse reflection of every path at every surface ad infinitum. The furnace was subdivided into a set of isothermal zones. Each zone extended the entire length of the furnace and end effects were neglected. Sets of these furnaces can be set up one next to the other to produce a three-dimensional furnace of any degree of complexity. Some error will result due to the assumption that no interaction takes place between any furnace and its neighbor.

The results produced, however, are still an improvement over most computational techniques.

A computational technique developed by Cohen (18) is able to handle zoning along the length of the reactor as well as across and vertically. His methods, however, were principally graphic, and do not lend themselves to the digital computer.

The emission rate from a gas volume of Area A is given by the following equation:

$$E_g = 4(kL) (A) \cdot \phi \cdot \sigma T_g^4 \quad (1-1)$$

where E_g is the rate of emission in energy per unit time, kL is the absorption coefficient of the gas times its path length, and ϕ is the fraction of the energy originating within the volume which leaves the boundaries of the volume. The escape factor, ϕ , is a function of kL only and has been obtained by multiple numerical integrations as described in a later Chapter.

The emission rate from a surface area of Area A is given by:

$$E_s = \epsilon_s (A) \sigma T_s^4 \quad (1-2)$$

where ϵ_s is the emissivity of the surface.

The interchange between any two zones in the system is more complex, involving not only the direct radiant flux between the two zones, but also the sum of the infinite number of reflected beams within the enclosure due to energy originating at either of the zones under consideration with due allowance for multiple attenuation. It is profitable to consider first only the direct interchange between the two zones; i.e. the interchange in a black-walled system.

The one-way radiation flux - surface to surface, surface to gas, gas to surface, and gas to gas respectively may be written as:

$$q_{ss} / (\sigma T_s^4) = ss \quad (1-3)$$

$$q_{sg} / (\sigma T_s^4) = sg \quad (1-4)$$

$$q_{gs} / (\sigma T_g^4) = gs \quad (1-5)$$

$$q_{gg} / (\sigma T_g^4) = gg \quad (1-6)$$

where the terms ss , sg , gs , and gg , designated as direct interchange factors, also termed in the literature as interchange areas due to the dimensional units. These factors may be thought of as the product of a radiation

factor f , having any of the subscript combinations indicated on the right-hand sides of equations (1-3) through (1-6) with the first subscript representing the source of the energy and the second the receiver, which represents the fraction of the energy originating in any zone in the enclosure which reaches and is absorbed by any other zone, and a radiating-ability factor, $(\text{area}) \cdot (\text{emissivity})$ for a surface zone and $4 \times (\text{volume}) \times (\text{absorption coefficient})$ for a gas zone. Values of these radiation factors have been evaluated. These factors are functions of the path length and k , where k is the absorption coefficient of the gas. It is to be noted that these factors have been evaluated assigning a uniform k to each characteristic gas, a characteristic gas being a mathematical representation of a gas, which, in conjunction with other characteristic gases predicts the properties of gases in the system. The details of this technique, involving evaluation of determinants of order equal to the number of surface zones and of volume zones in the system, are given in Chapter 3.

With all the interchange factors for the system evaluated, it is possible to return to the original energy balances and solve for the temperature and flux distribution in the "two-dimensional enclosure." It will be

recalled that the details of the fuel-air combustion, convection, and internal flow patterns are assumed known so that all terms in the energy balances have been evaluated and only temperatures or net wall fluxes appear as unknowns. Unfortunately, the set of equations contains unknown temperature in mixed first and fourth powers. For obtaining numerical solutions, these equations were linearized in T^4 by forcing the convection and enthalpy flux terms into a fourth-power law; this technique necessitates an iterative solution since the coefficients on the convection and enthalpy flux terms are now strong functions of temperature. The sets of equations are solved iteratively until the assumed values are verified.

The use of the digital computer enables a parametric study of furnace conditions and designs criterions. The results were an optimization of a pyrolysis reactor which maximizes the ratio of product to fuel consumption. The results are given in Chapter (4).

The over-all performance of the furnace (i.e., the total amount of energy transferred from the gas) as calculated by the method presented in this thesis was found to give good agreement with the performance as calculated by existing techniques in the literature. (49) The distribution

of the heat flux within the enclosure, however, was found to be very different.

The technique developed in this dissertation is capable of giving far more detailed information as to the radiant interchange within the enclosure than has been possible up to the present time. Its chief weaknesses are:

1. Finite sized zones, assumed to be isothermal, have been chosen so as to facilitate numerical solutions.
2. It has been assumed that detailed knowledge of the combustion and mixing pattern is available. This is not actually the case for most enclosures.
3. It has been assumed that no interaction takes place between furnace subsections along the reactor length.
4. The furnace is assumed to be of infinite length. This assumption can be eliminated with moderate additional complexity.

The furnace model was used in connection with a reactor model. The reactor model is able to handle large numbers of interrelated chemical reactions. The model is set up to accept any set of reactions so long as the

kinetic data of reactions and the physical properties of the components are known.

From this initial data, the heat of reaction, heat of formation and the equilibrium constants are defined as functions of temperature. These functions are later evaluated to give point conditions in the reaction fluids.

The reactor is sectioned off into increment sections. Simultaneous material, momentum, and energy balances are performed on each section.

The temperature, pressure and composition of reaction fluids at the inlet of an incremental section are known from previous calculation. The temperature of the outside of the reactor wall is supplied by the furnace model. A temperature, pressure and composition are assumed at the end of the increment. A better estimate is made by calculating the reaction rates at the two ends and averaging the result. This procedure is continued until agreement is reached between two successful estimates.

The increment of heat flow to the reactor is calculated by summing the sensible heat gain of the reaction mass and the heat of reaction of each competing reaction. This must equal the net heat flux through the walls. The

increment heat flux is then summed over the length of each reactor section.

The reactor model also calculates the coke buildup as a function of reaction rates. The reaction rates are assumed to be invariant over the time span during which the carbon is deposited. New reactor conditions are then used during each additional time span of carbon deposition. The coke's chief effect on reactor conditions is a decrease in overall reaction rate due to the following effects:

1. A decrease in the net heat flux through the wall of the reactor due to the presence of a coke layer.
2. A reduction in reactor volume and hence, reactor mean residence time.
3. A larger pressure drop throughout the reactor length necessitating a higher inlet pressure, adversely affecting equilibrium.

The reactor model results in a new temperature profile for the reactor. The new profile is then mapped into three corresponding process temperature profiles which is then transferred into the furnace model.

The furnace model and the reactor model are solved repeatedly until good agreement is reached between assumed and calculated temperature profiles. The net heat flux

through the wall is also forced to converge. The net heat flux into the reactor is solved by the relationship

$$Q = UA \Delta T \quad (1-7)$$

The overall heat transfer coefficient (U_R) used by the reactor model, is a function of the thickness of the reactor wall, the thickness, if any, of the coke layer and the inside film coefficient (H_i). H_i is in turn a function of the reaction mixture velocity, thermal conductivity and composition.

The overall heat transfer coefficient used by the furnace model (U_F) to calculate the outside wall temperature from the known temperature of the process fluid must be mapped into the tube plane. The mapping is necessary due to the pseudo two dimensional nature of the furnace model. The mapping is done through a net heat flux balance on the reactor wall. The value of U_F is thus mapped by forcing agreement between the overall heat flux calculated by the furnace model and the heat flux calculated by the reactor model. U_F does not correspond with U_R calculated by the reactor model.

Since both the reactor and furnace models were set up in a computer program it was possible to make a parametric

study on the complete system. Thus the effect of tube placement, oil fired rate, furnace dimensions, reactor length, reactor composition can be correlated to design a furnace of optimum yield with minimum fuel consumption. One of the major contributions of this thesis is to correlate these quantities to predict optimum furnace and reactor design.

CHAPTER II

1. The Furnace Model

A. Introduction

This analysis depends on the development of two unrelated, but interdependent models. These two models are then coupled together and form an effective method to predict optimum furnace design.

One model, the furnace model, will be discussed in Chapter II-1. The other model, the kinetic model, will be discussed in Chapter II-2. The coupling model is then explained in Chapter II-3.

An increased understanding of the basic principles underlying heat transfer processes has forced a realization of the importance of thermal radiation as the dominant mode of heat transfer in high temperature industrial furnaces. High installation and maintenance costs as well as the competitive market of today call for the design of furnaces or heaters which will perform efficiently and economically. Furthermore, because of variations in process conditions one would like to be able to predict the effect of such variations on furnace operation. To these ends, therefore, considerable effort has been extended to put the calculation and prediction of radiant heat interchange on a firm engineering basis.

The model makes use of work done by Cohen (18) and Roche (63) which allows for the non-uniformity of gas temperatures in an enclosure.

B. Fundamental Laws Governing Surface and Gas Radiation

1. Radiation from Solid Surfaces

All solids, at any temperature other than absolute zero, emit and absorb radiant energy. Both the magnitude of the emission and its quality (i.e., its spectral distribution) depend primarily on the temperature of the material, but also, to a lesser extent, on the particular nature of its surface. The rate of emission from a perfect radiator (defined as a black body) is given by the familiar Stefan-Boltzmann Law: the emitted flux (energy per unit time per unit area) is proportional to the fourth power of the absolute temperature. The spectral distribution of black-body radiation is a function of temperature only and is given by Planck's Law. Any real surface always emits less than black-body radiation, and if its spectral distribution is the same as the Planck distribution, the body is said to be gray. The ratio of the energy emitted by any gray body at a fixed temperature to black-body emission at the same temperature is termed the

emissivity; by the very nature of its definition, numerical values of emissivity must always lie between zero and unity.

For a further review of surface emissivities and radiation from solids Jakob⁽³⁶⁾, McAdams⁽⁴⁹⁾ and Hottel and Sarofim⁽³³⁾ or other standard references on heat transfer may be consulted.

2. Radiation from Gases

In addition to surfaces, certain gases absorb and emit energy when heated. Of greatest interest to the furnace designer are water vapor and carbon dioxide, the primary products of combustion. Data on the radiating and absorbing characteristics exist for both carbon dioxide and water vapor. (32), (35), (49) Somewhat more limited data are available for carbon monoxide, sulfur dioxide and ammonia. (16), (26), (59), (88)

Gas radiation differs from surface radiation in one important respect. Gas radiation is by no means gray, rather these gases exhibit very strong emission and absorption bands in certain spectral regions and are practically transparent in others. This non-grayness of real gases leads to enormous complications in furnace design calculations if it is to be allowed for rigorously. Fortunately, approximation techniques exist for handling the real-gas case; they will be discussed in later sections of this

chapter.

C. Techniques Available for Predicting Radiant Heat Interchange in Furnace Enclosures

The calculation of the radiant interchange in a furnace enclosure may be resolved into three different, though not completely separable, problems:

1. Allowance for the geometry of the system.
2. Emission of radiation from the gas and its absorption and/or reflection at the various surfaces.
3. Absorption by the gas of radiation emitted by or reflected at the different surfaces.

A little thought will show that a completely rigorous calculation of the interchange in an enclosure would be exceedingly complex, and, in fact, a perfectly rigorous solution appears to be almost impossible to attain. One of the most important reasons for this complexity is the fact that in a radiating system, what goes on at any point is influenced by every other point in the system. That is, one must write an integral equation to express the heat transfer rates everywhere, instead of a differential expression expressing the local rate dependent only upon local conditions, as is possible for convective and conductive heat transfer. For this reason certain simplifications have been

made which have enormously decreased the complexity of the calculations but which nevertheless yield answers for certain cases of sufficient accuracy for engineering use. A brief review, without any derivations or elaborate explanations, of the methods presently available for calculating radiant heat transfer appears below.

A. Interchange in Gray Enclosures Containing Non-Absorbing Media

The radiant interchange in a gray furnace enclosure, of any degree of complexity so long as it does not contain any absorbing gas, is calculable by the method presented by Hottel⁽⁴⁶⁾. The net transfer by radiation between any two surfaces such as A_1 and A_2 is given as:

$$q_{A_1 \rightarrow A_2} = A_1 F_{12} \sigma (T_1^4 - T_2^4) \quad (2-1)$$

(A portion of the enclosure may be grouped together as a surface, e.g., A_1 , when it has a substantially uniform temperature and when all portions of it have substantially the same "view" of the remainder of the enclosure.) The term $A_1 F_{12}$ is dependent upon the geometry of the entire system as well as the emissivities (equal to the absorptivities for a gray system) of all surfaces, but it is not a function of the temperatures of any surfaces so long as their emissivities are themselves independent of temperature.

B. Interchange in Gray Enclosures Containing a Gray Isothermal Gas Mass

If now, the enclosure is filled with a gray gas of uniform temperature, the interchange between the gas and any surface or between any two surfaces separated by gas, may be calculated by a slight modification of the above method. Gas-surface interchange is defined by the following equation:

$$q_{G_1 \rightarrow A_1} = A_1 \mathcal{F}_{1G} \sigma (T_G^4 - T_1^4) \quad (2-2)$$

The surface-to-surface heat transfer is exactly the same as given in equation (2-1) with the modification, however, that the interchange factor $A_1 \mathcal{F}_{12}$ has been adjusted so as to allow for the fact that on each pass from surface A_1 to surface A_2 , directly or via any surface forming the enclosure, a portion of the energy is absorbed by the gas.

The interchange factors for this case, as before, are dependent upon the geometry of the entire system as well as the emissivities of all surfaces, and in addition are dependent upon the gas emissivity. For opaque surfaces, the emissivity is equal to the absorptivity and the complement of the reflectivity: that is $\epsilon = \alpha = (1 - \rho)$. They are not functions of any temperature in the system,

so long as the emissivities of the system, both gas and surface, are independent of temperature.

D. Allowance for a Real Gas

Non-luminous gas radiation, particularly radiation from carbon dioxide and water vapor, which are of greatest importance to the furnace designer, is not gray. The transmissivity of such a gas is not only a function of the gas properties, but is also very markedly influenced by the spectral distribution of the energy which is being absorbed. For example, the absorption of very high-temperature radiation by carbon dioxide, with its strong absorption bands in the long wavelength region would be very low because the source of radiation would be predominantly of short wavelength; but the absorption of lower temperature gray radiation, with a consequent larger fraction of the incident energy in the same spectral region as the gas absorption bands, would be much higher. In the treatment of the gray gas system mentioned in subsection 2, it was assumed that the absorptivity of the gas for surface radiation was independent of the quality of that incident radiation, and for this reason the gray-gas formulation is in error if applied directly to a real system.

Hottel and Sarofim⁽³³⁾ have shown it is possible to

approximate very closely real-gas radiation, without losing the mechanics of the gray-gas formulation. Since for the gray gas the transmittance of a gas beam of length x with a gas pressure p_G is given by:

$$\tau_x = e^{-k' p_G x} \quad (2-3)$$

where k' is the absorption coefficient of the gas and is independent of wavelengths, the emissivity and absorptivity are equal and may be expressed as:

$$\epsilon_x = a_x = 1 - \tau_x = 1 - e^{-k' p_G x} \quad (2-4)$$

It is, of course, possible to fit the $\tau_x = f(p_G x)$ curve for a real gas to any degree of precision by a series of exponential type terms such as:

$$\epsilon_x = a e^{-k'_a p_G x} + b e^{-k'_b p_G x} + c e^{-k'_c p_G x} \dots (2-5)$$

This equation indicates that the transmissivity of a real gas may be thought of as a weighted sum of a number of gray-gas transmissivities, each applicable over a different spectral region. The sum of the weighting factors, a, b, c, \dots must be unity, since the emissivity of a gray gas having no thickness ($x=0$) must be unity. The interchange in an enclosure, therefore, can be thought of as equivalent to the sum of the interchanges of a number of gray-gas systems each weighted in proportion to that fraction of the spectral region over which it acts. It is

to be noted that the gray gas in each region has a different absorption coefficient and hence a different emissivity.

In the limit, as one considers an infinite number of spectral regions each obeying the gray-gas formulation, the answer of course, must be exact. For engineering calculations, however, this type of approach would be extraordinarily complex if one had to consider a large number of zones. Numerical analysis of typical problems has indicated, fortunately, that if the $e^{-k'X}$ curve is to be fitted anew for each numerical problem, it is in general sufficient to consider only two spectral regions, a and b, where the fraction "a" consists of a gray gas with a finite absorption coefficient k_a and the fraction "b" (the complement of "a") consists of a gas with a zero absorption coefficient (i.e., a clear gas which neither absorbs nor emits). Again, space limitations prohibit a more adequate discussion of this problem and, for details, the reader is referred to Hottel⁽⁴⁹⁾ and Hottel and Sarofim.⁽³³⁾

E. Limitations on the Computational Techniques

Recapitulating, it has been shown that one is able to handle satisfactorily an enclosure made up of any number of gray surfaces and filled with a real isothermal gas mass. In actual practice it may be difficult to obtain a numerical

solution for a very complicated case; however, the principles governing the interchange in such enclosures and the technique for obtaining solutions have been formulated and are generally available.

perhaps the most serious limitation to the calculational methods outlined above is the fact that the gas temperature and composition have been assumed to be uniform throughout the enclosure. Obviously, this assumption is never completely true for any industrial furnace, and in a good many cases it may be very seriously in error. If the furnace chamber is roughly cubical in shape, and if turbulence and mixing are present to a high degree, then the gas temperature will be nearly uniform and equal to the temperature of the exit gas so that the above methods apply directly. Even if these conditions apply only approximately, that is, if the gas temperature and composition at the inlet and outlet of the furnace are not too different from each other, then some mean of the two temperatures ought to give a reasonably accurate answer. Unfortunately, few industrial furnaces fall in this category.

If, on the other hands, the furnace is very long compared to the dimensions of the cross-section normal to the direction of gas flow, and if combustion is rapid at the furnace entrance, the temperature of the gas falls continu-

ously as it passes through the furnace. In the limiting case of a furnace with length infinitely great relative to the transverse dimensions, allowance for this drop in gas temperature can be made by calculating local heat transfer rates at several points and graphically integrating along the furnace length. Long furnaces have been handled adequately by this technique, which in effect ignores radiant flux in the direction of gas flow, as long as there is a definitive negative temperature gradient from the bottom of the combustion chamber to the top. This tedious process, which applies only to one very special type of furnace, has been performed for a wide range of furnace variables, and a simplified method of predicting a mean gas temperature to give the answer in a single step is available. (17) (49)

In this thesis a furnace model of the infinite length relative to the transverse dimension is considered. However, the model incorporates radiant flux consideration in both transverse directions. Radiant flux along the infinite axis is also calculated, but ignores end conditions along the infinite axis. This makes it possible to section the model along the long axis and consider each section independently of the others. Some error is introduced

in that the model can not show any net heat flux between adjacent sections despite the existence of temperature gradients between sections. The errors thus generated are minimal due to the relatively small difference of temperature and the low value of the heat transfer due to eddy diffusion.

While one is able to handle the two limiting cases of furnaces mentioned above quite simply, it is rather unfortunate that most industrial furnaces fall into a category somewhere in between them. At the present time, only the method developed by Cohen⁽¹⁸⁾ allows one to take into account the fact that in actual furnaces, very substantial gas temperature gradients exist, both in the direction of gas flow and transverse to it. The method, however, is very tedious, and does not easily lend itself to computer calculations due to the graphical techniques or methodology employed.

Simply to illustrate the magnitude of the temperature gradients, a few numerical examples will be given.

1. Data obtained by Smith⁽⁷³⁾ and reported by Cohen⁽¹⁸⁾ on a scaled-down model of a steel-reheating furnace, using premixed air and gaseous fuel, have indicated that a drop of about 300-400 Centigrade degrees between the

gas temperature near the refractory roof and the cool floor sink, a total distance of about one foot in his equipment, is not at all unusual.

2. The large-scale furnace (about 6 feet by 6 feet by 20 feet) used by the International Flame Radiation Research Committee, and fired with either gaseous or liquid fuel in a burner jet, has shown temperature drops between the hot combustion zone near the center of the flame and the refractory wall of as much as 600 Centigrade degrees in a distance of about three feet. (37)

These figures have been quoted merely for illustrative purposes. However, when one considers that gas emission is roughly proportional to the second or third power of absolute gas temperature, it seems likely that the consequences of these large gradients might be extremely important.

It is possible for one to handle rigorously the simplest possible case of allowing for temperature non-uniformity in the gas. This method has been presented by Hottel⁽⁴⁹⁾ for the case of energy reception by a black wall adjacent to a gas mass having a known one-dimensional temperature gradient.

F. Methods Used to Solve Furnace Model

There are, of course, two fundamentally different approaches that one might use in attacking this problem. The first is completely theoretical and involves the development of calculational techniques to enable the prediction of the effect of temperature gradients on radiant heat interchange. Since basically the processes occurring within a furnace are determined solely by the fundamental laws of heat transfer, fluid flow, and combustion kinetics, the problem reduces itself to one of expressing the interrelationships of the various mechanisms interacting with one another in such a way that it becomes possible to obtain a numerical solution. The second technique would be to determine experimentally heat transfer rates under a wide variety of conditions with the hope of obtaining some sort of correlation which would enable one to predict the operation of furnaces other than those studied.

The first method of attack was felt to be the more profitable one in this case, and accordingly a purely calculational approach was used. The advent of the high speed digital computer has allowed implementation of this approach to handle far more complex systems than heretofore have been attempted. The speed of computation also allows

for solution of many furnace models with the ultimate objective of being able to simplify the result into some generalized empirical relationship. The solution has been set up in the most general terms possible, that is, in such a form that if one had specific knowledge of combustion and mixing, he would be able to incorporate such information directly into the recommended technique.

In all fairness to the reader, it must be pointed out that the combination of processes occurring in a furnace is extremely complex. The extent to which the method developed in this dissertation might be used by an engineer is dependent solely upon the amount of time which he is justified in spending on any particular problem. For one wishing only an approximate answer, it would be uneconomical to go through the costly and involved processes described later. On the other hand, if it is really important that one has the right answer, the author sees no alternative to following the methods recommended in this dissertation or their equivalent. Their use to prove the validity of engineering shortcuts is an interesting application, but not the subject of this dissertation. The use of the computer in handling the model will make it feasible for an investigator to find such simplified approaches.

2. The Reactor Model

A. Introduction

To perform an optimization one needs some sort of plant description to form an objective function such as production rate or profit margin which must be optimized in terms of the independent variables.

Historically, plant data were used in deriving mathematical models by regression analysis. Some plants had even been deliberately disturbed in order to obtain enough data to determine the independent variables into which the plant was being fitted.

This method has many drawbacks such as noise in the plant data causing unreliability in the reading and a limited range of conditions under which the data is collected. Conditions outside of the range of those specifically studied must be calculated by the relatively unreliable method of extrapolation.

An alternative method is to simulate the plant based on the physical and chemical conditions. This simulated model can then be perturbed to determine the effect on the function to be optimized.

In order to describe plant conditions as thoroughly and accurately as possible, a model should consider the entire plant, including recycle streams, separators and peripheral equipment, as well as the reactor. This is not

the intent of this study.

It was decided that the optimization of fuel consumption would be most meaningful and would give optimum conditions close to the optimum based on an overall profit objective function.

The purpose of this dissertation is to develop an algorithm which successfully predicts the behavior of a reactor-furnace. In order to be able to verify the results a reaction system was chosen which has been extensively reported in the literature. The reaction system thus decided upon was the cracking of ethane to form ethylene.

B. Pyrolysis of Ethane Process

Ethylene is a basic raw material used in the manufacture of polyethylene and polyethylene copolymers and as an intermediate in the synthesis of many organic compounds, with plant sizes ranging between 50 to 250 million pounds per year. The pyrolysis of ethane is very profitable because the raw material, ethane, would have a minimum value as a fuel gas. Ethylene is produced by "cracking" of the feed stock in fired reactors at temperatures up to 1250°K.

Almost all larger petrochemical facilities have several

furnaces which operate with different feed stocks, notably various proportions of ethane, propane, butane and 'naphtha'. The reactor pressure and temperature profiles and feed rates are also varied. The products from these different streams are generally combined into one stream after "quenching" to terminate the production of unwanted byproducts.

The reactor model is able to handle each set of feed stocks independently and perform separate optimizations for each furnace. In this study, the cases of pure ethane, propane, and combinations, each mixed with steam, were considered. The steam provides a chemical mechanism to minimize the rate of coke deposition. The model is also capable of optimizing the production of acetylene by increasing the residence time.

C. Carbon Deposition

Carbon is one of the byproducts of the pyrolysis reactions. Carbon is deposited on the wall of the reactor and results in a continuously decreasing reactor radius. This results in larger pressure drops occurring within the reactor tube. Eventually the pressure drop reaches a value which is too high to keep the system operating, and the reactor must be shut down for cleaning. Another effect of the carbon deposition is to reduce the overall heat

heat transfer coefficient making the fired heater less efficient.

An increase in reactor outlet temperature increases both the yield of ethylene and the rate of carbon deposition, hence causing an increase in the frequency of reactor shutdown for cleaning. As fuel consumption in the furnace increases, so does the reactor yield. The function of reactor yield divided by fuel consumption plotted against fuel consumption goes through a maximum which represents an optimum operating condition for any given set of furnace and reactor parameters, i.e.

$$\text{Yield/Fuel Consumption} = f(\text{reactor parameters, furnace parameters})/\text{fuel consumption} \quad (2-4)$$

The reactor-furnace model developed in this dissertation is able to determine this ideal operating point for most existing furnaces. The model also lends itself to the determination of the optimum design of most new furnace-reactor systems.

D. Chemistry of Pyrolysis

The chief products from thermal cracking furnaces-reactors vary from feed to feed. For the feed considered in this study, the chief products were ethane, ethylene,

acetylene, methane, propane, propene, hydrogen and coke. Small amounts of aromatics were also formed. As an approximation these were defined to have the properties of C4's and C6's alpha olefins.

The eight equations considered in this study are: ⁽⁷¹⁾

	Order Forward	Order Reverse
$C_2H_6 \rightleftharpoons C_2H_4 + H_2$	1	1-1 (2-5)
$C_2H_6 \rightleftharpoons CH_4 + \frac{1}{2}C_2H_4$	1	1-1 (2-6)
$C_2H_4 \rightleftharpoons C_2H_2 + H_2$	1	1-1 (2-7)
$C_2H_2 \rightleftharpoons 2C + H_2$	2	1-1 (2-8)
$2C_2H_2 \rightleftharpoons C_4H_4$ (i.e.) C4's	1	1 (2-9)
$C + H_2O \rightleftharpoons CO + H_2$	1-0	1-1 (2-10)
$C_3H_8 \rightleftharpoons C_3H_6 + H_2$	1	1-1 (2-11)
$C_3H_8 \rightleftharpoons C_3H_4 + CH_4$	1	1-1 (2-12)

A detailed explanation of the kinetic reactor model can be found in the M.S. Thesis of Robertson. ⁽⁶²⁾ It was necessary to modify Robertson's model in order to incorporate the calculation of the net heat flux through the wall of the reactor when the details of the pointwise temperature

distribution are known.

Further detail may be found in the following ^{discussions} references:

1. Use of computers in pyrolysis - see Reference Numbers (3, 9, 12, 23, 25, 44, 45, 53, 60, 62, 65, 68, 69, 70, 86, 95)
2. Chemistry of Pyrolysis (2, 38)
3. Reaction Rate (80, 81)
4. Equilibrium Rate (40)
5. Heat of Reaction (77)
6. Heat Transfer (13, 76)
7. Carbon Deposition (10, 14, 20, 28, 55, 57, 82)
8. Furnace Construction (15, 37, 48, 67, 74, 78)
9. Supersonic Oxidative Pyrolysis (90)
10. Sub-sonic Oxidative Pyrolysis (89)
11. Pyrolysis of Heavy Feed Stock (79, 86)

3. The Mapping Function

The development of the kinetic model and the furnace model are independent of each other. In order to make the two models interdependent it was necessary to develop a third model which could communicate between the first two models. This third or mapping model is the author's specific contribution in this dissertation. It was utilized to investigate the product yield, fuel consumption geometry and tube placement of the reactor-furnace. The firing patterns produced by different tips on the burners can also be studied with the idea of designing a firing tip which would yield an optimum firing pattern.

The mapping model has to take into account a number of inconsistencies which include:

1. The furnace model assumes that there is no variation in temperatures along its infinite axes. The kinetic model, however, shows a continuous increase in temperature as the reaction mass flows through the reactor tube, which has vertical as well as longitudinal variations in geometry.
2. The furnace model "views" the furnace wall as a continuous semi-porous plane, a portion of which

is a heat sink to the ambient (through the insulating walls of the furnace). The kinetic model considers itself a discrete section of tubing with a radial uniform outside surface temperature.

3. The furnace model was picked to have a height of 28' feet. The reactor model was 400 feet long. This made it necessary to fold the reactor tube into a series of "u" bends which run up and down along the wall of the furnace.
4. The furnace model considered itself infinitely long with no end effects due to the presence of walls at both ends of the furnace. The reactor model was clearly finite in length.

Methods used to handle each of these inconsistencies will be discussed later in this section.

In order to make the models compatible, both temperature and net heat flux profiles through the reactor wall had to be in agreement. As each of these quantities is calculated independently by both models, a trial and error type of solution was developed.

The temperature profile of the outer reactor wall was assumed. With this assumed profile, the kinetic calculations

were completed. The kinetic calculations included a reactor fluid temperature profile and a net heat flux. The furnace calculations were then performed and yielded a new outer reactor wall temperature profile and a net heat flux to the reaction fluids.

This new outer wall temperature profile was then used to repeat the kinetic calculations. This process was then repeated until the maximum difference between old and new reactor fluid temperatures was less than 1.25°K and the net heat fluxes calculated by the two models were within 2% of each other.

A. Temperature Variations Along Reactor Length

The temperature of the reaction fluids increases continuously as the reactions take place. The net heat flux into the reactor results in two net effects:

1. An increase in the temperature of the reaction mass due to a sensible heat gain.
2. A change in reactor mass composition due to chemical change. (The principal reaction being endothermic).

In the initial stage of reaction the mixture has an insufficient temperature for any appreciable reaction to take place, hence, most of the heat flux results in a sensible heat gain.

In a second portion of the reactor the reaction mass is at reaction temperature with large quantities of unreacted species present. A majority of the heat flux goes to supplying the reaction mass with the necessary heat of reaction, with some sensible heat gain still occurring.

A final portion of the reactor consists of an ever declining portion of the net heat flux contributing to the heat of reaction;

It becomes possible to take advantage of these tendencies by splitting the furnace into three zones. In the first zone there is considerable increase in the temperature of the reaction mass. This in turn results in rapidly changing wall flux. However, since in this section of the reactor little reaction takes place, an averaging technique of the the temperature flux along the infinite axis for each isothermal wall zone will not seriously affect the kinetic model.

In the second zone the kinetic model predicts large extent of reaction but only mild increasing temperatures. Again an averaging technique for each isothermal wall zone along the infinite axis gives temperature distributions which can be used by the kinetic model, since only relatively small temperature differences exist.

In the third zone both relatively extensive amounts of reaction and fairly large reactor fluid temperature changes take place. By minimizing the size of this section, the averaging technique is again applicable.

The reader should note that considerable flue gas temperature gradients exist between each isothermal zone in adjoining sections. This would suggest that a subdivision of each section into two or more sub-sections would result in still more precise results. However, the additional computational time required by the computer for such an undertaking would be prohibitively large.

B. Mapping the "Plane Into A Reactor Tube

The furnace model views the wall of the furnace as a continuous plane with isotherms running along the horizontal and discrete temperatures of radiation running along the vertical. The plane is porous in that it "views" the furnace wall and reactor tubing simultaneously, differentiating between them as the ratio of their respective areas. The furnace model does not distinguish individual sections of tube and wall, rather "considers" the two as the wall of the furnace.

The kinetic model "uses" the outer skin temperature of the reactor to calculate the net heat flux to the reaction mixture. In a furnace tube there would be some radial

temperature distribution since the side of the tube facing the wall of the furnace would have a lower temperature than the side facing the bulk of the hot flue gases. The net temperature difference is not too great since the major resistance to heat flow is the result of the inside film heat transfer coefficient. (The resistance to heat flow through the coke layer would also be large, but this quantity is a variable, depending on the length of time the coke has been forming and the particular location in the reactor tube). The ratio of heat resistance in the tube metal to that caused by the inside film coefficient is an order of magnitude greater than 10 to 1, as was calculated by Robertson. (62)

In order to make some allowance for this effect, the net heat transfer coefficient calculated from reaction mixture to outer tube wall temperature used by the furnace was adjusted in such a fashion that the net heat flux as calculated from the furnace equation was equal to the net heat flux as calculated from the reactor equations.

The net heat transfer coefficient found by the reaction equation was calculated from considerations of physical properties of the reactor tube, the thickness of the coke layer and the chemical composition and physical properties

of the reaction mass.(62)

C. Placement of Reactor Tube

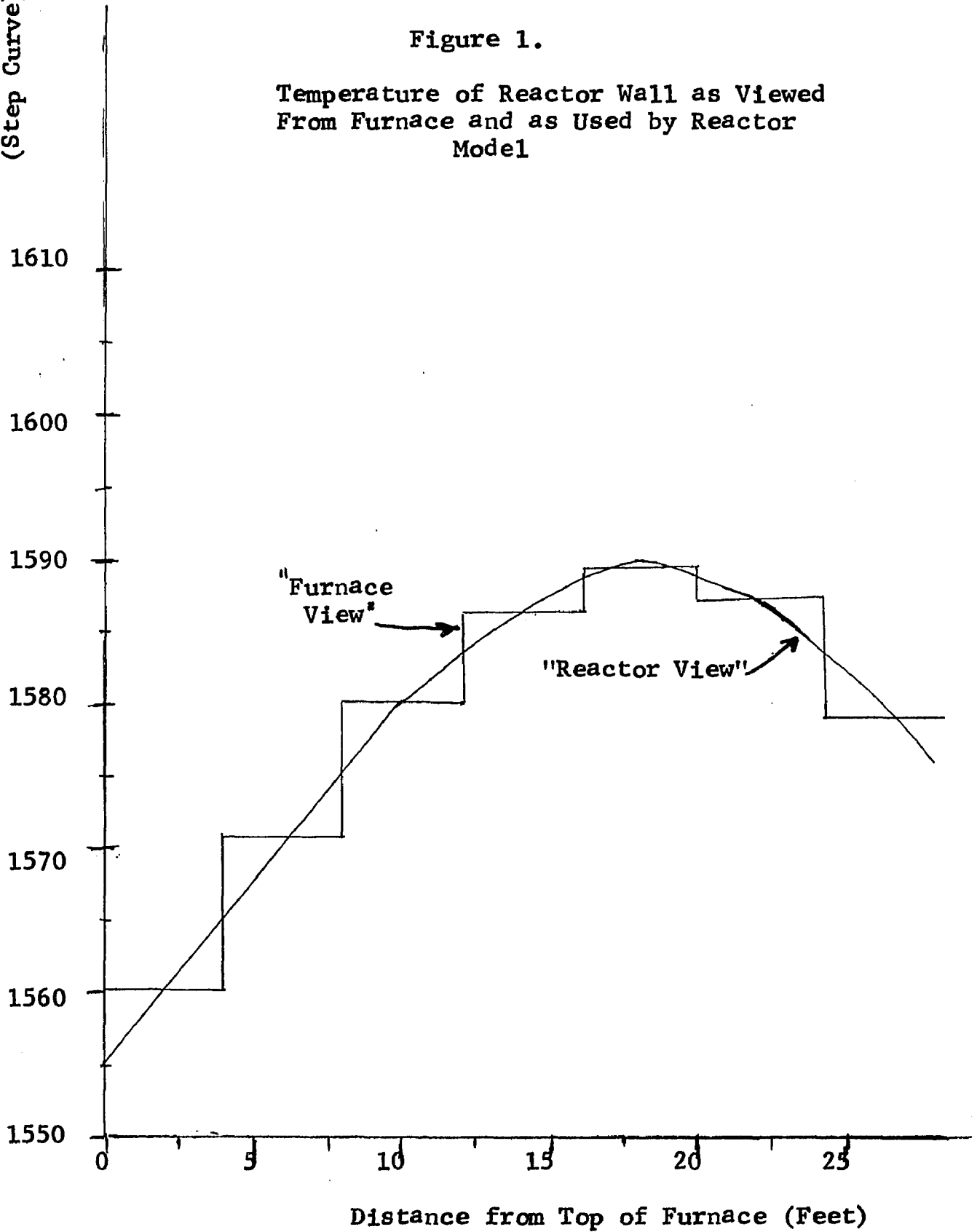
The reactor being 400 feet of continuous tubing which is hung in the vertical direction (to avoid gradual bending of the tube near its center if the tube were placed in a horizontal position due to the excessive heat required for pyrolysis) would not fit into a furnace 20 feet in height. It was therefore placed in the furnace in a series of "U" bends running first from top to bottom and then bottom to top. A total of 14 such bends was required to accommodate the entire reactor length. A total of 14 such reactors can be placed in the 40 foot length of the furnace, seven on each side of the flame wall. The "U" bends provide mechanical support while allowing for thermal expansion.

Within the series of 14 "U" bends, the furnace was further subdivided into three distinct reactor zones discussed earlier in this Chapter. The mapping model had to be able to distinguish in which furnace zone the corresponding reactor segment lay. It is also necessary to know whether the tube was running up the furnace or down. The temperature profiles used by the furnace and the reactor are illustrated in Figure 1.

Temperature of Outer Reactor Wall of (Continuous Curve) Temperature of Furnace Wall of (Step Curve)

Figure 1.

Temperature of Reactor Wall as Viewed From Furnace and as Used by Reactor Model



The smooth curve shown in Figure 1 was calculated by fitting a fourth power polynomial of $T - f(Z) = a + bZ + cZ^2 + dZ^3 + eZ^4$ using the midpoint of each discrete furnace zone temperature as calculated by the furnace model. These discrete temperature zones were adjusted at the end of each furnace calculation and smooth curves were refitted for each of the three furnace zones recalculated.

Figures 2 and 3 show the actual location of the tubing in the furnace as well as the placement of the isothermal zones. The bridge wall extends on half the distance along the top of the furnace, the remaining half being the opening into the convection section and the stack.

D. End Effects

The furnace model studied in this thesis was considered to be infinitely long and end effects were ignored. As the dominant mode of heat transfer is radiation, an estimate of the distance necessary to completely absorb all incident radiation was made for the gray gases consisting of the flow gas. It was determined that for beam lengths of 65 feet, less than one part per million of the original radiation was still present in the beam. The clear gas contribution was somewhat higher.

The furnace model was further complicated by assuming

subdivisions along the reactor length (See Figure 2). Each subdivision assumes that its unique properties exist unchanged through neighbor subdivisions in the horizontal plane. In the furnace model studied, which was 70 feet long, there occurred 21 subdivisions. There were, however, only three distinct furnace subdivisions which had to be calculated.

Figure 2
Front and Side View of a "Zoned" Furnace with 3 Subsections

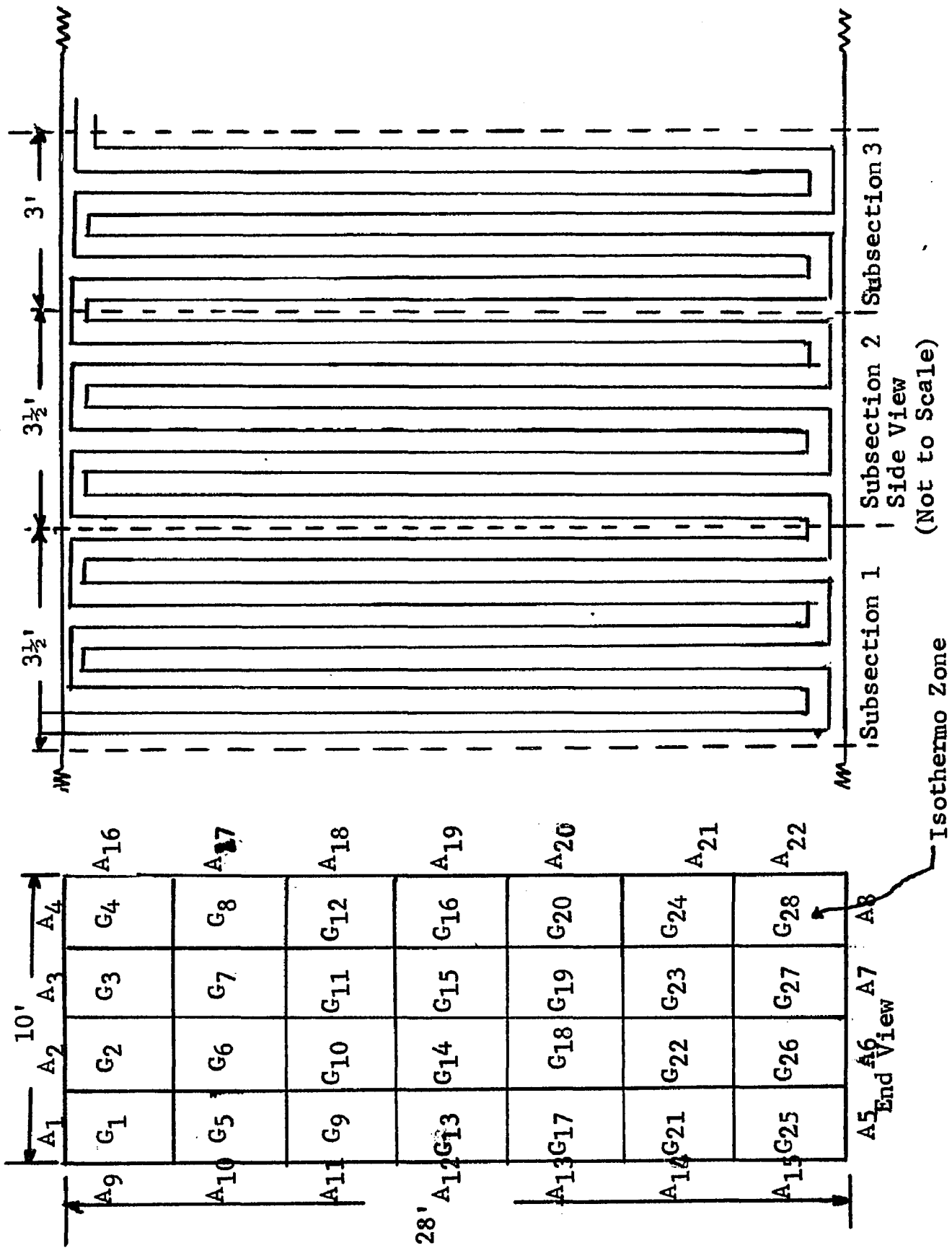
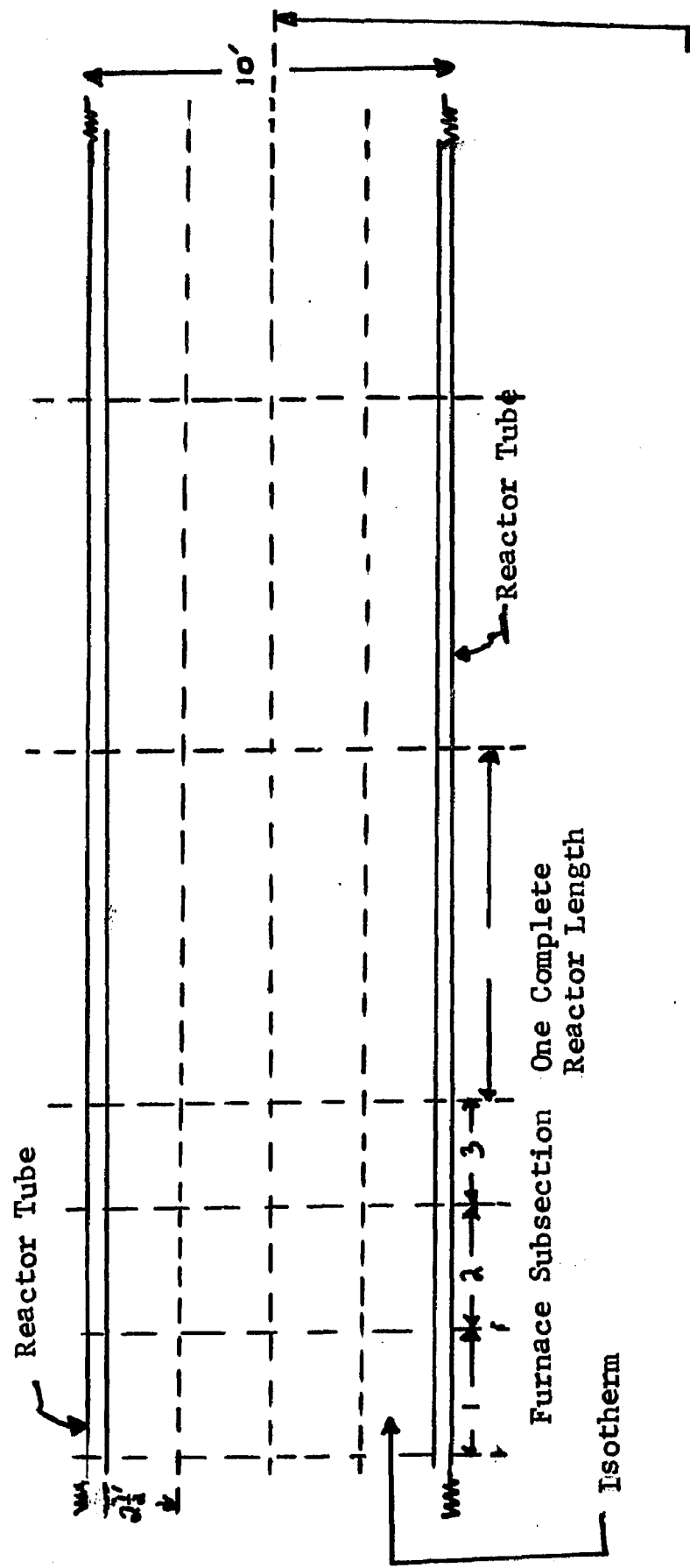


Figure 3
Top View of Furnace-Reactor Showing Isotherm
Zone Placement



Burners Located Along
this Plane (Bottom Fired)

Chapter III

Procedures Used in Solution of the Zoned Furnace-Reactor

Model

1. The Furnace Model

This Chapter will discuss in detail the mechanism used in the solution of each of the problems handled in this study. The furnace model will be discussed in Chapter III-1, the kinetic model in Chapter III-2, and the mapping model in Chapter III-3. In addition, Chapter III-4 will show the computational procedure used in order to arrive at the solution which comprises this study. In the remainder of this dissertation, all discussion will be limited to steady-state conditions in an enclosure.

In this study the furnace was zoned into isothermal gas volumes and surfaces areas. The volumes run through the entire length of the furnace and are in fact treated as infinite in length; the height and width of each of these zones being finite. Likewise the surface areas are infinite in length and finite in width if in the horizontal plane, or in height if in the vertical plane. The model does not consider any plane or volume which is not either mutually parallel or perpendicular to the infinite axis (see Figures 2, 3, 4). These limitations should be kept in mind for all future references to surface area and gas

volumes.

The furnace was further subdivided along the infinite axis in order to make allowance for the nonuniformity along that axis. However, for the calculation, each subdivision is treated as if those conditions in that subdivision existed along the entire length of the furnace. This procedure allows the handling of each subdivision as an independent calculation, greatly reducing the complexities of the calculation procedure.

The general approach to be used consists of dividing the space enclosed and the bounding surfaces into zones, each zone being taken small enough so that it may be considered isothermal.

An energy balance may be written for each zone in the system, and when this is done it will be found that the series of equations contains only gas temperatures, surface temperatures or wall fluxes as unknowns. Furthermore, the number of unknowns will be found to equal exactly the number of equations. In principle then, one can solve either for the temperature at any given point in the system or the flux through the wall.

A. Energy Balances on the System

Consider the enclosure to be made up of isothermal volumes of space containing a gray gas, and designated as

$g_1, g_2, g_3 \dots$ and isothermal areas of bounding surface (either heat sinks or refractory) designated as $s_1, s_2, s_3 \dots$. The surface areas will coincide exactly with the gas volumes that touch them.

The conventions of naming the various surfaces and gas volumes used in this dissertation are as follows:

(Refer to Figure 2, cross section view).

1. The gas volumes are numbered from left to right, starting in the upper left hand corner and working down as each row is completed. Hence the first gas volume in the upper left hand corner would be g_1 .
2. The surface areas are numbered from left to right along the floor of the furnace. The sides of the furnace are then enumerated from top to bottom going down the right wall, then from top to bottom going down the left wall. Hence the last surface area, number 22, would be on the bottom of the right side of the vertical wall of the furnace and would be called s_{22} .

Since the temperature of the gas in any volume g (a volume defined as fixed in space) will remain unchanged once steady state has been reached, an energy balance on any volume such as g_1 may be written as follows:

Total outward radiation in all directions = through the bounding walls of volume g_1	Radiation absorbed by g_1 from all volumes both direct and by multiple reflections at the walls	Radiation absorbed by volume g_1 , from all surface elements, both direct and by multiple reflections
	+ Net energy to volume g_1 by bulk transport of the flowing gas stream	+ Net energy to volume g_1 by convection from adjacent gas volumes or surface elements

(3-1)

Rewriting in terms of symbols, where the various terms correspond directly:

$$E_{g_1} = \sum_i q_{g_i g_1} + \sum_j q_{s_j g_1} + q_{B g_1} + q_{C g_1} \quad (3-2)$$

In the above and all subsequent equations a double set of subscripts such as $g_i g_1$, g_s or ss indicates the direction of the energy transfer, the first subscript denoting the source of the energy and the second the receiver. Subscripts on the last 2 terms refer to bulk transport B or convection C, with an additional subscript to indicate which single gas or surface element is involved.

Similarly, writing an energy balance on any surface

s_1 :

Total outward radiation in all directions from surface s_1	= Radiation absorbed by s from all volumes both direct and by multiple reflections at the walls.	+ Radiation absorbed by surface s_1 from all surface elements both direct and by multiple reflections.
	+ Net energy to surface s_1 by convection from adjacent gas cubes	- Energy flux through wall s_1

(3-3)

Rewriting again in symbols:

$$E_{s_1} = \sum_i q_{g_i} s_i + \sum_j q_{s_j} s_j + q_{c_{s_1}} - q_{w_{s_1}} \quad (3-4)$$

A little consideration of equations (3-2) and (3-4) will show that all the terms with the exception of wall-flux $q_{w_{s_1}}$ may be written as functions of temperatures, the coefficients on the temperature terms being functions of the geometry, heat capacities, flow rates and emissivities (and absorptivities) of the system. If it may be assumed that these temperature coefficients can all be evaluated at some mean temperature for the system, then there will result a total of $g + s$ equations on g unknown gas temperatures and s unknown wall temperatures or wall fluxes.

It is to be noted at this point that, most unfortunately, the resulting series of simultaneous equations is

neither linear in temperature nor in any power of temperature. If one is willing to assign to the temperature coefficients mean values for the system then the radiation terms will be proportional to the fourth power of temperature while the convection and bulk flow terms are proportional to the first power of temperature. In order to simplify the final solution of the equations, it is advisable to linearize them by forcing the convection and bulk flow terms into a fourth power law. It would also be possible to force the radiant terms into the first power law. However, this alternate procedure does not reflect the radiant dominant nature of the fired heater or furnace. Using the first method means that the coefficients on these terms are very strong functions of temperature and hence of the solution to the equations, necessitating an iterative procedure in solution. Details of this technique will be presented later in this section.

B. Radiant Interchange in a Black Enclosure
Containing a Gray Gas

To simplify the problem of determining the radiant interchange factors in the most general case, it was decided to determine them first for this simple case: An enclosure containing black walls (and thus no multiple

reflections) and filled with a gray gas. In the case of a single-temperature gas zone as was described in Chapter 2, it was found possible to build up the interchange factor which allows for multiple reflections from the much simpler one of direct interchange only; a similar situation is found in the multi-gas zone cases. Furthermore, the technique for allowance for a real gas as the weighted sums of a number of gray gases also applies. For these reasons, the direct interchange factors for the gray-gas case will be evaluated first; then the method of building up solutions to the more complex situation of gray walls and a real gas will be indicated.

1. Emission from a Volume of Gas

The rate of emission of energy from an isothermal gas volume, if there were no attenuation of radiation within the volume, would be equal to the gas emissivity per unit volume multiplied by the volume and by "black body" emission at the same temperature:

$$E_g^* = \mathcal{V} \cdot V_g \cdot \sigma T^4 \quad (3-5)$$

where E_g^* is the rate of emission if no attenuation occurs

\mathcal{V} is the gas emissivity on a volume base

V_g is the volume of the gas
 σT^4 is the Stefan-Boltzmann Constant times the temperature to the fourth power

Since the gas volume is infinite in length, some distance (such as the actual length of the furnace) is used in calculating this volume.

It may readily be shown that the gas emissivity on a volume basis is equal to $4k$, where k is the absorption coefficient for a characteristic gas such that the gas emissivity, ϵ_g , is equal to $(1 - e^{-kx})$. (18) (33)

Since for any restricted volume of gas there will be attenuation of energy originating within the volume, the actual emission will be less than that given by equation (3-5).

2. Emission from a Surface Area

There is no problem involved in the formulation of the total rate of energy emission from a surface which is simply equal to the surface emissivity multiplied by black radiation at the temperature of the surface. The values of emissivity for a wide variety of materials encountered in industrial practice are available in the literature. (34, 45)

3. Interchange Between Two Surfaces

The one-way radiation from surface s_1 to surface s_2 is given by the following equation which may be considered a definition of the factor $f_{s_1 s_2}$:

$$q_{s_1, s_2} = f_{s_1, s_2} A_{s_1} \sigma T_{s_1}^4 \quad (3-6)$$

The factor $f_{s_1 s_2}$ plainly represents the fraction of the energy leaving surface s_1 that is intercepted by surface s_2 and is a function of the areas and geometrical configurations of the two surfaces as well as the absorption coefficient of the intervening gas mass. For evaluation of the factors of the type f_{ss} it will be assumed that the intervening gas has constant absorption properties, that is, a constant absorption coefficient k , no matter how far apart the surfaces are. This is in accordance with an earlier statement that it is desirable to evaluate the coefficients on the temperature terms in the energy balances, equations (3-2) and (3-4) at some mean temperature for each isothermic gas volume.

Consider two differential areas dA_1 and dA_2 separated by distances Δx , Δy and Δz measured on the three coordinate axes and therefore separated by a center-to-center distance r , where:

$$r = \sqrt{\Delta x^2 + \Delta y^2 + \Delta z^2} \quad (3-7)$$

The one-way radiation between the two differential areas is plainly proportional to the areas of each as viewed from the other, inversely proportional to the square of the separating distance, and must be diminished by the transmissivity of the intervening gas of absorption coefficient k and path length r . Expressing this mathematically and putting in the proportionality constant $1/\pi$ which has been established elsewhere,⁽⁴⁶⁾ one obtains:

$$dq_{12} = \frac{dA_1 \cos \phi_1 \cdot dA_2 \cos \phi_2}{\pi r^2} \cdot e^{-kr} \sigma T_1^4 \quad (3-8)$$

It is now necessary to integrate this expression over the two finite areas A_{s_1} and A_{s_2} to obtain the interchange, and combining this result with equation (3-6) one can evaluate the factors $f_{s_1 s_2}$. Due to the presence of both an exponential term and a polynomial it is not possible to integrate equation (3-8) analytically. At this point it is adequate to point out that two distinct cases of interchange between surfaces must be handled - surfaces in parallel planes and surfaces in perpendicular planes. Considering these two cases only for the parallel and

orthogonal cases, one arrives at the two following expressions to be numerically integrated to obtain the

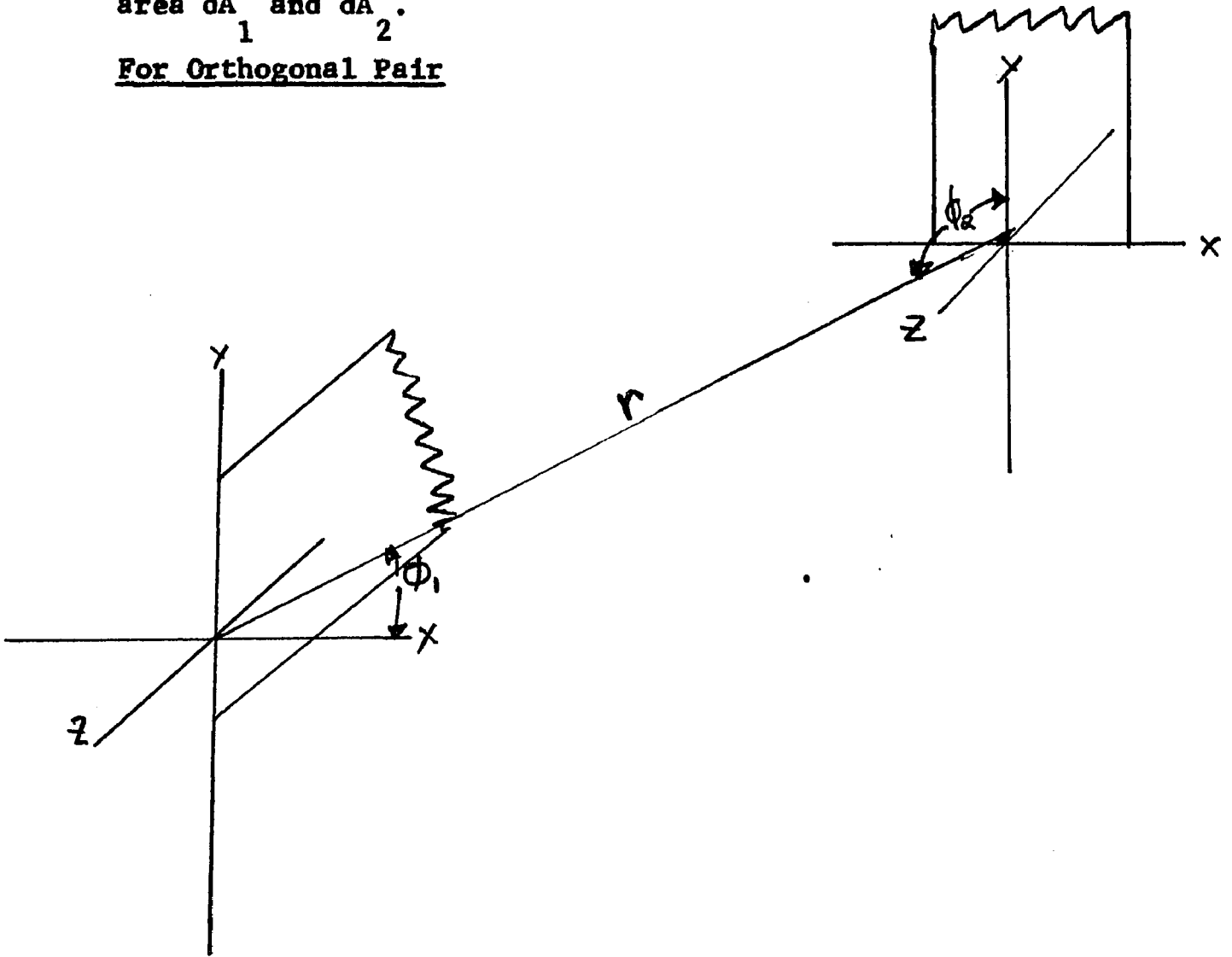
$$F_{ss}:$$

$$F_{ss} = \frac{q_{s_1 \rightarrow s_2}}{\sigma T^4} = f_{ss} A_s$$

$$f_{ss} = \int_{A_1} \int_{A_2} \frac{e^{-kr}}{\pi r^2} \cos \phi_1 \cos \phi_2 dA_1 dA_2 \quad (3-9)$$

where r is the distance separating the incremental area dA_1 and dA_2 .

For Orthogonal Pair



$$\cos \phi_1 = \frac{y}{r}$$

$$\cos \phi_2 = \frac{x}{r}$$

$$dA_1 = dy dz$$

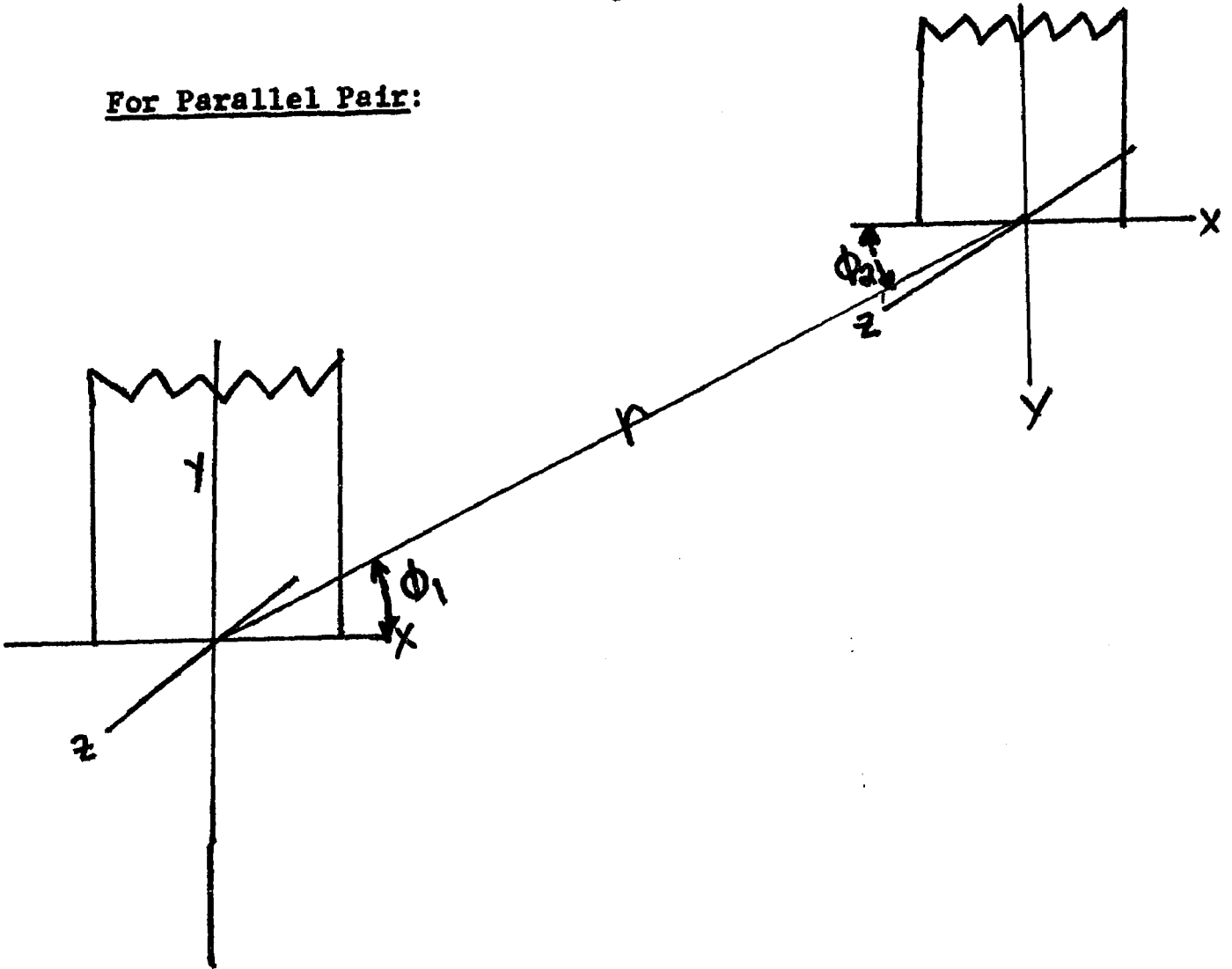
$$dA_2 = dx dz$$

$$r = \sqrt{\Delta x^2 + \Delta y^2 + \Delta z^2}$$

$$f_{SS} = \int \int \int \int e^{-kr/n^2} \cdot \frac{y}{r} \frac{x}{r} dz_R dy dx dz_E$$

$$= \int_0^L \int_{x_1}^{x_2} \int_{y_1}^{y_2} \int_{-\infty}^{+\infty} xy e^{-kr/n^2} dz_R dy dx dz_E$$

For Parallel Pair:



$$\cos \phi_1 \equiv y/r$$

$$\cos \phi_2 \equiv x/r$$

$$dA_1 \equiv dy dz$$

$$dA_2 = dx dz$$

$$f_{ss} = \iiint \frac{e^{-kr}}{r^2} \frac{y_1}{r} \frac{y_2}{r} dz_R dy_1 dy_2 dz$$

oh

(3-12)

$$f_{ss} = \int_0^L \int_{y_1'}^{y_1''} \int_{y_2'}^{y_2''} \int_{-\infty}^{\infty} \frac{e^{-kr}}{r^4} y^2 dz_R dy_1 dy_2 dz_E$$

(3-13)

Similar relationships exist for the other possible orientations, but will not be given here. It now becomes possible to perform numerical integration on equations (3-10) and (3-11) and any of the other required orientations.

The method of Gaussian quadratures was combined with Simpson's integration⁽¹⁾ to yield the numerical results.

All of the possible orientations were of the following form:

$$f_{ss} = \int_0^L \int_{q_1'}^{q_1''} \int_{q_2'}^{q_2''} f(x, y) \int_{-\infty}^{\infty} \frac{e^{-k\sqrt{u^2+z^2}}}{(u^2+z^2)^2} dz_R dq_1 dq_2 dz_E$$

where

$$u = \sqrt{x^2 + y^2}$$

and $f(x,y)$ takes into account the particular orientation being evaluated, the function can be brought outside of the two inner integrals because it is independent of z .

The limits of integration Q_1 and Q_2 are either both x , or both y , or x and y , again depending on the orientation of the surfaces under evaluation.

Evaluating the two indefinite integrals using Simpson's integration of the following form: (1)

$$\int_a^b f(x) dx = \frac{h}{3} \left[f(a) + 4f(a+h) + 2f(a+2h) + 4f(a+3h) + \dots + 4f(a+(2m-1)h) + f(b) \right] \quad (3-15)$$

where $h = (b - a)/2m$

and m is the number of subdivisions used.

Considering the inner integral of (3-14) and allowing

$U^2 = \sqrt{x^2 + y^2}$ and $r = \sqrt{x^2 + y^2 + z^2}$ results in:

$$\int_{-\infty}^{\infty} e^{-kr} \frac{dz}{r^4} = \int_{-\infty}^{\infty} \frac{e^{-kU\sqrt{1+z^2/U^2}} dz}{U^4 (1+z^2/U^2)^2} \quad (3-16)$$

Letting $w = z/u$ or $dz = udw$ yields:

$$\int_{-\infty}^{\infty} \frac{e^{-kU\sqrt{1+w^2}} U dw}{U^4 (1+w^2)^2} = \frac{1}{U^3} \int_{-\infty}^{\infty} \frac{e^{-kU\sqrt{1+w^2}}}{(1+w^2)^2} dw \quad (3-17)$$

Defining:

$$F(KU) = \int_{-\infty}^{\infty} \frac{e^{-KU\sqrt{1+w^2}}}{(1+w^2)^2} dW \quad (3-18)$$

Noting:

$$F(KU) = 2 \int_0^{\infty} \frac{e^{-KU\sqrt{1+w^2}}}{(1+w^2)^2} dW \quad (3-19)$$

$$\approx \int_0^{40} \frac{e^{-KU\sqrt{1+w^2}}}{(1+w^2)^2} dW$$

Equation (3-19) can now be evaluated from equation (3-15).

The replacement of the upper limit in equation (3-19) to a value of 40 was justified by evaluating (3-19) for a value of $KU = 0$, since when this substitution is made, equation (3-19) can be evaluated analytically yielding a value of $\pi/2$.

$$\begin{aligned} F(0) &= 2 \int_0^{\infty} \frac{dW}{(1+w^2)^2} \\ &= 2 \left[\frac{w}{2(1+w^2)} + \frac{1}{2} \tan^{-1}(w) \right]_0^{\infty} = \pi/2. \end{aligned} \quad (3-20)$$

The numerical evaluation of (3-19) using the upper limit of 40 and using $h = .05$ i.e. evaluating 800 terms

in the Simpson integration) resulted in a value of $F(0) = 1.570795 (= \pi/2)$.

It is important to note that KU will always be positive, so that the evaluation of (3-19) by Simpson's Rule will result in numerical values smaller than for $K = 0$ (a clear gas).

Setting $KU = 0$ to evaluate $F(KU)$ results in the largest numerical deviation from the correct value of the function.

The value of $F(KU)$ can now be evaluated separately for various values of KU . This procedure was carried out for values of KU varying between 0 and 20, as shown on Figure 4. Above 20 the contributions of the terms constituting the numerical equivalent of the integral made no significant contribution to the calculation of the view factor and thus was taken as 0. This would correspond to a beam length of approximately 60 feet. The value being discarded results in an error less than one part in a million. Previous to this, graphical integration techniques could only yield results that were accurate to one part in a hundred. (18)

The function of $F(KU)$ versus $\log(KU)$ was then fitted to a 7th order polynomial. In order to get the best possible fit, the function was broken down into four ranges,

a separate polynomial being used for each interval. The results of these curve fits can be found in Appendix B which gives the Fortran listing of the calculation procedure. The results are shown in Function W. ⁽¹⁹⁾

Once the value of $F(KU)$ is determined, it is necessary to evaluate the rest of the equation (3-14). This is done by using Gaussian quadratures, ⁽¹⁾ the relationship is:

$$\int_{-1}^1 f(x) dx = \sum_{i=1}^N w_i \cdot f(x_i) \quad (3-21)$$

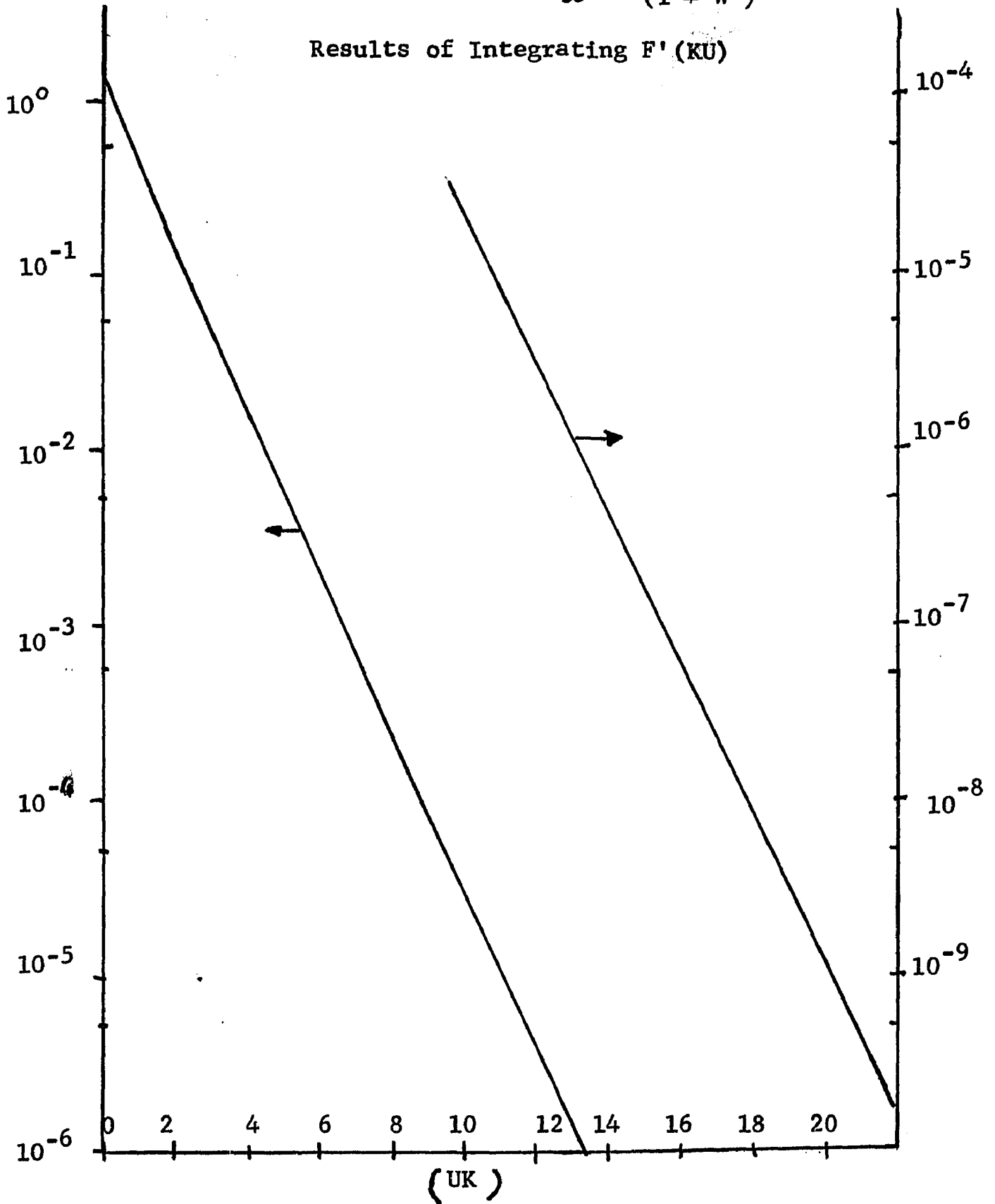
Where w_i is the weight factor different from w_i used by the Hermite integrations

x_i is the associated value of the independent variable

Figure 4.

$$F(UK) = \int_{-\infty}^{\infty} \frac{e^{-KU} \sqrt{1+W^2}}{(1+W^2)^2} dW$$

Results of Integrating F' (KU)



This relationship is applied twice to equation (3-14)

to yield:

$$f_{ss} = \sum_i^N w_i \cdot \sum_j^N w_j \cdot f(x_i, y_j) \cdot F(UK) \quad (3-22)$$

In doing the calculation it was decided to use a value of 9 for N, resulting in 81 calculations for the determination of each F_{ss} term. The value of 9 for N was selected as a compromise between accuracy and time required to perform the calculation.

4. Interchange Between a Volume of Gas and a Bounding Surface

The defining equations for the one-way radiation, gas to surface or surface to gas, are as follows:

$$q_{sg} = A_s \cdot f_{sg} \cdot \sigma T_s^4 \quad (3-23)$$

$$q_{gs} = 4KV_g \cdot f_{gs} \sigma T_g^4 \quad (3-24)$$

As T_s approaches T_g , that is as the temperatures of the two elements approach each other, the values of q must likewise approach each other and it follows that:

$$A_s f_{sg} = 4KV_g \cdot f_{gs} \quad (3-25)$$

Formerly, when the values of F_{ss} were calculated by techniques with an estimated error in one part per hundred, the difference between the six values was small in comparison to the magnitude of the solution. By using the computer this problem has been eliminated, and the error reduced to approximately one part in a million.

In our two dimensional model the radiation entering and leaving the infinite areas can not be "viewed" by the surface. This means that only a total of four values of f_{ss} need to be calculated and summed together with the appropriate sign to yield the desired value of f_{sg} .

In instrumenting this procedure on the computer, great care must be taken in the determination of the correct orientation. Once this is accomplished, it becomes possible to use the already existing procedures for the calculations of the values of f_{ss} . The reader is referred to the Fortran listing of the calculation procedures and specifically to FUNCTION SG, on page 96 of Appendix B.

5. Interchange Between Two Gas Volumes

The defining equation for this final case of one-way radiation exchange, that is the energy transfer from one volume to another in the system may be written as:

$$q_{gg} = 4kV_g f_{gg} \cdot \sigma T_g^4$$

(3-26)

The meaning of this type of interchange areas, as before, is the fraction of the radiation originating in one element that reaches and is absorbed by any other in the system. If the two subscripts g refer to the same gas volume, q_{gg} represents the radiation originating in the volume q_{gg} and absorbed by itself before reaching the boundary surface.

Once again the factor f_{gg} is function of the geometry of the system and the absorption coefficient of the gas. Just as it was possible to obtain f_{sg} by properly adding up six values of f_{ss} it is also possible to calculate f_{gg} by the appropriate addition of six values of f_{gs} in a system where the gas volumes have finite length. Plainly, f_{gg} must equal the sum of the f_{gs} values to the near faces of the second volume, minus the sum of the f_{gs} values seen dimly through the volume.

In the two dimensional model being developed in this study, only four values of f_{gs} need to be computed, the two edges at the end of the finite axis being unable to view each other.

The evaluation of f_{gs} again requires the evaluation of four f_{ss} terms. This means for each f_{gg} term calculated, a total of sixteen f_{ss} terms need to be evaluated. With the orientation determined, the evaluation of f_{gg} is accomplished by using FUNCTION SG which in turn uses FUNCTION SS.

C. Calculation of Direct Energy Transfer

It will be useful at this point to define a new type of interchange factor - one that when multiplied by σT^4 the black emissive power of a unit surface at the temperature of the radiating zone will yield directly the rate of energy absorption by any other zone in the system. Again the reader is reminded that discussion is presently restricted to one in which all surfaces are perfect absorbers. These factors, in simplified nomenclature, will always be written as two letters - either ss, sg, gs or gg - where g and s stand for gas and surface respectively. Furthermore each of the letters will have a numerical subscript to identify which particular volume or surface is under consideration. For example the energy transferred from surface 2 to gas volume 4 is equal to $s_2 g_4 \cdot W_{s2}$; similarly, the transfer from gas volume 4 to surface 2 is $g_4 s_2 \cdot W_{g4}$, where W_{sn} is equal to the rate of emission from unit area of a black body at a temperature

indicated by subscript (i.e. temperature of surface n). Since, as the temperature of the gas zone and the surface zone approach each other (i.e. as the values of W approach each other) the net transfer between the two zones must be zero; the only way that this can happen is for $s_2 g_4$ to equal $g_4 s_2$, and thus, in this type of formulation the order in which two zones are mentioned is immaterial. This same reasoning applies to both surface-surface and gas-gas radiation.

The use of four symbols to describe interchange areas - two to indicate the types of zones involved (gas or surface) and two to indicate the particular zones - is a necessary consequence of having more than one gas zone in the enclosure.

It is noted that the total of all the interchange areas from any one zone to all other zones in the enclosure including itself must add up to the energy originating from that same area per unit emissive power. Expressed mathematically:

$$s_1 s_1 + s_1 s_2 + s_1 s_3 + \dots + s_1 g_1 + s_1 g_2 + s_1 g_3 + \dots = A_{s_1} \quad (3-27)$$

or

$$\left\{ s_1 s_i + \left\{ s_1 g_i = A_{s_1} \quad (3-28) \right. \right.$$

$$\text{and } g_1 g_1 + g_1 g_2 + g_1 g_3 + \dots + g_1 s_1 + g_1 s_2 + g_1 s_3 + \dots \quad 69$$

$$= 4K V g_1 \quad (3-29)$$

$$\text{or } \sum_i g_1 g_i + \sum_i g_1 s_i = 4K V g_1 \quad (3-30)$$

D. Allowance for Grayness of Walls

The discussion which follows summarizes the work of Hottel^(33-A) and Cohen⁽¹⁸⁾

All discussion up to this point has been concerned with a system in which all walls were perfect absorbers so that any energy which reached a wall surface was not reflected back into the system, hence total or perfect absorption took place. In general, however, the walls of a furnace are not black but are capable of reflecting some of the energy incident upon them. This reflected energy is distributed among all the gas and all the surfaces in accordance with the geometrical configuration of the various surfaces and the absorbing power of the gas; and that portion incident on the surface is again partially absorbed and partially reflected to repeat the process ad infinitum. The result is an extremely complex situation necessitating a consideration of all possible beams of original energy and the results of an infinite number of reflections at the walls.

The technique for making allowance for this complicated problem to be given here is simply an extension of the one presented by Hottel⁽⁴⁹⁾ for the one-gas zone, multi-surfaced enclosure. As in Hottel's treatment where the direct interchange between two zones was equal to $A_1 F_{1G}$ or $A_1 F_{12}$ multiplied by the difference in emissive powers, so in the present case it is equal to a factor $g_1 g_2, s_2 s_3,$ etc. Similarly, if one allows for the multiple reflections within the enclosure, defined as $G_1 G_2, G_1 S_1$ or $S_1 S_1,$ one can evaluate such factors as $GS, GG,$ or SS from the direct factors gs, gg or $ss.$ Note that the factors $GG, GS,$ and SS like their lower-case counterparts all have the dimensions of area.

It is plain that the interchange area between any two zones in the enclosure cannot be a function of temperature as long as the physical properties of the system (emissivities and absorptivities) are independent of temperature. Therefore one is justified in evaluating the interchange areas at any convenient temperature and the results will be completely general. The problem of evaluating the interchange areas is very much simplified if one causes the temperature of every surface and gas zone except one to be maintained at absolute zero and as a consequence the emissive powers of every zone except one area are

all zero. This necessitates some sort of energy withdrawal from all zones, including the gas zones, by means unspecified but not interfering with transmission. Furthermore, one can let the temperature of the one emitting zone be such that its black emissive power is unity; i.e. such that σT^4 is unity. As a result of maintaining the temperature at $\sigma T^4 = 1$ at the single surface or gas zone, there will be a radiant flux at and toward every surface in the system, and at and away from it as well due solely to original emission from the one zone and to the multiple reflections within the enclosure. In a black system this reflected flux would, of course, be equal to zero. The terminology to describe this outgoing flux density will be R with a presubscript designating the original source of the energy and a final subscript, the reflecting surface. Thus if gas zone g_1 were the only emitter in the system, the flux density at surfaces s_1, s_2, \dots would be indicated by $g_1 R_{s_1}, g_1 R_{s_2}, \dots$. Similarly if surface s_1 were the only original emitter the flux density at surfaces s_2, s_3, \dots would be $s_1 R_{s_2}, s_1 R_{s_3}, \dots$ but the flux density at surface s_1 would be equal to $s_1 R_{s_1}$ due to reflections corrected for ξ_{s_1} to allow for original emission from the surface.

i. Original Emitter is a Gas Zone

If, for example, gas zone g_1 is the sole original emitter then the total radiant flux at and away from any surface such as s_1 in the system is designated as $G_1 s_1$. Since this is the reflected flux, $G_1 s_1 = R_{s_1} \cdot A_{s_1} \cdot \sigma T^4$. If one multiplies it by the ratio of the absorptivity (equal to emissivity) of the surface to the reflectivity of the surface (the complement of absorptivity) the result will be the absorbed energy at the surface, and since the value of σT^4 of the original emitter was made equal to unity, this must by definition be identical with the desired factor $G_1 s_1$. Expressing this statement more generally by considering the i -th gas zone and the j -th surface zone:

$$G_i s_j = s_j G_i = g_i R_{s_j} \cdot \frac{A_{s_j} E_{s_j}}{\rho_{s_j}} \quad (3-31)$$

In order to determine the value of the reflected flux R at any surface one can write an energy balance on each surface. The total rate of energy impingement on surface s_1 is equal to the contributions from all the surfaces in the system including itself plus the energy it receives directly from the single gas zone which is the original emitter. If the sum of all these terms is then multiplied

by the surface reflectivity, then the result which is the reflected flux must be equal to $g_i R_{s_i} \cdot A_{s_i}$. This summation can be carried out for every surface in the system yielding a set of equations, one for each surface, as follows:

$$\begin{aligned}
 [s_1 s_1 \cdot g_i R_{s_1} + s_1 s_2 \cdot g_i R_{s_2} + \dots g_i s_1] \Psi_{s_1} &= A_{s_1} g_i R_{s_1} \\
 [s_1 s_2 g_i R_{s_1} + s_2 s_2 \cdot g_i R_{s_2} + \dots g_i s_2] \Psi_{s_2} &= A_{s_2} g_i R_{s_2} \\
 [s_1 s_3 g_i R_{s_1} + s_3 s_2 \cdot g_i R_{s_2} + \dots g_i s_3] \Psi_{s_3} &= A_{s_3} g_i R_{s_3} \\
 \cdot & \cdot \cdot \cdot \cdot \cdot \\
 \cdot & \cdot \cdot \cdot \cdot \cdot \\
 \cdot & \cdot \cdot \cdot \cdot \cdot
 \end{aligned}$$

(3-32)

It is apparent that the total number of equations in set (3-32) is exactly equal to the number of unknown reflected-flux densities R_s .

Expression (3-32) in matrix form:

$$|D| \cdot |g_i R_{s_L}| = |-g_i s_L| \quad (3-33)$$

$S_1 S_2 - A_{s_1} / \rho_{s_1}$	$S_1 S_2$	$S_1 S_3 \dots$	$g_i R_{s_1}$	$-g_i s_1$
$S_1 S_2$	$S_2 S_2 - A_{s_2} / \rho_{s_2}$	$S_2 S_3 \dots$	$g_i R_{s_2}$	$g_i s_2$
$S_1 S_3$	$S_3 S_3 - A_{s_3} / \rho_{s_3} \dots$	$S_3 S_3 - A_{s_3} / \rho_{s_3} \dots$	$g_i R_{s_3}$	$g_i s_3$
$D =$	$S_2 S_3$	$g_i R_{s_L}$	$-g_i s_L =$	
\bullet	\bullet	\bullet	\bullet	\bullet
\bullet	\bullet	\bullet	\bullet	\bullet
\bullet	\bullet	\bullet	\bullet	\bullet

(3-33A)

Equation (3-33) can then be solved by taking the matrix inverse:

$$|g_i R_{s_i}| = |D|^{-1} \cdot |-g_i s_i| \quad (3-34)$$

The reader is again referred to Appendix B to SUBROUTINE INVERT page 104 to get the details of the inversion procedure. The invert algorithm takes advantage of the fact that D is a diagonally dominant matrix.

From the values of the reflected flux density at the various surfaces it is also possible to calculate the total interchange factor between any two gas cubes. If gas zone g_1 is the original emitter, then the total reception at any other gas zone g_2 is equal to the direct radiation from g_1 to g_2 (equal to $g_1 g_2$) plus the sum of the products of the reflected flux at each surface in the system multiplied by the fraction of that flux which reaches and is absorbed by gas zone g_2 . Again, since the black-body emission from zone g_1 has been set at unity this sum represents the desired factor $G_1 G_2$. The general expression for this factor between any two gas zones m and n then becomes:

$$G_m G_n = g_m g_n + \sum_i (g_m R_{s_i}) \cdot (s_i g_n) \quad (3-35)$$

ii. original Emission in a Surface Zone

In order to obtain the one remaining factor - interchange between two surfaces - it is necessary to let one of the surface zones be at such a temperature that its black body emission would be equal to unity and to let all other surfaces as well as all gas zones be at absolute zero. One can again write energy balances on each surface in the system, the only changes being that there will be no direct radiation from the gas and that the surface that is the original emitter will send out, in addition to the reflected flux term, an amount of energy per unit area equal to its emissivity. The set of resultant equations for this case where surface s_1 is the sole original emitter is:

$$\begin{aligned} [s_1 s_1 (s_1 R_{s_1} + \epsilon_{s_1}) + s_1 s_2 \cdot s_1 R_{s_2} + \dots] \Psi_{s_1} &= A_{s_1} \epsilon_{s_1} R_{s_1} \\ [s_1 s_2 (s_1 R_{s_1} + \epsilon_{s_1}) + s_2 s_2 \cdot s_1 R_{s_2} + \dots] \Psi_{s_2} &= A_{s_2} \cdot s_1 R_{s_2} \\ [s_1 s_3 (s_1 R_{s_1} + \epsilon_{s_1}) + s_3 s_2 \cdot s_1 R_{s_2} + \dots] \Psi_{s_3} &= A_{s_3} \cdot s_1 R_{s_2} \\ &\vdots \\ &\vdots \\ &\vdots \end{aligned}$$

Just as before the total number of equations is equal to the total number of unknown reflected flux densities and the solution for any one of them may be written as:

$$|g_i R_{s_L}| = |D|^{-1} \cdot |S_i S_L| \quad (3-37)$$

where D is exactly the same as the expression obtained earlier and given in equation (3-33).

Hottel⁽⁴⁶⁾ and Cohen⁽¹⁸⁾ demonstrate that

$$S_i S_j = S_j S_i \quad (3-38)$$

E. Allowance for a Real Gas

It has already been shown in Chapter 2, that it is possible to approximate the behavior of a real gas in a system by considering it to be a weighted sum of gray gases and one clear gas, each weighted in proportion to the energy fraction of the spectrum that it occupies. Furthermore, since in most systems it is the first beam that is the important one all successive beams undergo double attenuation by the gas and the surface on each pass, an adequate approximation to the real gas is the simple sum of two characteristic gases - one having an absorption coefficient k and occupying the fraction "a"

of the spectrum, the second being a clear gas (absorption coefficient equals zero) and occupying the fraction "1-a" of the spectrum.

One is cautioned that such an approximation would not be valid in a system where the K_1 is so low that the gas transmissivity is very high and where the walls are highly reflective. For the single-gray + clear-gas case the emissivity and absorptivity are then related to the path length x as follows:

$$\epsilon_x = a(1 - e^{-Kx}) \quad (3-39)$$

If one then fits the above exponential to the actual emissivity versus path length curve for a real gas, at a path length equal to the primary path length for the system, and at twice this value, mathematical manipulation leads to the following expression for "a", the fraction of the spectrum occupied by the gray portion:

$$a = \frac{\epsilon_1^2}{2\epsilon_1 - \epsilon_2} \quad (3-40)$$

The value of kL for this case is then equal to:

$$kL = LN \left(\frac{\epsilon_1}{\epsilon_2 - \epsilon_1} \right) = LN \left(\frac{1}{1 - \epsilon_1/a} \right) \quad (3-41)$$

In both the above expressions ϵ_1 refers to the gas emissivity evaluated at the characteristic path length for the system L , and ϵ_2 is the emissivity evaluated at twice that path length.

Since ϵ_x is a function of temperature, it is now possible to find a series of " ϵ " at different temperatures and calculate the corresponding values of "a".

The resulting values of "a" can now be fitted to polynomials in temperature resulting in:

$$a = b_0 + b_1 T + b_2 T^2 + b_3 T^3 + b_4 T^4 + b_5 T^5 \quad (3-42)$$

The value of ϵ_x was calculated from a regression fit of the emissivity data reported by Hottel in McAdams Chapter 4. ⁽⁴⁹⁾ The regressed data fit considers carbon dioxide, sulfur dioxide and water vapor. The calculation procedures are presented in the Fortran program in Appendix B FUNCTION EMISS. The regressed curve fit takes into

consideration the partial pressure of the components, the total pressure of the system and the temperature of the gas system being determined.

Once the value of "a" has been determined as a function of temperature it can be applied to the following equation:

$$SS = a [SS]_{kL} + (1-a) [SS]_{kL=0} \quad (3-43)$$

The value of $[SS]_{kL=0}$ represents the value of the interchange area evaluated for a clear gas.

$$GS = a [GS]_{kL} \quad (3-44)$$

$$GG = a [GG]_{kL} \quad (3-45)$$

It is to be noted that, as a result of this real-gas approximation, several important changes have been made:

1. In addition to the factors SS, SG and GG evaluated at kL by the methods of the previous sections, one must evaluate a new set of the SS-factors for the clear gas portion; i.e. at $kL = 0$.
2. As before, the sum of the total interchange factors from any surface to all surface and gas zones is

equal to the surface emissivity times the area.

The sum of the factors from one gas zone to all zones, however, is now given by:

$$\sum_j G_i G_j + \sum_j G_i S_j = 4kaV_g \quad (3-46)$$

The values of the partial pressure of CO_2 , SO_2 and H_2O are calculated via a flue gas analysis. No attempt was made to calculate the values of partial pressure within each isotherm, the flow patterns being assumed known throughout the system.

In evaluating the total interchange areas within a given zone, each in turn was considered to be the original emitter. This enabled the evaluation of the set of factors at the KU of the emitting zone. This means that $G_1 G_2$ no longer is equal to $G_2 G_1$, since each is now based on evaluations at different temperatures.

It was necessary first to estimate all the temperatures in the system and then, after the final solution to the problem, revise the estimates of temperature and repeat the computational procedure. This procedure was continued until the difference between the guessed values and the actual values was less than $.5^\circ$ Rankin.

This procedure, however, is not completely rigorous since one should allow for that fact that the k_L of the gas is constantly changing with path length. It is conceivable that one could, for each individual problem, start at the beginning and repeat the numerical integrations, allowing for the fact that the absorption coefficient was changing as one moved along a path length. It should be stated that the computer time involved in such a technique would be absolutely prohibitive for engineering calculations.

F. Energy Balance of Gas Volumes

The energy balance on the gas volumes and the surface area have been decoupled. This procedure has two chief advantages:

1. It reduces the computational magnitude of the energy balances to more manageable size.
2. It takes advantage of wall temperature being relatively stable due to the presence of sinks (i.e. the reactor).

The disadvantage of the procedure is that the convergence procedure has to be repeated for the surface and volume energy balances.

The term q_B in the energy balance on a gas zone in equation (3-2) represents the net energy transferred to the

gones by the bulk flow of the gas stream. It is equal to the total enthalpy above any arbitrary base temperature of all entering streams minus the total enthalpy above the same base temperature of all leaving streams. In order to formulate this enthalpy flux correctly, one would need to know the details of the gas flow pattern within the enclosure. Unfortunately, for most enclosures one does not have a detailed description of the flow pattern.

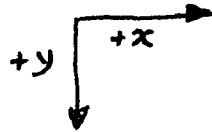
Some studies have been carried out utilizing the use of metal filings being introduced into the flow stream. Stop action photography techniques are then employed to determine actual flow distribution. The results of one such study were reported by Yeich⁽⁹³⁾ and are used in this study. The details of this flow pattern are presented in Appendix A.

The flow patterns were defined for an infinite furnace, hence no flow is permissible along the infinite axis. The flow in the plane perpendicular to the infinite axis was resolved into the flow along the other two mutually perpendicular directions. Flow from the eighteen gas volumes would thus be represented as (GM_{x18}, GM_{y18}) .

A computational check was performed to verify that the gas volume had neither a positive or a negative accumulation term. It should be noted that GM_{xj} is a vector quantity

and is used in the same sense as are the gas volume orientations, as shown in Figure 2.

i.e. the coordinate system is:



It now becomes possible to write an energy balance on the gas volume:

Note the subscript I refers to inlet conditions

U refers to outlet conditions

$$\text{Heat In} - \text{Heat out} + \text{Sources} = 0 \quad (3-47)$$

$$\left[\text{Enthalpy}_I - \text{Enthalpy}_U \right] \text{Bulk Flow} + \left[\text{Heat}_I - \text{Heat}_U \right] \text{Convection}$$

$$+ \left[\text{Radiant Energy}_I - \text{Radiant Energy}_U \right] + \text{Heat Release}$$

$$\text{by Combustion} = 0 \quad (3-48)$$

Equation (3-48) can now be rewritten for gas volume i

$$\begin{aligned}
 & [GM_{x_I} \cdot H(T_{j_1}) - GM_{x_I} H(T_{j_2})] + [GM_{y_I} \cdot H(T_{j_3}) - GM_{y_I} \cdot H(T_{j_4})] \\
 & + [h_{x_I} A_{x_I} (sT_{x_I} - T_i) - h_{x_0} A_{y_0} (T_i - sT_{x_0})] \\
 & + [h_{y_I} A_{y_I} (sT_{y_I} - T_i) - h_{y_0} A_{y_0} (T_i - sT_{y_0})] \\
 & + \left[\sum_j G_j G_i \cdot T_j^4 + \sum_j S_j G_i \cdot T_j^4 - T_i^4 \left(\sum_j G_i G_j + \sum_j G_i S_j \right) \right] \\
 & + E_T \cdot \phi(x_i, y_i) = 0
 \end{aligned}$$

(3-49)

where

$H(T)$ is the enthalpy of the flue gas and is calculated

$$\text{by integrating } C_p(T) = c_0 + c_1 T + c_2 T^2 + c_3 T^3$$

between absolute 0 and T

$$H(T) = c_0 T + \frac{1}{2} c_1 T^2 + \frac{1}{3} c_2 T^3 + \frac{1}{4} c_3 T^4$$

(3-50)

h_{x_I}

is converted heat transfer coefficient between

the gas and the gas surface with contact area

A_{x_I} and sT_{x_I} is the surface temperature in contact with the volume.

$\phi(x_i, y_i)$

is the fraction of the total heat released within the isothermal gas volume by combustion

E_T

is the total heat released within the furnace.

$$a_{ii} \sigma T_i^4 + \sum_j b_{ij} T_j^4 + \frac{1}{4} \frac{\alpha}{T_{x_I}^3} T_{x_I}^4 + \frac{1}{4} \frac{\beta}{T_{x_I}^3} T_{y_I}^4 + \frac{1}{4} \frac{\gamma'''}{T_{x_0}} T_{x_0}^4 + \frac{\delta'''}{T_{y_0}^3} T_{y_0}^4 = C_i \quad (3-51)$$

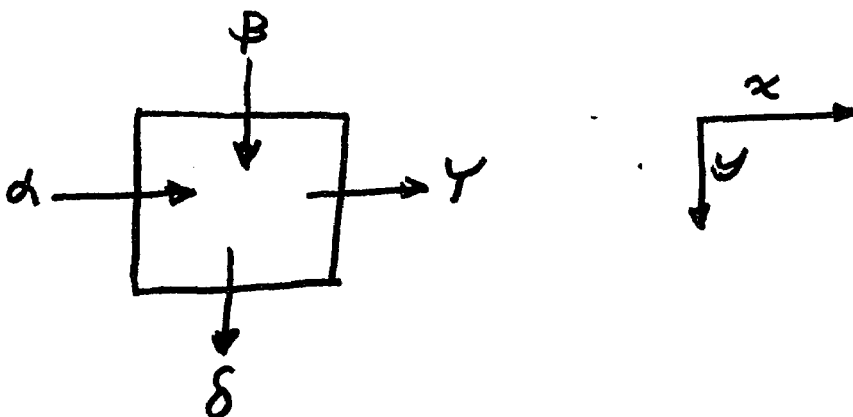
where

$$a_{ii} = -\sigma \left[\sum_j G_i G_j + \sum_j G_j S_i \right] + \frac{1}{4} [h_{x_I} A_{x_I} - h_{y_I} A_{y_I} - h_{x_0} A_{x_0} - h_{y_0} A_{y_0}] \frac{1}{T_i^3} + \frac{1}{4} [\alpha'' + \beta'' + \gamma'' + \delta'] \cdot \frac{1}{T_i^3}$$

$$b_{ij} = \sigma G_j G_i$$

$$C_i = \left[-\sigma \sum_j G_i G_j \cdot T_j^4 + (-h_{x_I} A_{x_I} s_{T_{x_I}} - h_{y_I} A_{y_I} s_{T_{y_I}} - h_{y_0} A_{y_0} s_{T_{x_0}} - h_{y_0} A_{y_0} s_{T_{y_0}}) - E_T \phi(x, y) + \alpha'' + \beta'' + \gamma'' + \delta'' \right] - \frac{3}{4} [\alpha' T_{x_I} + \alpha'' T_i + \beta' T_{y_I} + \beta'' T_i + \gamma' T_i + \gamma'' T_{x_0} + \delta' T_i + \delta'' T_{y_0}] + HT - T_i$$

Where $\alpha, \beta, \gamma, \delta$ are the bulk flow terms from the four sides of the isotherm under consideration.



The single prime on the bulk flow term indicates that there is a sensible heat flow from the facing isotherm. The double prime on the bulk flow term indicates the sensible heat flow from within the isotherm. The triple prime of the bulk flow term indicates the enthalpy gain within the isotherm.

The bulk flow terms are evaluated as follows: (3-51a)

No Area Contact $GM_{X_I} \geq 0$

$$d' = GM_{X_I} \cdot c_p(T_{O_{X_I}})$$

$$d'' = 0.0$$

$$d''' = -GM_{X_I} [H(T_{O_{X_I}}) - c_p(T_{O_{X_I}}) \cdot T_{O_{X_I}}]$$

Area Contact

$$d' = 0.0$$

$$d'' = 0.0$$

$$d''' = -GM_{X_I} \cdot H(T_{F_i})$$

$GM_{X_I} < 0.0$

$$d' = 0.0$$

$$d'' = GM_{X_I} \cdot c_p(T_{O_i})$$

$$d''' = -GM_{X_I} (-H(T_{O_i}) - c_p(T_{O_i}) \cdot T_{O_{X_I}})$$

$GM_{X_I} = 0.0$

$$d' = 0.0$$

$$d'' = 0.0$$

$$d''' = 0.0$$

$$d = d' + d'' + d'''$$

$$GM_{y_I} > 0$$

No Area Contact

Area Contact

$$\beta' = GM_{y_I} \cdot c_p(T_{0y_I})$$

$$\beta' = 0.0$$

$$\beta'' = 0.0$$

$$\beta'' = 0.0$$

$$\beta''' = -GM_{y_I} [H(T_{0y_I}) - c_p(T_{0x_I}) \cdot T_{0y_I}] \quad \beta''' = -GM_{y_I} \cdot H(T_{0x_I})$$

$$GM_{y_I} < 0$$

$$GM_{y_I} = 0.0$$

$$\beta' = 0$$

$$\beta'' = GM_{y_I} \cdot c_p(T_{0x_I})$$

$$\beta' = 0.0$$

$$\beta''' = -GM_{y_I} [H(T_{0x_I}) - c_p(T_{0x_I}) \cdot T_{0x_I}] \quad \beta''' = 0.0$$

$$\beta'' = 0.0$$

$$\beta = \beta' + \beta'' + \beta'''$$

$$GM_{x_0} > 0$$

$$GM_{x_0} = 0$$

$$\gamma' = 0$$

$$\gamma' = 0.0$$

$$\gamma'' = GM_{y_I} \cdot c_p(T_{0x_I})$$

$$\gamma'' = 0.0$$

$$\gamma''' = -GM_{y_I} [H(T_{0x_I}) - c_p(T_{0x_I}) \cdot T_{0x_I}] \quad \gamma''' = 0.0$$

$$\gamma''' = 0.0$$

$GM_{x_0} < 0$
No Area Contact

$GM_{x_0} < 0$
Area Contact

$$\gamma' = 0.0$$

$$\gamma' = 0.0$$

$$\gamma'' = GM_{x_0} \cdot c_p(T_{0x_0})$$

$$\gamma'' = 0.0$$

$$\gamma''' = GM_{x_0} \cdot [H(T_{0x_0}) - c_p(T_{0x_0})]$$

$$\gamma''' = GM_{x_0} [H(T_{Fa})]$$

$$\gamma = \gamma' + \gamma'' + \gamma'''$$

$GM_{y_0} > 0$

$GM_{y_0} < 0$
Area Contact

$$\delta' = 0$$

$$\delta' = 0.0$$

$$\delta'' = -GM_{x_0} c_p(T_{0x_0})$$

$$\delta'' = 0.0$$

$$\delta''' = GM_{x_0} [H(T_{0x_0}) \cdot T_{0x_0}]$$

$$\delta''' = -GM_{y_0} H(T_{Fa})$$

$GM_{y_0} < 0$

No Area Contact

$GM_{y_0} = 0$

$$\delta' = 0.0$$

$$\delta'' = -GM_{x_0} \cdot c_p(T_{0x_0})$$

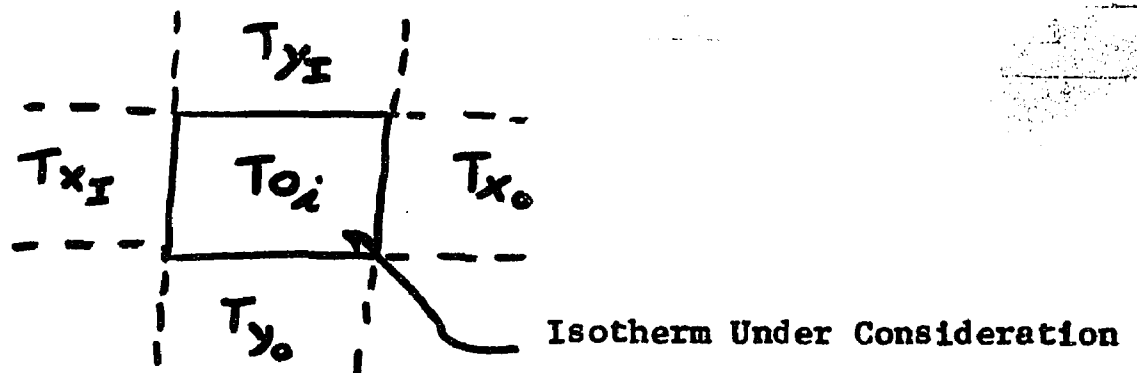
$$\delta' = 0.0$$

$$\delta'' = 0.0$$

$$\delta''' = GM_{y_0} [H(T_{0y_0}) - c_p(T_{0y_0}) \cdot T_{0y_0}]$$

$$\delta''' = 0.0$$

$$\delta = \delta' + \delta'' + \delta'''$$



The relationship used in equation (3-51) can be changed by reference to the above figure. The gas volume i has a temperature T_{0i} . The temperature for the isotherm to the left is T_{X_I} . The subscript I refers to inlet temperatures in reference to positive X axis. Similarly, the 0 in T_{X_0} refers to outlet temperature. The T_{Y_I} and T_{Y_0} have similar meanings in reference to the positive Y area. The temperature T_{FA} refers to the fuel-air temperature of the incoming fuel. The reader should note that all possible burner locations are accounted for by the four special cases of area contact. To illustrate this point, consider the case for $GM_X = 0$. If $GM_X = 0$, no fuel-air mixture could enter since no bulk flow term is present. If $GM_X > 0$ the bulk flow would have to go in the direction of the furnace wall and since the gas volume is in contact with the wall, there could clearly be no flow. Consideration of the other three cases leads to similar results.

Temperature terms which have a presubscript S such as $T_{S X_I}$ would refer to a surface temperature of the enclosing furnace wall. The subscript X_I would have the same meaning as previously discussed.

Equation (3-51) may now be written for every gas volume with the number of unknown gas volume temperatures equal to the number of equations. The matrix is again diagonally dominant and can be solved by the methods of Gauss-Jordan without double pivoting. The matrix contains surface area temperatures which are assumed constant in the solution of the gas volume temperature. In the next section the surface area temperature balance will be made assuming known gas volume temperature. This procedure allows for separation of the surface energy balance from the gas volume energy balance.

The two energy balances are then solved repeatedly (adjusting the total interchange area for the newly calculated temperature) using the Newton-Raphson technique.

G. Energy Balance on surface Area

The heat balance on the surface is expressed as:

$$\text{Heat In} - \text{Heat Out} = 0 \quad (3-52)$$

or

$$\begin{aligned}
 &\text{Heat release due to combustion} + \text{Radiant Energy In} - \\
 &\text{Radiant Energy Out} + \text{Heat Transfer In} - \text{Heat} \\
 &\text{Transfer Out by convection} - \text{Heat Loss to Ambient} \\
 &\text{surroundings} = 0 \qquad \qquad \qquad (3-53)
 \end{aligned}$$

The enthalpy consideration is zero as a result of considering heat transfer due to bulk flow to have occurred before flue gas has passed through the "porous membrane."

i. The source Term

The source term accounts for burner heat release that is very near the furnace. It is assumed that the detailed information of such heat release is known. This term is presented as:

$$H_s = E_{\text{Total}} \psi(x, y) \qquad (3-54)$$

where $\psi(X, Y)$ = fractions of total heat released at surface area.

ii. Radiant Energy Term

The radiant energy term accounts for all radiation in the system. Radiant energy from all the surface zones and all of the gas volumes over surface i may be expressed as

$$R = \left[\sum_j G_j G_{i,j} \sigma T_j^4 + \sum_j S_j S_{i,j} \sigma T_j^4 \right] \\ + \left[- \sum_j S_{i,j} G_j \sigma T_j^4 - \sum_j S_{i,j} S_j \sigma T_j^4 \right]$$

(3-55)

iii. Convective Heat Transfer

Convective heat transfer can take place in the bounding wall as well as internal heat transfer surface.

If the heat transfer takes place in the bounding wall, the net convected heat transfer becomes:

$$= h_c (T_G - T_i) A_i - h_c'' (T_i - T_{\text{sink}}) A_i \quad (3-56) \\ - h_c' (T_i - T_{\text{proc}}) A_i$$

where

- T_G is the temperature of the adjoining gas volume
- T_i is the temperature of Area A_i
- T_{sink} is the temperature of ambient
- T_{proc} is the temperature of the process fluid
- h_c is the adjusted overall heat transfer coefficient between surface i and the flue gas
- h_c' is the adjusted overall heat transfer coefficient between the area A_i and the process fluid

h'_c is the adjusted overall heat transfer coefficient between the area A_i and the ambient temperature

The net convected heat transfer for internal surface becomes:

$$h_c (T_c - T_i) A_i \Big|_{\text{Left}} + h_c (T_c - T_i) A_i \Big|_{\text{Right}} - h'_c (T_i - T_{\text{proc}}) A_i \quad (3-57)$$

Note internal surfaces always have a vertical orientation.

iv. Net Heat Absorbed by a surface

The net heat absorbed by a surface can be expressed as:

$$[E_{\text{Total}} \psi(x, y)] + [h_c (T_c - T_i) A_i] + \left[\sum_j G_j s_j \sigma T_j^4 + \sum_j s_j s_i \sigma T_j^4 - \sigma T_i^4 \left(\sum_j s_i s_j + \sum_j s_i s_j \right) \right] \quad (3-58)$$

The overall heat balance on surface zone i

$$E_T \psi(x, y) + \sum_j G_j s_i \sigma T_j^4 + \sum_j s_j s_i \sigma T_j^4 - \sigma T_i^4 \left[\sum_j s_i s_j + \sum_j s_i s_j \right] + h_c (T_c - T_i) A_i - h'_c (T_i - T_{\text{proc}}) A_i - h''_c (T_i - T_{\text{sink}}) A_i = 0 \quad (3-59)$$

It is now possible to write (3-59) for each surface area and linearize it in terms of T^4 . The resulting equation can be solved for T_i^4 by assuming the gas volume temperature as constant. The equation has the form:

$$A_{ii} T_i^4 + \sum_j B_{ij} T_j^4 = C_i \quad (3-60)$$

where

$$A_{ii} = \sigma \left[\sum_j \epsilon_j s_j - \sum_j \epsilon_j s_j G_j \right] - \left[(h_c + h_c' + h_c'') A_i \frac{1}{T_i^3} \right]^{1/4}$$

$$B_{ij} = \sigma s_j s_i$$

$$C_i = -\sigma \sum_j G_j s_j T_j^4 - (h_c T_G + h_c' T_{Proc} + h_c'' T_{Sink}) A_i - E_T \psi(\alpha, \gamma) + \left[(h_c + h_c' + h_c'') A_i T_i \right]^{3/4}$$

The reader should note that T_i is treated as a constant and the equation is then solved. The solution is then used to resolve the equation. This procedure is repeated until the maximum difference between two successive T_i 's is less than some abstract small quantity. $1^\circ R$ was used as the criterion for convergence in this study.

2. The Kinetic Model

The complete description of the kinetic model is given by Robertson⁽⁶²⁾ and will not be repeated here.

A brief discussion, however, will be presented and the method of incorporating the pointwise temperature distribution of the reactor wall will be explained.

A. Description of Reactor

The reactor is a tube 400 feet long placed in a furnace in a series of U bends. The tube runs up and down in the reactor to prevent bending of the tube in the center which would occur if it was strung out in an elongated position.

The tube itself is 3.640 inches in inside radius and the walls are .226 inches thick (a nominal four inch tube). The tube is assumed to have scale both on its inner and outer walls that add to the resistance of heat flow. The reactor tube was considered to be free of coke deposit. All initial design considerations did not consider the effect of coke on overall performance. However, a coke profile was calculated and later used to determine its effect on reactor yield.

The reactor inlet pressure was adjusted to give an

outlet pressure of two atmospheres. The initial reactor feed consisted of steam, ethane and propane. It is possible to include other material as long as the various mechanisms of reaction are known. The user would have to input kinetic and thermo-dynamic data. These however, were not included as a part of this study.

B. The Material Balance

Considering any incremental length of reactor the material balance can be written as:

$$IN = OUT + \text{Change By Reaction} + \text{Accumulation} \quad (3-61)$$

Since steady state is assumed, the only accumulation term involved in this study was the deposition of carbon on the reactor wall. When (3-61) is rewritten in

$$\begin{aligned} \sum_i N_i \Big|_{INLET} &= \sum_i \left[N_i \Big|_{OUTLET} + \sum_j A_{ij} N_{i,j} \Big|_{INLET} \cdot \Delta X_j \right] \\ \sum_i N_i \Big|_{INLET} &= \sum_i \left[N_i \Big|_{OUTLET} + \sum_j A_{ij} N_{i,j} \Big|_{INLET} \cdot \Delta X_j \right] \\ &+ A_{cc} \end{aligned} \quad (3-62)$$

where

N_i = number of molar flow rate into incremental reactor

A_{ij} = stoichiometric coefficient of the i^{th} chemical component in the j^{th} reaction

N_{ij} = the molar flow rate of the j^{th} reaction of the i^{th} component

ΔX_j = the incremental conversion calculated within the incremental length

A_{cc} = accumulation term

Equation (3-62) can be written for the i^{th} component to yield a component balance.

C. Calculation of Incremental Conversion

For the plug flow reactor the space time is defined by

$$\tau = \frac{V}{F_a} = C_{A_0} \int_{X_1}^{X_2} \frac{dX_A}{-r_A} \quad (3-63)$$

where

τ = is the reactor space time =

dX_a = differential conversion of A component

$-r_A$ = rate of reaction

C_{A_0} = initial concentration of component A

V = reactor volume =

F_a = volumetric flow rate

S = space time

Considering finite differences in equation (3-63) and solving for $X_a = X_2 - X_1$ results in:

$$\Delta X_A = -r_A \Delta T / C_{A_0}$$

(3-64)

Equation (3-64) can now be expressed in terms of flow rates:

$$\Delta X_A = \pi R^2 / F_{A_0} (-r_A) \Delta L$$

(3-65)

Where ΔL = the incremental reactor length under consideration.

Defining the reaction rate $(-r_A)$ in terms of the Arrhenius rate law:

$$(-r_A) = e^{-E_A^* / RT} \left[K_0 \prod_j C_{A_i}^{N_{A_i}} - K \prod_j C_{A_i}^{N_{A_i}} \right]$$

(3-66)

Where

- K_0 = the Arrhenius frequency factor
- E_A^* = the Arrhenius energy of reactivation
- R = gas constant
- T = absolute temperature
- N_{A_i} = order of reaction j of the i^{th} component
- K = equilibrium constant
- C_{A_i} = concentration of component

The reader should note π_j refers to the Pi product of the concentration terms. The concentration terms can be calculated from the ideal gas law:

$$C_a = P_a / R'T \quad (3-67)$$

where

P_a = Pressure of component a

R' = Gas constant

D. Calculation of Pressure Profile

In order to calculate the pressure at the end of the incremental reactor section a momentum balance was performed using the Bernouli equation. (51)

$$\Delta P = \left[\frac{v_1 + v_2}{2} \Delta F F \Delta L / R + v_2^2 - v_1^2 \right] / 2g \quad (3-68)$$

where

P = Pressure drop

v_1, v_2 = Reactor gas velocity at inlet, outlet conditions

F = Friction factor

L/R = Incremental length of reactor radius ratio

g = Gravitational constant

E. Calculation of Temperature Profile

In order to calculate the temperature at the end of the reactor increment, a heat balance was performed on the incremental reactor segment.

Heat flux in = sensible heat gain + heat of reaction (3-69)

$$UA\Delta T_1 = \sum_j F_j C_{Pj} \Delta T_2 + \sum_i \Delta H_i F_{K(i)} \Delta X_i \quad (3-70)$$

where

- U = to the overall heat transfer coefficient from reactor tube outer wall to reaction fluid
- A = the area through which heat flux is transmitted = $2 R L$
- T_1 = The temperature between outside wall and reaction fluid
- T_2 = Temperature difference between reaction fluid at start of increment and end of increment
- H_i = Heat of reaction i
- $F_{K(i)}$ = Molar flow rate of key component K(i) of the i^{th} reaction
- X_i = Extent of i^{th} reaction between the start and end of reactor increment
- CP_j = Heat capacity of the j^{th} component.

The reaction rate ($-r_A$) was determined by calculating its value at both ends of the incremental portion of the reactor and averaging the results. The average value was then used to recalculate the reactor conditions at the far end of the increment. This procedure was repeated until good values were obtained between the assumed end conditions and the actual end conditions. Thus an implicit method of solving differential equations was combined with Euler's method.

The convergence of reaction rate ($-r_A$) took place simultaneously with convergence of the pressure profile. The concentration profile and the temperature profile converged through repeated applications of momentum, component, overall material and energy balances.

F. Calculation of Overall Heat Transfer Coefficient

The previous discussion has been condensed; readers who are interested in more details are again referred to Robertson . (62)

However, more detailed information will be given on the calculation of U the overall heat transfer coefficient, as the concept was not fully developed in Robertson's work. The overall heat transfer coefficient from outer wall to reaction mass can be defined as:

$$\frac{1}{UA} = \sum_i R_i = \frac{R_o}{A_o} + \frac{\Delta x_{ST}}{K_{ST} A_{ST}} + \frac{R_I}{A_I} + \frac{\Delta x_c}{K_C A_c} + \frac{1}{h_I A_I} \quad (3-71)$$

where

- R_i = Resistance to heat flow
- R_o, R_I = Scale resistance to heat flow on outside and inside of reactor tube = $.001 \frac{\text{hr. ft}^2 \text{ of}}{\text{BTU}}$
(44A)
 .001 from Ludvig
- X_{ST}, X_C = Thickness of heat resisting material
 ST = steel reactor tube thickness
 C = coke thickness
- K_{ST}, K_C = Thermal conductivity, $\text{BTU/hr. ft}^2 (\text{°F/ft.})$
 $K_{ST} = 26., K_C = 2.90$ (44-A)
- A, A_C, A_I = Average area of heat transfer area
 $A_{ST} = 2 L (r_o - r_i) / \ln (r_o / r_i)$
 $A_C = 2 L (r_I - r_C) / \ln (r_I / r_C)$
 $A_I = 2 L r_C$

and where

r_o = radius of reactor tube (center to outer wall)

r_i = radius of reactor tube (center to inner wall)

r_c = radius of coke deposit (center of tube to coke surface)

h_I = heat transfer coefficient from coke surface to reaction fluid.

The value of h_I is a function of reaction fluid temperature, pressure, composition, velocity and temperature and can be calculated from the Seiden Tate equation since the flow is maintained in the turbulent regime to minimize residence time and product degradation via carbon deposition.

$$\frac{h_o D_i}{K} = 0.023 (N_{Re})^{.8} (N_{Pr})^{.43} \left(\frac{\mu}{\mu_i}\right)^{.14} \quad (3-72)$$

$$h = 0.023 \frac{K}{2r_i} \left(\frac{2r_i V \rho}{\mu}\right)^{.8} \left(\frac{C_p \mu}{K}\right)^{.43} \left(\frac{\mu}{\mu_i}\right)^{.14} \quad (3-73)$$

where

V = velocity of reaction fluid

ρ = density of reactor fluid

μ = viscosity of reaction fluid

μ_i = viscosity of reaction fluid at wall temperature

C_p = heat capacity of reaction fluid

K = thermal conductivity of the fluid

N_{Re} = Reynold's number

N_{Pr} = Prandtl's number

D_i = Diameter of the reactor radius after i increments of coke deposition

The methods of calculating C_p , μ , V and P are discussed in Robertson's Thesis (62). However, the calculation of the thermal conductivity has not been discussed.

The Mason equation was used: (11, 91)

$$K_{mix} = \sum_i \frac{x_i K_i}{\sum_j x_j \phi_{ij}} \quad (3-74)$$

where

$$\phi_{ij} = \frac{1}{\sqrt{8}} \left[\left(1 + \frac{M_i}{M_j} \right) \right]^{-1/2} \left[1 + \left(\frac{\mu_i}{\mu_j} \right)^{1/2} \left(\frac{M_j}{M_i} \right)^{1/4} \right]$$

M = molecular weight of the component

X_i = mole fraction of the component

The value of K_i was calculated from Eucken's (19-A) development of handling energy exchange in polyatomic gases and is given by

$$K_i = \left(C_{p_i} + \frac{5}{4} \frac{R'}{M_i} \right) \mu_i \quad (3-75)$$

The method used to calculate the viscosity utilizes the Lennard Jones equation, (11)

$$\mu_i = 2.6693 \times 10^{-5} \sqrt{M_i T} / \delta_i \Omega_{\mu} \quad (3-76)$$

where

δ_i is the characteristic of collision diameter of the molecule

Ω_{μ} is a slowly varying function of the dimensionless temperature KT/ϵ

δ_i and K/ϵ are commonly known as the Lennard Jones constants.

The reader is referred to Robertson's Thesis (62) for the details of the evaluation of Ω_{μ} .

The reactor model now is able to calculate an increment of conversion but requires the outer tube metal temperature. This calculation procedure is repeated for the entire length of the reactor.

3. the mapping models

A. Furnace Model to Reactor Model

The furnace model supplies the furnace plane wall temperature. This plane wall temperature is split into m isothermal temperature areas. In addition there were n sets of these isothermal zones, one for each subdivision of the furnace-reactor model.

It would be possible to use these discreet isothermal zones as the tube metal temperature used by the reactor. However, it was felt that a better approximation of the net heat flux could be obtained by considering the m isothermal temperatures as m points in a continuous curve. The location of each point would be the mid point of the isothermal zone. These points are then fitted to a fourth order polynomial in Y (the furnace height). The fit is accomplished by a linear least square fit (function FITT), which is given in Appendix B. An actual fit is illustrated in Figure 2 of Chapter I.

This procedure is repeated for the other $n-1$ furnace subsections. In order to determine what the reactor tube

wall temperature is at any point, all that is required is to determine which subsection of the furnace the reactor tube is located in, and what height that location lies relative to the furnace wall. This can be determined by the following relationship:

$$y_i = z_i - \text{Integer}(z_i/L_i) * L_i \quad (3-76)$$

where L_i is twice the furnace height

Integer implies that the result of $z_i/56$ is rounded off to the lower whole number. That is, the result of Integer (51.9971) is 51

z_i is the position of the reactor tube being evaluated for the tube metal temperatures.

If the value of Y is greater than $(L_i/2)$ Y is redefined in terms of the original Y by

$$y_i = L_i - y_{\text{original}} \quad (3-77)$$

The furnace subsection the tube is in is easily determined by knowing the length of each reactor subdivision.

The standard deviation of the temperature as function of wall height was approximately one half of a Fahrenheit degree.

By using the method described, it is possible to take into account the fluctuation of temperature with wall height. Variations along the long axes are handled as a set of three discontinuous isotherms.

One method would entail the determination of some continuous and smooth functions which would yield the temperature as a function Y and Z , which is:

$$T = f(Y, Z) \quad (3.78)$$

One such method would be to determine the best straight line, or the best second order polynomial through the three temperatures for the value of X and then determine the value for the particular location above the long or Z axis.

This procedure was not incorporated in this study, but it is recommended that consideration be given to it in any future refinement of this work.

B. Reactor Model to Furnace Model

It was necessary to map the reactor process fluid temperature into a set of $(n \times m)$ isothermals. This was accomplished by considering each one of the n subdivisions separately. The temperature of the reactor process fluid was recorded at m furnace height for every up and down pass

of the reactor tube in the furnace. It then became possible to sum the temperatures for any given furnace height and average the result. Thus:

$$\overline{T_{PF_i}} = \frac{\sum_i (T_{PF_i})}{\eta} \quad (3-79)$$

Where T_{PF_i} = average temperature of process fluid for isotherm at height Y

(T_{PF}) = successive temperatures of the process plane each time the tube passes through the height .

η = number of times the reactor tube passes through the height

Referring to Figure 5 for example, to calculate the temperature of isothermal zone being in isotherm 4, X_4 would result in:

$$\overline{T_{I(1,t)}} = \frac{\sum_{i=1}^5 (T_{I(1,t)})}{5} = \frac{T_4 + T_{11} + T_{18} + T_{26} + T_{32}}{5} \quad (3-80)$$

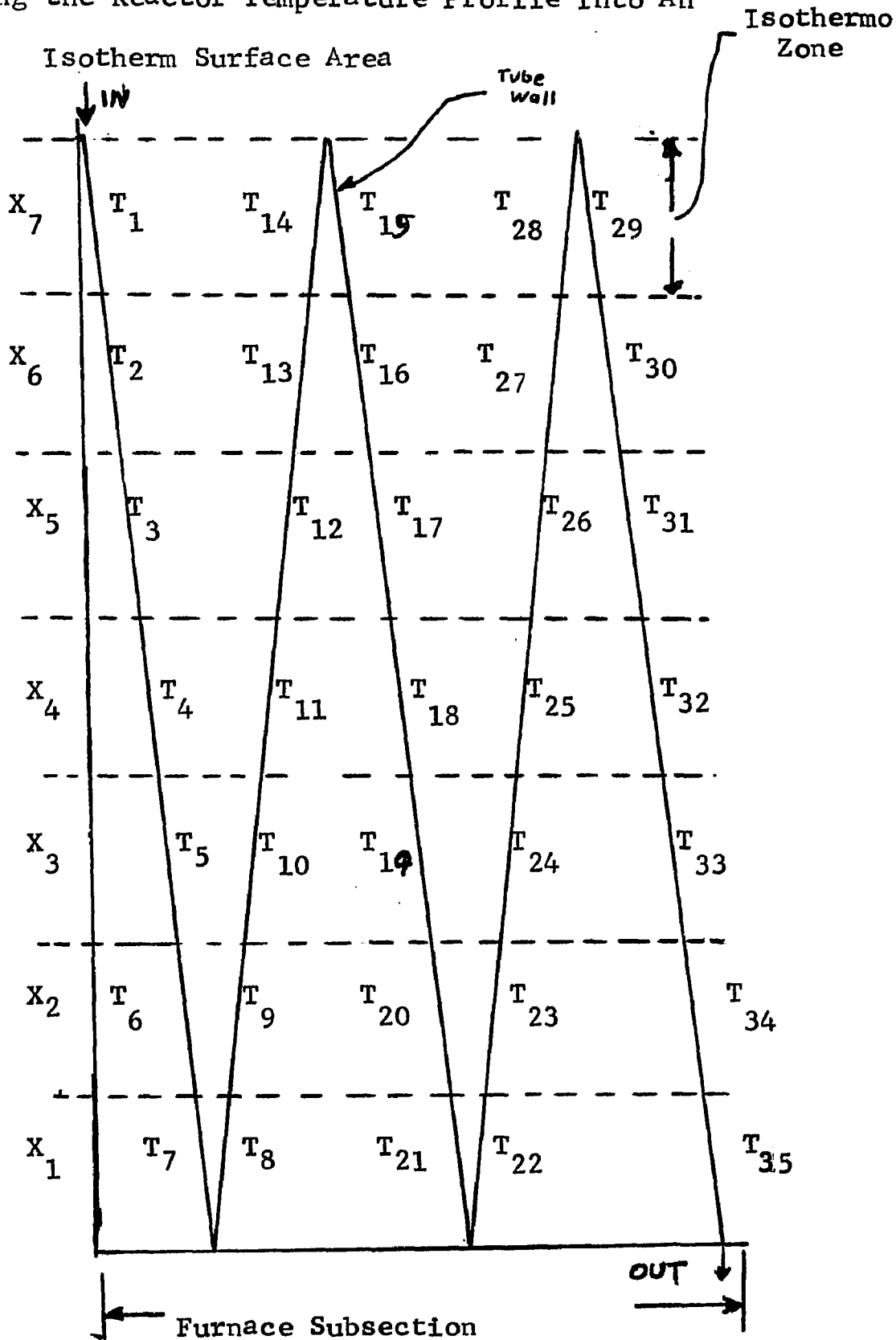
In order to determine the value of $\overline{T_{I(1,t)}}$ it was necessary to manually determine which temperature lay in which isotherm. This procedure was repeated for each of the furnace subsections under investigation. The

temperature locations were then stored as a part of the computer program (Appendix B).

Any further user who had a different set of furnace or reactor conditions or who desired to zone the furnace in a different way would have to redo these determinations and rewrite the main program. No changes in any subroutines or functions (with the exception of ~~TEMP~~) would have to be performed.

Figure 5

Mapping the Reactor Temperature Profile Into An Isotherm Surface Area



The average process temperature can thus be calculated from any set of isotherms for any furnace subsection.

The overall heat transfer coefficient from tube plane to process fluid plane will not be the same coefficient calculated from outer tube wall to process fluid in the reactor model. This is due to the differences in geometry between the two models. It was decided to allow the models themselves to do the mapping between the two geometries.

This mapping was accomplished by calculating the net heat flux Q_R through the reactor tube via the method described in Chapter III-2 for each furnace subsection. The furnace model then uses a guessed value for the overall heat transfer U_F to calculate the net heat flux Q_F to the process fluid.

At the next repeat of the furnace calculation the value of the overall heat transfer is adjusted according to:

$$U_F = U'_F (D + Q_R/Q_F) / (D + 1)$$

(3-81)

Where U'_F = former guessed value of the overall heat transfer coefficient

D = Damping factor

It was necessary to damp the change in the value of U_F as the undamped change i.e.:

$$U_F = U_F' Q_R / Q_F \quad (3-82)$$

results in divergent oscillation of the solution around the solution. The value of U_F was calculated independently for each furnace subsection.

4. Calculation "Flow"

A. Introduction

This section is an attempt to give the reader a "feel" for the computational sequence. The reader is reminded that the calculations were carried out on a high speed computer so some references will be made to data "input" and "output".

It would be extremely complicated to give detailed calculations of each step. In order to avoid this difficulty, whole groups of calculations will be referred to by a few descriptive words. It would also be difficult to give a "flow diagram" but reference will be made referring back to previous steps. This will be accomplished by numbering the various steps.

B. The "Flow"**STEP I.** Input Furnace Data

1. Total heat release distribution
2. Fuel-excess air analysis
3. Geometry of furnace
4. Bulk flow pattern
5. Surface properties
 - a. Transmissivity
 - b. Emissivity
 - c. Heat transfer coefficient
6. Surface boundary conditions

STEP II. Preliminary Furnace Calculations

1. Flue gas analysis
2. Specific heat enthalpy data
3. Initial temperature profile (if not inputted)
4. Characteristic flue gas by clear-gray gas combination. (isolate temperature dependence)

STEP III. Calculate Direct Interchange Area

1. Surface to surface - ss (clear gas, gray gas(es))
2. Surface-gas/ gas-surface, sg, gs (gray gas(es))
3. Gas - gas gg (gray gas(es)),

STEP IV. Account for Surface Reflectivity

1. Reflection with gas volume as the emitter.

Solve for $R_{g's}$ (gray gas(es))

2. Reflection with surface area as the emitter

Solve for $R_{s's}$ (gray gas(es))

STEP V. Calculate Total Interchange Area - For a

Characteristic Gas (Temperature Independent)

1. Gas to gas $GG = gg + \sum R_{g's} \cdot g$ (Gray gas(es))

2. Gas to surface/surface to gas

$$GS = R_{g's} \cdot \frac{AE}{\rho} \quad (\text{Gray gas(es)})$$

3. surface to Surface

$$a. \quad SS_c = R_{s_c} \cdot \frac{AE}{\rho} \quad (\text{Clear Gas})$$

$$b. \quad SS = R_{s_c} \cdot \frac{AE}{\rho} \quad (\text{Gray gas(es)})$$

STEP VI. Input Reaction Data

1. Initial Tube Wall Temperature (Guessed)

2. Description of Reactions

3. Description of Reactor

4. Initial Reactant Concentration

5. Physical Data

- a. Heat Capacity

- b. Arrhenius Kinetic Data

- c. Enthalpy

- d. Entropy

- e. Reaction Equilibrium
- f. Lennard - Jones Constants

6. Miscellaneous Control Parameter

STEP VII. Calculate Parameter Needed for Reactor

Calculation as a function of Temperature

STEP VIII. Output the Reaction System and Generate Parameters

STEP IX. Calculate Reactor Pressure, Component, Temperature, Heat Flux and Carbon Deposition profiles

1. Determine the Temperature profiles for Each Furnace subsection
2. Determine Rates for Beginning of Increment (All Conditions Known)
3. Guess or Update Temperature, Composition and Pressure at End of Increment and Determine Reaction Rates at End of Increment
4. Calculate Average Reaction Rates
5. Using Average Rates do:
 - A. Material Balance
 - i. Component Balance
 - ii. Pressure Drop Calculation
 - iii. Material Balance
 - B. Heat Balance
 - i. Sensible Heat Gain

ii. Heat Flux Calculation Using $T=f(z)$

6. Compare End Conditions. (if in agreement with set used (go to step IX-7) otherwise (go to step IX-3)
7. Calculate Next Reactor Increment Using End Conditions as initial Conditions
 - a. If Finished the Length of the reactor, Go to Step X.
 - b. Otherwise - step IX-3

STEP X Using the Reactor Fluid Temperature Profile, Calculated in Step IV, Calculate Isothermal Area Temperature for Each Isotherm in each Furnace subsection.

STEP XI Calculate New Surface and Gas Volume Temperatures Using the Isothermal Temperature Calculated in Step X or Step XI-3

1. Total interchange area for real gas (temperature dependent) 1 corrected for intermediate surface if any transmissivity

a. Surface to Gas $SG = \left[\sum_n A_n \cdot SG_n \right] T$

b. Surface to Surface $SS = \left[\sum_n SS_n \cdot SS_n + (1 - \sum_n a_n) SS_c \right]$

2. Total interchange area for real gas (temperature dependent) 2 Corrected for intermediate surface, if any transmissivity

$$a. \text{ Gas to Gas } GG = \left[\sum_n GG_n \right] \uparrow$$

$$b. \text{ Gas to Surface } GS = \left[\sum_n \cdot GG_n \right] \uparrow$$

3. Gas Volume Heat Balance

a. Surface area temperatures are assumed constant

b. Heat Balance

i. Bulk Flow

ii. Radiation

iii. Source

iv. Convection

c. Linear Heat Balance Equation Using Iterated Newton-Raphson

d. Solve for T

e. Update Gas Volume Temperature

f. Test the Size of the max T

4. Surface Area Heat Balance

a. Gas Volume Temperatures are assumed Constant

b. Heat Balance

i. radiation

ii. Sources

iii. Convection

c. Linearize Heat Balance Equation Using Iterated Newton-Raphson (as in Step XI-3c)

Chapter IV
Results and Conclusions

The calculation procedures described in the first three chapters were used to make a parameter study of a typical large scale industrial furnace producing ethylene and propylene (as a secondary product).

The chief parameters which were adjusted were the fuel rate and the wall to wall separation. The results obtained were compared with plant observations. It should be realized that an exact matching of the two is difficult in view of the errors in plant measurements and the uncertainties in the value of kinetic data, emissivities, and other physical properties of furnace and reactor.

The values of yields obtained have good agreement with data obtained with adjusted of the Arrhenius frequency factor (A_i). As these adjustments were in the unimportant side reactions, it was decided to perform the optimization with the unadjusted constants.

Comparing the overall furnace performances was somewhat more difficult as these results are highly dependent on the physical properties of the furnace being studied. The author was unable to locate any data from industrial furnaces with sufficient amount of detail to duplicate the calculations. However, excellent agreement was found with general operating

conditions of industrial plants. The point of optimum operation determined in this study corresponds to actual operating conditions found in existing furnaces.

1. Verification of Results

The results from this study were compared with results reported by two other investigators, Shah⁽⁷⁰⁾ and Nelson⁽⁵⁴⁾

Shah had simulated a reactor system using the method of Lobo⁽⁴⁶⁾ to calculate the outer tube wall temperature. Shah then adjusted the Arrhenius rate constant to force agreement of his results with data he had available.

Nelson reported data from a variety of industrial furnaces. As a result, the individual furnace characteristics are not available.

Table I shows a comparison of Shah, Nelson and results from this study. It should be noted that good agreement exists between Shah's results and the results reported in this study. There is some disparity in the reported outlet temperature. The two cases reported in this table represent different rates of firing. The two rates bracket the firing rates found in some industrial furnaces is in excellent agreement.

The operating point of the industrial furnaces as reported by Nelson was in agreement with the optimum operating report as developed in this study.

TABLE I
 COMPARISON OF RESULTS OF THIS STUDY WITH SHAH (70) AND
 NELSON (54)

	Shah's Results	Nelson Reports	Robertson Case 1	Robertson Case 2
Heat Availability 10 ⁶ BTU/Hr.-Foot Furnace	-	-	2.86	3.22
Total Feed (lb/ moles/hr.)	171	-	280	280
Steam-Feed Ratio	.363	.3 - 1.1	.35	.35
Inlet Pressure (atm.)	4.43		6.6	6.6
Outlet Pressure (atm.)	?	1.2 - 3	2.0	2.2
Reactor Length (feet)	394	-	400	400
Tube Radius (inches)	?	-	4	4
Gas Inlet Temperature °F	1010°	-	1012°	1012°
Gas Outlet Temperature °F	1400°	1515-1525°	1544°	1560°
Mole % Ethylene Yield	47.6%	58 - 62%	52.48%	60.05%
Mole Ratio Methane/Ethane (+)	.0177	.025-.067	.0142	.0157
Mole Ratio Acetylene/Ethane (+)	.00053	.0014	.00101	.00145
Thermo Efficiency Ratio BTU to Reactor/ BTU Fired	-	-	.350	.315

2. Furnace Temperature Driving Force

Figure 6 shows a typical temperature driving force calculated by the procedure outlined in this study.

It should be noted that fluctuations ranging up to 790°F are found between adjoining gas zone isotherms. Differences of 1100°F exist between the highest and the lowest isothermal temperature zones.

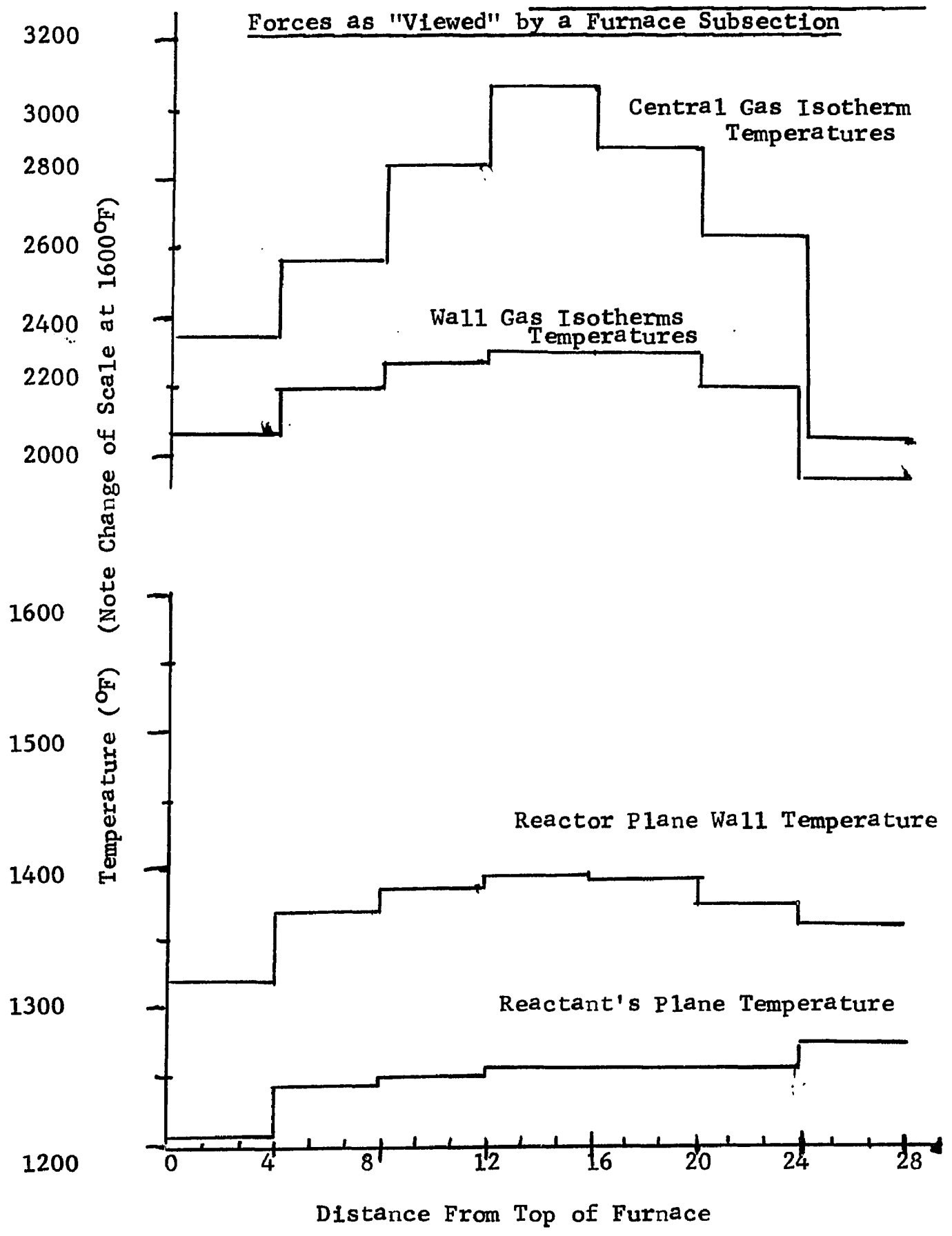
The large differences calculated are a strong justification for the use of this complex procedure, especially when highly temperature dependent calculations are being used.

It is also interesting to note that the temperature driving force between the tube wall "plane" and the process "plane" is not constant, but is dependent on tube height.

Normally the process plane temperature would be nearly constant at the average temperature of the process fluid. However, in this example there is an increase near the bottom of the furnace due to an uneven number of tubes in this subsection.

Figure 7 is a numerical example of the temperature driving force in each of the three furnace subsections.

Figure 6. Typical Temperature Driving Forces as "Viewed" by a Furnace Subsection



Each subsection represents only half of the plane of the furnace subsection (the missing half would be symmetrical to that shown).

Several interesting observations may be drawn from this figure:

1. Once again, considerable temperature differences exist between adjoining isothermal zones in different furnace subsections.

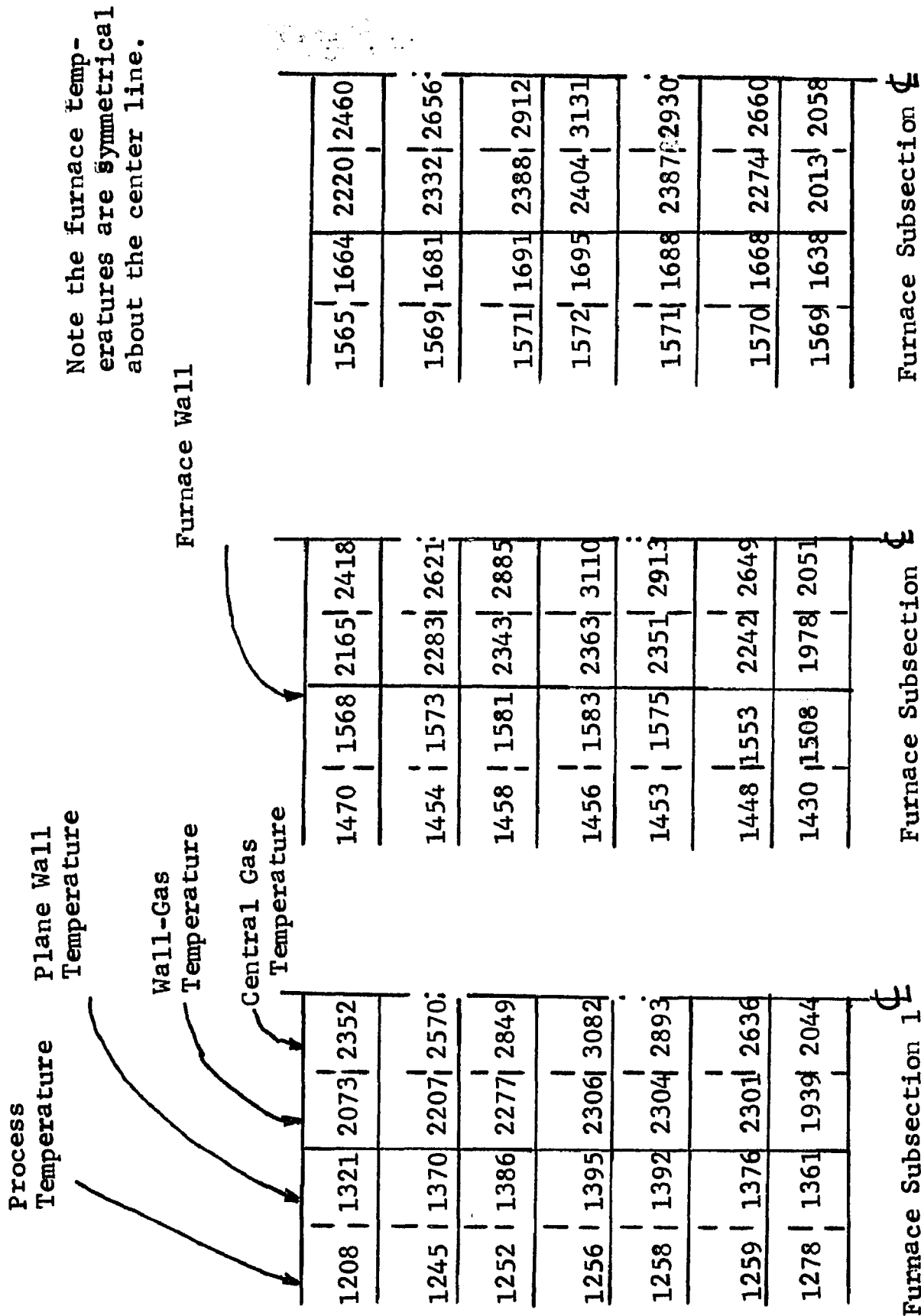
2. The temperature of the central isothermal zone shows only relatively small variation from subsection to subsection.

3. Considerably larger temperature fluctuations exist in those isotherms abutting the furnace wall. This is important as these isotherms act as the chief driving force for convective heat transfer. It has been generally accepted that radiation is the dominant mode of heat transfer in the fire box. The results of this study suggest that convection also plays a significant role. It should be given consideration in the design of an "optimum furnace."

The use of a single gas isotherm for the entire furnace zone would do a poor job at estimating the importance of the convected heat transfer.

Figure 7

Temperature Profile in Furnace Subsection in (°F)



3. Convected Heat Transfer in the Radiant Section of the Furnace

In order to dramatize the effect of convected heat transfer, a series of calculations were made which varied the wall to wall separation. During the first set of calculations, no correction was made to the gas to surface heat transfer coefficient. (Normally as the walls of the furnace get closer together retaining the same fuel consumption rate, the convected heat transfer coefficient would increase according to the .8 power of the bulk flow rates.)

The result (See Figure 8 and Table 2) was an increase in reactor yield with increasing wall separation. The result is a representation of an isolation of the radiative heat transfer rate which would increase as the surface area is able to view larger sections of the flame boundary at less oblique angles.

If the distance separating the wall continued to increase, the rate would ultimately drop off as the area would "view" a line source of radiation.

In the second set of calculations, the surface to gas volume heat transfer coefficient was corrected for bulk flow consideration. (See Figure 9 and Table 3.) The results were reversed, with the closer the wall to wall separation, the higher the yield for the same amount of fuel fired.

Table 2

Effect of Wall Separation on Reactor Yield Radiation Effects
Isolated by Using Uncorrected Surface to Gas Heat Transfer
Coefficient

Heat Availability 2.142×10^6 BTU/hr.-foot(furnace)

<u>Wall-Wall Separation Feet</u>	<u>% Yield Ethylene</u>	<u>Uncorrected Heat Transfer Coefficient Area Base BTU/hr °F/ft</u>
6	32.27	3.14
8	32.52	3.14
10	33.20	3.14
50	37.16	3.14

Table 3

Effect of Wall Separation on Reactor Yield Using Corrected
Surface to Gas Heat Transfer Coefficient

Heat Availability 2.142×10^6 BTU/hr.-foot^{1/2}furnace

<u>Wall-Wall Separation Feet</u>	<u>% Yield Ethylene</u>	<u>Corrected Heat Transfer Coefficient (Area Bases) BTU/hr °F/ft</u>
6	34.35	4.73
8	33.83	3.76
10	33.20	3.14
14	31.95	2.40
18	31.59	1.96

Figure 8.

Effect of Wall to Wall Separation on Ethylene Yield
 (Radiant Effect Isolated - No Adjustment of Gas to Wall
 Heat Transfer Coefficient)

Heat Available 2.142×10^6 BTU/Hour - Foot Furnace

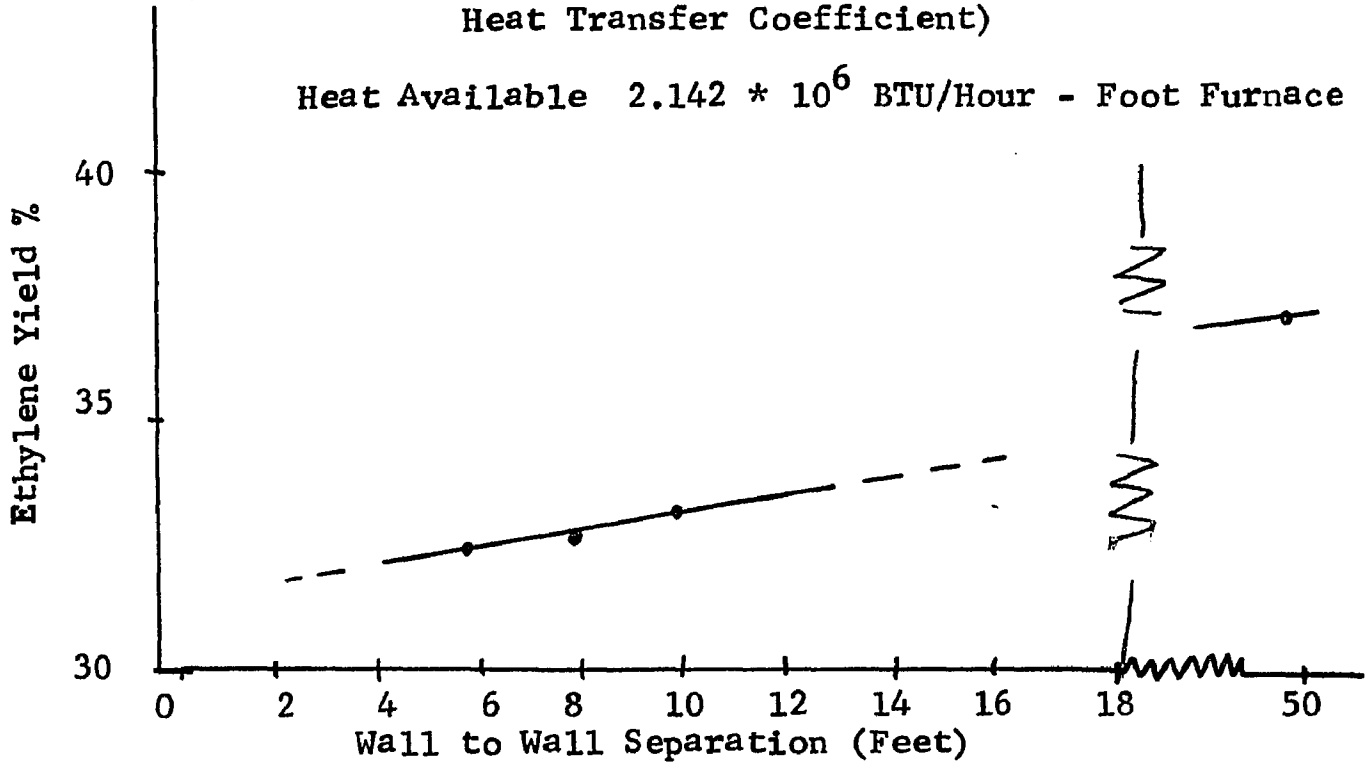
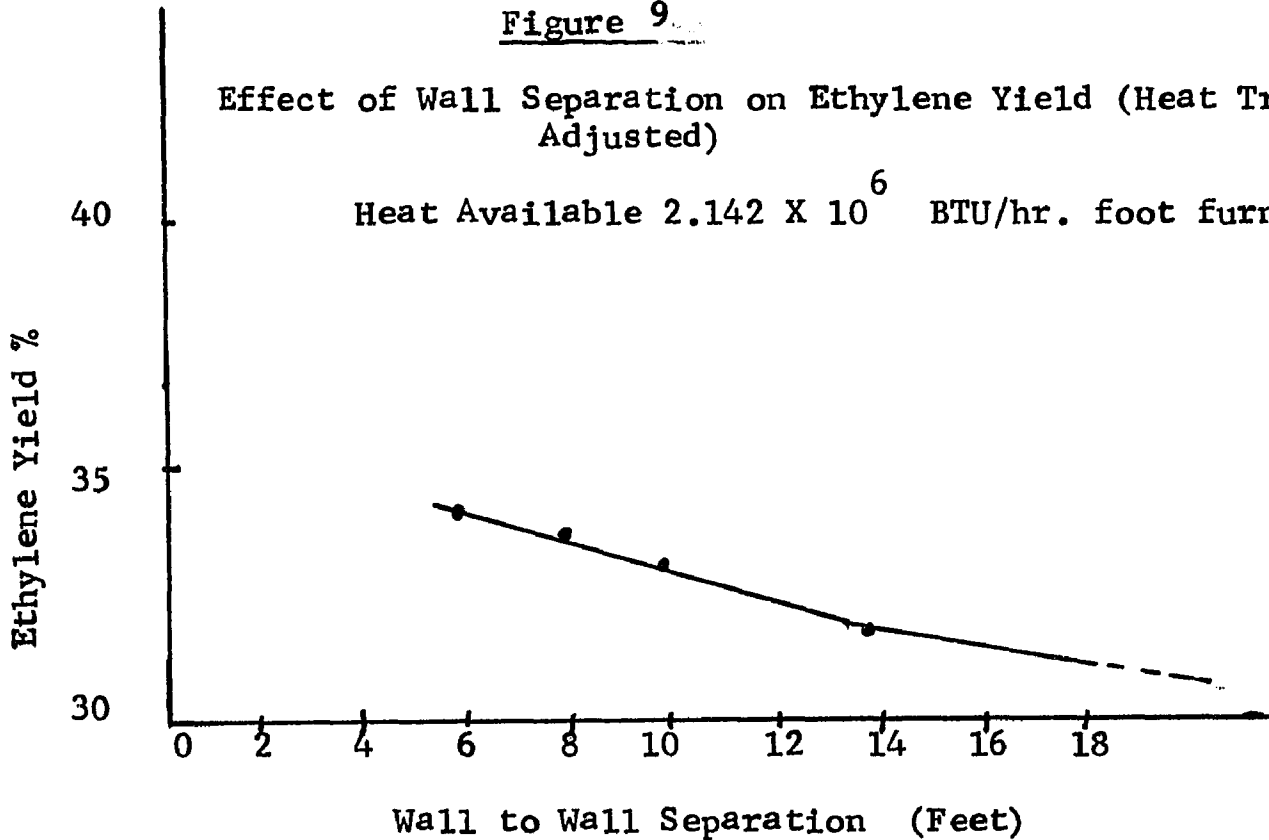


Figure 9

Effect of Wall Separation on Ethylene Yield (Heat Transfer
 Adjusted)

Heat Available 2.142×10^6 BTU/hr. foot furnace



This would suggest that optimum furnace construction should have the walls as close as possible while allowing sufficient volume for the complete combustion of the fuel.

The above discussion did not allow for the introduction of more isotherm~~o~~l zones as the wall separation was increased. It is likely that if such a procedure had been followed, the effects would have been less pronounced, but still valid.

4. Optimization of the Furnace-Reactor as a Function of Fuel Rate

Several sets of calculations were performed varying the net heat availability (E_t). The ethylene yield was then plotted as a function of net heat availability (Figure 9). The wall to wall separation was kept constant at 10 feet, 10 ft. separation being used as a basis for all variations.

Figure 10 and Table 4 predict the possibility of ethylene yields in excess of 70% per pass. There are, however, two main reasons why this yield is not practical.

The first reason is illustrated in Figure 10 which shows the rate of ethylene production in terms of pounds of ethylene produced/pound of fuel consumed versus net heat availability of the furnace. The plot goes through a

Table 4

Effect of Heat Availability on Reactor Yield for
10 Foot Wall - Wall Separation

<u>Heat Availability</u> <u>BTU/hr, Foot Furnace</u> <u>X 10⁶</u>	<u>% Ethylene</u> <u>Yield</u>	<u>Surface to Gas Heat Trans-</u> <u>fer Coefficient* Adjusted</u> <u>Area Bases BTU/hr. F/ft.</u>
1.79	23.18	2.72
2.14	33.20	3.14
2.50	43.42	3.55
2.86	52.48	3.95
3.22	60.05	4.35
3.57	66.67	4.73
3.93	72.14	5.10

*Adjustment takes into consideration increase in flue gas velocity due to increase in fuel fired.

Figure 10
Ethylene Yield as a Function of
Heat Availability

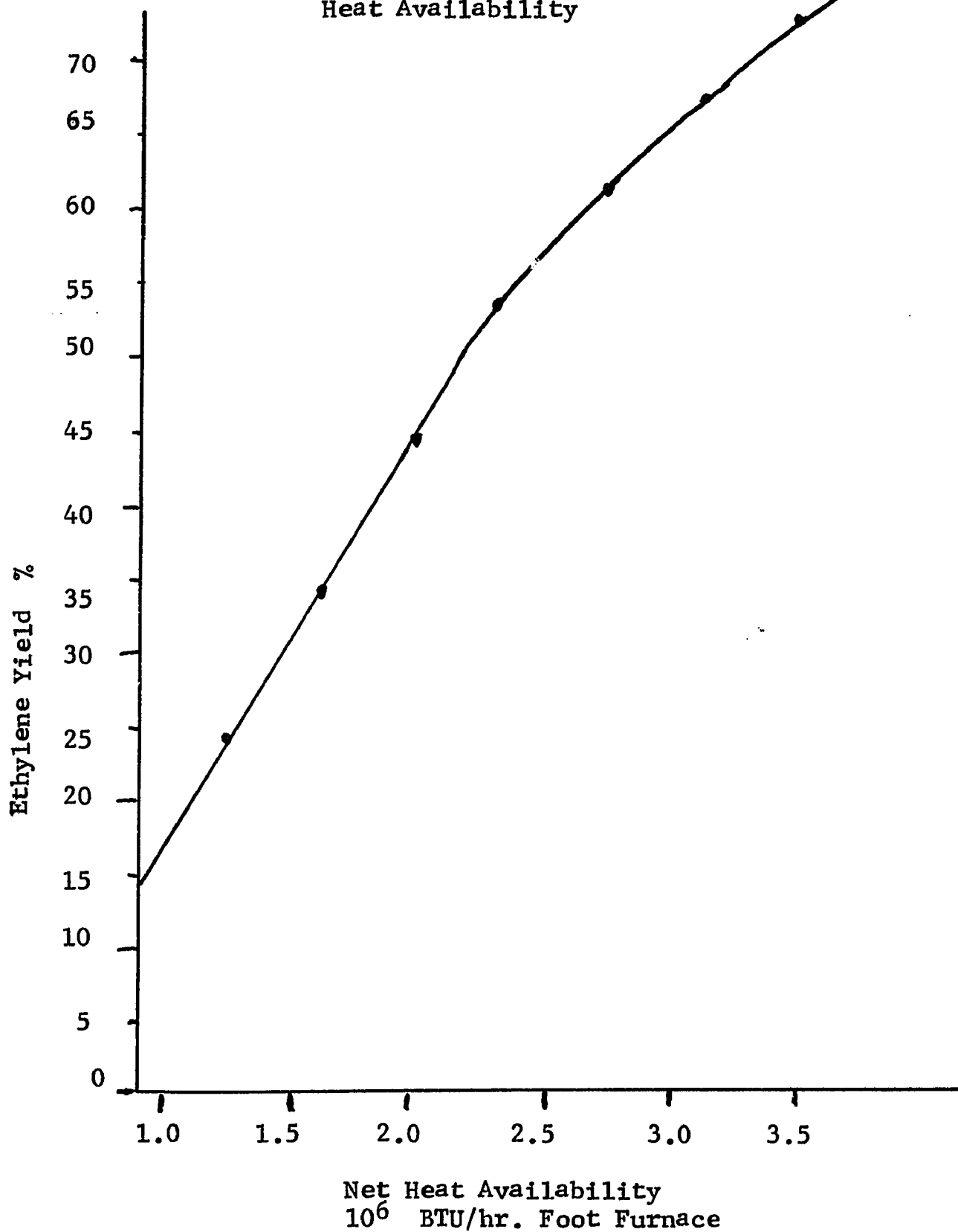


Figure 11

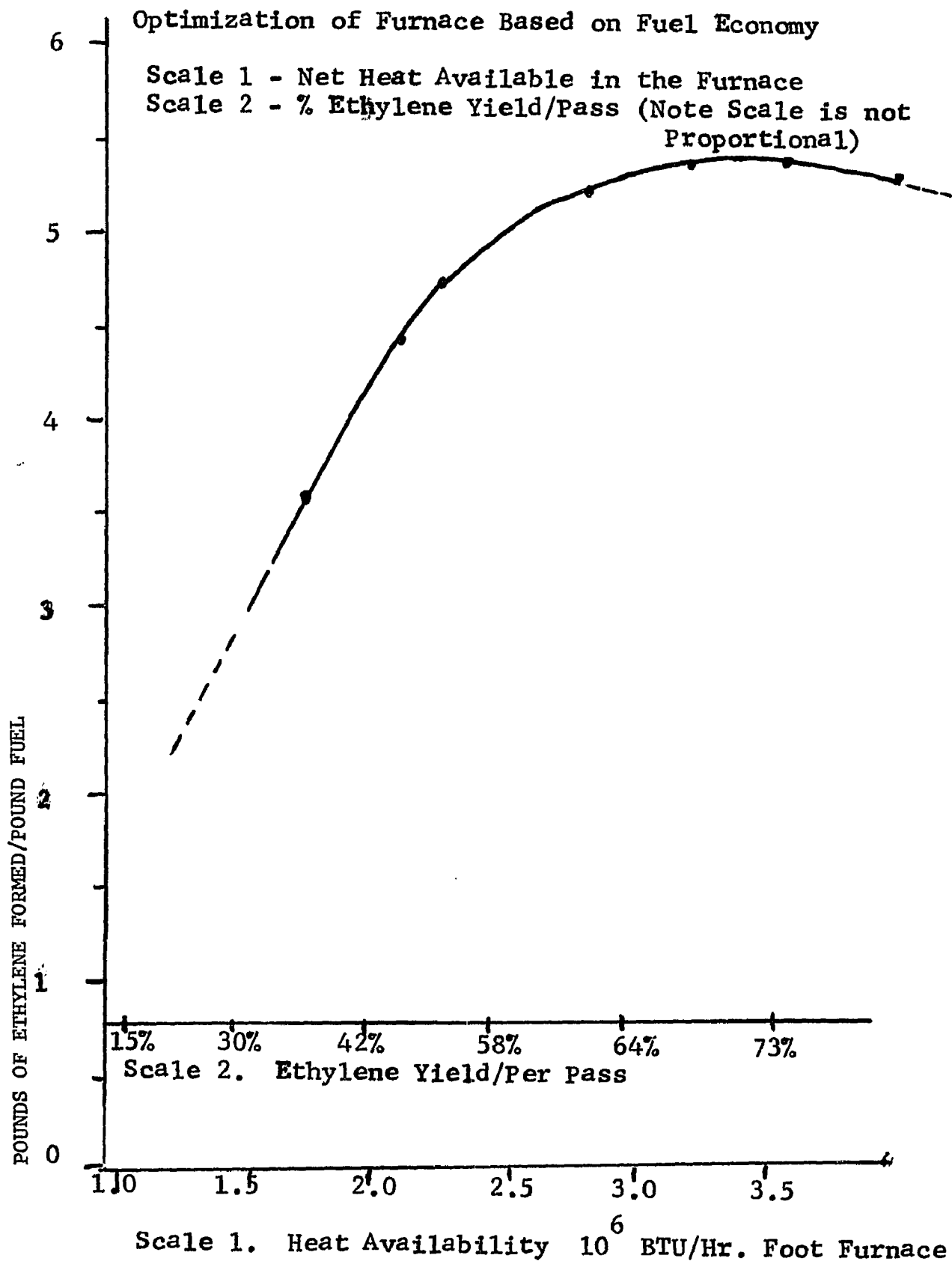
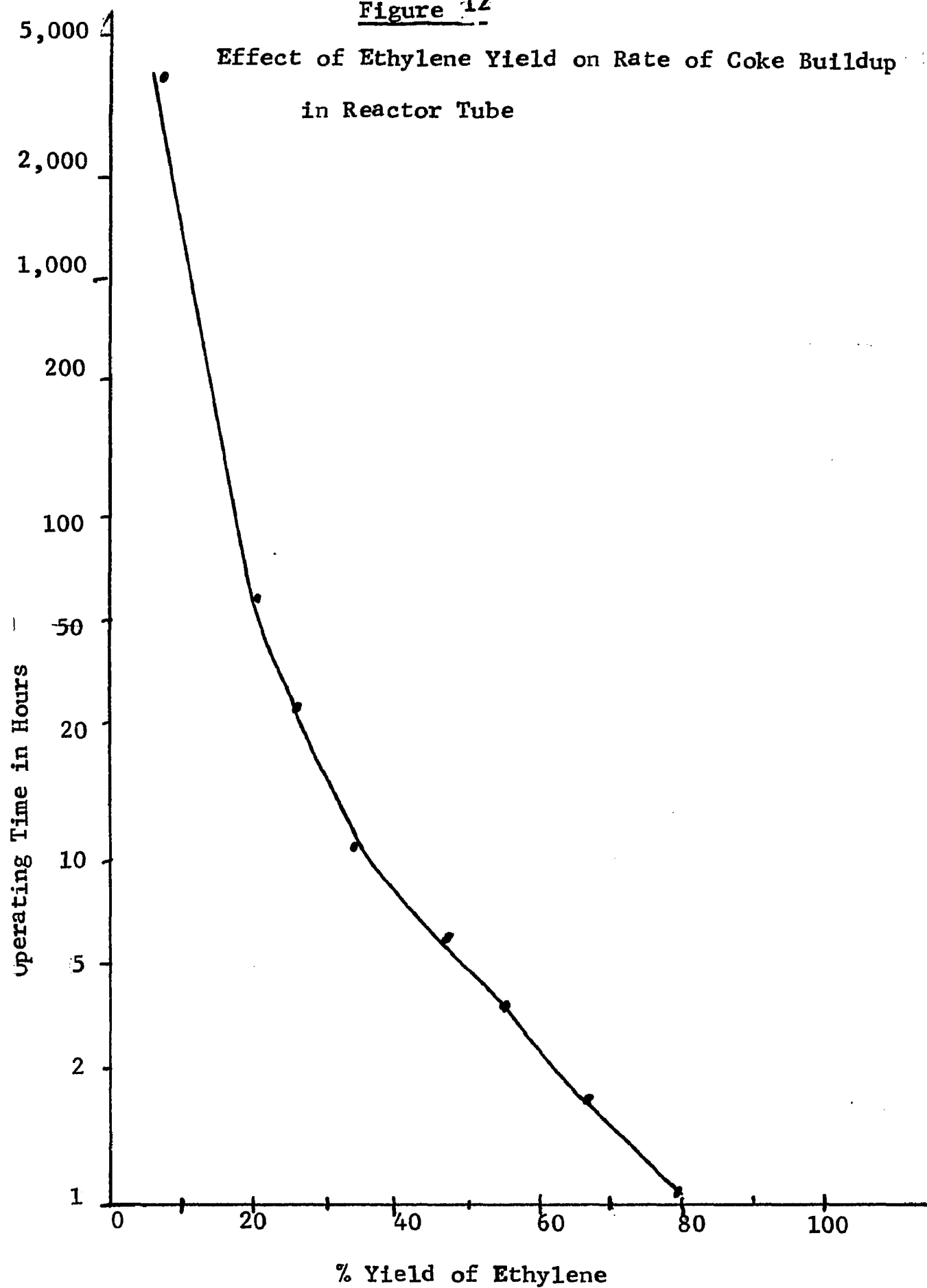


Figure 12

Effect of Ethylene Yield on Rate of Coke Buildup
in Reactor Tube



maximum. The curve is flat near the top, however, and at first consideration it would be possible to assume yield of 65-70% would be possible. This would correspond with an optimum fuel economy of 5.4 pounds of ethylene/pound of fuel consumed.

Figure 12 however, shows that the rate of coke buildup in the pyrolysis tubes becomes very rapid when large yields of ethylene are desired. A yield of 65-70% would necessitate the cleaning of the reactor every 3-4 days. A 40% yield with a corresponding fuel economy of 4.1 pounds of ethylene/pound of fuel would result in a reactor requiring cleaning only every 18 - 20 days.

If a manufacturer wishes to obtain the higher fuel economy predicted in this study, clearly something would have to be done about the coke buildup. One possible solution lies in the supersonic oxidative pyrolysis of Vasil'ev (90) or his subsonic oxidative pyrolysis (89) which incorporated the introduction of oxygen into the reactant stream. This resulted in a blocking of the coke reaction and 58% yields of ethylene.

Chapter V
Recommendations

The computational procedures developed in this study are very extensive, enabling the handling of complex furnace-reactor design. The furnace design utilizes the complex method of Hottel and Cohen in handling zoned furnaces. It incorporates several suggestions of Cohen, notably the evaluation of the gas emissivities and absorption at individual zone temperatures instead of a system mean temperature.

There are, however, important limitations:

1. The furnace was assumed to be infinite in length, thus no end effects were taken into consideration. The subdivision of the furnace into furnace subsections enabled the handling of variable wall fluxes, but allowed no interreaction between subsections.

2. The zones in the system have been assumed to be isothermal. The solution could only become exact as the size of the zones are shrunk to infinitesimal size.

3. The reactor model calculates coke deposit as a function of reaction rate. No mechanism was supplied to allow a portion of the coke to be carried out of the furnace. The exact mechanism of coke formation is not known. It has been considered to be catalytic in nature.

This depends on whether sufficient deposition takes place on the bare metal of the reactor or on other coke deposits.

4. The reactor increments were to have uniform average properties. The solution could only become exact as the increments are shrunk to infinitesimal size.

It is therefore recommended:

1. To take end effect into consideration in order to make a "true" three dimensional model.
2. To determine the exact nature of the coke formation.
3. To apply the calculation procedure to a large variety of furnaces with the objective of formulating a general correlation which would allow for rapid estimation of design criterion.
4. To apply the calculation procedure to the optimization of existing furnace-reactor structures.
5. To design optimum furnace configurations by repeated application of the calculation procedures.

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APPENDIX ATABLE OF NOMENCLATURE

- Area of a surface, square feet; A_1 , A_2 area of a source-sink surface; A_{s_1} , A_{s_2} , area of surface zones s_1 , s_2 ,
- AMWT Average molecular weight of reacting system
- B Normal distance between differential radiating volume elements and a plane, feet
- B(I,K) Coefficient of component in K^{th} position I^{th} reaction
- BB(I,K) Order of reaction of component in I^{th} position K^{th} reaction
- C Convective-flux coefficient, square feet, C_g evaluated at T_g , C_s evaluated at T_s
- c Exponent on temperature ratio in obtaining G from G' dimensionless
- c Heat capacity, B.t.u./lb., $^{\circ}\text{F}$.
- C(J) Concentration of J^{th} component (lb. moles/ft.³)
- CF Temporary constant used in calculating the product of concentration raised to order of reaction components in the forward direction
- CLJ(J,1) Constant of Lennard and Jones - collision diameter $(A) J^{\text{th}}$ component

- CLJ(J,2) Constant of Lennard and Jones - $\frac{1}{K-(^{\circ}K)^{J^{\text{th}}}}$
component
- CP(J,1-4) Heat capacity data for J^{th} component $C_p = CP(J,1) + CP(J,2)*T + CP(J,3)*T^2 + CP(J,4)*T^3$ (BTU/lb. mole $^{\circ}F$)
- CR Temporary constant used in calculating the products of concentration raised to the order of reaction of each reaction component in the reverse direction
- CT = C(J) (lb. moles/ft.³)
- D = MAX(ABS(DXA(I))) i.e. the max of the absolute incremental change of reaction
- D Basic determinant for the system of simultaneous equations used to obtain total interchange factors
- $\epsilon_i^D \epsilon_j$ Determinant formed by replacing the ϵ_j -column of D by a column of ϵ_i -functions
- d $\frac{\ln G}{\ln PL}$, dimensionless
- DCP(I,1-4) = $\frac{SR(I)}{K-SF(I)+1} \frac{B(I,K)}{B(I,1)} CP(I,1-4) - \frac{SF(1)}{K=1}$
(BTU/lb. mole $^{\circ}F$) (1)
- $\frac{B(I,K)}{B(I,1)} CP(I,1-4)$
(i.e.) Summation of heat capacity of products - heat capacity of reactants

- DF(I) Summation of free energy of products - free energy of reactants I^{th} reaction (BTU/lb. mole)
- DH(I) Summation of heat of formation of products - heat of formation of reactants (BTU/lb. mole)
- DS(I) Summation of entropy of products - entropy of reactants (BTU/lb. mole)
- EA(I) Arrhenius frequency factor of I^{th} reaction
- EE(I) Arrhenius activation energy of I^{th} reaction (cal/m)
- E Radiation-emission rate, energy per unit time;
 E_{g_1}, E_{g_2}, \dots from surface zone s_1, s_2, \dots
- E Eddy diffusivity, square feet per hour
- F View Factor = Fraction of radiation from one surface zone intercepted by another surface zone in the presence of a non-absorbing medium, dimensionless;
 $F_{s_1 s_2}$ from surface s_1 to s_2
- F Fraction of energy from a point radiating source absorbed by a sphere of gas, dimensionless; F_1 intercepted by a portion of spherical surface F_2 absorbed by a portion of a spherical shell
- f Fraction of radiation originating in one zone which reaches and is absorbed by another zone in a black-walled enclosure, dimensionless; f_{ss} between two

- surface zones, f_{gg} between two gas zones, f_{sg} from a surface zone to a gas zone; f_{gs} from a gas zone to a surface zone
- F(J)** Factor by which the Arrhenius frequency factor is changed - assumed to be one
- FI(I)** Constant of integration used in calculating the equilibrium constant
- GC** Gas constant = 1.341 At/lb mole $^{\circ}K$
- G_m** Molal flow rate per unit area mols/hr. sq. ft.
- GG** Total interchange factor between any two gas zones including reflections at all surfaces, square ft.; G_{12} (G_{21}) is equal to $q_{g_1 g_2} / W_{g_1}$ or $q_{g_2 g_1} / W_{g_2}$
- GS** Total interchange factor between any gas and surface zone including reflections at all surfaces, square feet; G_{1s_1} ($S_{11} G$) is equal to $q_{g_1 s_1} / W_{g_1}$ or $q_{s_2 g_1} / W_{s_1}$
- g** Gas zone with a numerical subscript to designate the particular zone under consideration
- gg** Direct interchange factor between any two gas zones, square feet; g_{12} (g_{21}) is equal to $(q_{g_1 g_2})_{direct} / W_{g_1}$ or $(q_{g_2 g_1})_{direct} / W_{g_2}$

- g_s Direct interchange factor between any gas and surface zone, square feet; g_{1s_1} (s_1g_1) is equal to $(q_{s_1})_{\text{direct}}/W_{g_1}$ or $(q_{s_1g_1})_{\text{direct}}/W_{s_1}$
- H_{ex} Total enthalpy of entering fuel and air per unit time, B.t.u./hr.
- H_g Enthalpy-flux coefficient evaluated at T_g , square ft.
- h_c, h_c', h_c'', h_c''' Convective coefficient of heat transfer, B.t.u./hr. sq. ft. $^{\circ}\text{F}$
- h Enthalpy content, B.t.u./mol; h_s sensible enthalpy; h_{ch} chemical enthalpy
- HR Number of hours in which carbon has been accumulating
- HT(J) Heat of reaction of the (J) component (BTU/lb. mole)
- I Temporary storage to denote I^{th} reaction
- IA(I,K) Used to identify J in the reaction species in the I^{th} reaction the K^{th} position (i.e. $J=IA(J,K)$)
- IB Number of increments the reactor will calculate before it is forced off
- K, K' Correction factors by which to multiply $T_{\text{avg.}}$, dimensionless.
- k Absorption coefficient of a gas, ft.^{-1}
- L Mean beam length for gas radiation, feet.
- P Pressure, atmospheres; P_w partial pressure of water vapor; P_c partial pressure of carbon dioxide; P_g gas pressure

- P Dimensionless ratio r/δ for evaluating f_p
- P(J) Pressure of J component (at.)
- PD Pressure drop increment (in at.)
- PDIP Initial incremental pressure change used in convergence (at.)
- PI Pressure into reactor (at.)
- P OUT Pressure out of reactor (at.)
- PPI(J) Initial pressure of Jth component (at.)
- Pr Prandtl Number ν/k , dimensionless
- Heat transfer rate, B.t.u. per hour; $q_{1,2}$ net between surfaces 1 and 2; $q_{1,G}$ net between surface 1 and the gas; q_{g_i,g_1} one-way from g_i to g_1 ; q_{s_j,g_1} one-way from g_i to s_1 ; q_{B,g_1} net to g_1 by bulk transport; q_{C,g_1} net to g_1 by convection; q_{C,s_1} net to s_1 by convection; q_{w,s_1} net through surface s_1 .
- R Relative flux density, dimensionless; $s_1 R_{s_2}$, flux density away from s_2 , due solely to radiation originating at s_1 , and expressed as a ratio to W_{s_1} ; $g_1 R_{s_2}$, same, but due to radiation originating in gas zone g_1 .
- R Gas constant 1.987 cal/gram mole $^{\circ}K$
- r Linear distance between two elements (feet)
- RA Rate of reaction
- RAD Radius of the reactor (feet)

RADD(I)	Radius of reactor at 1% temporary storage
RADF(I)	Radius of reactor at 1% previously calculated
RADI(I)	Radius of reactor at 1% presently being calculated
RADU	Original radius of clean reactor (feet)
RAF	Original radius of clean reactor (feet)
RATE	Total rate of reaction
Re	Reynolds Number DG/μ , dimensionless
SS	Total interchange factor between any two surface zones including reflections at all surfaces, sq. ft. $S_1 G_1$ ($G_1 S_1$) is equal to $q_{s_1 g_1} / W_{s_1}$ or $q_{g_1 s_1} / W_{g_1}$
s	Surface zone with a numerical subscript to designate the particular zone under consideration
sg	Direct interchange factor between any surface and gas zone, sq. ft; $s_1 g_1$ ($g_1 s_1$) is equal to $(q_{s_1 g_1})_{\text{direct}} / W_{s_1}$ or $(q_{g_1 s_1})_{\text{direct}} / W_{g_1}$
ss	Direct interchange factor between any two surfaces, sq. ft.; $s_1 s_2$ ($s_2 s_1$) is equal to $(q_{s_1 s_2})_{\text{direct}} / W_{s_1}$ or $(q_{s_2 s_1})_{\text{direct}} / W_{s_2}$

- SR(I) (Integer) number of components in Ith reverse reaction
- T Temperature, °R; T_{g_1} , T_{g_2} , ... of gas zone g_1 , g_2 , ... ; T_{s_1} , T_{s_2} , ... of surface zone s_1 , s_2 , ...; T_G and T_S of gas and surface respectively; T_1 and T_2 of surfaces 1 and 2
- T Temperature of reactor (any point) (°F)
- TIN Temperature of inlet conditions (°F)
- TMPH Total moles per hour (lb moles/hour)
- TMPHI Initial molar flow rate (lb. moles/hour)
- U Over-all coefficient of heat transfer through a wall, based on inside surface and outside air temperatures, B.t.u./hr. sq. ft.°F
- V Gas volume cubicfeet
- VELI Velocity of gas at any point in reactor (ft/sec)
- VC(J,L) Concentration of component J at L% into reactor
- W Rate of emission from a unit area of a black-body at the temperature indicated by a subscript (W_{g_1} at the temperature of g_1), B.t.u./hr. sq. ft.
- WDZA(I,L) Rate of reaction I at distance L% into reactor
- WPJ(L) Pressure L% into reactor (At)
- WT(L) Temperature L% into reactor (°F)
- WTM(J,L) Total mole/hour of component J, L% into reactor

WTMPH(L)	Total mole/hour L% into reactor
VVELI(L)	Velocity ft/sec L% into reactor
WZIC(L)	Length ft L% into reactor
X	Used as temporary in calculating heat of reaction, heat capacity
XN	Used to calculate temperature profile in reactor
x_1, x_2	Thickness of gas layers, feet.
x, y, z	Linear dimensions along the three coordinate axes, ft
α	Absorptivity, dimensionless, α_s of a gas for surface radiation; α_x of a gas of path length x , α_s of a surface.
$\alpha, \beta, \delta, \gamma$	Positional parameter indicating the magnitude and direction of bulk flow heat exchange between gas volumes
γ	Factor by which to multiply center-to-center distance between two zones to obtain correct mean beam length between them for radiation, dimensionless.
γ	Emission coefficient, sq. ft. $\gamma_g = 4kaV_g$; $\gamma_s = \epsilon_s A_s$
Δ	Denotes a difference
Δ	Determinant formulation of energy balances
ϵ	Emissivity, dimensionless; ϵ_s of a surface; ϵ_g or ϵ_g of a gas; $\epsilon_{T_{avg}}$ evaluated at the arithmetic mean of the gas and surface temperatures; ϵ_x of path

length x ; $\epsilon_1, \epsilon_2, \dots$ of a gas at PL_1, PL_2, \dots

 F

Overall interchange factor, dimensionless; F_{1G} = radiation reaching gas and F_{12} radiation reaching surface A_2 , due to original emission from A_1 only, but including assistance given by reflection at all surfaces, expressed as a ratio to σT^4

 ϕ

Angle between line joining centers of two zones and the normal to a surface, radians.

 ϕ_1, ϕ_2

Angles used in evaluation of f_p , radians

 μ
 ν

Viscosity, lb/ft. hr.

Emissivity of a gas on a volume basis, ft.⁻¹

 ρ

Density, lb/cu. ft.

 ρ_s

Reflectivity of a surface, dimensionless

 σ

Stefan-Boltzmann constant = 0.1713×10^{-8} B.t.u./hr. sq. ft. °R⁴

 τ

Gas transmissivity, dimensionless; τ_x of path length x

 ψ

Escape factor for radiation from a cube of gas (ratio of energy leaving boundaries to energy originating within volume), dimensionless

 θ_1, θ_2

Angles between radiant beam and normals to a surface, radians

 ω

Solid angle, steradians

Appendix B

Computer Program


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1 PROGRAM MAIN MAIN 1
2 COMMON/ZZREAD/ID MAIN 2
3 COMMON/TIME2/TIME,TX(100),QT(4),QFF MAIN 3
4 COMMON/ANVDV1/TPL(60),TP2(60),TP3(60),I1(60),I2(60),I3(60) MAIN 4
5 I=1,H1(60),H2(60),I3(60) MAIN 5
6 COMMON/URNXY(40),URBANT MAIN 6
7 DIMENSION ID(105),TXF(85),TXFOLD(85),TXOLD(85),QF(4) MAIN 7
8 DEFINE FILE 20(2400,41,0,0,0),21(4800,61,0,0,0),22(4800,61,0,0,0), MAIN 8
9 I 1 23(18,40),U,10),24(2400,61,0,0,0),25(4800,61,0,0,0) MAIN 9
10 DATA ID , /1,12,25,30,100,212,14,24,25,31,15,23,27,4,10,16, MAIN 10
11 /2,28,5,9,17,21,29,0,0,0,13,20,20,7,19,31,100,100, MAIN 11
12 /37,49,61,100,100,36,38,48,50,60,35,39,47,51,59,34,40, MAIN 12
13 /46,52,58,33,41,45,51,57,32,42,44,54,56,31,43,55,100,100, MAIN 13
14 /61,73,85,100,100,62,72,74,84,100,63,71,75,83,100,84,70, MAIN 14
15 /78,82,100,65,69,77,81,100,66,68,78,80,100,67,79,100,100, MAIN 15
16 /6,100/ MAIN 16
17 C CALL ERRSET(209,,1,0,0,0) MAIN 17
18 CALL READ(4,1,START,URBANT,URNXY(I),400) MAIN 18
19 CALL ZERO(TPL(1),540) MAIN 19
20 READ(1,904)(I1,I1,I1,22),I2(I1,I1,I1,22),I3(I1,I1,I1,22) MAIN 20
21 C T1 T2 T3 ARE THE THREE ASSUMED OUTER WALL REACTOR TEMPERATURE PROFILES MAIN 21
22 P2=3,1,1,1592672. MAIN 22
23 READ(5,904)ITREC MAIN 23
24 C DIRECT IS THE CONVERGENCE CRITERION FOR THE REACTOR IN KELVIN DEGREES MAIN 24
25 CALL FOUR MAIN 25
26 I=1 MAIN 26
27 NP=INT=1 MAIN 27
28 NSURE=22 MAIN 28
29 CALL WRITE(3,ITEM1,T1(1),60) MAIN 29
30 CALL WRITE(3,ITEM2,T2(1),60) MAIN 30
31 CALL WRITE(3,ITEM3,T3(1),60) MAIN 31
32 CALL EVAL MAIN 32
33 CALL REAR(2,INCP ,H1(1),60) MAIN 33
34 CALL REAR(2,INCP ,H2(1),60) MAIN 34
35 CALL REAR(2,INCP ,H3(1),60) MAIN 35
36 DO 1000-1000=1,10 MAIN 36
37 IJ=1 MAIN 37
38 DO 10 I=1,15 MAIN 38
39 TXOLD(I)=TX(I) MAIN 39
40 IJ=TX(I)*I MAIN 39
41 WRITE(6,901)TXF MAIN 41
42 TX(100)=0.0 MAIN 42
43 J1=0 MAIN 43
44 DO 2 J=9,15 MAIN 44
45 X1=0. MAIN 45
46 X2=0. MAIN 46
47 X3=0. MAIN 47
48 DO 1 K=1,5 MAIN 48
49 J1=J1+1 MAIN 49
50 I1=I1(I1) MAIN 50

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51      I2=I0(J1+35)
52      I3=I0(J1+70)
53      IF(I1.NE.100)X1=X1+1.
54      IF(I2.NE.100)X2=X2+1.
55      IF(I3.NE.100)X3=X3+1.
56      TP1(J)=TP1(J)+IX(I1)
57      TP2(J)=TP2(J)+TX(I2)
58 1     TP3(J)=TP3(J)+IX(I3)
59      TP1(J)=TP1(J)/X1*1.8
60      TP2(J)=TP2(J)/X2*1.8
61      TP3(J)=TP3(J)/X3*1.8
62      TP3(J)=TP3(J)/X3*1.8
63      TP3(J)=TP3(J)/X3*1.8
64 2     TP3(J)=TP3(J)
65      CALL WRITE(2,ITEMP1,TP1(1),60)
66      CALL WRITE(2,HCPL,HI(1),60)
67      CALL FURJ1
68      QF(IJ)=QF
69      CALL READ(2,ITEMS1,T1(1),60)
70      DO 11 I=1,60
71 11     T1(I)=T1(I)/1.8
72      WRITE(6,905)IJ,(T1(I),I=1,NSURF)
73      CALL WRITE(3,ITEM1,T1(1),60)
74      CALL WRITE(2,HCPL,H2(1),60)
75      CALL WRITE(2,TEMP1,TP2(1),60)
76      IJ=IJ+1
77      WRITE(6,902)IJ,(TP2(I),I=1,NSURF)
78      CALL FURJ1
79      QF(IJ)=QF
80      CALL READ(2,ITEMS1,T2(1),60)
81      DO 12 I=1,60
82 12     T2(I)=T2(I)/1.8
83      WRITE(6,900)IJ,(T2(I),I=1,NSURF)
84      CALL WRITE(3,ITEM2,T2(1),60)
85      CALL WRITE(2,TEMP1,TP3(1),60)
86      CALL WRITE(2,HCPL,H3(1),60)
87      IJ=IJ+1
88      WRITE(6,902)IJ,(TP3(I),I=1,NSURF)
89      CALL FURJ1
90      QF(IJ)=QF
91      CALL READ(2,ITEMS1,T3(1),60)
92      DO 13 I=1,60
93 13     T3(I)=T3(I)/1.8
94      WRITE(6,900)IJ,(T3(I),I=1,NSURF)
95      CALL WRITE(3,ITEM3,T3(1),60)
96      INDI=1
97      CALL PYRJI
98      DO 101 I=1,22
99      T1(I)=T1(I)/1.8
100     T2(I)=T2(I)/1.8

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MAIN 51
 MAIN 52
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 MAIN 93
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 MAIN 99
 MAIN 100

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101 101 T3(I)=T3(I)/L8
102 102 A=400./84.
103 103 INO=2
104 104 DO 4 IJ=1,85
105 105 ZIC=A*FLGAT(I)-A
106 4 CALL TEMPI(IXE(I),ZIC,IAD)
107 107 WRITE(6,903)TXF
108 108 DO 3 IJ=1,3
109 109 H1=(IJ-1)*60+1
110 110 H2=H1+ISURE=1
111 3 WRITE(6,502)IJ,(TPI(I),I=H1,H2)
112 112 DT=0.0
113 113 DO 5 IJ=1,205
114 114 DT=A*MAX(DT,ABS(TX(IJ))-TX(IJ))
115 5 TXOLD(IJ)=TX(IJ)
116 116 IF(DT.LT.1E-2)GO TO 6
117 117 IF(DT.LT.1.0)GO TO 6
118 118 CALL PZERO(TPI(I),360)
119 119 WRITE(6,907)DT,I300
120 120 DO 100 IJ=1,ISURE
121 121 H1(IJ)=H1(IJ)*QT(1)/(QF(1)*5./3.)
122 122 H2(IJ)=H2(IJ)*GI(2)/(GE(2)*5./3.)
123 123 H3(IJ)=H3(IJ)*QT(3)/(QF(3)*5./3.)
124 100 CONTINUE
125 125 WRITE(6,908)H1(9),H2(9),H3(9)
126 1000 CONTINUE
127 127 WRITE(6,905)DT
128 128 GO TO 7
129 6 WRITE(6,906)I000,DT
130 900 FORMAT(//I1,20X,ISUREACE TEMPERATURE PROFILE FOR FURNACE SEGMENT,MAIN 130
131 1,110,1 DEG K,20X,60(1-1),/(25X,6F15.1))
132 901 FORMAT(//I11,20X,REACTION PROCESS TEMPERATURE PROFILE,1/20X,35(I=MAIN 132
133 1),20X,1DEG K,1,/(25X,6F15.1))
134 902 FORMAT(//I11,20X,IBCESS TEMPERATURE PROFILE FOR FURNACE SEGMENT,1,10MAIN 134
135 1,1 DEG K,20X,60(1-1),/(25X,6F15.1))
136 903 FORMAT(//I11,20X,REACTION OUT WALL TEMPERATURE PROFILE,1/20X,35(I=MAIN 136
137 1),20X,1DEG K,1,/(25X,6F15.1))
138 904 FORMAT(2(3(7E10.0),E10.0),3(7E10.0),E10.0)
139 905 FORMAT(1 INSIDE TEMPERATURE PROFILE DID NOT CONVERGE AFTER 10 TRMAIN 139
140 11LS MAX TEMPERATURE=1,E10.3,1 DEG K,1,1,90(I=1))
141 906 FORMAT(1 INSIDE TEMPERATURE PROFILE CONVERGED AFTER,13,1TRAILS MMAIN 141
142 1LX TEMPERATURE DIFFERENCE=1,E10.3,1 DEG K,1,1,95(I=1))
143 907 FORMAT(20X,MAXIMUM TEMPERATURE DIFFERENCE CALCULATED=1,PF16.3,1 AFTMAIN 143
144 1E1,15,2X,1TRAILS,1)
145 908 FORMAT(10ADJUSTED HEAT TRANSFER COEFFICIENT PROCESS FLUID TO JUTSIDMAIN 145
146 1E TUBE WALL HTU/HR EQCT DE FURNACE LENGTH,1,1,20X,3E20.3)
147 7 CALL WRITE(4,'STAR',JUMY(1),400)
148 148 STOP
149 149 END

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51 C 1 PLOT RESULTS DO NOT WRITE DETAILED CALCULATIONS PYRO 200
52 C 2 PLOT RESULTS WRITE OUT DETAILED CALCULATIONS PYRO 201
53 C 3 PLOT NOT DONE WRITE OUT DETAILED CALCULATIONS PYRO 202
54 C 4 PLOT NOT DONE DO NOT WRITE DETAILED CALCULATIONS PYRO 203
55 READ(5,95B)I0,I2Z,IPL0T PYRO 204
56 C I IS TEMPERATURE AT INLET Z(I) PYRO 205
57 C PT IS INITIAL PRESSURE AT STARTUP PYRO 206
58 C PRESS IS MAX ALLOWABLE PRESSURE AT INLET PYRO 207
59 C POUT IS DESIRED PRESSURE AT OUTLET PYRO 208
60 C ALL PRESSURES IN ATMOSPHERES PYRO 209
61 C ZT IS TITIAL REACTOR LENGTH FEET PYRO 210
62 C DL IS INCREMENT OF LENGTH USED TO CALCULATE REACTOR CONDITIONS PYRO 211
63 READ(5,919)T,PT,PRES,ZT,DL,POUT PYRO 212
64 DLSEUL PYRO 213
65 TIME=T PYRO 214
66 C IALL,M IDENTIFIY OF CHEMICAL SPECIES IN CHEMICAL REACTION POSITION M PYRO 215
67 GC=1,3143 PYRO 216
68 C KE(I) IS NUMBER OF REACTANTS IN REACTION I PYRO 217
69 C KR(I) IS NUMBER OF PRODUCTS IN REACTION I PYRO 218
70 READ(5,91)I,KE(I),KR(I),I,IR) PYRO 219
71 DO 1 I=1,IR PYRO 220
72 I=KE(I)+KR(I) PYRO 221
73 C IA(I,M) REPRESENTS THE CHEMICAL SPECIES IA IN REACTION I PYRO 222
74 C POSITION M PYRO 223
75 READ(5,901)ID,(IA(I,M),M=1,IT) PYRO 224
76 IF (LD,NE,I)GO TO 101 PYRO 225
77 I CONTINUE PYRO 226
78 C B(I,M) COEFFICIENT OF M CHEMICAL SPECIES IN REACTION I PYRO 227
79 DO 2 I=1,IR PYRO 228
80 I=KE(I)+KR(I) PYRO 229
81 C S(I,M) IS THE STOICMETRIC COEFFICIENT REACTION I PYRO 230
82 C POSITION M PYRO 231
83 C SB(I,M) IS THE PSEUDO ORDER OF REACTION REACTION I PYRO 232
84 C POSITION M PYRO 233
85 READ(5,903)ID,(S(I,M),M=1,IT),(SB(I,M),M=1,IT) PYRO 234
86 IF (LD,NE,I)GO TO 102 PYRO 235
87 I CONTINUE PYRO 236
88 C C(I) IS THE INITIAL CONCENTRATION OF THE I CHEMICAL SPECIES (8 PER CARRY) PYRO 237
89 READ(5,904)(P(J),J=1,IS) PYRO 238
90 PI=0.0 PYRO 239
91 DO 220 I=1,IS PYRO 240
92 220 PI=PI+P(I) PYRO 241
93 DO 18 I=1,IS PYRO 242
94 P(I)=P(I)*PI/PT PYRO 243
95 P(I)=P(I) PYRO 244
96 18 C(I)=P(I)/GC/I PYRO 245
97 C INAME(I) IS THE NAME OF EACH CHEMICAL SPECIES (MAX 20 LETTERS) 4 PER CARRY PYRO 246
98 I=IS*20 PYRO 247
99 C INAME(J) IS THE ALPHANUMERIC IDENTIFICATION OF CHEMICAL PYRO 248
100 C SPECIES I PYRO 249

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101 READ(5,905)(I,NAME(J),J=1,I) PYRO 250
102 DO 3 J=1,I PYRO 251
103 C CP(J,M) IS THE HEAT CAPACITY OF CHEMICAL SPECIES J PYRO 252
104 C EXPRESSED AS A 3-RD POWER POLYNOMIAL IN TEMPERATURE PYRO 253
105 READ(5,906) (CP(J,M),M=1,4),ID PYRO 254
106 IF(ID.NE.J)GO TO 103 PYRO 255
107 3 CONTINUE PYRO 256
108 DO 4 I=1,I PYRO 257
109 C EA(I) IS ARRHENIUS FREQUENCY FACTOR OF REACTION I PYRO 258
110 C EE(I) IS THE ARRHENIUS ACTIVATION ENERGY OF REACTION I PYRO 259
111 C CAL/MOLE OK PYRO 260
112 READ(5,907)ID,EA(I),EE(I) PYRO 261
113 EA(I)=EA(I)*F(I) PYRO 262
114 IF(ID.NE.J)GO TO 104 PYRO 263
115 4 CONTINUE PYRO 264
116 DO5 J=1,I5 PYRO 265
117 C DS(J) IS THE ENTROPY OF CHEMICAL SPECIES J 25 C PYRO 266
118 C DH(J) IS THE ENTHALPY OF CHEMICAL SPECIES J 25 C PYRO 267
119 C DF(J) IS Gibbs FREE ENERGY OF CHEMICAL SPECIES J 25 C PYRO 268
120 READ(5,908) ID,DS(J),DH(J),DF(J) PYRO 269
121 IF(ID.NE.J) GO TO 105 PYRO 270
122 5 CONTINUE PYRO 271
123 DO 21 J=1,I5 PYRO 272
124 C G(LJ,M) ARE THE CONSTANTS OF LEHARD-6 JONES PYRO 273
125 C M PYRO 274
126 C 1 COLLISION PARAMETER PYRO 275
127 C 2 E/K PYRO 276
128 C SMWT(J) IS THE MOLECULAR WEIGHT OF THE JTH CHEMICAL SPECIES PYRO 277
129 C DE(J) IS THE DENSITY OF SOLID CHEMICAL SPECIES J PYRO 278
130 READ(5,911) ID,(CLJ(J,M),M=1,2),S,SMWT(J) PYRO 279
131 IF(CLJ(J,2).EQ.0.)READ(5,940)DE(J) PYRO 280
132 IF(ID.NE.J)GO TO 106 PYRO 281
133 21 CONTINUE PYRO 282
134 DO 6 I=1,I6 PYRO 283
135 DO 7 L=1,4 PYRO 284
136 7 DCP(I,L)=0. PYRO 285
137 I1=KF(I)+1 PYRO 286
138 I2=KRL(I)*KE(I) PYRO 287
139 DO 8 N=1,I2 PYRO 288
140 J=IA(I,N) PYRO 289
141 DO 8 L=1,4 PYRO 290
142 8 DCP(I,L)=DCP(I,L)+B(I,N)*CP(J,L)/S(I,1) PYRO 291
143 I2=KF(I) PYRO 292
144 DO 6 M=1,I2 PYRO 293
145 J=IA(I,M) PYRO 294
146 DO 6 L=1,4 PYRO 295
147 6 DCP(I,L)=DCP(I,L)-B(I,M)*CP(J,L)/B(I,1) PYRO 296
148 C TEMPERATURE PYRO 297
149 R1=1.987 PYRO 298
150 DO 9 I=1,I8 PYRO 299

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151 FT(I)=0.
152 ST(I)=0
153 HT(I)=0
154 I1=KE(I)+1
155 I2=KR(I)+KF(I)
156 DO 10 N=1,I2
157 J=IA(I,M)
158 ST(I)=ST(I)+B(I,M)*DS(J)/B(I,I)
159 FT(I)=FT(I)+B(I,M)*DF(J)/B(I,I)
160 DO 10 HT(I)=HT(I)+B(I,M)*DM(J)/B(I,I)
161 I2=KF(I)
162 DO 9 N=1,I2
163 J=IA(I,M)
164 FT(I)=FT(I)+B(I,M)*DE(J)/B(I,I)
165 ST(I)=ST(I)+B(I,M)*DS(J)/B(I,I)
166 HT(I)=HT(I)+B(I,M)*DM(J)/B(I,I)
167 TO=298.15
168 DO 19 I=1,IR
169 READ(5,908)(J,VT,FI(I))
170 HO(I)=HT(I)
171 DO 29 N=1,4
172 X=N
173 HO(I)=HO(I)-DCP(I,M)/X*TO**M
174 IF(FI(I).GT.0,FI(I))=LOG(FI(I))
175 IF(FI(I).LE.0)FI(I)=-FI(I)/TO/R1
176 FI(I)=HO(I)/B(I,I)+FI(I)-LOG(FI(I)/R1*LOG(FI(I)-DCP(I,2))/2./R1)*T
177 IT=DCP(I,3)/6./R1*TT**2-DCP(I,4)/12./R1*TT**3
178 C BOX WE HAVE THE REACTION SYSTEM, IT WILL BE PRINTED OUT.
179 C CHEMICAL SPECIES IDENTIFICATION
180 J WRITE(6,909)
181 WRITE(6,910)
182 DO 11 J=1,IS
183 JJ1=1+20*(J-1)
184 JJ2=20*J
185 11 WRITE(6,912)(I,NAME(JJ),JJ=JJ1,JJ2),IDATA(J),J,(CP(J,M),M=1,4),DH(J)
186 11,DS(J),DE(J)
187 IGTU=1
188 WRITE(6,920)
189 DO 17 J=1,IS
190 JJ1=1+20*(J-1)
191 JJ2=20*J
192 17 WRITE(6,917)(I,NAME(JJ),JJ=JJ1,JJ2),IDATA(J),J,(CP(J,M),M=1,4),DH(J)
193 17,DS(J),DE(J)
194 WRITE(6,913)
195 DO 12 I=1,IR
196 II=2
197 IF(EE(I).EQ.0)II=1
198 I2=KE(I)
199 DO 14 M=1,I2
200 J=IA(I,M)

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201 MM=M*3-1 PYRO 350
202 IDATB(MM)=IDATA(J) PYRO 351
203 J=P(I,M)+29*01 PYRO 352
204 MM=M*3-2 PYRO 353
205 IDATB(MM)=IDATA(J) PYRO 354
206 MM=M*3 PYRO 355
207 14 IDATB(MM)=IDATA(28) PYRO 356
208 MM=KE(I)*3 PYRO 357
209 KK=40 PYRO 358
210 GO TO (122,121),I PYRO 359
211 121 IDATB(MM)=IDATA(KK) PYRO 360
212 MM=MM+1 PYRO 361
213 122 KK=KK+1 PYRO 362
214 IDATB(MM)=IDATA(KK) PYRO 363
215 MM=MM+1 PYRO 364
216 KK=KK+1 PYRO 365
217 IDATB(MM)=IDATA(KK) PYRO 366
218 I=KF(I)+1 PYRO 367
219 I2=KF(I)+KP(I) PYRO 368
220 DO 15 M=I,I2 PYRO 369
221 J=IA(I,M) PYRO 370
222 MM=M*3-1+I PYRO 371
223 IDATB(MM)=IDATA(J) PYRO 372
224 J=P(I,M)+29*01 PYRO 373
225 MM=M*3-2+I PYRO 374
226 IDATB(MM)=IDATA(J) PYRO 375
227 MM=M*3+I PYRO 376
228 15 IDATB(MM)=IDATA(28) PYRO 377
229 DO 16 J=MM,44 PYRO 378
230 16 IDATB(J)=IDATA(29) PYRO 379
231 12 WRITE(6,15)I,(IDATB(M),M=1,40),EA(I),EE(I),(DCP(I,M),M=1,4) PYRO 380
232 WRITE(6,127) PYRO 381
233 DO 28 J=1,IR PYRO 382
234 I2=KF(J)+KR(J) PYRO 383
235 DO 32 I=1,I2 PYRO 384
236 I3=IA(J,I) PYRO 385
237 32 IDATB(I)=IDATA(I3) PYRO 386
238 28 WRITE(6,32A)J,EI(J),EII(J),IDATB(I),DB(J,I),IA(I,I2) PYRO 387
239 C RAD IS THE RADIUS OF THE INSIDE OF THE REACTOR TUBE PYRO 388
240 C AD IS THE RADIUS OF THE OUTSIDE OF THE REACTOR TUBE PYRO 389
241 C TMPH IS THE MOLAR FLOW RATE IN LB MOLES ORE HOUR PYRO 390
242 C KEYP IS THE KEY REACTANT PYRO 391
243 C KEYP IS THE KEY PRODUCT PYRO 392
244 READ(5,202)RAD,AD,IMPH PYRO 393
245 READ(5,900)KEYR,KEYP PYRO 394
246 IMPH=TMPH PYRO 395
247 RADU=RAD PYRO 396
248 ZTFRZ PYRO 397
249 IGOIO=1 PYRO 398
250 PDPE=2 PYRO 399

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251 PSAVE=PT PYRO 400
252 IE(KEYR, EQ, 0) GO TO 92 PYRO 401
253 WRITE(6, 918) PYRO 402
254 DO 205 I=1, IR PYRO 403
255 MM=C PYRO 404
256 IFIN=1 PYRO 405
257 I1=1 PYRO 406
258 I2=KE(I) PYRO 407
259 GO TO 206 PYRO 408
260 207 I1=KE(I1+1) PYRO 409
261 I2=KF(I1)+KP(I) PYRO 410
262 IFIN=2 PYRO 411
263 206 DO 214 M=1, I2 PYRO 412
264 JJ1=1+20*(I1-I, M)-1 PYRO 413
265 JJ2=JJ1+19 PYRO 414
266 DO 208 I3=JJ1, JJ2 PYRO 415
267 IF(INAME(I3), EQ, INAME(20), AND, INAME(I3+1), EQ, INAME(20)) GO TO 209 PYRO 416
268 208 CONTINUE PYRO 417
269 GO TO 210 PYRO 418
270 209 JJ2=I3 PYRO 419
271 210 J=I(I, H)+29, 01 PYRO 420
272 MM=MM+1 PYRO 421
273 IDATB(MH)=IDATA(J) PYRO 422
274 MN=MN+1 PYRO 423
275 IDATB(MN)=IDATA(29) PYRO 424
276 DO 211 I3=JJ1, JJ2 PYRO 425
277 MM=MM+1 PYRO 426
278 211 IDATB(MN)=INAME(I3) PYRO 427
279 IF(M, EQ, I2) GO TO 214 PYRO 428
280 MN=MN+1 PYRO 429
281 IDATB(MN)=IDATA(28) PYRO 430
282 214 CONTINUE PYRO 431
283 IF(IFIN, EQ, 2) GO TO 205 PYRO 432
284 DO 212 I3=1, 3 PYRO 433
285 MM=MM+1 PYRO 434
286 KK=39+I3 PYRO 435
287 212 IDATB(MN)=IDATA(KK) PYRO 436
288 GO TO 207 PYRO 437
289 205 WRITE(6, 971)(IDATB(I3), I3=1, MN) PYRO 438
290 ENTRY PYRO 439
291 110 WRITE(6, 918) PYRO 440
292 HR=0 PYRO 441
293 MAZE=1 PYRO 442
294 KKE1 PYRO 443
295 C T=GAS TEMPERATURE AT ENTRANCE, PRES=PRESSURE OF GAS, ZT=LENGTH OF TUBE PYRO 444
296 HREO PYRO 445
297 C DZ=INCREMENTAL CHANGE IN REACTOR, C1=CONCENTRATION OF INERTS, A1=A(1) PYRO 446
298 C A(2)Z + A(3) Z**2 + A(4) Z**3 PYRO 447
299 900 FORMAT(212) PYRO 448
300 901 FORMAT(4, 12) PYRO 449

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301 902 FORMAT(3F10.5) PYRO 450
302 903 FORMAT(12,25E3,2) PYRO 451
303 904 FORMAT(12F6.5) PYRO 452
304 905 FORMAT(4A1) PYRO 453
305 906 FORMAT(4E16.8,17) PYRO 454
306 907 FORMAT(12,4E7,1,F10,4) PYRO 455
307 908 FORMAT(12,3F9.2) PYRO 456
308 909 FORMAT(1) PROGRAM PYRO,1 PROGRAMMER RICHARD GREENGLASS,1 ADVYRD 457
309 LISORS,1 DK ROCHE,1 DR HANESTAM,1 AS PARTIAL FILM,1 PYRO 458
310 OF PhD Thesis,1 NEWARK COLLEGE OF ENGINEERING,1 PYRO 459
311 910 FORMAT(1H,145,1 IDENTIFICATION OF REACTION SYSTEM,1,15,1 CONFORM,1 PYRO 460
312 LENT,122,1 CO NO,1,144,1 HEAT CAPACITY DATA,181,1 DELTA-HI,198,1 DELPYRO 461
313 2TA-S,1,116,1 LOG(K),1,1,133,1A,144,181,156,1C,169,1D,1 PYRO 462
314 911 FORMAT(12,2X,3E5,0) PYRO 463
315 912 FORMAT(1,120A1,1X,1A,1X,12,4(2X,1PE10.3),3(3X,1PE15.8)) PYRO 464
316 913 FORMAT(1,1,145,1 REACTION SYSTEM,1,1,1 EQUATION,1,145,1 ARRHENIUS,1 FAPYRO 465
317 ITE CONSTANT,1,175,1 DELTA HEAT CAPACITY DATA FOR REACTION,1,1H,171,1 PYRO 466
318 2 DELTA-A,1,23,1 DELTA-B,1,195,1 DELTA-C,1,167,1 DELTA-D,1,151,1 K(0),1, PYRO 467
319 361,1E1) PYRO 468
320 915 FORMAT(1,1,12,2X,40A1,6(1PE10.3,2X)) PYRO 469
321 916 FORMAT(14) PYRO 470
322 917 FORMAT(1,1,21A1,12,5X,5,3,5X,5,5,1,5X,5,7,2,1PE12,4) PYRO 471
323 918 FORMAT(1H1) PYRO 472
324 919 FORMAT(6E12,5) PYRO 473
325 920 FORMAT(10 COMPONENT,1,122,1 CO NO,1,136,1 LENNARD-JONES MOL. WT,1,162,1 PYRO 474
326 1,1 INITIAL,1,1,136,1 PARAMETERS,1,1,156,1 CONCENTRATION,1,1,131,1(A) PYRO 475
327 2 (DEG-K)) PYRO 476
328 921 FORMAT(1,1,1 IDENTIFICATION,1,12,1 OUT OF PLACE,1,15,1 IDI,1 PYRO 477
329 922 FORMAT(1,1,1 COEFFICIENT IDENTIFICATION,1,12,1 OUT OF PLACE,1,15,1 IDI,1 PYRO 478
330 923 FORMAT(1,1,1 HEAT CAP. IDENTIFICATION,1,12,1 OUT OF PLACE,1,16,1 IDI,1 PYRO 479
331 924 FORMAT(1,1,1 ARRHENIUS IDENTIFICATION,1,12,1 OUT OF PLACE,1,15,1 IDI,1 PYRO 480
332 925 FORMAT(1,1,1 ENTHALPHY IDENTIFICATION,1,12,1 OUT OF PLACE,1,15,1 IDI,1 PYRO 481
333 926 FORMAT(1,1,12,2(5X,1PE12.5),5X,6(5X,1A1,**(1,OPF3,1,1))) PYRO 482
334 927 FORMAT(1,1,13,1 LOG(K),1,9X,1 CONSTANT,1,1,10X,1 ORDER OF REACTI,1 PYRO 483
335 1N BY COMPONENT,1,1,11,1 REACTION,1,129,1 INTEGRATION) PYRO 484
336 928 FORMAT(1,1,12,1PE14,4,14,4,14,4) PYRO 485
337 929 FORMAT(1 ITERATION NUMBER=,1,13,1 NO CONCENTRATION TMPH PYRO 486
338 1 DXA) PYRO 487
339 930 FORMAT(10,1 OL CHANGED TO,1,1PE15.5,5X,1ZIC=,1,1PE14.5) PYRO 488
340 931 FORMAT(11 ALL DXA= 0, SYSTEM MUST BE CHANGED TO ALLOW REACTION) PYRO 489
341 932 FORMAT(1,1,1,12,2X,1PA=,1,1PE14.5,2X,1DXA(1)=,1,1PE14.5,2X,1CF,CR=,1 PYRO 490
342 1,2E14.5,2X,1REC=,1,1PE14.5,1,5,1 SHORATE,1,1,1PE14.5) PYRO 491
343 933 FORMAT(1,1,25(1PE14.5,5X,12,1 1)) PYRO 492
344 934 FORMAT(1,1,12,1PE12.5) PYRO 493
345 935 FORMAT(11,1 LENNARD JONES CONSTANTS,1,12,1 CARD IDI,1,12,1 INTERNAL) PYRO 494
346 936 FORMAT(10,1,315X,1PE16.7)) PYRO 495
347 937 FORMAT(1,1 REACTOR IS 1,1,10,2,1 FEET LONG AND 1,1,6,3,1 FEET IN RADI,1 PYRO 496
348 15,1,1 TOTAL MOLES / HOUR ARE,1,1,6,1,1 POUND MOLES AT PRESSURE,1,1 PYRO 497
349 2,3,1A VELOCITY OF 1,1PE12.5,1 AT TEMPERATURE,1,OPF8,1,1 DEG K,1,1 PYRO 498
350 3 INITIAL REACTOR INCREMENT,1,1PE12.5,1 FEET)) PYRO 499

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401 IF(IP,EQ,IS)IG0=3
402 IF(IR,LI,IS)IG0=2
403 RAD=RAQU
404 DO 48 I=1,100
405 RADF(I)=RAD
406 48 RAD(I)=RAD
407 ITEST=1
408 58 NA=1
409 TMPH=TMPHI
410 PI=0.
411 DO 57 I=1,IS
412 57 PI=PI+R(I)
413 DO 60 I=1,100
414 60 RAD(I)=RADF(I)
415 RAD=RAOF(1)
416 I=IIN
417 PI=PT
418 VELL=1.1620929600E=4*TMPH*PI/PI/RAD**2
419 WRITE(6,937)ZT,RAD,MPH,PT,VELL,T,DL
420 8=1.967
421 ZT=ZTT
422 ZIC=0.
423 MB=0
424 HMB=1
425 MZ=0.
426 ZICL=0.
427 CALL TURE(T,MPH)
428 IF(MZ,GE,1000)GO TO 200
429 IMPZ=MB
430 DO 93 I=1,IS
431 TM(I)=WT*(I,MB)
432 93 C(I)=C(I,MB)
433 IZ=1
434 GO TO 65
435 200 MB=MB/1000
436 GO TO(201,201,201,201,203,303),MB
437 201 WRITE(2,964)
438 GO TO 213
439 202 WRITE(2,952)
440 213 DL=DLS
441 GO TO 49
442 203 WRITE(2,954)
443 204 MB=20
444 STOP
445 300 CONTINUE
446 MB=MB+1
447 25 CONTINUE
448 IF(MA,GT,916)GO TO 55
449 ZIC=ZIC+DL
450 1E/2IC,GE,211)GO TO 33

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PYRD 550
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PYRD 579
PYRD 580
PYRD 581
PYRD 582
PYRD 583
PYRD 584
PYRD 585
PYRD 586
PYRD 587
PYRD 588
PYRD 589
PYRD 590
PYRD 591
PYRD 592
PYRD 593
PYRD 594
PYRD 595
PYRD 596
PYRD 597
PYRD 598
PYRD 599

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451 XN=ZIC/ZIT#10.+1. PYRD 600
452 IIP=XX PYRD 601
453 XXN=IIM PYRD 602
454 TR=Z(IIP)+Z(IIP+1)=Z(IIM)*(XN-XXN) PYRD 603
455 PAF=RAD PYRD 604
456 IJ=100.001-(ZIT-ZIC)/ZIT#99. PYRD 605
457 RIJ=IJ PYRD 606
458 RJ=100.000-(ZIT-ZIC)/ZIT#99. PYRD 607
459 IF(IJ.LE.99)RAD=KADF(IJ)+(RADF(IJ+1)-RADF(IJ))*(RIJ-RJ) PYRD 608
460 IF(IJ.GE.100)RAD=RADE(100) PYRD 609
461 TT=T PYRD 610
462 I=TR PYRD 611
463 D034 I=1,IR PYRD 612
464 D030 PYRD 613
465 I1=1 PYRD 614
466 I2=KE(I) PYRD 615
467 K=IA(I/I) PYRD 616
468 CF=1 PYRD 617
469 D0 35 M=I1,I2 PYRD 618
470 J=IA(I,M) PYRD 619
471 IF(CLJ(J,2).EQ.0.)NO=1 PYRD 620
472 IF(BB(I,M).NE.0.)CE=CF#C(J)#BB(I,M) PYRD 621
473 35 CONTINUE PYRD 622
474 CRE PYRD 623
475 I1=KF(I)+1 PYRD 624
476 I2=KR(I)+E(I) PYRD 625
477 D0 36 M=I1,I2 PYRD 626
478 J=IA(I,M) PYRD 627
479 IF(CLJ(J,2).EQ.0.)NO=1 PYRD 628
480 IF(BB(I,M).NE.0.)CR=CR#C(J)#BB(I,M) PYRD 629
481 36 CONTINUE PYRD 630
482 EA(I)=EA(I)*EXP(-EE(I)/R/T)*(CE=CR#KEC(I,I)) PYRD 631
483 IF(P(K).NE.0.)DXA(I)=1.13097335E4*DL*RA(I)*RAD**2/TMP#PT/P(K) PYRD 632
484 IE(P(K).EQ.0.)DXA(I)=0. PYRD 633
485 IF(NO.NE.0)GO TO 54 PYRD 634
486 GO TO 68 PYRD 635
487 54 IF((ABS(DXA(I)).GE.1.E-2).AND.(F(I).LE.9.))GO TO 20 PYRD 636
488 68 IE(DXA(NO).LE.0.)DXA(I)=0. PYRD 637
489 IF(DXA(I).GE.0.)DXA(I)=DXA(I)*.1 PYRD 638
490 IF(DXA(I).GE.0.)GO TO 20 PYRD 639
491 34 CONTINUE PYRD 640
492 GO TO 23 PYRD 641
493 20 ZIC=ZIC-DL PYRD 642
494 DL=ARS(DL*.005/DXA(I)) PYRD 643
495 RE=REOC(T,I) PYRD 644
496 RATE=EA(I)*EXP(-EE(I)/R/T) PYRD 645
497 WRITE(6,930)DL,ZIC PYRD 646
498 WRITE(6,932)I,RA(I),DXA(I),CE,CR,REQ,RATE PYRD 647
499 NA=MA+1 PYRD 648
500 GO TO 25 PYRD 649

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501 23      DN=0,
502      PT2=PRR(1S)
503      DO 39 I=1,IR
504      K=IA(I,1)
505      I1=1
506      I2=KF(I)
507      DO 38 M=I1,I2
508      J=IA(I,M)
509      DN=DH-R(I,M)/B(I,1)*C(K)*DXA(I)
510 38      P(J)=P(J)+A(I,M)/B(I,1)*P(K)*DXA(I)
511      I1=KF(I)+1
512      I2=KR(I)+KF(I)
513      DO 39 M=I1,I2
514      J=IA(I,M)
515      DN=DH+R(I,M)/B(I,1)*C(K)*DXA(I)
516 39      P(J)=P(J)+A(I,M)/B(I,1)*P(K)*DXA(I)
517      CT=0.
518      DO 37 I=1,IS
519      C(I)=P(I)/T/GC
520 37      CT=CT+C(I)
521      RN1=CT
522      RH2=CI-DL
523      THPH=THP+DN*GC*T/PT+TMPH
524      DN=TMPH
525      PD=PRESO(T)
526      PT=PRR(1S)
527      IF(NB.EQ.500)GO TO 72
528      IF(NB.EQ.300)GO TO 71
529      IF(NB.EQ.200)PT=.5
530      IF(PT.LE.(PMUL-.2))GO TO 69
531 40      J=1,IS
532 40      IM(J)=IMEH*P(J)/PT
533      DN=0,
534 44      DO 43 IX=1,IR
535 43      D=AMAX1(ABS(DXA(IX)),D)
536      IF(D.EQ.0)GO TO 26
537      IF(D.GE.001)GO TO 24
538 27      IF(DL.GE.0)ZII=GO TO 24
539      DL=ABS(DL*.005/D)
540      IF(DL.GE.0)ZII=DL*.01001*ZII
541      WRITE(6,930)DL,ZIC
542      WRITE(6,933)(DXA(I),I,1,IR)
543 24      IF(MB.NE.1)GO TO 31
544      WRITE(6,942)P1,VEL1
545      WRITE(6,928)(J,C(J),TM(J),DXA(J),J=1,IM)
546      GO TO(46,47,31),IGD
547 46      II=IS+1
548      WRITE(6,93E)(J,DXA(J),J=1,IR)
549      GO TO 31
550 47      II=IR+1
PYRD 650
PYRD 651
PYRD 652
PYRD 653
PYRD 654
PYRD 655
PYRD 656
PYRD 657
PYRD 658
PYRD 659
PYRD 660
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PYRD 693
PYRD 694
PYRD 695
PYRD 696
PYRD 697
PYRD 698
PYRD 699

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551 WRITE(6,939)(J,C(J),TM(J),J=1,IS) PYRD 700
552 31 CONTINUE PYRD 701
553 ZIC=ZIC+DL PYRD 702
554 IF(ZIC.LE.(ZIT/25.))GO TO 30 PYRD 703
555 ZIC=C PYRD 704
556 MZ=MZ+1 PYRD 705
557 WZIC(MZ)=ZIC PYRD 706
558 WTMZ(MZ)=1 PYRD 707
559 WTMZ(MZ)=TMPH PYRD 708
560 WPIZ(MZ)=1 PYRD 709
561 WVELL(MZ)=VEL1 PYRD 710
562 DO 70 J=1,ISS PYRD 711
563 WC(J,MZ)=C(J) PYRD 712
564 WTA(J,MZ)=TM(J) PYRD 713
565 70 WDXA(J,MZ)=DXA(J) PYRD 714
566 30 GO TO 300 PYRD 715
567 33 PT=PT2 PYRD 716
568 69 I=I+1 PYRD 717
569 WRITE(6,914) PYRD 718
570 WRITE(6,951)CARD PYRD 719
571 WRITE(6,934)ZIC,T,TMPH PYRD 720
572 PIVE=PT PYRD 721
573 IF(MAZE.FQ.2)PT=2 PYRD 722
574 WRITE(6,942)PT,VEL1 PYRD 723
575 PT=PTTE PYRD 724
576 DO 64 I=1,IS PYRD 725
577 64 P(I)=PPI(I) PYRD 726
578 IF(PT.GE.(PQUT=2))AND.(PT.LE.(PQUT+2))GO TO 65 PYRD 727
579 IF(KK.FQ.2)PDP=PDP/2 PYRD 728
580 IF(KK.FQ.2)IGU TO 63 PYRD 729
581 IF(PT.GE.PQUT+2)AND.(ITEST.EQ.2))PDP=PDP/2 PYRD 730
582 IF(MAZE.EQ.2)AND.(PT.GE.(PQUT=2))GO TO 65 PYRD 731
583 IF(MAZE.EQ.2)GO TO 63 PYRD 732
584 IF(PI.LE.PQUT+2)AND.(ITEST.EQ.2))PDP=PDP/2 PYRD 733
585 IF(PT.GE.PQUT+2)AND.(ITEST.EQ.2))KK=2 PYRD 734
586 IF(PI.LE.PQUT+2)AND.(ITEST.EQ.3))KK=2 PYRD 735
587 GO TO 63 PYRD 736
588 71 MAZE=2 PYRD 737
589 PT=5 PYRD 738
590 WRITE(6,952) PYRD 739
591 GO TO 69 PYRD 740
592 65 IF(IPLDT.GT.2)GO TO 91 PYRD 741
593 WRITE(6,918) PYRD 742
594 WRITE(6,951)CARD PYRD 743
595 WRITE(6,963)HR PYRD 744
596 WRITE(6,960) PYRD 745
597 WRITE(6,962) PYRD 746
598 DO 81 I=1,116 PYRD 747
599 81 CALL PLOT(I,'#N') PYRD 748
600 CALL PLOT(I,1) PYRD 749

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601 DO 82 I=1,IWHZ PYRO 750
602 J=JMN2+1,I11 PYRO 751
603 J1=TM(KEYP,1)/WTH(KEYP,1)*100.+15. PYRO 752
604 J2=TM(KEYP,1)/WTH(KEYP,1)*100.+15. PYRO 753
605 J3=(WT(1)-WT(1))/WTH(WHZ)*WT(1)*100.+15. PYRO 754
606 J4=JPT(I1)/5.*100.+15 PYRO 755
607 WRITE(6,974)ZIC(I) PYRO 756
608 82 CALL PLUT(14,IEN1,5,I9ATOW(I1),I1,IEN1,J2,IRN1,J3,ITN1,J4,IRN1,116,PYRO 757
609 11*01) PYRO 758
610 DO 83 I=14,116 PYRO 759
611 83 CALL PLUT(I,1*01) PYRO 760
612 CALL PLUT(I,1) PYRO 761
613 WRITE(6,918) PYRO 762
614 91 KK=1 PYRO 763
615 IF((IPLUT,CT,3).OR.(IPLUT,LT,2))GO TO 90 PYRO 764
616 IWHZ=2 PYRO 765
617 DO 75 I=1,IWHZ PYRO 766
618 PT=PT(I) PYRO 767
619 VELL=VEL1(I) PYRO 768
620 ZIC=ZIC(I) PYRO 769
621 T=PT(I) PYRO 770
622 TMEH=TMPH(I) PYRO 771
623 DO 76 J=1,ISS PYRO 772
624 C(J)=WC(J,I) PYRO 773
625 TM(J)=TM(J,I) PYRO 774
626 76 DXA(J)=DXA(J,I) PYRO 775
627 IWHZ=IWHZ+1 PYRO 776
628 IF(IWHZ=I)GO TO 41 PYRO 777
629 IWHZ=0 PYRO 778
630 WRITE(6,919) PYRO 779
631 WRITE(6,951)CARD PYRO 780
632 41 WRITE(6,934)ZIC,I,TMPH PYRO 781
633 YIELD=TH(KEYP)/TMPH/PPH(KEYP)*PI*100. PYRO 782
634 J2=KEYR*20 PYRO 783
635 J1=J2-19 PYRO 784
636 J4=KEYR*20 PYRO 785
637 J3=J4-19 PYRO 786
638 WRITE(6,965)(I,NAME(I),I=1,I,J2),(I,NAME(I),I=J3,J4),YIELD PYRO 787
639 WRITE(6,942)PT,VEL1 PYRO 788
640 WRITE(6,929)I PYRO 789
641 WRITE(6,926)(J,C(J),TM(J),DXA(J),J=1,IM) PYRO 790
642 GO TO(42,45,75),IGD PYRO 791
643 42 II=IS+1 PYRO 792
644 WRITE(6,933)(J,DXA(J),J=II,IR) PYRO 793
645 GO TO 75 PYRO 794
646 45 II=IR+1 PYRO 795
647 WRITE(6,939)(J,C(J),TM(J),J=II,IS) PYRO 796
648 75 WRITE(6,916) PYRO 797
649 WRITE(6,916) PYRO 798
650 90 WRITE(6,951)CARD PYRO 799

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701      P(I)=PPI(I)
702 66    C(I)=R(I)/50.320,
703      ITEST=1
704      MAX1
705      IF(IGOTO,GE,I77)GO TO 56
706      IF(PT.LT,PRESIG0,TO 58
707      GO TO 56
708 72    WRITE(6,954)
709      IGOIN=I2Z
710      GO TO 50
711 55    WRITE(6,945)
712 56    WRITE(6,919)
713      IF(IPL0T,GT,2)GO TO 95
714      WRITE(6,955)
715      WRITE(6,965)ZIT
716      IGOIN=IGOIN-1
717      DO 77 J=14,116
718 77    CALL PLOT(J,I*H)
719      CALL PLOT(1, I)
720      DO 74 J=2,100+2
721      J1=102-J
722      IJK=0,
723      DO 79 I=1,IGOTO
724      IJK=IJK+1
725      IF(IJK,GT,9)IJK=1
726      J2=READ(I1,I1/RAS*50,+65,
727      J3=130-J2
728 79    CALL PLOT(I4,I*H,J2,ICATP(IJK),J3,ICATP(IJK),I16,I*H)
729      IJ=(J+2)/4
730      IF(FL0AT(J/4),EQ,FL0AT(J)/4,IIJ=1
731 78 -   CALL PLOT(5,ICAT3(IJ),65,I+ I)
732      DO 80 J=14,116
733 80    CALL PLOT(J,I*H)
734      CALL PLOT(I, I)
735      WRITE(6,966)
736      WRITE(6,967)CARD
737 95    CONTINUE
738      IGOIN=1
739      MAX1
740      PTE=0,
741      DO 73 I=1,IS
742 73    PTEPT=PPI(I)
743      DO 74 I=1,IS
744      PRILEPPI(I)PSAVE/PT
745 74    P(I)=PPI(I)
746      IF(I,NE,C)RETURN
747      READ(5,943)IGOW,(Z(I),I=1,11)
748      READ(5,950)CARD
749      READ(5,958)I8,I2Z,IPL0T
750      GO TO,LOG,I10,I11,I16,IGOW

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PYRO 850
PYRO 851
PYRO 852
PYRO 853
PYRO 854
PYRO 855
PYRO 856
PYRO 857
PYRO 858
PYRO 859
PYRO 860
PYRO 861
PYRO 862
PYRO 863
PYRO 864
PYRO 865
PYRO 866
PYRO 867
PYRO 868
PYRO 869
PYRO 870
PYRO 871
PYRO 872
PYRO 873
PYRO 874
PYRO 875
PYRO 876
PYRO 877
PYRO 878
PYRO 879
PYRO 880
PYRO 881
PYRO 882
PYRO 883
PYRO 884
PYRO 885
PYRO 886
PYRO 887
PYRO 888
PYRO 889
PYRO 890
PYRO 891
PYRO 892
PYRO 893
PYRO 894
PYRO 895
PYRO 896
PYRO 897
PYRO 898
PYRO 899

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751 101 CONTINUE
752 WRITE(6,921)I,I,D
753 STOP111
754 102 CONTINUE
755 WRITE(6,922)I,I,D
756 STOP112
757 103 CONTINUE
758 WRITE(6,923)I,I,D
759 STOP113
760 104 CONTINUE
761 WRITE(6,924)I,I,D
762 STOP114
763 105 CONTINUE
764 WRITE(6,925)I,I,D
765 STOP115
766 111 CONTINUE
767 WRITE(6,919)
768 92 WRITE(6,970)(I,I=1,IR)
769 DO 84 IT=800,1200,10
770 J=(IT-800)/10+1
771 T=IT
772 DO 85 N=1,IR
773 85 MC(J,N)=1./REGC(T,N)
774 84 WRITE(6,969)IT,(MC(J,N),N=1,IR)
775 WRITE(6,972)(I,I=1,IR)
776 DO 86 IT=800,1200,10
777 J=(IT-800)/10+1
778 T=IT
779 DO 87 N=1,IR
780 87 MC(J,N)=HEATR(T,N)
781 86 WRITE(6,969)IT,(MC(J,N),N=1,IR)
782 WRITE(6,975)(I,I=1,IS)
783 DO 88 IT=800,1200,10
784 J=(IT-800)/10+1
785 T=IT
786 DO 89 N=1,IS
787 89 MC(J,N)=HCP(T,N)
788 88 WRITE(6,973)IT,(MC(J,N),N=1,IS)
789 99 RETURN
790 106 WRITE(6,935) I,D,J
791 STOP116
792 26 WRITE(6,931)
793 WRITE(6,944)(J,C(J),DXA(J),J=1,IS)
794 STOP26
795 END

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```
1 FUNCTION REOC(I,1) REOC 983
2 COMMON/EE/DCP(25,4),HT(25),SOL(25),FO(25),EI(25),HO(25) REOC 984
3 COMMON/SET/MY,MZ,IB,IPLOT,DLS REOC 985
4 REAL*4 LIG REOC 986
5 DATA R/1.987/ REOC 987
6 ELINK=HO(1)/R/T+DCP(I,1)/R#LOG(T)+DCP(I,2)/(2.*R)*T+DCP(I,3)/(3.*R)REOC 988
7 1)*T+DCP(I,4)/(12.*R)*T#3+FI(I) REOC 989
8 REOC=EXP(-ELINK) REOC 990
9 RETURN REOC 991
10 END REOC 992
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1 FUNCTION PRES0(T)
2 COMMON/RYR03/2(1),Z1,C(25),CP(25,4)
3 1,DM(25),DS(25),DF(25)
4 COMMON/TUBCL/IK,ISAKE(25),KR(25),B(25,10),BB(25,10),DL,LA(25,10)
5 1,EA(25),EE(25),RAD,AD
6 COMMON/RO/R(25),DN,SMWT(25),CLJ(25,2),VI(25),AMWT,VEL1,HI
7 COMMON/PT2/TT,RNI,RNG,VIS
8 COMMON/ASEI/MY,MZ,IB,IPLOT,DLS
9 REAL*4 LRG
10 PT=PRR(15)
11 IF(MZ.EQ.500)RETURN
12 C THIS SUBROUTINE CALCULATES PRESSURE DROP FROM BERNOULIE LAW
13 C MODIFIED TO TAKE FRICTION LOSS INTO CONSIDERATION
14 DATA MY,1/
15 IF(MY.NE.1)GO TO 1
16 MY=2
17 MAZE=1
18 PDR=2
19 DATA A/,439818/,BI/-.44245917/,CC/,86401820E-1/,D/,.77486511E-2/
20 DATA AI/2.6623E-5/,A2/1.1620929E-4/,A3/7.37495E4/
21 PRES0T=0.
22 11 DO 2 1,1,15
23 IF(CLJ(1),EQ.0) GO TO 2
24 E=LOG(A/CLJ(1,2))
25 VI(1)=A1*SKT(SMWT(1)*T)/(CLJ(1,1)**2*EXP(A+BI*E+CC*E**2+D*E**3))
26 2 CONTINUE
27 VIS=0.
28 DO 3 1,1,15
29 IF(CLJ(1),EQ.0)GO TO 3
30 V=PI/(PT*VI(1))
31 U=0.
32 DO 4 1,1,15
33 IF(CLJ(1),EQ.0)GO TO 4
34 U=PI/(PT*VI(1)/SQRT(1+SMWT(1)/SMWT(1))**1+*(VI(1)/VI(1))**5)PRES0T26
35 1*(SMWT(1)/SMWT(1))**25)**2
36 4 CONTINUE
37 VIS=VIS+V/U
38 3 CONTINUE
39 VIS=VIS*.0672
40 1 AMWT=0.
41 VEL2=A2*T/(PT-PRES0T)/RAI**2*DN
42 DO 5 1,1,15
43 5 AMWT=P(1)/PT*SMWT(1)+AMWT
44 C GC IN AT.#ET#3 /OK LB,MOLES)
45 GC=1.3143
46 DEN=PT/(GC*RT)*AMWT
47 IF(DEN.LE.0)GO TO 21
48 6 VELA=(VEL1+VEL2)/2.
49 REMU=2.*RAD*DEN*VELA/VIS
50 IF(REMU.LE.0)GO TO 19

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PRES 993
PRES 994
PRES 995
PRES 996
PRES 997
PRES 998
PRES 999
PRES1000
PRES1001
PRES1002
PRES1003
PRES1004
PRES1005
PRES1006
PRES1007
PRES1008
PRES1009
PRES1010
PRES1011
PRES1012
PRES1013
PRES1014
PRES1015
PRES1016
PRES1017
PRES1018
PRES1019
PRES1020
PRES1021
PRES1022
PRES1023
PRES1024
PRES1025
PRES1026
PRES1027
PRES1028
PRES1029
PRES1030
PRES1031
PRES1032
PRES1033
PRES1034
PRES1035
PRES1036
PRES1037
PRES1038
PRES1039
PRES1040
PRES1041
PRES1042

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51 IF(RENUL,LE,3500.160 TO 20
52 GO TO 10
53 20 F=64./RENU
54 10 F=0.00560+.5/(RENU#.32)
55 GO TO 100
56 100 PRES=DEN*(VELA#2#F*DL/EA0+VEL2#2=VEL1#2)/62.4/2116.8
57 PRES=ABS(PRES0)
58 P2=PI*PRES
59 IF(P2,LE,0.)GO TO 21
60 VEL2=A2#T/P2/RAD#2*DN
61 IF(PRES0,EQ,0.)GO TO 7
62 IF(ABS((PRES01-PRES0)/PRES0).LE,.001160 TO 7
63 PRES01=PRES0
64 DEN=(P2*PI)/(2.*GC#T)*AMWT
65 GO TO 6
66 7 P2#0.
67 GO 9 I=1,15
68 P2=PI*P2#P(I)
69 DO 8 I=1,15
70 8 P11=P(I)*P(I2-PRES01/P2
71 IF((I*PLOT,EQ,2).OR,(I*PLOT,EQ,3).AND,(M2,EQ,1))GO TO 1001
72 VEL1=VEL2
73 IF(VEL1,GE,1214.5)GO TO 22
74 IF(VEL1,GE,SQR(43#P2/DEN))GO TO 22
75 RETURN
76 22 M2=3000
77 PT=0.5
78 RETURN
79 1001 WRITE(6,9001)RENU, VIS,DEN,F,VEL1,VEL2,VELA,T,PRES0
80 VEL1=VEL2
81 RETURN
82 19 WRITE(6,9002)RAD,DEN,VELA,VIS,RENU
83 WRITE(6,902)T,PT,(P(1),I=1,15),GC,AMWT,P2
84 M2=2000
85 RETURN
86 21 WRITE(6,902)I,P1,P11,P11,IS),GC,AMWT,P2
87 M2=2000
88 RETURN
89 900 FORMAT(I RAD=1,1PE12.5,1DEM,VELA,VIS,RENU,4(2X,1PE12.5))
90 901 FORMAT(I PRESSURE DROP =1,1PE12.5,1DEN,VELA,DL,VEL1,VEL2,1,5(2X,1PPRES10E2
91 1E12,5))
92 902 FORMAT(I T PI P(1)=P(12), GC AMWT 1,10(1X,F8.2))
93 9001 FORMAT(I FUNCTION PRES0(I),/1 RENU=1,1PE14.5,5X,1VIS=1,1PE14.5,5PRES10E5
94 1X,1DEN=1,1PE14.5,/,1 ERICTION FACTOR = 1,1PE14.5,5X,1V1,V2,VA=1,3(1PRES10E6
95 1PE14.5,5X),1 TEMPERATURE=1,UPF8.2 ,5X,1PRESSURE D=1,1PE14.5)
96 END

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```
1 FUNCTION HCP(T,I) HCP 1089
2 COMMON/USE1/IR,IS,KF(25),KB(25),B(25,10),BB(25,10),DL,IA(25,10) HCP 1090
3 1,EA(25),EE(25),RAD,AD HCP 1091
4 CQHNDH/RVRB3/Z(11),ZTT,C(25),CP(25,4) HCP 1092
5 1,DDH(25),DS(25),DF(25) HCP 1093
6 HCP=CP(I,1)+CP(I,2)*T+CP(I,3)*T*T+CP(I,4)*T**3 HCP 1094
7 RETURN HCP 1095
8 END HCP 1096
```



```

1 SURROUTINE RATE(C1,T,RA) RATE1097
2 DATA R(1,9A7) RATE1098
3 DIMENSION PA(25),C1(25) RATE1099
4 COMMON/PA/SLURP(52),CLJ(25,2) RATE1100
5 COMMON/TUBE1/IR,IS,KF(25),KR(25),B(25,10),BB(25,10),DL,IA(25,10) RATE1101
6 ,CA(25),EE(25),RAD,AC RATE1102
7 C1 RATE1103
8 DO34 I=1,IP RATE1104
9 NO=0 RATE1105
10 I1=1 RATE1106
11 I2=KF(I) RATE1107
12 CF=1 RATE1108
13 DO 35 N=1,12 RATE1109
14 J=IA(I,N) RATE1110
15 IF (CLJ(J,2).EQ.0.)NO=1 RATE1111
16 IF (BB(I,N).NE.0.)CF=CF+C1(J)**BB(I,N) RATE1112
17 35 CONTINUE RATE1113
18 CR=1 RATE1114
19 I1=KF(I)+1 RATE1115
20 I2=KR(I)+KE(I) RATE1116
21 DO 36 N=1,12 RATE1117
22 J=IA(I,N) RATE1118
23 IF (CLJ(J,2).EQ.0.)NO=1 RATE1119
24 IF (BB(I,N).NE.0.)CR=CR+C1(J)**BB(I,N) RATE1120
25 36 CONTINUE RATE1121
26 PA(I)=EA(I)*EXP(-EE(I)/R/T)*(CF=CR*REQC(I,I)) RATE1122
27 RETURN RATE1123
28 END RATE1124

```

```

1 SUBROUTINE MATB(RA1,RA2,PC2,DXA,X1,X2,T1,T2,PT1,PT2) MATB1125
2 DATA GC/1,3413/ MATB1126
3 DIMENSION DXA(25),X1(25),X2(25),PC2(25),RA1(25),RA2(25) MATB1127
4 COMMON/TUBE/IR,IS,KF(25),KR(25),S(25),IO),BB(25),I(1),DL,JA(25,10) MATB1128
5 I,EA(25),EE(25),RAD,AD MATB1129
6 DN=0.0 MATB1130
7 DO 1 I=1,IR DO 1 I=1,IR MATB1131
8 K=IA(I,1) K=IA(I,1) MATB1132
9 RA=(RA1(I)+RA2(I))/2. MATB1133
10 IF(X1(K).NE.0.)DXA(I)=1.130973355E+0DL*RA*RAD**2/XI(K) MATB1134
11 5 CONTINUE MATB1135
12 IF(X1(K).EQ.0.)DXA(I)=0. MATB1136
13 1 CONTINUE MATB1137
14 DO 37 J=1,IS DO 37 J=1,IS MATB1138
15 X2(J)=X1(J) MATB1139
16 37 CONTINUE MATB1140
17 DO 39 I=1,IR DO 39 I=1,IR MATB1141
18 K=IA(I,1) K=IA(I,1) MATB1142
19 I1=1 MATB1143
20 J2=KE(I) MATB1144
21 DO 38 M=1,12 MATB1145
22 J=IA(I,1) MATB1146
23 DN=DM-R(I,M)/B(I,1)*X1(K)*DXA(I) MATB1147
24 38 X2(J)=X2(J)+B(I,4)/B(I,1)*X1(K)*DXA(I) MATB1148
25 I1=KF(I)+1 MATB1149
26 J2=KR(I)+KF(I) MATB1150
27 DO 39 M=1,12 MATB1151
28 J=IA(I,1) MATB1152
29 DN=DM+R(I,M)/B(I,1)*X1(K)*DXA(I) MATB1153
30 39 X2(J)=X2(J)+B(I,4)/B(I,1)*X1(K)*DXA(I) MATB1154
31 TMPH=0.0 MATB1155
32 DO 42 I=1,IS MATB1156
33 42 TMPH=TMPH+X2(I) MATB1157
34 CALL PRESC(T1,T2,PD,TPH) MATB1158
35 XT2=0.0 MATB1159
36 DL=0 I=1,IS MATB1160
37 XT2=XT2+X2(I) MATB1161
38 40 CONTINUE MATB1162
39 PT2=PT1-PD MATB1163
40 DO 41 I=1,IS MATB1164
41 BC2(I)=X2(I)/XT2+PT2/T2/GC MATB1165
42 41 CONTINUE MATB1166
43 RETURN MATB1167
44 END MATB1168

```

```

1 FUNCTION HEATR(T2,I)
2 COMMON/EE/DCP(25,4),HT(25),ST(25),EI(25),EI(25),HC(25)
3 COMMON/SET/MY,NB,IB,IPLDT,DLS
4 HEATR=HC(I)
5 DO 1 L=1,4
6 X=L
7 1 HEATR=HEATR+DCP(I,L)*(T2*L/X)
8 C WRITE(2,2001)HEATR,T2,I
9 IF((IPLDT.EQ.2).OR.(IPLDT.EQ.3).AND.(MZ.EQ.1))GO TO 1001
10 RETURN
11 1001 WRITE(6,9001)HEATR,T2,I
12 RETURN
13 9001 FORMAT(1 HEATR(T,I),1PE14.5,(1,0PF8,2,1,12,1))
14 END

```

```

HEAT1169
HEAT1170
HEAT1171
HEAT1172
HEAT1173
HEAT1174
HEAT1175
HEAT1176
HEAT1177
HEAT1178
HEAT1179
HEAT1180
HEAT1181
HEAT1182

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1 SUBROUTINE HEATB(RADC,TB1,TB2,DXA,X1,X2,TB2C,Q,U) HEAT1183
2 REL*4 LOG HEAT1184
3 COMMON/PO/P(25),ON,SHMT(25),CLJ(25,2),VI(25),AMWT,VEL1,HI HEAT1185
4 CORONA/TUBE1/IR,IS,KE(25),KR(25),B(25,10),BB(25,1),D1,1A(25,10) HEAT1186
5 1,EA(25),EE(25),RAOI,RADO HEAT1187
6 CORONA/TUBE2/INO,TX(100) HEAT1188
7 COMMON/TH/TMPZ,RADZ(100),DE(25),ZIC HEAT1189
8 DATA BU,OO,RI,OO,XST/26,TSKIN/1120, HEAT1190
9 1,PI/3.1415926/2,XKC/2.90/1C/0/ HEAT1191
10 C QJ AND AI FOULING FACTORS FROM APPLIED PROCESS DESIGN FOR HEAT1192
11 C CHEMICAL AND PETROCHEMICAL PLANTS BY E.E. LUDWIG PAGES 55-59 HEAT1193
12 C THERMAL CONDUCTIVITY OF CARBON(GRAPHITE) XKC FROM HEAT1194
13 C TRANSPORT PHENOMENA BIRD STUART AND LIGHTFOOT PAGE249 HEAT1195
14 DISPERSION XL(25),X2(25),DXA(25) HEAT1196
15 IF(IND.EQ.0)GO TO 10 HEAT1197
16 CALL THERM(TSKIN,ZIC,INO) HEAT1198
17 10 TAVG=(TB2+TB1)/2. HEAT1199
18 DT1=TSKIN-TAVG HEAT1200
19 DT2=TB2-TB1 HEAT1201
20 DT2=TB2-TB1 HEAT1202
21 HR=0.0 HEAT1203
22 QB=1-I-I-IR HEAT1204
23 K=IA(I,I) HEAT1205
24 J HR=H*HEAT2(I,AVG,I)*(X2(X1)+X1(K))/2.*DXA(I)/1.8 HEAT1206
25 SH=0.0 HEAT1207
26 DO 2 I=1,18 HEAT1208
27 2 SH=SH+(X2(I)*HCP(TB2,I)+X1(I)*HCP(TB1,I))/2.*1.8 HEAT1209
28 C HI=FAVEL,CCMP) HEAT1210
29 AD=PI*NL*RAOU*2.0 HEAT1211
30 AJ=PI*RAI*#9L*2.0 HEAT1212
31 AC=PI*RAIC*NL*2.0 HEAT1213
32 AAVG=(AU-AI)/LOG(AD/AI) HEAT1214
33 RST=(RADO-RAUI)/XKST HEAT1215
34 AAVGC=1.0 HEAT1216
35 IF(RADI,NE,RADC)AAVGC=(AI-AC)/LOG(AI/AC) HEAT1217
36 RC=(RAUI-RADCI)/XKL HEAT1218
37 RU=RD+RST*AD/AAVG+RI*1./((HI*AC/AU)+RC*AI/AAVGC HEAT1219
38 UEL,URU HEAT1220
39 4 TB2C=TRI+(U*AD*DT1-HR)/SH HEAT1221
40 HR=HR/DL HEAT1222
41 Q=U*AU*DT1 HEAT1223
42 IC=IC*1 HEAT1224
43 IF(IC.LT.10)GO TO 5 HEAT1225
44 ICE1 HEAT1226
45 C WRITE(2,901)Q,HR,SH,HI HEAT1227
46 C901 FORMAT(10E14.5,1 HR=1,E14.5,1 SH=1,E14.5,1 HI=1,E14.5) HEAT1228
47 5 RETURN HEAT1229
48 END HEAT1230

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1 SUBROUTINE TUBE(T1, TMPH)
2 COMMON/PYRD3/Z(I1), ZTT, C(25), CP(25,4)
3 PDH(25), CS(25), DF(25)
4 COMMON/EP/PL(25), DN, SXXI(25), CL(25,2), VI(25), AMWT, VELL, HI
5 COMMON/TUBE1/IR, IS, KF(25), KR(25), B(25,10), BB(25,10), DL, LA(25,10)
6 LEA(25), EE(25), RAD, AD
7 COMMON/TUBE2/IND, TX(100), QT(4), QFF
8 COMMON/IN/INPZ, RAD1(100), DE(25), ZIC
9 COMMON/W/ WZIC(50), WT(50), WTMPH(50), WPT(50), WVEL1(50), WC(25,50), WTTUBE1239
10 LA(25,50), WEXA(25,50), RAD2(100,50)
11 COMMON/SET/MY, MZ, IB, IPIOT, DLS
12 DIMENSION X1(25), X2(25), XA1(25), BRA2(25), BRA2(25), BC2(25)
13 I, BC2(25), OXA(25), BDXA(25), RADF(100)
14 DATA IL2/1/
15 QTUT=0.0
16 JW=0
17 CALL PZERO(QT(1),4)
18 N3=1
19 XN=1.
20 Z85=ZTT/85.
21 Z33=ZTT/3.
22 PIR=0.0
23 DO 1 I=1, IS
24 PI=PI+P(I)
25 1 CONTINUE
26 ISS=MAXO(4P, IS)
27 ZIC1=0.0
28 NZ=0
29 DO 7 I=1, IS
30 XI(I)=TMPHP(I)/PT
31 7 CONTINUE
32 IE(I)=2.0*GT(I)GO ID 9
33 DO 8 I=1, 100
34 8 RAGE(I)=RAC
35 C DL=10.
36 9 ZIC=0.0
37 T2=T1+10.
38 DL=DLS
39 CALL RATE(C, T1, RAI)
40 2 CALL RATE(C, I2, RA2)
41 T2=0.0+T2
42 ZIC=ZIC+DL
43 ZIC1=ZIC1+DL
44 IE(ZIC, I1, ZTT)GO ID 4
45 DL=ZTT-(ZIC-DL)
46 IE(OL, LE, O)GO ID 10
47 ZIC=ZTT
48 ZIC1=ZTT
49 4 CI=RADF(INT((ZTT-ZIC)/ZTT*99.+1.))
50 IE(OL, LE, O, O)CI=RAD

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TUBE1231
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TUBE1280

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51 C906 FORMAT(1 I J K M1,3X,1X1(K),5X,1X2(J),4X,1DXA(I),5X,10XTURE1281
52 C 11,1) TURE1282
53 CALL MATP(RA1,RA2,BC2,DXA,X1,X2,T1,T2,PT,PT2) TURE1283
54 CALL HEATB(G1,T1,T2,DXA,X1,X2,BT2,QINC,UINC) TURE1284
55 IF(MZ,GE,1000)RETURN TURE1285
56 IC=0 TURE1286
57 3 CALL RATE(BC2,BT2,BRA2) TURE1287
58 CALL MATP(A1,BRA2,BRC2,DXA,X1,X2,T1,BT2,PT,PT2) TURE1288
59 CALL HEATB(C1,T1,BT2,DXA,X1,X2,BBT2,QINC,UINC) TURE1289
60 IF(MZ,GE,1000)RETURN TURE1290
61 IF(ABS((BBT2-BT2)/BBT2).GE,0.0001)GO TO 5 TURE1291
62 GO TO 6 TURE1292
63 5 BT2=(BBT2+BT2)/2. TURE1293
64 IC=IC+1 TURE1294
65 IF(IC,GE,25)STOP1000 TURE1295
66 DO 50 I=1,IS TURE1296
67 DO 50 I=1,IS TURE1297
68 50 BC2(I)=BRC2(I) TURE1298
69 GO TO 3 TURE1299
70 6 DT=T2-DT-BBT2 TURE1300
71 IF(ZIC,LE,DL)DT=0.0 TURE1301
72 T2=BBT2*(BBT2-T1)-DT TURE1302
73 T1=BBT2 TURE1303
74 TAPM=0.0 TURE1304
75 DO 60 I=1,IS TURE1305
76 P(I)=P(I)*BT2/PT TURE1306
77 C(I)=BRC2(I) TURE1307
78 X1(I)=X2(I) TURE1308
79 TMPH=TMPH+X1(I) TURE1309
80 60 CONTINUE TURE1310
81 PT=PRR(15) TURE1311
82 IF(MZ,GE,1000)RETURN TURE1312
83 DO 61 I=1,IS TURE1313
84 61 P(I)=PT*X1(I)/TMPH TURE1314
85 IF(ZIC,LT,285*XN)GO TO 63 TURE1315
86 XN=XN+1. TURE1316
87 JH=JH+1 TURE1317
88 TX(JH)=I1 TURE1318
89 63 CONTINUE TURE1319
90 IF(ZIC,LE,(ZII/30.)*JCC,TO,30) TURE1320
91 C WRITE(2,901)T1,T2,PT,ZIC TURE1321
92 ZIC=C TURE1322
93 MZ=MZ+1 TURE1323
94 MZIC(MZ)=ZIC TURE1324
95 WT(MZ)=T2 TURE1325
96 WTMPH(MZ)=TMPH TURE1326
97 WPT(MZ)=PT TURE1327
98 WVELL(MZ)=VELL TURE1328
99 DO 70 J=1,ISS TURE1329
100 WC(J,MZ)=C(J) TURE1330

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101      WM(J,MZ)=X2(J)
102 70      WDXA(J,MZ)=DXA(J)
103      IF(ZIC,GE,ZTT)GO TO 10
104 6901  FORMAT(1X,F10.3,F10.3,F10.3,F10.3,F10.3,F10.3,F10.3,F10.3,F10.3)
105 30      QTOT=QTOT+QING
106      QI(M3)=QI(M3)+QING
107      IF(ZIC,LT,Z33#FLOAT(M3))GO TO 2
108      M3=M3+1
109      GO TO 2
110 10      DO 20 I=1,ICU
111      RADD(I)=FADJ(I)
112 20      RACF(I)=RAC(I)
113      WRITE(6,902)QTOT
114      IEL=I+1,B5)GO TO 66
115      KRETURN
116 64      DO 65 I=JH,65
117 65      TX(I)=T1
118 902  FORMAT(1
119      RETURN
120      END
NET HEAT FLUX TO PROCESS FLUID 1.8167, 1.8101

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TUBE1331
TUBE1332
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TUBE1349
TUBE1350

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1  FUNCTION VIS(T,TCOND)
2  REAL*4 LOG
3  COMMON/TUBE1/IR,IS,KF(25),KR(25),B(25,10),BB(25,10),DL,IA(25,10)
4  REAL(25),EE(25),RAO,AD
5  COMMON/PYR03/Z(11),ZTT,C(25),CP(25,4)
6  DEL(25),DS(25),DE(25)
7  COMMON/PO/P(25),DN,SMWT(25),CLJ(25,2),VI(25),AMWT,VEL1,HI
8  DATA AA,439818,511,54245917,CC/,E6601820E-1,02,77,80511E-2/
9  DATA A1/2.6693E-5/,TILC/10./
10 IF(ABS(T-10.0),LE,25,10) GO TO 5
11 TOLD=T
12 PT=0.0
13 DO 1 I=1,IS
14 PT=PI*PI*I
15 PRESPT=0.
16 DO 2 J=1,IS
17 IF(CLJ(I,1),EQ,0) GO TO 2
18 E=LOG(T/CLJ(I,2))
19 VI(I)=A1*SORT(SMWT(I)*T)/(CLJ(I,1)**2*EXP(A+BI*E+CC*E**2+D*E**3))
20 CONTINUE
21 VIS=0.
22 TCOND=0.0
23 DO 3 I=1,IS
24 IF(CLJ(I,1),EQ,0,1) GO TO 3
25 V=PT(I)/PT*VI(I)
26 TC=(CP(T,1)+2.434)*V/(1+SMWT(I))
27 U=0.
28 DO 4 J=1,IS
29 IF(CLJ(J,1),EQ,0,1) GO TO 4
30 U=U+P(J)/PT*V/(SORT(J)/1+SMWT(J))/SMWT(J)*V/(1+SMWT(J))**5
31 1*(SMWT(J)/SMWT(I))**25)*2
32 CONTINUE
33 VIS=VIS+V/U
34 TCOND=ICOND+P(I)/PI*TC/U
35 CONTINUE
36 VIS=VIS*.0672
37 TCOND=TCOND*.435,15
38 C TERM=CONDUCTIVE IN BTU/(HR*FT**2/FT**K)
39 C WRITE(2,907)VIS,TCOND
40 C907 FORMAT(1,VIS=1,E15,5,1 TCOND=1,E15,5)
41 RETURN
42 VIS=VIS
43 RETURN
44 END

```



```

1 SUBROUTINE PRESC(T1,T2,PD,TPH)
2 REAL*4 LEG
3 COMMON/PYRC/3/2(11),ZTT,C(25),CP(25,4)
4 DDH(25),DS(25),DE(25)
5 COMMON/TUBE/IR,IS,KF(25),KR(25),B(25,10),BB(25,10),DL,IA(25,10)
6 EA(25),EA(25),RAD,AO
7 COMMON/PE/P(25),NH,SMWT(25),CLJ(25,2),VI(25),AMWT,VEL1,HI
8 COMMON/PTZ/IT,RI1,RI2,VISS
9 COMMON/SET/MY,MZ,IB,IPLOT,OLS
10 C THIS SUBROUTINE CALCULATES PRESSURE DROP FROM BERNOULIE LAW
11 C MODIFIED TO TAKE FRICTION LOSS INTO CONSIDERATION
12 DATA A2/1.1620925E-4/A3/7.37495E4/
13 DATA PRESOT/0.0/GC/1.3143/
14 I=1,I2=2
15 VISS=VIS(T,TCUND)
16 RT=C*Q
17 DO 2 I=1,15
18 2 PT=PI*P(I)
19 1 AMWT=0.
20 HCFB=0.0
21 VEL2=A2*T2/(PY-PRESDT)/RAD**2*TPH
22 DO 5 I=1,15
23 HCPB=H(CP(I)*P(I))*P(I)/PT/SMWT(I)
24 5 AMWT=P(I)/I*SMWT(I)*AMWT
25 C GC IN AT,*FT**3 /((OK LB,MOLES)
26 DELT=(LCAT)*AMWT
27 IF(DEL,LE,0.)GO TO 21
28 6 VELA=(VEL1+VEL2)/2.
29 REMU=2.*RAD*DEN*VELA/VISS
30 IF(REMUE,0.)GO TO 19
31 IF(REMUE,LE,3500.)GO TO 20
32 GO TO 19
33 20 F=64./REMUE
34 GO TO 100
35 10 F=0.00560+.5/(REMUE**.32)
36 100 PD=DEL*(VELA**2*F*DL/RAD+VEL2**2*VEL1**2)/62.4/2.16*B
37 PD*ABS(PD)
38 PD=PI*PD
39 IF(P2,LE,0.)GO TO 21
40 VEL2=A2*PI/P2/RAD**2*TPH
41 IF(PD,EQ,0.)GO TO 7
42 IF(A3*((PRESDT-PD)/PD),LE,.001)GO TO 7
43 PRESOT=PD
44 DEL=(P2+PI)/I2.*GC*II*AMWT
45 GO TO 6
46 7 PT2=0.
47 DO 9 I=1,15
48 9 PIR=PI*P(I)
49 IF((IPLOT,EQ,2),OR,(IPLOT,EQ,3),AND,(MZ,EQ,1))GO TO 1001
50 VELL=VEL2

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PRES1395
PRES1396
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PRES1443
PRES1444

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51 HI=.0207*TCND/RAD*RENL**,8*(HCP*.VISS/TCND*3600.*1,8)**,.333333 PRES1443
52 C HI=JL*ETU/JET**2-HR-3K) PRES1446
53 IF(VEL1,GE,1214.5)GO TO 22 PRES1447
54 IF(VEL1,GE,SUBT(A3*P2/DELT))GO TO 22 PRES1448
55 31 CONTINUE PRES1449
56 RETURN PRES1450
57 22 MZ=3000 PRES1451
58 RT=5 PRES1452
59 RETURN PRES1453
60 1001 WRITE(2,9001)REHU, VISS,DEN,F,VEL1,VEL2,VELA,T,PD PRES1454
61 VEL1=VEL2 PRES1455
62 RETURN PRES1456
63 19 WRITE(2,900)RAD,DEN,VELA,VISS,PREHU PRES1457
64 WRITE(2,902),I,PI,P(I),I=1,IS)+GC,AMWT,P2 PRES1458
65 MZ=2000 PRES1459
66 RETURN PRES1460
67 21 WRITE(2,902),I,PT,(P(I),I=1,IS),GC,AMWT,P2 PRES1461
68 MZ=2000 PRES1462
69 RETURN PRES1463
70 900 FORMAT(1 BAR=1,1PE12.5,1LEM,VELA,VIS,RENU,1/4(2X,1PE12.5)) PRES1464
71 901 FORMAT(1 PRESSURE DROP =1,1PE12.5,1DEN,VELA,DL,VEL1,VEL2,1/5(2X,1PPRES1465
1E12.5)) PRES1466
72 902 FORMAT(1 T PI P(1)=P(IS), GC AMWT,PT2 1,5(1X,FR,2)/) PRES1467
73 903 FORMAT(1 FRICTION PD(T),1/1,1,RENU=1,1PE14.5,5X,1VISS=1,1PE14.5,5X,PRES1468
1,1PE14.5,1/1 FRICTION FACTOR=1,1PE14.5,5X,1VI,V2,VA=1,3(1PEPRES1469
1,4.5,5X),1,TEMPERATURE=1,OPREB,2,1PRESSURE DE1,1PE14.5)
74 904 END PRES1470
75 905 PRES1471
```

```

1  SUBROUTINE TEMPT(TSKIN,ZIC,IND)
2  COMMON/ANDY/I1(60),I2(60),I3(60),C1(10),C2(10),C3(10),ZX(7)
3  IF(IND.EQ.2)GO TO 5
4  ZX(1)=0.0
5  DO I =2,7
6  ZX(I)=ZX(I-1)+.14/.73
7  CALL PZERU(T1(1),Z10)
8  CALL READ(3,ITEM,I1(1),60)
9  CALL READ(3,ITEM,I2(1),60)
10 CALL READ(3,ITEM,I3(1),60)
11 X1=FITIT(ZX(1),I1(9),7,5,C1(1),1,1,1)
12 X2=FITIT(ZX(1),I2(9),7,4,C2(1),1,1,1)
13 X2=FITIT(ZX(1),I3(9),7,4,C2(1),1,1,1)
14 WRITE(4,101)X1,X2,X3
15 901 FORMAT(1 STANDARD DEVIATION TEMPERATURE CURVE',3E16.7)
16 IND=2
17 5 ZSE=ZIC-FLUAT(INT(ZIC)/56)*56.
18 IF(ZSE.GT.20.0)ZSE=20.0
19 IF(ZIC.LT.140.)GO TO 10
20 IF(ZIC.LT.220.)GO TO 15
21 TSKIN=EQVA(ZSE,C3(1))
22 GO TO 16
23 10 TSKIN=EQVA(ZSE,C1(1))
24 GO TO 18
25 15 TSKIN=EQVA(ZSE,C2(1))
26 18 IF(TSKIN.LT.700.)DR,TSKIN,GI,1400.,1GO TO 20
27 RETURN
28 20 WRITE(6,500)TSKIN
29 900 FORMAT(1 TEMPERATURE OF REACTOR WALL OUTSIDE OF RANGE T= ',E18.5)
30 TSKIN=1120
31 RETURN
32 END
TEMP1472
TEMP1473
TEMP1474
TEMP1475
TEMP1476
TEMP1477
TEMP1478
TEMP1479
TEMP1480
TEMP1481
TEMP1482
TEMP1483
TEMP1484
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TEMP1486
TEMP1487
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TEMP1495
TEMP1496
TEMP1497
TEMP1498
TEMP1499
TEMP1500
TEMP1501
TEMP1502
TEMP1503

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1  SUBROUTINE FURN          FURN1504
2  COMMON // DUMHY(3),KK, ICODE, HCODE, EURN1505
3  A TAU(9), VAREA, HAREA, XLX, XK(3), ACOEF(8,3), FURN1506
4  A TBRIDG, PLES, FLUET, ELUELS), XMAX, TSINK, FURN1507
5  A NCR, HDUTY, HTVAL, FRATE, KFUEL, XAIR, FTMP, FURN1508
6  A HSSBLK, NGSBLK, NSGSLK, HSURE, NVCL, FURN1509
7  A XSURFX(9), XJ, YJ, ZLONG, NCUL, NRDW, NXSYN, FURN1510
8  A RSTART, ICODE, SCODE, NGRAY, JHCHC, EURN1511
9  A K1, K2, RCRU(10), TDEP(100), PERM(200), NPRINT FURN1512
10 C                                     FURN1513
11 COMMON /CPIV/ CPCP(11), HNV(12) FURN1514
12 C                                     FURN1515
13 C                                     FURN1516
14                                     FURN1517
15 INTEGER SCODE, ICODE, RSTART, HCODE FURN1518
16 EQUIVALENCE (DUMHY(1),KHTCL5), (DUMHY(2),KHTCL6), FURN1519
17 1 (PERM(199),DHTCL5), (PERM(200),DHTCL6) EURN1519
18 C                                     FURN1520
19 C                                     FURN1521
20 C                                     FURN1522
21 CALL PZERO(DUMHY(1),400) FURN1523
22 K1=1 FURN1524
23 K2=6 FURN1525
24 WRITE(K2,876) FURN1526
25 876 FORMAT (1H1) FURN1527
26 C READ AND WRITE TABLE TITLE CARDS HERE FURN1528
27 DO 802 J=1,3 FURN1529
28 READ(K1,101)(PERM(N),N=1,18) FURN1530
29 801 FORMAT (18A4) FURN1531
30 WRITE(K2,821)(PERM(N),N=1,18) FURN1532
31 821 FORMAT(15X,18A4) FURN1533
32 802 CONTINUE FURN1534
33 C                                     FURN1535
34 NCODE = 0 FURN1536
35 C                                     FURN1537
36 C RSTART = 0 DO RSTART FURN1538
37 C 1 GENERATE RESTART DISKS FURN1539
38 C 2 CASE USES RESTART DISKS FURN1540
39 C                                     FURN1541
40 C ICODE = 0 ALL VOL AND SURF TEMP TO BE READ IN FURN1542
41 C 1 MIN MAX TEMP KNOWN FURN1544
42 C 2 CALC MIN MAX TEMP FROM ADIABATIC FLAME TEMP FURN1545
43 C 3 USE TEMP DATA FROM RESTART DISKS FURN1546
44 C                                     FURN1547
45 C SCODE = 0 VOL AND SURF TEMP ARE ALL VARIABLES FURN1548
46 C 1 SOME VOL TEMP ARE TO BE HELD CONSTANT FURN1549
47 C 2 SOME SURF TEMP ARE TO BE HELD CONSTANT FURN1550
48 C 3 SOME VOL + SURF TEMP ARE TO BE HELD CONSTANT FURN1551
49 C JHCHC = 0 HEATINGLESS FURN1552
50 C 1 REVISE HEAT TRANSFER COEFFICIENTS ONLY IF RSTART = 2 FURN1553

```

```

51 C      NSTART = 0 NEW CASE
52 C      1 PREVIOUS CASES HAVE BEEN RUN - TREAT AS RESTART CASE
53 C
54 C      NCASE = 0 NO MORE CASES TO FOLLOW
55 C      1 ANOTHER CASE WILL FOLLOW
56 C
57 C      NPRINT = 0 DETAIL RESULTS PRINTED
58 C      1 DETAILED RESULTS NOT PRINTED
59 C
60 C      READ(K1,2) NSTART, TCODE, SCODE, NGRAY, JHCHC, NSTART, NCASE, NPRINT
61 C      2 FORMAT (BI10)
62 C
63 C      IF ( NSTART .EQ. 0 ) NSTART = 2
64 C
65 C      IF ( NSTART .EQ. 2 ) GO TO 6
66 C
67 C      4 CONTINUE
68 C      GO TO 10
69 C
70 C      CALL READ(4, NSTART, DUMMY(1), 400)
71 C      IF ( ZLUNG .LE. 0 .OR. QUANT(3) .LE. 0 .OR.
72 C      1 NCOL .LE. 0 .OR. NROW .LE. 0 .OR.
73 C      2 NSURE .LE. 0 .OR. INVL .LE. 0 .OR.
74 C      3 NCR .LE. 0 ) GO TO 111
75 C      NSTART = 1
76 C      10 READ (K1, 11) NVMS, NVMAX, NSMAX, KHICL5, KHICL6, DWICL5, DWICL6
77 C      11 FORMAT ( 5I10, 2F10, 2 )
78 C
79 C      CALL CL1 ( NCASE, NSTART, NVNSH, NVMAX, NSMAX )
80 C
81 C      IF ( RSTART .EQ. 2 ) GO TO 40
82 C
83 C      RETURN
84 C      ENTRY EUPND
85 C      CALL CL2
86 C      CALL CL3
87 C      RETURN
88 C      ENTRY EUPN1
89 C      NDCINE = 0
90 C
91 C      DO 60 N=1, NVNSH
92 C      WRITE (K2, 2) J, N
93 C      1 FORMAT (I11, 14X, 35HE) ENERGY BALANCE INTERMEDIATE RESULTS/15X,
94 C      1 25(I11=) /15X, 12HE) SERIAL NO)
95 C      HCODE = 0
96 C      ICODE = 0
97 C      CALL CL4
98 C
99 C      DO 52 NV=1, NVMAX
100 C      WRITE (K2, 20) J, NV

```

FURN1554
EURN1555
FURN1556
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FURN1596
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FURN1598
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FURN1600
EURN1601
FURN1602
EURN1603

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101 2011 F0RMA7 (////15X,60HGAS VOLUME ENERGY BALANCE RESULTS, INTERMEDIATFURN1604
102 IF TRIAL NUMBER 110 ) FURN1605
103 CALL CL5 FURN1606
104 IF ( HCODE .EQ. 2 .OR. NV .EQ. NVMAX ) GO TO 54 FURN1607
105 51 CONTINUE FURN1608
106 HCODE = 10 FURN1609
107 CALL CL4 FURN1610
108 HCODE = 1 FURN1611
109 52 CONTINUE FURN1612
110 C FURN1613
111 54 DD 56 NS=1, NSMAX FURN1614
112 WRITE (42,2021) NS FURN1615
113 2021 F0RMA7 (////15X,62HSURFACE AREA ENERGY BALANCE RESULTS, INTERMEDIATFURN1616
114 DATE TRIAL NUMBER110) FURN1617
115 CALL CL6 FURN1618
116 55 IF ( ICODE .EQ. 2 .OR. NS .EQ. NSMAX ) GO TO 57 FURN1619
117 ICODE = 10 FURN1620
118 CALL CL4 FURN1621
119 ICODE = 1 FURN1622
120 56 CONTINUE FURN1623
121 C FURN1624
122 57 IF ( HCODE .EQ. 2 .AND. NV .EQ. 1 .AND. FURN1625
123 1 ICODE .EQ. 2 .AND. NS .EQ. 1 ) HCODE = 1 FURN1626
124 IF ( HCODE .EQ. 1 ) GO TO 70 FURN1627
125 60 CONTINUE FURN1628
126 C FURN1629
127 70 KK = NDOVE FURN1630
128 CALL CL7 FURN1631
129 C FURN1632
130 C FURN1633
131 RETURN FURN1634
132 90 IF ( RSTART .EQ. 0 ) GO TO 999 FURN1635
133 IF ( NCASE .NE. 0 ) GO TO 999 FURN1636
134 111 WRITE(2,112) FURN1637
135 112 F0RMA7(11,20X,'RESTART NO GOOD CHECK DS231') FURN1638
136 999 RETURN FURN1639
137 END FURN1640

```

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1 SURROUTINE CL1 ( NCASE, NSTART, NVNSM, NVMAX, NSMAX ) CL1 1641
2 C CL1 1642
3 COMMON // DUMMY(3), KK, ICODE, HCODE,
4 A TAU(9), VAREA, HAREA, XLX, XK(3), ACDEF(8,3),
5 A TERIDG, PRES, FLOET, FLUE(5), XPMX, TSINK,
6 A NCR, HUBY, HVAL, ERATE, KEUEL, XAIR, FTEMP,
7 A NSSBLK, HGSBLK, NSGBLK, NGGRBK, HSURF, NVOL,
8 A XSUREX(4), XQ, YQ, ZLONG, NCOL, URDQ, HXSKN,
9 A RSTART, TCODE, SCODE, NCFAY, JCHGC,
10 A K1, K2, RCRD(10), TDEP(10), PERM(200)
11 C
12 INTEGER SCODE, TCODE, RSTART, HCODE
13 EQUIVALENCE (DUMMY(1), KHTCL5), (DUMMY(2), KHTCL6),
14 I (PERM(10), DHTCL5), (PERM(200), DHTCL6)
15 C
16 COMMON /50/ A(10,5), S(12,7), C(11,7), G(4,7)
17 C
18 WRITE (K2,11) RSTART, TCODE, SCODE, JCHGC, NSTART, NCASE,
19 I NVNSM, NVMAX, NSMAX, KHTCL5, KHTCL6, DHTCL5, DHTCL6
20 ALL FORMAT ( // // // 15X 14HPROBLEM CODES / 15X 13(1H, )
21 A // 20X 12HPRESTART CODE I28
22 B / 20X 21HTEMPERATURE DATA CODE I19
23 C / 20X 23HTEMPERATURE CALCULATION CODE I12
24 D / 20X 31HHEAT TRANSFER COEFFICIENT CODE I10
25 E // 20X 18HPREVIOUS CASE CODE I22
26 F / 20X 22HSUBSEQUENT CASE CODE I20
27 G // 20X 32HNUMBER OF OVERALL ENERGY BALANCES I17
28 H / 20X 36HNUMBER OF GAS VOLUME ENERGY BALANCES I14
29 I / 20X 38HNUMBER OF SURFACE AREA ENERGY BALANCES I12
30 M // 20X 26HNUMBER OF GAS VOLUME ENERGY BALANCES USING CURRENT INTECL1 1670
31 NCHARGE AREAS, I12
32 D / 20X 7HNUMBER OF SURFACE AREA ENERGY BALANCES USING CURRENT INTCL1 1672
33 PERCHANGE AREAS, I10
34 A // 20X 57HTOLERANCE ON GAS VOLUME ENERGY BALANCE, DEG. F.
35 I F13.3
36 K / 20X 49HTOLERANCE ON SURFACE AREA ENERGY BALANCE, DEG. F.
37 L F11.3 )
38 C
39 KERR = 0
40 C
41 C DEFINE FURNACE GEOMETRY, AND HEAT RELEASE PATTERN
42 C
43 15 CALL AAA ( KERR )
44 C
45 C READ FUEL CODE, EXCESS AIR, FUEL TEMP, BRIDGE WALL TEMP,
46 C AND BOX PRES.
47 C
48 C KEUEL --- 0 OIL FIRING
49 C 1 GAS FIRING
50 C

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```

51 IF ( RSTART .EQ. 2 ) GO TO 31
52 21 READ (K1,23) KFUEL, XAIR, FIEMP, TBRIDG, PRES
53 23 FORMAT (110,4F10,0)
54 IF ( FIEMP .EQ. 0 ) FIEMP = 60.0
55 IF ( TBRIDG .EQ. 0 ) TBRIDG = 460.0
56 WRITE (K2,3020) KFUEL, XAIR, FIEMP
57 8020 FORMAT ( 1H1, 14X, 13HFUEL ANALYSIS / 15X, 13H-----//
58 120X, 23HFUEL CODE (OIL,GAS) 125 / 20X, 20HEXCESS AIR, PER CENT 1698
59 2, F20.2 / 20X, 30HFUEL-AIR MIXTURE TEMP., DEG, F 1699
60 FIEMP = FIEMP + 460.0
61 TBRIDG = TBRIDG + 460.0
62 C
63 C COMPUTE FUEL ANALYSIS AND THE SPECIFIC HEAT + ENTHALPY DATA
64 C
65 31 CALL SUB ( KERR )
66 C
67 C ESTABLISH TEMPERATURES
68 C
69 IF ( RSTART .EQ. 2 .AND. TCODE .EQ. 3 ) GO TO 41
70 CALL CCC
71 C
72 C ESTABLISH VOLUME AND SURFACE DATA
73 41 JUNK = 0
74 IF ( RSTART .EQ. 2 .AND. JHCHC .EQ. 0 ) JUNK = 1
75 IF ( RSTART .EQ. 2 .AND. JHCHC .EQ. 1 ) JUNK = 2
76 CALL DDU ( JUNK, KERR )
77 C
78 C CHARACTERIZE FLUE GAS
79 C
80 51 IF ( RSTART .EQ. 2 ) GO TO 61
81 CALL EEE
82 C
83 61 IF ( KERR .EQ. 0 ) RETURN
84 STOP
85 END

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CLI 1691
CLI 1692
CLI 1693
CLI 1694
CLI 1695
CLI 1696
CLI 1697
CLI 1698
CLI 1699
CLI 1700
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CLI 1724
CLI 1725

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1 SUBROUTINE AAKKAPUT)
2 COMMON // CUNNY(3),KK, ICODE, HCODE,
3 A TAU(9), VAREA, HAREA, XLX, XK(3), ACOEF(6,3),
4 A TERIDG, PRES, FLUEL, FLUE(5), XMAX, ISINK,
5 A NCR, HOUTY, HTVAL, FPATE, KFUEL, XAIR, FTEMP,
6 A NSSBLK, NGGBLK, NSSBLK, NGGBLK, NSURE, NVOL,
7 A XSURFX(9), XG, YD, ZLNG, NCOL, NROW, NXSN,
8 A RSTART, TCODE, SCODE, NGRAY, JGANG,
9 A K1, K2, RCRD(10), TDEP(100), PERP(200)
10 C
11 INTEGER SCODE,TCODE,RSTART,HCODE
12 EQUIVALENCE (Z1(1),Z(1)),(Z2(1),Z(61))
13 DIMENSION Z(120),Z1( 60),Z2( 60)
14 KEPR=0
15 IF(RSTART.EQ.2) GO TO 30
16 C FURNACE GEOMETRY-- DIMENSIONS ARE IN FEET
17 READ(K1,16) NCOL,NROW,XWIDE,YHIGH,ZLONG,XLX,(XSURFX(J),J=1,9)
18 16 FORMAT(2I10,4F10,2(3F10,2))
19 IF(FLOAT(NCOL*NROW)*XWIDE*YHIGH*ZLONG.GT.0.0)GO TO 21
20 KEPR=1
21 WRITE(K2,1F) NCOL,NROW,XWIDE,YHIGH,ZLONG
22 18 FORTNAT(27H FURNACE GEOMETRY INCORRECT/10X,5HCOL =15,10X,5HROW =15
23 1/10X,3HX =F10.4,10X,3HY =F10.4,10X,3H Z=F10.4)
24 GO TO 30
25 21 X0=XWIDE/FLDAT(NCOL)
26 Y0=YHIGH/FLDAT(NROW)
27 NVOL=NCOL*NROW
28 NXSN=0
29 DO 22 J=1,9
30 IF(XSURFX(J).EQ.0)GO TO 24
31 NXSN=1+NXSN+1
32 XSURFX(J)=(AINT(XSURFX(J)/X0+.5))*X0
33 CONTINUE
34 24 NSURE=2*(NCOL+NROW)+1+XSUN*NROW
35 NCR=2*(NCOL+NROW)
36 NSSBLK=NSURE/15
37 IF(NSSBLK#15=NSURF.EQ.0)GO TO 25
38 NSSBLK=NSSBLK+1
39 25 NGGBLK=NVOL/15
40 IF(NGGBLK#15=NVOL.EQ.0) GO TO 26
41 NGGBLK=NGGBLK+1
42 26 NSSBLK=NSSBLK
43 NSGGLK=NGGGLK
44 IF(NVOL.E.60.AND.NSURE.E.60)GO TO 28
45 KEPR=1
46 WRITE(K2,27) NVOL,NSURF
47 27 FORTNAT(1 NUMBER OF GAS VOLUMES AND/OR SURFACE AREAS EXCEEDED : 60),AAA 1772
48 1/10X,1 GAS VOLUMES =15,10X,1 SURFACE AREAS=1,15)
49 GO TO 30
50 28 WRITE(K2,8000)XWIDE,YHIGH,ZLONG,(J,XSUBEX(J),J=1,9),NCOL,
AAA 1726
AAA 1727
AAA 1728
AAA 1729
AAA 1730
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AAA 1773
AAA 1774
AAA 1775

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51 1NR0W,XD,YD,NVOL,NSURF          AAA 1776
52 8000  FURNACE GEOMETRY,15X,1,1  AAA 1777
53 1,2,20X,15HSIZE OF FURNACE  F33,2,25X,11H,10TH, FEET,  F33,2,25AAA 1778
54 2X,12HEIGHT, FEET, F33,2,25X,12LENGTH, FEET, F32,2,25X, AAA 1779
55 36INTERMEDIATE TUBE ROW LOCATION, FEET9(1,53X,15,F10,2)///,20X,  AAA 1780
56 4SUBDIVISIONS OF FURNACE,25X,100, OF COLUMNS,129,25X,  AAA 1781
57 5IND. OF ROWS,132///,25X,100, OF COLUMNS,129,25X,  AAA 1782
58 6RCD, HEIGHT, FEET, F33,2,25X,100, OF GAS VOLUMES,125,25X,  AAA 1783
59 7 I NO OF SURFACE AREAS,123)  AAA 1784
60 C DUTY(MM-RV,HR),HEAT-AVAILABILITY(BTU/LB-FUEL)  AAA 1785
61 30 READ(K1,31)HDUTY,HTVAL  AAA 1786
62 31 FORMAT(2E15,2)  AAA 1787
63 IF(HDUTY*HTVAL,NE,0,0)GO TO 33  AAA 1788
64 KERR1  AAA 1789
65 WRITE(K2,32)HDUTY,HTVAL  AAA 1790
66 32 FORMAT(1,FURNACE FIRING RATE AND OR FUEL HEATING VALUES ARE NOT  AAA 1791
67 1COMPLETE/10X,1 FIRING RATE (MM BTU/HR) =1,F20,5 ,10X,1FUEL HEAT,AAA 1792
68 2INC-VALUE (BTU/LB) =1,E15,0)  AAA 1793
69 GO TO 34  AAA 1794
70 C FDATE=10, FUEL/FT OF FURNACE LENGTH  AAA 1795
71 33 FDATE=HDUTY/HTVAL*1.E6/ZLONG  AAA 1796
72 C HEAT RELEASE PATTERN EXPRESSED AS BTU/HR/FT OF FURNACE  AAA 1797
73 C READ DATA IN AS A PERCENTAGE OR FRACTION OF TOTAL HEAT RELEASED  AAA 1798
74 34 CALL PZERR(Z1,1,120)  AAA 1799
75 READ(K1,35)(Z1(N),N=1,NVPL)  AAA 1800
76 READ(K1,35)(Z2(N),N=1,NSURF)  AAA 1801
77 35 FORMAT(7F10,0)  AAA 1802
78 SUM=0.0  AAA 1803
79 DO 36 N=1,120  AAA 1804
80 SUM=SUM+Z(N)  AAA 1805
81 36 CONTINUE  AAA 1806
82 IF(HDUTY*ZLONG*SUM,EQ,0,0)GO TO 40  AAA 1807
83 FAC=HDUTY/ZLONG*1.E6/SUM  AAA 1808
84 DO 37 N=1,120  AAA 1809
85 Z(N)=Z(N)*FAC  AAA 1810
86 37 CONTINUE  AAA 1811
87 CALL WRITE(2,1HGAS,1,Z1(1), 60)  AAA 1812
88 CALL WRITE(2,1HSURF,1,Z2(1), 60)  AAA 1813
89 WRITE(K2,60)HDUTY,HTVAL  AAA 1814
90 8010 FORMAT(1E15,15X,1EURNACE HEAT DUTY AND HEAT RELEASE PATTERN,1/  AAA 1815
91 115X,1-----1///,20X,1HEAT DUTY  AAA 1816
92 2,MN,1BTU/HR ,1,E16,5/23X,1HEAT AVAILABILITY/25X,1BTU/LB OF FUEL,1AAA 1817
93 316,0)  AAA 1818
94 WRITE(K2,8020)(Z1(N),N=1,NVOL)  AAA 1819
95 8020 FORMAT(1/20X,1HEAT RELEASE PATTERN --- BTU/HR/FOOT OF FURNACE,1/25AAA 1820
96 1X,1GAS VOLUMES,1/25X,6E15,0)  AAA 1821
97 WRITE(K2,8030)(Z2(N),N=1,NSURF)  AAA 1822
98 8030 FORMAT(1/25X,1 SURFACE AREAS,1/25X,6E15,0)  AAA 1823
99 IF(KERR,NE,0)KAPUT=KERR  AAA 1824
100 40 CONTINUE  AAA 1825

```

101 RETURN
102 END

AAA 1826
AAA 1827

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1  SURROUTINE BBB(KAPUT)
2  C  COMPUTE FUEL-CAS SPECIFIC HEAT+ENTHALPY
3  C  (SPECIFIC HEAT AND ENTHALPY DATA TO BE STORED IN POLYNOMIAL FORM)
4  C
5  COMMON // DUMMY(3),KK, ICODE, HCODE,
6  A TAU(9), WAREA, WAREA, XLX, XK(3), ACDEF(8,3),
7  A TFRIDG, PRES, FLUET, FLUE(5), XMX, TSINK,
8  A MCR, HOLTY, HVAL, ERATE, KEUEL, XAIR, FTEMP,
9  A NSSBLK, MSGBLK, MSGBLK, NGG6LK, NSURF, NVOL,
10 A XSUREX(2), XG, YD, ZLNG, NCOL, NROW, HXSXN,
11 A RSTART, TCODE, SCODE, NGRAY, JCHCG,
12 A K1, K2, ROAD(10), IDEP(100), PERM(200)
13 C
14 INTEGER SCODE, ICODE, RSTART, HCODE
15 COMMON/ED/ A(10,5),Z(12,7),C(11,7),CMW(7)
16 COMMON/CRHW/ CR(11),HW(12)
17 REAL COMP(25),CMWGAS(25),FWT(5)
18 DATA CMWGAS /16.30,1.44,1.258,1.2*72+1.86,2.100,2.114,2.28,0.42,
19 11,4*56,1,26,1,40,1,54,1,28,0,44,0,2,0,34,1,18,0,28,0/
20 KEPR=0
21 IF(RSTART.EQ.2)GO TO 60
22 FLUET=1.
23 XMX=1.
24 IF(KFUEL.NE.1)GO TO 60
25 C  COMPUTE FUEL GAS ANALYSIS ON A PER FOOT OF FURNACE BASIS
26 C  FLUE(1)  CO2
27 C  FLUE(2)  H2O
28 C  FLUE(3)  SO2
29 C  FLUE(4)  O2
30 C  FLUE(5)  H2
31 C  FUEL DATA -- OIL FIRING
32 C  CRATO= WFC/WT BASIS
33 C  FSULF = WT % SULFUR IN FUEL OIL
34 C  STEAM = LB STEAM/LB FUEL OIL
35 READ(K1,35)FMW,FAP1,FBP,FWATK,HCRATO,FSULF,STEAM
36 35  FORMAT(7E10,0)
37 IF(STEAM.LT.0.0)OR(STEAM.GT.1.0)STEAM=0.5
38 34ATE=FBP*STEAM
39 C  PRIORITY OF MOL WT DETERMINATION
40 C  1  MOL WT-K40W
41 C  2  API+BP
42 C  3  BP+WATK
43 C  4  API+WATK
44 C  5  BP
45  KJ=0
46 IF(FMW.GT.0)GO TO 57
47 IF(FBP.NE.0)KJ=4
48 IF(FAP1*WATK.NE.0)KJ=3
49 IF(FBP*WATK.NE.0)KJ=2
50 IF(FAP1*FBP.NE.0)KJ=1

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BBB 1828
BBB 1829
BBB 1830
BBB 1831
BBB 1832
BBB 1833
BBB 1834
BBB 1835
BBB 1836
BBB 1837
BBB 1838
BBB 1839
BBB 1840
BBB 1841
BBB 1842
BBB 1843
BBB 1844
BBB 1845
BBB 1846
BBB 1847
BBB 1848
BBB 1849
BBB 1850
BBB 1851
BBB 1852
BBB 1853
BBB 1854
BBB 1855
BBB 1856
BBB 1857
BBB 1858
BBB 1859
BBB 1860
BBB 1861
BBB 1862
BBB 1863
BBB 1864
BBB 1865
BBB 1866
BBB 1867
BBB 1868
BBB 1869
BBB 1870
BBB 1871
BBB 1872
BBB 1873
BBB 1874
BBB 1875
BBB 1876
BBB 1877

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```

51 IF(KJ.EC.0)GO TO 53
52 GO TO (42,45,46,52),KJ
53 C KJ=1 B3 CHART 3=25
54 42 FSP=AMINI(FBP,1200.)
55 FBP=AMAX1(FBP,100.)
56 B=(FBP+460.)/1000.
57 IF(FBP.LE.750.)GO TO 43
58 FAPI=AMINI(FAPI,40.)
59 FAPI=AMAX1(FAPI,-30.)
60 S=141.5/(FAPI+131.5)
61 GO TO 44
62 43 EAPI=AMAX1(FAPI,0.)
63 S=141.5/(FAPI+131.5)
64 SWIN=(0.6255337E-2**3-C.40641530)*B**2+
65 1 S=AMAX1(S,SWIN)
66 44 FMN=-458.6322+58.096181*S**4-314.00029*S**3+16.97091*(S**2)**3
67 44 1 -401.56651E-23.8014649#0**6+24.871805/(S**2**4)-10.016105/(S**8)8888 1895
69 2**31+94.833174*S**4/R+457.375285/R-77.255634*(S/3)**3+3.448174*(888 1896
70 3S/R)**6-39.225111*S**3+22.007545*(R/S)**3-92716166*(R/S)**6 888 1897
71 GO TO 57
72 C KJ=2 BB CHART 2=20 TO OBTAIN API THEN DO KJ=1
73 45 FBP=AMINI(FBP,1000.)
74 FBR=AMAX1(FBP,100.)
75 FWATK=AMINI(FWATK,14.)
76 FWATK=AMAX1(FWATK,9.)
77 B=(FBP+460.)/1000.
78 AK=FWATK/10.
79 FAPI=-102.40915+139.36071*AK-7.90343*AK**2-28.81656*AK**3+0.06136**8**5888 1906
80 1+9.84756*AK/B-0.16243*(AK/B)**5
81 GO TO 42
82 C KJ=3 B4 CHART 2=20 TO OBTAIN BP THEN DO KJ=1
83 46 FWATK=AMINI(FWATK,14.)
84 FWATK=AMAX1(FWATK,9.)
85 FAPI=AMINI(FAPI,105.)
86 FAPI=AMAX1(FAPI,20.)
87 47 S=141.5/(FAPI+131.5)
88 AK=FWATK/10.
89 X1=S/AK
90 X2=AK/S
91 B=-0.466039378+(-0.094640507*S**4+0.39503379)*S-0.01592527*AK**5
92 1+((-0.1002351*X1+0.19565272)*X1**2+0.6665293E=1)*X1**2+(-0.317791883 1919
93 282E-3*X2**4+0.1485872)*X2+0.10089545E+1*(S*AK)**3
94 FBP=1000.-460.
95 IF(FBP.GE.100.)GO TO 51
96 FAPI=AMAX1(FAPI,24.)
97 GO TO 47
98 48 LE(FBP,LE.1000.)GO TO 42
99 FAPI=AMINI(FAPI,42.5)
100 GO TO 47

```

```

101 C KJ=4 BB CHART 3-20      888 1926
102 52 B=(FRP+460.)/1000.      888 1929
103 FMW=-1.446891+81.959317*F+152.39287*8**3-9.97706*8**5      888 1930
104 GO TO 57                    888 1931
105 53 KERR=1                    888 1932
106 WRITE(K2,55)                 888 1933
107 55 FORMAT(1 INSUFFICIENT DATA TO COMPUTE MOL WT OF FUEL OIL 1)  888 1934
108 GO TO 80                    888 1935
109 C HC COMPOSITION X=ATOMS OF CARBON Y = ATOMS OF HYDROGEN      888 1936
110 57 IF(HCRATIO.NE.0.0)GO TO 59 888 1937
111 KERR=1                       888 1938
112 WRITE(K2,58)                 888 1939
113 58 FORMAT(1 HYDROGEN CARBON RATIO MUST BE GIVEN TO FUEL GAS COMPOSITION 888 1940
114 )                              888 1941
115 GO TO 80                    888 1942
116 59 HCFAC=12.*HCRATIO        888 1943
117 X=FMW/(12.+HCFAC)          888 1944
118 Y=HCFAC*X                  888 1945
119 FMOL=FRATE/FMW             888 1946
120 C SULEUR RATE IN LB/HR/FT  888 1947
121 SLOHR=FRATE*FSULF/100.      888 1948
122 WRITE(K2,8030) FMW,EAR1,EBP,EWATK,HCRATIO,FSULE,SIFAM      888 1949
123 FORMAT(//20X, 'OIL FIRING',F27.2/25X,'API',F27.2/25X,'API',F27.2/25X,' 888 1950
124 F40.2/25X,'BULLING POINT (MEAN)',F23.2/25X,'WATSD',F35.2/25X,'ASB',F35.2/ 888 1951
125 2H/C RATIO, WT BASIS',F24.4/25X,'WT. % SULFUR',F31.4/25X,'ATOMIZA',F31.4/ 888 1952
126 25X,'STEAM',F30X, 'LBS. STEAM/ LB. FUEL OIL',F13.4) 888 1953
127 FLUE(1)=X*FMOL             888 1954
128 FLUE(2)=Y/2.*EMOL*SRATE/LB. 888 1955
129 FLUE(3)=SLOHR/32.          888 1956
130 RECO2=(1+(X+Y/4.)*EMOL)*SLOHR/32. 888 1957
131 FLUE(4)=RECO2*XAIR/100.    888 1958
132 FLUE(5)=79./721.*RECO2*(1.+XAIR/100.) 888 1959
133 GO TO 67                    888 1960
134 C FUEL DATA --- GAS FIRING 888 1961
135 60 READ(K1,35)(COMP(J),J=1,25) 888 1962
136 SUM=0.                      888 1963
137 DO 62 N=1,25                888 1964
138 SUM=SUM+COMP(N)            888 1965
139 62 CONTINUE                 888 1966
140 IF(SUM.NE.0.0)GO TO 64      888 1967
141 KERR=1                      888 1968
142 WRITE(K2,63)                888 1969
143 63 FORMAT(1 FUEL COMPOSITION REQUIRED!) 888 1970
144 GO TO 80                    888 1971
145 64 FMW=0.                   888 1972
146 DO 65 N=1,25               888 1973
147 COMP(N)=COMP(N)/SUM        888 1974
148 FMW=FMW+COMP(N)*CMWGAS(N) 888 1975
149 65 CONTINUE                 888 1976
150 WRITE(K2,8040)FMW,COMP(J),J=1,25) 888 1977

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151 FMOL=FRATE/FMW
152 B040 FORMAT(/2JX,IGAS FIPRNGI//25X,IMOLECULAR WEIGHT,15X,E12.2//25X,1BBB 1279
153 1FUEL COMPOSITION MOLE FRACTION//30X,1METHANE,1F20,6/30X,1ETHANE,1F20,6/30X,1F29,6/30X,1BUTANE,1F29,6/30X,1PENTANE,1F29,6/30X,1HEXANE,1F29,6/30X,1HEPTANE,1F29,6/30X,1OCTANE,1F29,6/30X,1NONANE,1F29,6/30X,1DECANE,1F29,6/30X,1DODECANE,1F29,6/30X,1ETHYLENE,1F27,6/30X,1PROPYLENE,1F26,6/30X,1BUTYLENE,1F26,6/30X,1PENTYLENE,1F26,6/30X,1HEXYLENE,1F26,6/30X,1OCTYLENE,1F26,6/30X,1CARBON MONOXIDE,1F20,6/30X,1PROPANE,1F20,6/30X,1BUTANE,1F20,6/30X,1PENTANE,1F20,6/30X,1HEXANE,1F20,6/30X,1HEPTANE,1F20,6/30X,1OCTANE,1F20,6/30X,1NONANE,1F20,6/30X,1DECANE,1F20,6/30X,1WATER,1F20,6/30X,1NITROGEN,1F27,6)
160 86./30X,1CARBON DIOXIDE,1F21,6./30X,1HYDROGEN,1F27,6/30X,1HYDROGEN,1F27,6)
161 9SULFIDE,1F19,6/30X,1WATER,1F20,6/30X,1NITROGEN,1F27,6)
162 DD 66 N=1,25
163 COMP(N)=COMP(H)*FMOL
164 66
165 CONTINUE
166 FLUE(1)=COMP(1)+2.*COMP(2)+3.*COMP(3)+4.*(COMP(4)+COMP(5))+5.*(COMP(8)+
167 1P(7))+6.*COMP(8)+7.*COMP(9)+8.*COMP(10)+2.*COMP(11)+3.*COMP(12)+4.*COMP(13)+
168 2*(COMP(14)+COMP(15))+COMP(16)+2.*COMP(17)+3.*COMP(18)+4.*COMP(19)+
169 3*(COMP(20)+COMP(21)+COMP(22)+COMP(23))+COMP(24)+COMP(25)+COMP(26)+COMP(27)+
170 161+COMP(71)+7.*COMP(28)+8.*COMP(29)+9.*COMP(30)+10.*COMP(31)+11.*COMP(32)+
171 212)+4.*COMP(13)+4.*(COMP(15)+COMP(16))+COMP(14)+COMP(17)+2.*COMP(18)+1999
172 38)+3.*COMP(19)+COMP(22)+COMP(23)+COMP(24)
173 FLUE(3)=COMP(23)
174 RECD2=2.*COMP(1)+3.*COMP(2)+5.*COMP(3)+6.*COMP(4)+COMP(5)+3.*COMP(8)+200
175 1COMP(6)+COMP(7)+9.*COMP(8)+11.*COMP(9)+12.*COMP(10)+5.*COMP(13)+2002
176 2)+COMP(14)+COMP(15)+COMP(16)+2.*COMP(17)+4.*COMP(18)+5.*COMP(19)+2003
177 39)+5.*COMP(20)+5.*COMP(22)+11.*COMP(23)
178 FLUE(4)=RECD2*XAIR/100
179 FLUE(5)=79./21.*EQD2*(1.+XAIR/100.)*COMP(25)
180 C NORMALIZE FUEL GAS COMPOSITION AND COMPUTE TOTAL MOLES OF FUEL
181 C GAS PER FOOT OF FURNACE
182 67 FLUE=0.
183 DUMPY(3)=FRATE
184 DD 68 N=1,5
185 FLUE=FLUE+FLUE(N)
186 68
187 DD 69 N=1,5
188 FLUE(N)=FLUE(N)/FLUE
189 69
190 C SPECIFIC HEAT AND ENTHALPY DATA ARE TO BE IN TERMS OF DEG R
191 XHMX=0.
192 DD 71 N=1,5
193 XHMX=XHMX+FLUE(N)*CMW(J)
194 71
195 CONTINUE
196 B050 FLUE(K,8050)FLUE(XMX),(FLUE(J),J=1,5)
197 FORMAT(/20X,1FUEL GAS//25X,1RATE MOLES/HR,1F20,6/30X,1FOOT OF FURNACE,1F20,6/30X,1
198 2FUEL GAS//25X,1MOLECULAR WEIGHT,15X,1F12.2//25X,1FUEL GAS COMPOSITION,1F20,6/30X,1
199 2FUEL GAS//25X,1MOLECULAR WEIGHT,15X,1F12.2//25X,1FUEL GAS COMPOSITION,1F20,6/30X,1
200 DD 72 N=1,5

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```

201 FWT(J)=FLUE(J)*CFW(J)/XMX
202 72 CONTINUE
203 HV(1)=10.
204 HV(2)=0.
205 DO 75 K=1,10
206 HV(K+2)=0.
207 DO 74 J=1,5
208 HV(K+2)=HV(K+2)+A(K,J)*E-T(I)
209 74 CONTINUE
210 75 CONTINUE
211 CP(1)=9.
212 DR=77-K*3,12
213 CP(K-1)=FLIAT(K-2)*HV(K)/1000.
214 77 CONTINUE
215 CALL WRITE(2,1,HV 1,HV(1),12)
216 CALL WRITE(2,1,CP 1,CP(1),11)
217 GO TO R2
218 C BULK FLOW PATTERN
219 80 FLUET=FLUET/DUMY(3)*FRATE
220 DUMY(3)=FRATE
221 82 CALL FLUO(FLUET*XMX,KERR)
222 IF(KERR.NE.0)KADUT=KERR
223 RETURN
224 END
    
```

```

BBB 2028
BBB 2029
BBB 2030
BBB 2031
BBB 2032
BBB 2033
BBB 2034
BBB 2035
BBB 2036
BBB 2037
BBB 2038
BBB 2039
BBB 2040
BBB 2041
BBB 2042
BBB 2043
BBB 2044
BBB 2045
BBB 2046
BBB 2047
BBB 2048
BBB 2049
BBB 2050
BBB 2051
    
```



```

1 SUBROUTINE FLOW (FAC,KAPLT) FLOW2052
2 C FAC= TOTAL FLUE GAS FLOW RATE PER FOOT OF FURNACE -- LB/HR FLOW2053
3 COMMON // DUMHY(3),KK, ICODE, HCODE, FLOW2054
4 A TAU(2), VAREA, HAREA, XLX, XK(3), ACDEF(3,3), FLOW2055
5 A THRIDG, PPES, FLUET, FLUE(5), XHMX, TSIRK, FLOW2056
6 A HCR, HDUTY, HVAL, BRATE, KEUEL, XAIR, FTEMP, FLOW2057
7 A NSSRLK, HCSRLK, NSGRLK, MGGRLK, NSURF, NVOL, FLOW2058
8 A XSUREX(9), XD, YD, ZLNG, NCOL, HROW, NXSXP, FLOW2059
9 A RSTART, TCODE, SCODE, NGRAY, JHCHG, FLOW2060
10 A K1, K2, RORD(10), TDEP(100), BEAH(200) FLOW2061
11 INTEGER SCODE, TCODE, RSTART, HCODE FLOW2062
12 DIMENSION Z(240), RI(120), GMX(120), MY(120) FLOW2063
13 EQUIVALENCE (GMX(1),Z(1)), (GMX(1),Z(121)) FLOW2064
14 KEEP=0 FLOW2065
15 C READ IN THE BULK FLOW PATTERN -- BASIS IS 1.0 LB/HR/FOOT OF FURNACE FLOW2066
16 C X= DIRECTION (NCOL+1)*NROW FLOW2067
17 C Y= DIRECTION (NROW+1)*NCOL FLOW2068
18 CALL ZERO(Z(1),240) FLOW2069
19 NX=(NCOL+1)*NROW FLOW2070
20 READ(K1,35)(GMX(I),I=1,NX) FLOW2071
21 35 FURNAT(7F10.0) FLOW2072
22 NY=(NROW+1)*NCOL FLOW2073
23 READ(K1,35)(GMY(I),I=1,NY) FLOW2074
24 C ADJUSTS FLOW PATTERN BASED ON ACTUAL TOTAL FLUE GAS FLOW RATE FLOW2075
25 C PER FOOT OF FURNACE FLOW2076
26 36 EFAC=ZAC FLOW2077
27 DO 37 N=1,240 FLOW2078
28 Z(N)=Z(N)*EFAC FLOW2079
29 37 CONTINUE FLOW2080
30 CALL WRITE(2,IGMX,GMX(1),NX) FLOW2081
31 CALL WRITE(2,IGMY,GMY(1),NY) FLOW2082
32 WRITE(K2,5U99) FLOW2083
33 8099 FORMAT(11,15X,FLUE GAS FLOW PATTERN,10/HR/FOOT OF FURNACE,1/15X, FLOW2084
34 143(1-1)) FLOW2085
35 WRITE(K2,8110)(GMX(N),N=1,NX) FLOW2086
36 8110 FORMAT(//23X,IX= DIRECTION,1/(25X,6E15.0)) FLOW2087
37 WRITE(K2,8120)(GMY(N),N=1,NY) FLOW2088
38 8120 FORMAT(//23X,IY= DIRECTION,1/(25X,6E15.0)) FLOW2089
39 C CHECK EACH GAS VOLUME FOR FLOW BALANCE (IN = OUT) FLOW2090
40 C MATERIAL BALANCE CHECK ON GAS VOL JBAR=0 NO JCB=0 NO FLOW2091
41 C X = DIRECTION FLOW2092
42 C IN JX1=(JCB-1)*(NCOL+1)+(JC) FLOW2093
43 C OUT JX2= (JR-1)*(NCOL+1)+(JC+1) FLOW2094
44 C Y = DIRECTION FLOW2095
45 C IN JY1=(J) FLOW2096
46 C OUT JY2= (JR-1) FLOW2097
47 38 K=0 FLOW2098
48 CALL ZERO(M(1),150) FLOW2099
49 DO 43 J=1,NVOL FLOW2100
50 JR=0 FLOW2101

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51 JC=J
52 40 JR=JR+1
53 IF(JC.LE.NCOL)GO TO 41
54 JC=JC+NCOL
55 GO TO 40
56 41 JX1=(JR-1)*(NCOL+1)+JG
57 JX2=JX1+1
58 JY1=J
59 JY2=J+HCOL
60 TEST=GMX(JX1)+GMX(JY1)-GMX(JX2)-GMX(JY2)
61 THAX=(ABS(GMX(JX1))+ABS(GMX(JY1))+ABS(GMX(JX2)))/2,OFLOW2112
62 IF(ABS(TEST).LE.0.0001)*THAX)GO TO 43
63 K=K+1
64 H(K)=J
65 43 CONTINUE
66 IF(K.EQ.0)GO TO 46
67 KEPR=1
68 WRITE(K2,44)N(K),JX1,K)
69 C CHECK EACH GAS VOLUME FOR FLOW BALANCE (IN = OUT)
70 44 FORMAT(1,4,5) DO NOT MATERIAL BALANCE/(IX,10I5))
71 C MATERIAL BALANCE CHECK ON GAS VOL JR=ROW NO JC=COL NO
72 C Y = DIRECTION
73 C IN JY1=L L=1,2,3,.....,NCOL TOP
74 C OUT JY2=(NCOL+1)-L=1,2,3,.....,NCOL BOTTOM
75 C X = DIRECTION
76 C IN JX1=L*(NCOL+1)+1 L=0,1,2,3,.....,NROW LEFT
77 C OUT JX2=L*(NCOL+1) L=1,2,3,.....,NROW RIGHT
78 46 TEST=0.0
79 THAX=0.0
80 NN=NCOL+NRW
81 DO 47 L=1,NCOL
82 JY1=L
83 JY2=NRW+L
84 TEST=TEST+GMX(JY1)-GMX(JY2)
85 THAX=THAX+ABS(GMX(JY1))+ABS(GMX(JY2))
86 47 CONTINUE
87 NN=NCOL+1
88 DO 48 L=1,NRW
89 JX1=(L-1)*JH+1
90 JX2=L*JH
91 TEST=TEST+GMX(JX1)-GMX(JX2)
92 THAX=THAX+ABS(GMX(JX1))+ABS(GMX(JX2))
93 48 CONTINUE
94 IF(ABS(TEST).LE.0.0001)*THAX)GO TO 50
95 K=K+1
96 WRITE(K2,49)
97 49 FORMAT(1,FURFACE BOX DOES NOT OVER ALL MATERIAL BALANCE ' )
98 50 IF(KERE.E.CIKAPUT=KERR
99 RETURN
100 END

```

FLOW2102
FLOW2103
FLOW2104
FLOW2105
FLOW2106
FLOW2107
FLOW2108
FLOW2109
FLOW2110
FLOW2111
FLOW2112
FLOW2113
FLOW2114
FLOW2115
FLOW2116
FLOW2117
FLOW2118
FLOW2119
FLOW2120
FLOW2121
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FLOW2143
FLOW2144
FLOW2145
FLOW2146
FLOW2147
FLOW2148
FLOW2149
FLOW2150
FLOW2151

SUBROUTINE CCC

```

1      CCC 2152
2      CCC 2153
3      COMMON // DUMMY(3),KK, ICODE, HCODE,
4      A TAIL(9), VAREA, HAREA, XLX, XK(3), ACDEF(8,3),
5      A TERIDG, PKES, FLUET, FLUE(5), XMAX, TSINK,
6      A HGR, HOUT, HIVAL, FRATE, KEUEL, XAIR, ETEMP,
7      A NSSOLK, NGSOLK, NCGOLK, NGGOLK, NSURF, NVOL,
8      A XSUREX(S), XJ, YB, ZLCHC, NCEL, NADP, NXSXN,
9      A RSTART, TCODE, SCODE, NGRAY, JHCHC,
10     A K1, K2, RCAD(10), TREP(10), PERM(200)
11     C
12     INTEGER SCORE, ICODE, PSTART, HCODE
13     DIMENSION Z(120),Z1( 60),Z2( 60),NM( 60),NM( 60)
14     EQUIVALENCE (Z1(1),Z1(1),Z1(1)),(Z2(1),NM(1),Z1( 61))
15     WRITE(K2,8200)
16     B200 FORMAT(11,15X,TEMPERATURE DATA/15X,16(14,-))
17     C GAS VOLUME AND SURFACE AREA TEMPERATURES
18     GO TO 87
19     IF(TCODE.GT.0) GO TO 81
20     READ(K1,35)(Z1(N),N=1,NVOL)
21     35 FORMAT(7F10.0)
22     READ(K1,35)(Z2(N),N=1,LSURE)
23     GO TO 87
24     81 GO TO (82,85),ICODE
25     82 READ(K1,35)TMIN,TMAX
26     83 DO 84 N=1,NVOL
27     Z1(N)=TMAX
28     84 CONTINUE
29     DO 85 N=1,NSURF
30     Z2(N)=TMIN
31     85 CONTINUE
32     GO TO 87
33     86 CALL AFLAME (TMIN,TMAX)
34     GO TO 83
35     87 WRITE(K2,8210)(Z1(N),N=1,NVOL)
36     8210 FORMAT(/20X,IGAS VOLUME TEMPERATURE,DEG.F,1/(25X,6F15.0))
37     WRITE(K2,8220)(Z2(N),N=1,NSURF)
38     8220 FORMAT(/20X,LSURFACE AREA TEMPERATURES,DEG.F,1/(25X,6F15.0))
39     DO 89 N=1,120
40     IF(Z(N).EQ.0.0)GO TO 89
41     Z(N)=Z(N)+460.
42     89 CONTINUE
43     CALL WRITE(2,ITEMG,Z1(1), 60)
44     CALL WRITE(2,ITEMS,Z2(1), 60)
45     C IF ANY VOLUME AND OR SURFACE TEMP ARE TO BE HELD CONSTANT
46     C THEN READ IN VOLUME AND OR SURFACE NUMBER
47     CALL PZER(2(1),120)
48     IF(SCODE.EQ.0)GO TO 903
49     GO TO(900,903,900),SCODE
50     900 READ(K1,501)(N1,N2,N3,N4,N5,N6,N7,N8,N9,N10,N11,N12,N13,N14,N15,N16,N17,N18,N19,N20)

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51 901  FORMAT(110/(7110))
52  WRITE(K2,8250) (M(N),N=1,NM)
53 8230  FORMAT(/20X,'GAS VOLUME NUMBERS WHICH HAVE KNOWN TEMPERATURES ARCCC 2204
54 1E AS EQUIDIST// (25X,6115))
55 DO 902 N=1,NM
56 K=NM(N)
57 MN(K)=1
58 902  CONTINUE
59 903  CALL WRITE(2,'CONV',MM(1),60)
60 CALL PZERO(MN(1),60)
61 IF(SCODE.EQ.0) GO TO 913
62 GO TO( 913,914,914) SCODE
63 910  READ(K1,901) (M(N),N=1,NM)
64 WRITE(K2,8231) (M(N),N=1,NM)
65 8231  FORMAT(/20X,'SURFACE AREA NUMBERS WHICH HAVE KNOWN TEMPERATURES ARCCC 2216
66 1E AS EQUIDIST// (25X,6115))
67 DO 912 N=1,NM
68 K=MM(N)
69 MN(K)=1
70 912  CONTINUE
71 913  CALL WRITE(2,'CONV',MM(1),60)
72 C READ IN PROCESS TEMPERATURES ASSOCIATED WITH EACH SURFACE
73 CALL PZERO(Z(1),120)
74 READ(K1,8240) (Z(N),N=1,NR,SURF)
75 WRITE(K2,8240) (Z(N),N=1,NR,SURF)
76 8240  FORMAT(/20X,'PROCESS TEMPERATURE ASSOCIATED WITH EACH SURFACE, DEG, CCC 2227
77 1F.1// (25X,6115,0))
78 DO 93 N=1,NR,SURF
79 IF(Z(N).EQ.0) GO TO 93
80 Z(N)=Z(N)+454.
81 93  CONTINUE
82 CALL WRITE(2,'TEMP',Z(1),60)
83 C READ IN AMBIENT TEMPERATURES
84 READ(K1,8250) TSINK
85 WRITE(K2,8250) TSINK
86 8250  FORMAT(/20X,'AMBIENT TEMPERATURE, DEG, F, 1, F22,0)
87 TSINK=TSINK*460.
88 99  RETURN
89 END

```

1	FUNCTION H(TT,JJ)	H	2241
2	COMMON /ED/ A(10,5),B(12,7),C(11,7),CUM(7)	H	2242
3	H=EQUA(TT/100,PR(1,JJ))	H	2243
4	RETURN	H	2244
5	END	H	2245

```

1 SURROUTINE DDD(JUNK,KAPUT) DDD 2246
2 COMMON // DUMMY(3),KK, ICODE, HCODE, DDD 2247
3 A TAU(9), VAREA, HAREA, XLX, XK(3), ACDEF(8,3),
4 A TRADG, PRES, ELUE(5), XJUX, ISINK,
5 A NCR, HOUTY, HTVAL, FRATE, KFUEL, XAIR, FTEMP,
6 A NSBLK, HSBLK, HSGBLK, HGGBLK, NSURE, HVAL,
7 A XSURFX(9), XO, YO, ZLONG, NCOL, HPOW, HXSXN,
8 A RSTARI, ICODE, SCODE, NGRAY, JHCRG,
9 A K1, K2, RCRU(10), TDEP(100), PERM(200)
10 C
11 INTEGER SCODE, ICODE, ISTART, HCODE
12 DIMENSION Z(120), Z1(-60), Z2(-60), N1(-60)
13 DIMENSION ALPHA( 60)
14 EQUIVALENCE (Z1(1),Z11), (Z2(1),Z1(-61))
15 KERR=0
16 IF(JUNK.EQ.0) GO TO 80
17 GO TO(111,90), JUNK
18 80 WRITE(K2,8200)
19 8300 FORMAT(1F1,14X,1SURFACE AREA GAS VOLUME DATA//15X,30(1-1))
20 C READ IN SURFACE DATA
21 CALL PZE'D(Z(1),120)
22 C ELISSIVITY
23 READ(K1,35)(Z1(N),N=1,NSURF)
24 DO 81 J=1,NSURF
25 IF(Z1(J).LT.0001)Z1(J)=.0001
26 IF(Z1(J).GT.9999)Z1(J)=.9999
27 81 CONTINUE
28 CALL ERATE(1,IESUR1,Z11,60)
29 WRITE(K2,8310)(Z1(J),J=1,NSURF)
30 8310 FORMAT(72X,1SURFACE EMISSIVITY DIMENSIONLESS//125X,6F15.4)
31 C TRANSMISSIVITY( OUTSIDE SURFACES HAVE A VALUE OF ZERO
32 IF(NSURF.EQ.NCR)GO TO 82
33 READ(K1,35)(TAU(J),J=1,9)
34 25 EQMATE(10,0)
35 82 CALL NETAU
36 C TEST TO SEE THAT NO SURFACE HAS ZERO OR NEGATIVE REFLECTIVITY
37 C 1,0 EMISSIVITY+TRANSMISSIVITY+REFLECTIVITY
38 CALL WZEROL(1,60)
39 CALL REAR(1,TSUR1,Z2(1),60)
40 WRITE(K2,8220)(Z2(J),J=1,NSURE)
41 8220 FORMAT(72X,1SURFACE TRANSMISSIVITY DIMENSIONLESS//125X,6F15.4)
42 IHNCR=1
43 IF(NSURF.EQ.NCR)GO TO 832
44 DO 831 J=1,NSURE
45 831 ALPHA(J)=1.-Z2(J)
46 832 CONTINUE
47 CALL WRITE(1,ALP,1,ALPHA(1),60)
48 IF(HA.EQ.NCR+1) GO TO 850
49 830 H=0
50 DO 83 J=1,NSURE

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51 IF(1.0-Z1(J))=Z2(J),GT,0.0)GO TO 83
52
53 NI(N)=J
54 83 CONTINUE
55 IF(N.EQ,0)GO TO 850
56 KERR=1
57 WRITE(K2,84)(NI(J),J=1,N)
58 84 FORMAT(1 SURF HAVE ZERO OR NEGIIIVITY REFLECTIVITY/(1015))
59 C AREA
60 850 CALL PZERR(Z1(1), 60)
61 NM=2*HCCL
62 DO 85 N=1,NM
63 Z(N)=XD
64 85 CONTINUE
65 NM=NM+1
66 DO 86 N=1,NM,NCR
67 Z(N)=YD
68 86 CONTINUE
69 IF(NXSX1.EQ,0)GO TO 88
70 YAREA=VUR2
71 NM=NCR+1
72 DO 87 N=1,NM,NSURF
73 Z(N)=YAREA*ALPHA(N)
74 87 CONTINUE
75 88 CALL WRTTE(1,IASUR1,Z(1), 60)
76 WRTTE(K2,830)(Z(J),J=1,NSURF)
77 830 FORMAT(//20X,1SURFACE AREA PER FOOT OF FURNACE SQUARE FEET'/(25X)DD 2322
78 1.6E15,4))
79 C READ IN VOLUME DATA
80 90 CALL PZERR(Z1(1), 60)
81 C LUMINOSITY ( GAS VOLUME CORECTION FACTOR )
82 READ(K1,831)(Z(J),J=1,NSVOL)
83 CALL WRTTE(1,IXLUM1,Z(1), 60)
84 WRTTE(K2,834)(Z(J),J=1,NSVOL)
85 8340 FORMAT(//20X,1GAS VOLUME CORECTION FACTOR DIMENSIONLESS'/(25X,6FDD 2330
86 115,4))
87 C HEAT TRANSFER COEFFICIENTS
88 C HC SURFACE TO GAS
89 C HCP SURFACE TO PROCESS FLUID
90 C HCPP SURFACE TO AMBIENT SINK
91 C NOTE --- CORRECT BOTH HC AND HCP FOR TUBE-T/ -PLAIN AREA
92 WRTTE(K2,840)
93 8400 FORMAT(1H1,14X,1SURFACE HEAT TRANSFER COEFFICIENTS'/(15X,34(1-1))
94 HAREA=0.0
95 VAREA=0.0
96 C READ IN WALL ARRANGEMENT
97 READ(K1,35)H01A,HCLCL,FNR0W
98 IE(HCLCL.EQ,0)GO TO 91
99 HAREA=HNR0W*3.1415927*H01A/HCLCL
100 C READ IN INTERMEDIATE WALL TUBE ARRANGEMENT

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DDO 2296
DDO 2297
DDO 2298
DDO 2299
DDO 2300
DDO 2301
DDO 2302
DDO 2303
DDO 2304
DDO 2305
DDO 2306
DDO 2307
DDO 2308
DDO 2309
DDO 2310
DDO 2311
DDO 2312
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DDO 2332
DDO 2333
DDO 2334
DDO 2335
DDO 2336
DDO 2337
DDO 2338
DDO 2339
DDO 2340
DDO 2341
DDO 2342
DDO 2343
DDO 2344
DDO 2345

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101 91 READ(K1,35)VDIA,VCLCL,VNRDW
102 LE(VCLCL,EA,0,0)CD TO 92
103 VAREA=VRD0*3.1415927*VDIA/VCLCL
104 92 WRITE(K2,8410) HDIA,VDIA,HCLCL,VCLCL,HNRDW,VNRDW,AREA,VAREA
105 8410 FORMAT(/,20X,ITUBE ARRANGEMENT',65X,'WALL',1,6X,'INTERMEDIATE',25X, ODD 2349
DDO 2348
DDO 2349
DDO 2350
106 1 DIAMETER',4CHES L',F28.4,F15.4/25X,ICL-CL DISTANCE',4CHES L',F24.4,DDO 2351
DDO 2352
107 2 F15.4/25X,NUMBER OF ROWS',F31.4,F15.4/25X,ITUBE PLAIN AREA RATIO,DDO 2353
DDO 2354
108 3',F24.4,F13.4)
109 CALL PZERO(Z(1),120)
110 READ(K1,35)(Z1(N),N=1,NSURF)
111 READ(K1,35)(Z2(N),N=1,NSURF)
112 WRITE(K2,8415)
113 8415 FORMAT(/,20X,SURFACE HEAT TRANSFER COEFFICIENTS HAVE THE FOLLOWING,DDO 2358
DDO 2359
114 1 UNITS PER SQUARE FOOT OF PLAIN AREA)
115 C CONVERT WALL HEAT TRANSFER COEFFICIENTS
116 IF(HAREA.EQ.0) GO TO 95
117 DO 94 N=1,NSURF
118 Z1(N)=Z1(N)*HAREA
119 Z2(N)=Z2(N)*HAREA
120 94 CONTINUE
121 C READ IN SURFACE DATA
122 95 IF(NX5X,EG,0)GO TO 99
123 NN=NCR+1
124 DO 99 N=NN,NSURF
125 Z1(N)=Z1(N)*VAREA
126 Z2(N)=Z2(N)*VAREA
127 99 CONTINUE
128 99 CALL WRITE(2,1HC ,Z1(1), 60)
129 CALL WRITE(2,1HCF ,Z2(1), 60)
130 WRITE(K2,8420)(Z1(N),N=1,NSURF)
131 WRITE(K2,8430)(Z2(N),N=1,NSURF)
132 8420 FORMAT(/,20X,CORRECTED COEFFICIENTS SURFACE TO GAS',F15.4)DDO 2376
DDO 2377
133 1)
134 8430 FORMAT(/,20X,CORRECTED COEFFICIENT SURFACE TO PROCESS FLUID',F15.4)DDO 2378
DDO 2379
135 100 1X,F15.4)
136 100 CALL PZERO(Z(1),20)
137 READ(K1,35)(Z(N),N=1,NSURF)
138 CALL WRITE(2,1HCDP,Z1(1), 60)
139 WRITE(K2,8440)(Z(N),N=1,NSURF)
140 8440 FORMAT(/,23X,COEFFICIENT SURFACE TO ABIENT',F15.4)
141 110 IF(KERR.EQ.0)KAPUT=KERR
142 111 RETURN
143 END

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1 SUBROUTINE EEE EEE 2389
2 COMMON // DUMAY(5),KK, ICODE, HCODE, EEE 2390
3 A TAU(9), VAREA, HAREA, XLX, XK(3), ACDEF(8,3), EEE 2391
4 A TBRIDG, PRES, FLUET, FLUE(5), XMAX, ISTAR, EEE 2392
5 A NCR, HNTV, HTVAL, FKATE, KFUEL, XAIR, FTEMP, EEE 2393
6 A WSELK, NCSALK, HSGALK, HGGBLK, MSURE, NVOL, EEE 2394
7 A XSURFX(9), X0, Y0, ZLONG, NCOL, XROW, NXSXN, EEE 2395
8 A RSTART, ICODE, SCODE, NGRAY, JHCHC, EEE 2396
9 A K1, K2, RCRU(10), TDEP(100), PEPH(200) EEE 2397
10 INTEGER SCODE, ICODE, RSTART, HCODE EEE 2398
11 REAL T(10), A(10), TT(10) EEE 2399
12 REAL*4 LOG EEE 2400
13 DATA T/500.,1000.,1500.,2000.,2500.,3000.,3500.,4000.,4500.,5000./ EEE 2401
14 PCO2=FLUE(1)*PRES EEE 2402
15 PH2O=FLUE(2)*PRES EEE 2403
16 PSO2=FLUE(3)*PRES EEE 2404
17 C CHARACTERIZED REAL GAS BY EEE 2405
18 C 1 -- CLEAR GAS EEE 2406
19 C 3 -- GRAY GAS MAXIMUM (PRESENT LOGIC VALID FOR 1 GRAY GAS) EEE 2407
20 C COMPUTE ABSORPTION COEFFICIENT FOR THE SINGLE GRAY GAS EEE 2408
21 E1=EMIS(PCO2,PH2O,PSO2,PRES,TBRIDG,XLX) EEE 2409
22 E2=EMIS(PCO2,PH2O,PSO2,PRES,TBRIDG,XLX) EEE 2410
23 XK(1)=LOG(ABS(E1/(E2-EE1)))/XLX EEE 2411
24 DO 10 J=1,10 EEE 2412
25 E1=EMIS(PCO2,PH2O,PSO2,PRES,T(J),XLX) EEE 2413
26 E2=EMIS(PCO2,PH2O,PSO2,PRES,T(J),2.*XLX) EEE 2414
27 A(J)=E1#2/12.*E1-E2 EEE 2415
28 10 CONTINUE EEE 2416
29 DO 15 J=1,10 EEE 2417
30 TT(J)=T(J)/1000. EEE 2418
31 15 CONTINUE EEE 2419
32 SEAF=IIII(II,AA),6,ACDEF(1,1),2,1,1) EEE 2420
33 TBR=TBRING-460.0 EEE 2421
34 WRITE(K2,BUILDINGRAY,XLX,(J,XK(J),J=1,3),PRES,TBR,(J,A(J),T(J),J=1, EEE 2422
35 110) EEE 2423
36 B600 FORMAT(1H1,1X,1CHARACTERIZATION OF FLUE GAS/15X,28(I=1)///20X,1, EEE 2424
37 1NUMBER OF GRAY GASES',12R/20X,1MEAN REAN LENGTH ,FEET',F26,2//20X, EEE 2425
38 2 1ABSORPTIVITY OF GRAY GAS,RECIPROCAL FEET',3I/153,F15,7)///20X,1FREE EEE 2426
39 3PRESSURE ATM.',F32,4//20X,1BRIDGE WALL TEMPERATURE,DEG F',F17,2//20X EEE 2427
40 4,1DATA 11 CORRELATE ABSORPTIVITY WITH TEMPERATURE,1, EEE 2428
41 59X,1DEG. R.',10/138,F15,7,F15,1)) EEE 2429
42 20 RETURN EEE 2430
43 END EEE 2431

```

1	FUNCTION CP (TT)	CP 2432
2	C	CP 2433
3	C	CP 2434
4	FUNCTION COMPUTES SPECIFIC HEAT OF FLUE GAS COMMON /CPHV/CPCP(11), HPHV(12)	CP 2435
5	C	CP 2436
6	CP = EQVA (TT/1+00.0, CPCP)	CP 2437
7	C	CP 2438
8	RETURN	CP 2439
9	END	CP 2440

```
1 FUNCTION CZZ(TT,JJ) CZZ 2441
2 COMMON /ED/ A(10,5),B(12,7),D(11,7),C(6)(7) CZZ 2442
3 DATA NTIME /0/ CZZ 2443
4 IF(NTIME.NE.0)GO TO 20 CZZ 2444
5 DO 9 J=1,7 CZZ 2445
6 D(1,J)=3. CZZ 2446
7 DO 8 K=3,12 CZZ 2447
8 D(K-1,J)=ELC(1,K=2)*3(K,J)/1000. CZZ 2448
9 8 CONTINUE CZZ 2449
10 9 CONTINUE CZZ 2450
11 NTIME=1 CZZ 2451
12 20 CZZ=EQVA(TT/1000.,D(1,J)) CZZ 2452
13 99 RETURN CZZ 2453
14 END CZZ 2454
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1 SUPROUTINE AFLAME(TMIN,TRAX) AFLA2455
2 C AFLA2456
3 COMMON // DUMMY(3),KK, ICODE, HCODE, AFLA2457
4 A TAU(9), VAREA, HAREA, XLX, XK(3), ACCDF(8,3), AFLA2458
5 A TORIDG, PRES, FLUET, FLUE(5), XNWX, TSINK, AFLA2459
6 A HCR, HOUTV, HIVAL, ERAIE, KEUEL, XAIR, FTEMP, AFLA2460
7 A NSSBLK, NGSBLK, NSGALK, HGGALK, NSURF, NVOL, AFLA2461
8 A XSUREX(9), XG, YG, ZICMG, HCDL, HEDW, NXSXH, AFLA2462
9 A RSTART, ICODE, SCODE, NGRAY, JHCHC, AFLA2463
10 A K1, K2, RCDL(10), TDER(100), PERH(200) AFLA2464
11 C AFLA2465
12 INTEGER SCODE, ICODE, RSTART, HCODE AFLA2466
13 COMMON /ED/ A(10,5),B(12,7),D(11,7),CMW(7) AFLA2467
14 REAL F(7),H(6,6),AV(6),AA(6,7) AFLA2468
15 REAL*4 LG AFLA2469
16 EQUIVALENCE (AA(1,1),AA(1,1)),(AA(1,1)),(AA(1,7)) AFLA2470
17 C CONSTANTS NEEDED FOR DERIVATIVES AFLA2471
18 ZKP1(T)=EXP(A1/T*B1) AFLA2472
19 ZKP1(T)=ZKP1(T)*A1/T**2 AFLA2473
20 C EQUILIBRIUM CONSTANT AND PARTIAL DERIVATIVE FOR CO2,H2O,H2O AND O2 AFLA2474
21 C FOR H2O,H2 AND O2 AFLA2475
22 ZKP2(T)=EXP(A2/T*B2) AFLA2476
23 ZKP2(T)=ZKP2(T)*A2/T**2 AFLA2477
24 DEN1=(2500-1)/5500 AFLA2478
25 A1=(LOG(2.77E5)-LOG(17.8))/DEN AFLA2479
26 B1=LOG(2.77E5)-A1/2500 AFLA2480
27 A2=(LOG(1.26E6)-LOG(2.32))/DEN AFLA2481
28 B2=LOG(1.26E6)-A2/2500 AFLA2482
29 C MOLES OF FLUE GAS AFLA2483
30 C F(1) CO AFLA2484
31 C F(2) H2O AFLA2485
32 C F(3) SO2 = CONSTANT AFLA2486
33 C F(4) H2 AFLA2487
34 C F(5) O2 = CONSTANT AFLA2488
35 C F(6) CO AFLA2489
36 C F(7) H2 AFLA2490
37 DO 13 J=1,5 AFLA2491
38 F(J)=FLUE(J)*ELLUET AFLA2492
39 13 CONTINUE AFLA2493
40 F(6)=0,0 AFLA2494
41 F(7)=0,0 AFLA2495
42 C CONSTANT AFLA2496
43 C 1. TOTAL MASS AFLA2497
44 C 2. CARBON ATOMS AFLA2498
45 C 3. HYDROGEN ATOMS AFLA2499
46 COMWTECO AFLA2500
47 DO 14 J=1,7 AFLA2501
48 COMWT=COMWT+F(J)*CMW(J) AFLA2502
49 14 CONTINUE AFLA2503
50 CARBONE=(1)+F(7) AFLA2504

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51 HYDR0=F(2)+F(7)
52 C=RDUTY#1+.66/ZLDIG
53 C INITIAL GUESSES OF GAS AND TEMPERATURE
54 NTRY=0
55 CO2=0.25*F(1)
56 H2O=0.05*F(2)
57 F(1)=F(1)-C#2
58 F(2)=F(2)-#2#4
59 F(4)=F(4)+.5*(CO2+H2O)
60 F(6)=CO2
61 F(7)=H2O
62 T=5500.
53 C CALCULATE FROM LAST ITERATION TOTAL NUMBER OF MOLES PRESENT
64 20 TOTAL=0.
65 ON 22 J=1,7
66 TOTAL=TOTAL+F(J)
67 22 CONTINUE
68 C CALCULATE MOLES OF H2 AND CO KNOWING H2O+CO2+AND O2
69 C PLUS THE APPROPRIATE EQUILIBRIUM CONSTANTS
70 F(7)=F(2)/(ZKPI(T)*SQRT(F(4)/TOTAL))
71 F(6)=F(1)/(ZKP2(T)*SQRT(F(4)/TOTAL))
72 CALL PZKRO(AA(I,1),#42)
73 C SET UP MATRIX
74 C ROW 1
75 AM(1,1)=C#% (1)
76 AM(1,2)=C#% (2)
77 AM(1,3)=C#% (4)
78 AM(1,4)=C#% (5)
79 AM(1,7)=C#% (7)
80 C ROW 2
81 SQT=SQRT(TOTAL)
82 COM=E(1)/(2.*SQT)
83 AM(2,1)=-SQT-COM
84 AM(2,2)=COM
85 AM(2,3)=F(6)/2.*ZKPI(T)/SQRT(F(4))-COM
86 AM(2,4)=SQRT(F(4))*ZKPI(T)=COM
87 AM(2,5)=-COM
88 AM(2,6)=F(4)*SQRT(F(4))*ZKPI(T)
89 C ROW 3
90 COM=E(2)/(2.*SQT)
91 AM(3,1)=COM
92 AM(3,2)=SQT-COM
93 AM(3,3)=F(7)/2.*ZKP2(T)/SQRT(F(4))-COM
94 AM(3,4)=COM
95 AM(3,5)=SQRT(F(4))*ZKP2(T)=COM
96 AM(3,6)=F(7)*SQRT(F(4))*ZKPI(T)
97 C ROW 4
98 AM(4,1)=E(I,1)+H(I,TEMP,1)
99 AM(4,2)=H(I,2)+H(I,TEMP,2)
100 AM(4,3)=E(I,4)+H(I,TEMP,4)

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101 AM(4,4)=R(T,6)*H(FTEMP,6) AFLA2555
102 AM(4,5)=H(T,7)*H(FTEMP,7) AFLA2556
103 DO 26 J=1,7 AFLA2557
104 AM(4,6)=AM(4,6)+F(J)*CZZ(T,J) AFLA2558
105 26 CONTINUE AFLA2559
106 C ROW 5 AFLA2560
107 AM(5,1)=1. AFLA2561
108 AM(5,4)=1. AFLA2562
109 C ROW 6 AFLA2563
110 AM(6,2)=1. AFLA2564
111 AM(6,4)=1. AFLA2565
112 C SET UP VECTORS AFLA2566
113 AV(1)=CONWT-F(1)*CMW(1)-F(2)*CMW(2)-F(4)*CMW(4)-F(6)*CMW(6)-F(7)*CAFLA2567
114 1,4,7 AFLA2568
115 AV(2)=F(6)*SRT(F(4))*ZKP1(T)+F(1)*SQT AFLA2569
116 AV(3)=F(7)*SBI(F(4))*ZKP2(T)+E(2)*SQT AFLA2570
117 AV(4)=Q AFLA2571
118 DO 29 J=1,7 AFLA2572
119 AV(4)=AV(4)+F(J)*(H(FTEMP,J)-H(T,J)) AFLA2573
120 29 CONTINUE AFLA2574
121 AV(5)=F(1)-F(6)+CARRON AFLA2575
122 AV(6)=E(2)-E(6)+HYDRO AFLA2576
123 C SOLVE LINEARIZED SYSTEM AFLA2577
124 DO 34 J=1,6 AFLA2578
125 SUN=0 AFLA2579
126 DO 32 K=1,6 AFLA2580
127 SUN=SUM+AM(J,K) AFLA2581
128 32 CONTINUE AFLA2582
129 DO 33 K=1,6 AFLA2583
130 AM(J,K)=AM(J,K)/SUM AFLA2584
131 33 CONTINUE AFLA2585
132 AV(J)=AV(J)/SUM AFLA2586
133 34 CONTINUE AFLA2587
134 CALL ISMER(AA,6,7,6) AFLA2588
135 35 DF1=AV(1) AFLA2599
136 DF2=AV(2) AFLA2590
137 DF3=AV(3) AFLA2591
138 DF4=AV(4) AFLA2592
139 DF5=AV(5) AFLA2593
140 DT=AV(6) AFLA2594
141 C TEST FOR CONVERGENCE AFLA2595
142 CON=COL AFLA2596
143 IF(ABS(DF1).LT.CON*F(1).AND.ABS(DF2).LT.CON*F(2).AND. AFLA2597
144 ABS(DF4).LT.CON*E(4).AND.ABS(DF6).LT.CON*E(6).AND. AFLA2598
145 ABS(DF7).LT.CON*F(7).AND.ABS(DT).LT.1.)GO TO 59 AFLA2599
146 C TEST FOR NEGATIVE OR ZERO NOTIES AFLA2600
147 40 IF(F(1)+DF1.GT.0.AND.F(2)+DF2.GT.0.AND.F(4)+DF4.GT.0.AND.F(6)+DF6.GT.0.AND.F(7)+DF7.GT.0.GO TO 59 AFLA2601
148 1+DF6.GT.0.AND.F(7)+DF7.GT.0.GO TO 59 AFLA2602
149 DF1=DF1/2. AFLA2603
150 DF2=DF2/2. AFLA2604

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151 DF4=DF4/2.0 AFLA2605
152 DE6=DE6/2.0 AFLA2606
153 DF7=DF4 AFLA2607
154 GO TO 40 AFLA2608
155 C LIMIT MAXIMUM CORRECTION TO 10 PERCENT OF RATE AFLA2609
156 C AND 100 DEGREES FOR TEMPERATURE AFLA2610
157 50 DF1=SIGN(AMIN1(ABS(DF1),0.1*F(1)),DF1) AFLA2611
158 DE2=SIGN(AMIN1(ABS(DE2),0.1*E(2)),DE2) AFLA2612
159 DF4=SIGN(AMIN1(ABS(DF4),0.1*F(4)),DF4) AFLA2613
160 DE6=SIGN(AMIN1(ABS(DE6),0.1*E(6)),DE6) AFLA2614
161 DF7=SIGN(AMIN1(ABS(DF7),0.1*F(7)),DF7) AFLA2615
162 DI=SIGN(AMIN1(ABS(DI),100.0),DI) AFLA2616
163 NTRY=NTRY+1 AFLA2617
164 F(1)=F(1)+DF1 AFLA2618
165 F(2)=F(2)+DF2 AFLA2619
166 F(4)=F(4)+DF4 AFLA2620
167 F(6)=F(6)+DF6 AFLA2621
168 F(7)=F(7)+DF7 AFLA2622
169 T=T+DT AFLA2623
170 I=I+1 AFLA2624
171 60 TMIN=0.75*T-460. AFLA2625
172 RETURN AFLA2626
173 END AFLA2627
```

```

1 FUNCTION EMIS(PPC02,PH20,PPS02,PPRES,TEMP,XLXX)
2 DIMENSION PC(7),TC(7),PH(5),PS(4),IS(4),EZ(3),TD(3),CCOF(E),HCOF(EMIS2629
3 1B),SCOF(A),DCOF(B),TH(15)
4 REAL L,L6
5 DATA PC/0.01,0.02,0.03,0.04,0.05,0.06,0.063,TC/2350,2400,2950,3950,EMIS2632
6 14300,4500,4875,5000,PH/0.05,0.07,0.10,0.12,0.15,0.20,0.25,0.3EMIS2633
7 20,0.35,0.4,0.50,0.60,0.70,0.8,0.85,TH/1480,1795,2150,2330,25EMIS2634
8 340,2840,2160,2400,3590,3760,4100,4375,4625,4830,5000,EMIS2635
9 4PS/0.02,0.04,0.06,0.075,TS/1450,2400,3050,3500,TD/720,1460,EMIS2636
10 5,2160,LINE/0/
11 IF(NTIME.NE.0)GO TO 10
12 DO 1 J=1,7
13 TC(J)=TC(J)/1000,
14 1 CONTINUE
15 S1=FITIT(TC,PC,7,6,CCOF,2,1,0)
16 DO 2 J=1,15
17 TH(J)=TH(J)/1000,
18 2 CONTINUE
19 S2=FITIT(TH,PH,15,6,HCOF,2,1,0)
20 DO 3 J=1,4
21 TS(J)=TS(J)/1000,
22 3 CONTINUE
23 S3=FITIT(TS,PS,4,3,SCOF,2,1,0)
24 DO 4 J=1,3
25 TD(J)=TD(J)/1000,
26 4 CONTINUE
27 NTIME=1
28 C
29 10 PC02=PPC02
30 PH20=PH20
31 PPS02=PPS02
32 PRES=PPRES
33 TT=TEMP
34 XX=XLXX
35 C C12 EMISSIVITY
36 20 I=MAXL(500,TT)
37 T=AMINI(5000,TT)
38 IF(T.GE.2350)GO TO 21
39 PMIN=0
40 GO TO 22
41 21 PMIN=EXP(EQUALT/1000,CCOF)
42 22 PCL=AMAX1(ECU2*XX,PMIN)
43 PCL=AMINI(PCL,5,0)
44 ASI=LOG,
45 h=PCL
46 CALOG(PCL)
47 D=A*8
48 F=A*8
49 F=A/8
50 G=h/A

```



```

51 IF(T,GT,200,IGD TO 23
52 ECD2=-(.13214613E+01+(.0+1947089A*2+56891554)*A**2-.1112367E11)*AEHIS2679
53 1+(.020854976*8=0,36506376)*8+(.68552178E-4*C**3-.018511476)*C+.26EHIS2680
54 2049826.1*CL+(1,0012690888*U=.028818211)*D+.316569961)*D+(L=.5545739E-EMIS2681
55 35*E=.10411429E-3)*E**3+.052424691)*E+(.27741309E-13)*E**2-.20706962E*EMIS2682
56 4E=6)*E+.49935057E-3)*E+(.22535606E-2)*G+.076587927)*G
57 GO TO 24
58 ECD2=-(.15870691E+11,14026322E=3)*A**2-.67238054E-2)*A-.032322011)*AEHIS2685
59 1**2+(.900049276E-3)*8**2+.26297150)*8+(.37288750E-2)*C**2+.13660492)*EMIS2686
60 2*C+(.00392625E-3)*D=.77139670E=1)*D+(.35397314E-7)*E**2-.49179432E=EMIS2687
61 34)*E**2+.74160975E-1)*E+(.25856087E-16)*F+.73653414E-13)*F**3
62 5-.4560E351E-3)*F+(.22187893E-3)*G**4=.28814881)*G
63 24 ECD2=EXP(ECD2)
64 C CO2_EMISSIONITY_CORRECTION_FACTOR
65 30 PT=AMAX1(C,05,PRES)
66 PE=AMIN1(5,P)
67 PCL=AMAX1(PCU2*XX,02)
68 PCL=AMIN1(PCL,2.5)
69 A=LOG(P)
70 B=A*LOG(PC)
71 CC02=(((.86747709E-3)*A+.45999058E-2)*A-.56062809E-2)*A+.6220262E*EMIS2698
72 1-2)*A+.5412511)*A+(1,36989449E-5)*B+.64106038E-5)*B-.13012359E=3*EMIS2699
73 2)*8-.27531686E-3)*8-.53974179E-1)*8
74 CC02=EXP(CC02)
75 C H2O_EMISSIONITY
76 40 TE=AMAX1(500,TT)
77 T=AMIN1(500,TT)
78 IF(T,GE,1450,IGD TO 41
79 PHIN=,05
80 GO TO 42
81 41 PHIN=EXP(EGUA(T/1000,FCDF))
82 42 PCL=AMAX1(EH20*XX,PMTS)
83 PCL=AMIN1(PCL,20.)
84 A=T/LOGC.
85 B=PWL
86 CALOG(B)
87 D=0*3
88 C=0*0
89 F=0*7
90 G=0*4
91 EH20=-(.92160574+(.36785012E-4)*A**3-0,16945229E-1)*A-.283078E)*A-
92 1.1787129E-3)*B**2+(1,14206699E-3)*C+.1324707E-2)*C+.6148E015E-3)*C*EMIS2719
93 2-.36606564E-1)*C+.31305419)*C+(.46970019E-8)*D**2-.988288E1E-3)*D+
94 3(1.40022711E-5)*E**2-.24520578E-2)*E+.6456909E-1)*E+(1,143852337E-1)*EMIS2721
95 42)*F**2-.14865877E-6)*F+.495933045E-4)*F-.7292208E-2)*F+(.12739632E-
96 58)*G**4=.57217605E-2)*G
97 EH20=EXP(EH20)
98 C H2O_CORRECTION_FACTOR
99 50 PP=AMAX1(PH20+PRES)/2,0,0)
100 PP=AMIN1(PP,1,2)

```

```

EMIS2678
EMIS2679
EMIS2680
EMIS2681
EMIS2682
EMIS2683
EMIS2684
EMIS2685
EMIS2686
EMIS2687
EMIS2688
EMIS2689
EMIS2690
EMIS2691
EMIS2692
EMIS2693
EMIS2694
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EMIS2723
EMIS2724
EMIS2725
EMIS2726
EMIS2727

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101 PVL=AMAX1(PH20*XX,.05)      EMISS2728
102 PVL=AMIN1(PVL,1.0)        EMISS2729
103 A=PP-.5                    EMISS2730
104 B=PP*LOG(PVL)              EMISS2731
105 C=20*(((-.2029815E-1)*A+.25004224)*A-.12401985)*A+.5385303)*A+.1.06EMISS2732
106 1228883)*A+(((-.72108284E-2)*B+.07216391E-2)*B+.3961676E-1)*B+.84532EMISS2733
107 2464E-2)*B+.19942644)*B+1.0 EMISS2734
108 C=C2 AND H20 CORRECTION FACTOR EMISS2735
109 60 EZ(1)=0.0                EMISS2736
110 EZ(2)=0.0                  EMISS2737
111 EZ(3)=0.0                  EMISS2738
112 PP=AMAX1(PH20/(PC2+R202)+0.0) EMISS2739
113 PP=AMIN1(PP,1.0)          EMISS2740
114 PL=AMAX1((PC2+R202)/XX+.2) EMISS2741
115 PL=AMIN1(PL,5.0)          EMISS2742
116 KCODE=6                    EMISS2743
117 IF(TT.LE.720.)KCODE=1     EMISS2744
118 IF(TT.GE.2160.)KCODE=3    EMISS2745
119 IF(TT.EQ.1460.)KCODE=4    EMISS2746
120 IF(KCODE.EQ.0.)KCODE=2    EMISS2747
121 A=PP                        EMISS2748
122 B=LOG(PL)                  EMISS2749
123 C=A*B                        EMISS2750
124 GO TO (61,62,63,64),KCODE EMISS2751
125 61 EZ(1)=.6749563E-2+((-91419565E-1)*A+.60735416E-1)*A**3+.03244848EMISS2752
126 2)*A+(((-.7952405E-3)*A+.32302833E-3)*B+.7928822E-4)*B+.3945270E-2)*EMISS2753
127 3)*A+.011540225)*B+((-38471551E-2)*C+.44283372E-2)*C+.59025659E-2)*EMISS2754
128 4C+.017782741)*C+.3789872E-2)*C EMISS2755
129 EZ(1)=AMAX1(EZ(1),0.0)    EMISS2756
130 GO TO (65,62),KCODE       EMISS2757
131 62 EZ(2)=.51425029E-3+((-30954913E-1)*A**3-.27576063E-1)*A EMISS2758
132 1)*A+(((-.52277457E-1)*A+((-82787757E-2)*A+.84164564E-4)*B+.26212567E-2)*EMISS2759
133 2)*A+.72616575E-3)*B+.63547973E-2)*B+((-69847306E-3)*C+.16586396E-2EMISS2760
134 3)*C+.4152562E-2)*C+.20829105E-2)*C+.13114829E-1)*C EMISS2761
135 EZ(2)=AMAX1(EZ(2),0.0)    EMISS2762
136 IF(KCODE.EQ.4150.)GO TO 67 EMISS2763
137 63 EZ(3)=.3985195E-2+((-25438321E-6)*A**3-.131836E-2)*A+.15184442E-EMISS2764
138 1)*A+(((-.30301264E-3)*B+.13022345E-3)*B+.23495424E-2)*B+.1333573E-EMISS2765
139 22)*B+.18003497E-1)*B+((-64092179E-8)*C+.11118957E-5)*C+.69767036EMISS2766
140 3E-5)*C+.1335407E-3)*C+.12768373E-2)*C EMISS2767
141 EZ(3)=AMAX1(EZ(3),0.0)    EMISS2768
142 IF(KCODE.EQ.2100.)GO TO 65 EMISS2769
143 65 DELE=Z(KODE)           EMISS2770
144 GO TO 70                   EMISS2771
145 66 S4=FIT(TT,EZ,3,2,DCOF,1,1.0) EMISS2772
146 DELE=EQUA(TT/1000.,DCOF) EMISS2773
147 GO TO 70                   EMISS2774
148 67 DELE=Z(2)              EMISS2775
149 C SD2 EMISSIVITY          EMISS2776
150 70 IF(PSU2.EQ.0.0) GO TO 75 EMISS2777

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151 T=ANAX1(TT,700.) EMIS2778
152 T=AMIN1(T,3500.) EMIS2779
153 IF(T.GE.1450.)GO TO 71 EMIS2780
154 PMIN=002 EMIS2781
155 GO TO 72 EMIS2782
156 71 PMIN=EXP(EQUA(T/1000.+SCOE)) EMIS2783
157 72 PSL=ANAX1(PSU2*XX,PMIN) EMIS2784
158 PSL=AMIN1(PSL,2.0) EMIS2785
159 A=T/1000. EMIS2786
160 B=PSL EMIS2787
161 C=LJG(PSL) EMIS2788
162 D=A*B EMIS2789
163 F=A/B EMIS2790
164 G=D/A EMIS2791
165 ES02=2772374E1+(.202776E-2*A**3-.3155203)*A+.10762355E+1)*A+ EMIS2792
166 1/(.20794123*31+5.45024E-2)*B**3+((.9599255E-4*C**3-.17241112)*C-.5 EMIS2793
167 25857489)*C-.23427193)*D+((.32929102E-5*B+.75033122E-4)*E**3+.231592 EMIS2794
168 316)*E+((.45510705E-13*B+.33743806E-10)*F**3+.19602745E-2)*F+ EMIS2795
169 4*((.16829012E-1)*G**2+.5159196)*G+.16932033E1)*G+.20649587E1)*G EMIS2796
170 ES02=EXP(ES02) EMIS2797
171 GO TO RC EMIS2798
172 75 ES02=0.0 EMIS2799
173 80 EMIS=EC02*CC02+EM2D*CH2D-CELE+ES02 EMIS2800
174 RETURN EMIS2801
175 END EMIS2802

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1 SUBROUTINE NETTAU NETT2803
2 C ZTAUZ=0 DO INTERMEDIATE SURFACES EXIST ** NET TAU =1 NETT2804
3 C COMMON // DIM(13),KK, ICODE, HCODE ** COMPUTE NET TAU NETT2805
4 A TAU(9), VAREA, HAREA, XLX, XK(3), ACDEF(8,3), NETT2806
5 A BRIDGE, PRES, FLUET, FLUE(5), XHEX, ISINK, NETT2807
6 A NCR, HDUTY, HTVAL, FPATE, KFUEL, XAIR, FTEMP, NETT2808
7 A NSSLK, WCSBLK, NSGALK, JGGALK, USUPE, RVDL, NETT2809
8 A XSURFX(9), XQ, YQ, ZLONG, NCOL, NKOM, NXSN, NETT2810
9 A RSTART, ICODE, SCODE, NGRAY, JCHIC, NETT2811
10 A K1, K2, RCRD(10), TREP(100), PERM(200) NETT2812
11 C INTEGER SCODE,ICODE,RSTART,HCODE NETT2813
12 C DIMENSION ZSS(8),ZGS(8),ZSG(8),ZGG(8),Z( 60),AA( 60),GJJ NETT2814
13 C INTEGER ZTAUZ NETT2815
14 C NET TRANSMISSIVITY SURFACE TO SURFACE NETT2816
15 C DATA ZSS(1),ZSS2(1),ZSS3(1),ZSS4(1),ZSS5(1),ZSS6(1),ZSS7(1),ZSS8(1) NETT2817
16 C NET TRANSMISSIVITY SURFACE TO GAS NETT2818
17 C DATA ZSG(1),ZSG2(1),ZSG3(1),ZSG4(1),ZSG5(1),ZSG6(1),ZSG7(1),ZSG8(1) NETT2819
18 C NET TRANSMISSIVITY GAS TO SURFACE NETT2820
19 C DATA ZGS(1),ZGS2(1),ZGS3(1),ZGS4(1),ZGS5(1),ZGS6(1),ZGS7(1),ZGS8(1) NETT2821
20 C NET TRANSMISSIVITY GAS TO GAS NETT2822
21 C DATA ZGG(1),ZGG2(1),ZGG3(1),ZGG4(1),ZGG5(1),ZGG6(1),ZGG7(1),ZGG8(1) NETT2823
22 C XTEST=0.01*XQ NETT2824
23 C HALEXU=XU/2. NETT2825
24 C ZTAUZ=0 NETT2826
25 C IF(NXSN.NE.0)ZTAUZ=1 NETT2827
26 C COMPUTE SURFACE TRANSMISSIVITY AND STORE NETT2828
27 C IF(NXSN.NE.0)GO TO 9 NETT2829
28 C CALL PZERO(Z(1),60) NETT2830
29 C DO 5 J=1,NXSN NETT2831
30 M=NCR+(J-1)*NROW NETT2832
31 DO 4 K=1,NROW NETT2833
32 M=NCR+(J-1)*NROW NETT2834
33 Z(J)=TAU(J) NETT2835
34 CONTINUE NETT2836
35 CONTINUE NETT2837
36 CALL WRITE(1,YSUR,Z(1), 60) NETT2838
37 C NET TAU FOR SURFACE TO SURFACE INTERCHANGE AREA NETT2839
38 C IF ZTAUZ.NE.0 GO TO 15 NETT2840
39 C DO 14 K=1,NSURE NETT2841
40 C DO 13 J=1,NSURE NETT2842
41 AA(J,K)=1.0 NETT2843
42 CONTINUE NETT2844
43 GO TO 47 NETT2845
44 C COMPUTE NET TRANSMISSIVITY NETT2846
45 C CALCULATE LOWER LEFT HALF OF MATRIX NETT2847
46 C NET TRANSMISSIVITY SURFACE TO SURFACE INTERCHANGE AREA NETT2848
47 C DO 14 K=1,NSURE NETT2849
48 C DO 13 J=1,NSURE NETT2850
49 C COMPUTE NET TRANSMISSIVITY NETT2851
50 C CALCULATE LOWER LEFT HALF OF MATRIX NETT2852

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51 15 DO 43 K=1,NSURF NETT2853
52 CALL ZONE (O,K,XE,YE) NETT2854
53 DO 42 J=K,NSURF NETT2855
54 IF (J.EQ.K) GO TO 26 NETT2856
55 XE=XE NETT2857
56 IF (K.LE.N) XE=XE+HALFXD NETT2858
57 CALL ZONE (O,J,XR,YR) NETT2859
58 IF (ABS(XE-XR)+ABS(YE-YR).GT.XTEST) GO TO 26 NETT2860
59 XR=XR NETT2861
60 IF (J.LE.N) XR=XR+HALFXD NETT2862
61 C K AND J ARE BOUNDARY SURFACES NETT2863
62 IF (K.LE.NCR.AND.J.LE.NCR) GO TO 25 NETT2864
63 C K IS THE BOUNDARY SURFACE NETT2865
64 C J IS AN INTERMEDIATE SURFACE NETT2866
65 IF (K.GT.NCR) GO TO 18 NETT2867
66 IF (XE=XR) I=I+16 NETT2868
67 16 XE=XR+HALFXD NETT2869
68 GO TO 25 NETT2870
69 17 XR=XR+HALFXD NETT2871
70 GO TO 25 NETT2872
71 C K IS AN INTERMEDIATE SURFACE NETT2873
72 C J IS A BOUNDARY SURFACE NETT2874
73 18 IF (J.GT.NCR) GO TO 21 NETT2875
74 IF (XR=XE) I=I+19 NETT2876
75 19 XE=XE+HALFXD NETT2877
76 GO TO 25 NETT2878
77 20 XE=XE+HALFXD NETT2879
78 GO TO 25 NETT2880
79 C K AND J ARE INTERMEDIATE SURFACES NETT2881
80 21 IF (XR=XE) I=I+22 NETT2882
81 22 XE=XR+HALFXD NETT2883
82 XE=XE+HALFXD NETT2884
83 GO TO 25 NETT2885
84 23 XE=XR+HALFXD NETT2886
85 XE=XE+HALFXD NETT2887
86 25 ISICALC (XE,XR) NETT2888
87 GO TO 40 NETT2889
88 26 I=I
89 40 AA (J,K)=T NETT2891
90 42 CONTINUE NETT2892
91 43 CONTINUE NETT2893
92 C GENERATE JP EK RIGTH OF MATRIX FROM LOWER LEFT NETT2894
93 JJ=NSURF-1 NETT2895
94 DO 46 J=1,JJ NETT2896
95 KJ=J+1 NETT2897
96 DO 45 K=KJ,NSURF NETT2898
97 AA (J,K)=AA (K,J) NETT2899
98 45 CONTINUE NETT2900
99 46 CONTINUE NETT2901
100 C STORE RESULTS IN DISK NETT2902

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101 47 DO 48 J=1,NSGBLK NETT2903
102 CALL WRITE(I,ZGS(J),AA(1,15*(J-14)+900)) NETT2904
103 48 CONTINUE NETT2905
104 C NET TAU FOR SURFACE TO GAS INTERCHANGE AREA NETT2906
105 50 CALL PZERO(AA(1,1),3600) NETT2907
106 IF(ZIAUZ.NE.O)GO TO 55 NETT2908
107 DO 53 K=1,NSURF NETT2909
108 DO 52 J=1,NVUL NETT2910
109 AA(J,K)=1. NETT2911
110 52 CONTINUE NETT2912
111 53 CONTINUE NETT2913
112 GO TO 77 NETT2914
113 C CALCULATES NET TRANSMISSIVITY NETT2915
114 55 DO 76 K=1,NSURF NETT2916
115 CALL ZONE(O,K,XE,YE) NETT2917
116 DO 75 J=1,NVUL NETT2918
117 XE=XE NETT2919
118 IF(K.LE.N)XE=XXE+HALFXO NETT2920
119 CALL ZONE(1,J,XR,YR) NETT2921
120 IF(AA(J,XE-XR)EQ.1)XTST=1 GO TO 63 NETT2922
121 XXR=XR+HALFXO NETT2923
122 IF(K.LE.NGR)GO TO 62 NETT2924
123 IF(XXR-XE)EQ.50,57,57 NETT2925
124 57 XE=XXE+HALFXO NETT2926
125 GO TO 62 NETT2927
126 58 XE=XXE+HALFXO NETT2928
127 62 T=TCALC(XE,XR) NETT2929
128 GO TO 74 NETT2930
129 63 T=1.0 NETT2931
130 74 AA(J,K)=T NETT2932
131 75 CONTINUE NETT2933
132 76 CONTINUE NETT2934
133 C STORE RESULTS NETT2935
134 77 DO 78 J=1,NSGBLK NETT2936
135 CALL WRITE(1,ZGS(J),AA(1,15*(J-14)+900) NETT2937
136 78 CONTINUE NETT2938
137 C NET TAU FOR GAS TO SURFACE INTERCHANGE AREA NETT2939
138 C SINCE G-S IS ALL THAT REMAINS TO BE DONE IS TRANSPOSE MATRIX AA NETT2940
139 60 NL=NO(NSURF,NVUL) NETT2941
140 NN=NL-1 NETT2942
141 DO 82 M=1,NN NETT2943
142 LL=1 NETT2944
143 DO 81 L=1,NNL NETT2945
144 SAVE=AA(L,L) NETT2946
145 AA(NL,L)=AA(L,NL) NETT2947
146 AA(L,LL)=SAVE NETT2948
147 81 CONTINUE NETT2949
148 82 CONTINUE NETT2950
149 NL=NL+1 NETT2951
150 IE(NSURF,NVUL)BB,BA NETT2952

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151 C NVOL,GT,NSURF NETT2953
152 83 ISTART=1 NETT2954
153 LSTART=1 NETT2955
154 GO TO 85 NETT2956
155 C NSURF,GT,NVOL NETT2957
156 84 ISTART=1 NETT2958
157 LSTART=1 NETT2959
158 85 DO 87 N=1,START,NVOL NETT2960
159 DO 86 L=1,START,NSURF NETT2961
160 AA(L,N)=AA(N,L) NETT2962
161 AA(N,L)=0.0 NETT2963
162 86 CONTINUE NETT2964
163 87 CONTINUE NETT2965
164 C STORE RESULTS NETT2966
165 88 DO 89 J=1,NSGBLK NETT2967
166 CALL WRITE(I,ZSG,J),AA(I),15*NJ=14),900) NETT2968
167 89 CONTINUE NETT2969
168 C NET TAU FOR GAS TO GAS INTERCHANGE AREA NETT2970
169 CALL PZERO(AA(1,1),3600) NETT2971
170 IEZTAUZ=0.0 GO TO 92 NETT2972
171 DO 91 K=1,NVOL NETT2973
172 DO 90 J=1,NVOL NETT2974
173 AA(J,K)=1. NETT2975
174 90 CONTINUE NETT2976
175 91 CONTINUE NETT2977
176 GO TO 113 NETT2978
177 C CALCULATE NET TRANSMISSIVITY NETT2979
178 C CALCULATE LOWER LEFT HALF OF MATRIX NETT2980
179 92 DO 109 K=1,NVOL NETT2981
180 CALL ZONE(I,K,XE,YE) NETT2982
181 XE=XE+HALFXD NETT2983
182 DO 108 J=K,NVOL NETT2984
183 IF(J.EQ.K)GO TO 97 NETT2985
184 CALL ZONE(I,J,XR,YR) NETT2986
185 IF(ABS(XE-XR).LT.XTEST)GO TO 97 NETT2987
186 XRE=XR+HALEXD NETT2988
187 T=TCALC(XXE,XXR) NETT2989
188 GO TO 105 NETT2990
189 97 T=1. NETT2991
190 103 AA(J,K)=T NETT2992
191 109 CONTINUE NETT2993
192 109 CONTINUE NETT2994
193 C GENERATE UPPER RIGTH OF MATRIX FROM LOWER LEFT NETT2995
194 JJ=NVOL+1 NETT2996
195 DO 112 J=1,JJ NETT2997
196 K=J+1 NETT2998
197 DO 111 K=K,NVOL NETT2999
198 AA(J,K)=AA(K,J) NETT3000
199 111 CONTINUE NETT3001
200 112 CONTINUE NETT3002

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201 C STOK RESULTS NETT3003
202 113 DO 114 J=1,NUGC9LK NETT3004
203 CALL WRITE(17GG(J),AA(1,15+J-14), 900) NETT3005
204 114 CONTINUE NETT3006
205 RETURN NETT3007
206 END NETT3008


```

1 FUNCTION TCALC(XXE,XXR) TCAL3009
2 COMMON // DUBBY(3),KK, ICODE, HCODE, TCAL3010
3 A TAU(9), VAREA, HAREA, XLX, XK(3), ACOEF(6,3), TCAL3011
4 A BRIDG, DIES, FLUET, FLUE(5), XHWX, TSINK, TCAL3012
5 A NCR, HOUTV, HTVAL, FRATE, KFUEL, XAIR, FTEMP, TCAL3013
6 A NSSBLK, NCSBLK, NSGBLK, MGBLK, NSURE, MVOL, TCAL3014
7 A XSURFX(9), XU, YD, ZLONG, NCOL, NROW, NXSN, TCAL3015
8 A RSTART, ICODE, SCODE, NGRAY, JHC4C, TCAL3016
9 A K1, K2, RCRD(10), TOEP(100), PERM(200) TCAL3017
10 C TCAL3018
11 INTEGER SCODE,TCODE,KSTART,HCODE TCAL3019
12 REAL XD,JM(9) TCAL3020
13 DATA NTIME/D/ TCAL3021
14 IF(NTIME.NE.0)GO TO 10 TCAL3022
15 DO 2 L=1,NXSN TCAL3023
16 LI=NXSXL+L-1 TCAL3024
17 XDOWN(L)=XSURFX(LL) TCAL3025
18 C CONTINUE TCAL3026
19 XTEST=.001*XD TCAL3027
20 NTIME=1 TCAL3028
21 10 XLT=ANLN(XXE,XXR) TCAL3029
22 XRI=MAXI(XXE,XXR) TCAL3030
23 IF(ABS(XXE-XXR),LT,XTEST)GO TO 40 TCAL3031
24 M1=0 TCAL3032
25 M2=0 TCAL3033
26 C COMPUTE M1 TCAL3034
27 DO 12 L=1,NXSN TCAL3035
28 IF(XSUREX(LL),GT,XLI)GO TO 14 TCAL3036
29 12 CONTINUE TCAL3037
30 GO TO 40 TCAL3038
31 14 M1=L TCAL3039
32 DO 22 L=1,NXSN TCAL3040
33 IF(XDOWN(L),LT,XRT)GO TO 24 TCAL3041
34 22 CONTINUE TCAL3042
35 GO TO 40 TCAL3043
36 24 M2=NXSXL+L-1 TCAL3044
37 C COMPUTE TCALC TCAL3045
38 IF(M1,GT,M2)GO TO 40 TCAL3046
39 TCALC=1. TCAL3047
40 DO 32 N=1,M2 TCAL3048
41 TCALC=TCALC*TAU(M) TCAL3049
42 32 CONTINUE TCAL3050
43 GO TO 50 TCAL3051
44 C ALL INTERMEDIATE SURFACES ARE TCAL3052
45 C (1) TO LEFT OF XLT TCAL3053
46 C (2) TO THE RIGHT OF XRT TCAL3054
47 40 TCALC=1. TCAL3055
48 50 RETURN TCAL3056
49 END TCAL3057

```

```

1 C SUBROUTINE ZONE ( KODE, ND, XX, YY )
2 C
3 C KODE SURFACE AREA / GAS VOLUME ( 0=AREA, 1=VOLUME )
4 C NO NUMBER OF SURFACE OR VOLUME
5 C XX/YY COORDINATES REFERENCED TO UPPER LEFT CORNER
6 C
7 C
8 C COMMON // DUMHY(3), KK, ICODE, HCODE,
9 A TAU(9), VAREA, HAREA, XLX, XK(3), ACOEF(8,3),
10 A TRIDG, PRES, FLUE(5), XHWX, TSINK,
11 A NCR, HDUTY, HTVAL, FRATE, KFUEL, XAIR, FTEMP,
12 A NSSBLK, NGSBLK, NSGBLK, NGSBLK, NSURE, NVOL,
13 A XSURFX(9), XO, YO, ZLONG, NCOL, NROW, NXSNXN,
14 A RSTAKI, ICODE, SCODE, NG2AY, JUCHE,
15 A K1, K2, RCRD(10), TNEP(100), PERH(200)
16 C
17 C INTEGER SCODE, TCODE, RSTART, HCODE
18 C
19 C
20 C K = 0
21 L = ND
22 IF ( KODE .NE. 0 ) GO TO 80
23 C
24 C SURFACE AREA
25 IF ( L .GT. NCOL ) GO TO 12
26 C TOP SURFACE
27 X = XD * FLOAT ( L = 1 )
28 Y = 0.0
29 GO TO 99
30 12 L = L - NCOL
31 IF ( L .GT. NCOL ) GO TO 14
32 C BOTTOM SURFACE
33 X = XD * FLOAT ( L = 1 )
34 Y = YD * FLOAT ( -NROW )
35 GO TO 99
36 14 L = L - NCOL
37 IF ( L .GT. NROW ) GO TO 16
38 C LEFT SIDE
39 X = 0.0
40 Y = YD * FLOAT ( L = 1 )
41 GO TO 99
42 16 L = L - NROW
43 IF ( L .GT. NROW ) GO TO 20
44 C RIGHT SIDE
45 X = XD * FLOAT ( NCOL )
46 Y = YD * FLOAT ( L = 1 )
47 GO TO 99
48 20 K = K + 1
49 L = L - NROW
50 IF ( L .GT. NROW ) GO TO 20

```

ZONE3058
 ZONE3059
 ZONE3060
 ZONE3061
 ZONE3062
 ZONE3063
 ZONE3064
 ZONE3065
 ZONE3066
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 ZONE3069
 ZONE3070
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 ZONE3097
 ZONE3098
 ZONE3099
 ZONE3100
 ZONE3101
 ZONE3102
 ZONE3103
 ZONE3104
 ZONE3105
 ZONE3106
 ZONE3107

```

51 C INTERMEDIATE SURFACES
52 X = XSUREX(K)
53 Y = YD * FLOAT ( L = 1 )
54 GO TO 99
55 C GAS VOLUME
56 80 K = K - 1
57 IF ( L .LE. NCOL ) GO TO 81
58 L = L + 1
59 GO TO 60
60 81 X = XD * FLOAT ( L = 1 )
61 Y = YD * FLOAT ( K = 1 )
62 C
63 99 XX = X
64 YY = Y
65 RETURN
66 END
ZONE3108
ZONE3109
ZONE3110
ZONE3111
ZONE3112
ZONE3113
ZONE3114
ZONE3115
ZONE3116
ZONE3117
ZONE3118
ZONE3119
ZONE3120
ZONE3121
ZONE3122
ZONE3123

```

```
1 FUNCTION HV ( TT ) HV 3124
2 C HV 3125
3 C FUNCTION COMPUTES ENTHALPY OF FLUE GAS HV 3126
4 C HV 3127
5 COMMON /CPHV/ CPCP(11), HVHV(12) HV 3128
6 C HV 3129
7 HV = EQUA ( TT/1000.0, HVHV ) HV 3130
8 C HV 3131
9 RETURN HV 3132
10 END HV 3133
```

```

1 SUBROUTINE CL2 CL2 3134
2 C CORE LOAD 2 CL2 3135
3 C CL2 3136
4 C CL2 3137
5 COMMON // DUMHY(3),KK, ICODE, HCODE, CL2 3138
6 A TAU(9),VAREA,HAREA,XLX,XK(3),ACDEF(8,3), CL2 3139
7 A TBRIDG,PRES,FLUET,FLUE(5),XMX,TSINK, CL2 3140
8 A NCR,HDLTY,HVAL,FRATE,KEUEL,XAIR,EYHR, CL2 3141
9 A NSSBLK,NCSBLK,NSGBLK,NGSBLK,NSURF,NVNL, CL2 3142
10 A XSUBEX(9),X0,X0,ZLONG,NCOL,HDRG,MSXN, CL2 3143
11 A RSTART,TCODE,SCODE,NGRAY,JHCHC, CL2 3144
12 A K1,K2,RCRD(10),IDEP(100),PERM(200) CL2 3145
13 C CL2 3146
14 INTEGER SCODE, ICODE, RSTART, HCODE CL2 3147
15 COMMON/JA7Z/ SSHM(8,4),SGNM(8,3),GGNM(8,3), CL2 3148
16 ZSS(8),ZGS(8),ZSG(8),ZGG(8) CL2 3149
17 COMMON/SPCE2/ AA( 60, 60),BB( 60,15),CC( 60,15),ALPHA( 60) CL2 3150
18 COMMON/GAUSS/ WI(9),XY(9),AA6(9,9),APT CL2 3151
19 WRITE(K2,2001) CL2 3152
20 2001 FORMAT(//110,CL2 A1) CL2 3153
21 CALL SSCALC CL2 3154
22 WRITE(K2,2002) CL2 3155
23 2002 FORMAT(110,1CL2 B1) CL2 3156
24 60 CALL GSCALC CL2 3157
25 WRITE(K2,2003) CL2 3158
26 2003 FORMAT(110,1CL2 C1) CL2 3159
27 CALL GGCALC CL2 3160
28 C ***** CL2 3161
29 C TEST OF COMPUTION OF TOTAL INERTCCANCE AREAS CL2 3162
30 C (1) SURFACE AS THE EMITTER CL2 3163
31 C (2) VOLUME AS THE EMITTER CL2 3164
32 WRITE(K2,2004) CL2 3165
33 2004 FORMAT(110,1CL2 D1) CL2 3166
34 61 CALL PZEKD(BA(1,1),1320) CL2 3167
35 62 CALL READ(1,'ASUR',88(1,5), 60) CL2 3168
36 C SURFACE AS THE EMITTER CL2 3169
37 C NSSBLK=NUMBER OF SURFACE TO SURFACE BLOCKS CL2 3170
38 C NCSBLK=NUMBER OF SURFACE TO GAS BLOCKS CL2 3171
39 KMAX=NGRAY+1 CL2 3172
40 DD 82 K=1,KHAX CL2 3173
41 IF(K.EQ.KMAX)GO TO 63 CL2 3174
42 KK#K CL2 3175
43 GO TO 64 CL2 3176
44 63 KK#6 CL2 3177
45 64 DD 65 J=1,NSSBLK CL2 3178
46 CALL READ(1,SSNM(J,KK),AA(1,15),J=14), 900) CL2 3179
47 65 CONTINUE CL2 3180
48 DD 67 L=1,NSURF CL2 3181
49 DD 66 N=1,MSURF CL2 3182
50 BB(L,KK)=BB(L,KK)+AA(N,L) CL2 3183

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51 66 CONTINUE CL2 3184
52 67 CONTINUE CL2 3185
53 IF(K,EO,KHAX)GO TO 90 CL2 3186
54 DO 72 J=1,NGSBLK CL2 3187
55 CALL READ(1,GSNM(J,KK),AA(1,15*(J-14), 900) CL2 3188
56 72 CONTINUE CL2 3189
57 DO 74 L=1,NSURF CL2 3190
58 DO 73 J=1,NVOL CL2 3191
59 B(L,KK)=BB(L,KK)+AA(N,L) CL2 3192
60 73 CONTINUE CL2 3193
61 74 CONTINUE CL2 3194
62 C GAS AS THE EMITTER CL2 3195
63 C NGSBLK=NUMBER OF GAS TO GAS BLOCKS CL2 3196
64 C NSGBLK=NUMBER DE GAS TO SURFACE BLOCKS CL2 3197
65 KO=6+2*(KK-1) CL2 3198
66 DO 76 J=1,NGSBLK CL2 3199
67 CALL READ(1,GSNM(J,KK),AA(1,15*(J-14), 900) CL2 3200
68 76 CONTINUE CL2 3201
69 DO 79 L=1,NVOL CL2 3202
70 DO 78 J=1,NVOL CL2 3203
71 B(L,KO)=BU(L,KO)+AA(N,L) CL2 3204
72 78 CONTINUE CL2 3205
73 79 CONTINUE CL2 3206
74 DO 81 J=1,NSGBLK CL2 3207
75 CALL READ(1,GSNM(J,KK),AA(1,15*(J-14), 900) CL2 3208
76 81 CONTINUE CL2 3209
77 DO 83 L=1,NVOL CL2 3210
78 DO 82 J=1,NSURF CL2 3211
79 B(L,KO)=BR(L,KO)+AA(N,L) CL2 3212
80 82 CONTINUE CL2 3213
81 83 CONTINUE CL2 3214
82 CON=6+XX*(KK)*XQ*YD CL2 3215
83 DO 84 L=1,NVOL CL2 3216
84 B(L,KO+1)=CON CL2 3217
85 84 CONTINUE CL2 3218
86 89 CONTINUE CL2 3219
87 90 WRITE(K2,91) CL2 3220
88 91 FORMAT(11P,EACH CHARACTERISTIC GAS THE SUM OF ALL DIRECT INTERCHCL2 3221
89 RANGE AREAS WITH THE SURFACE AREA AS THE THE EMITTER MUST EQUAL THECL2 3222
90 2-AREAL/10X,IGRAY GAS 1,5X,IGRAY GAS 2,1,5X,IGRAY GAS 3,1,11X,1CL2 3223
91 2EAR GAS1,16X,AREAL) CL2 3224
92 WRITE(K2,92)(1,2B(1,N),M=1,5),1,1,NSURF) CL2 3225
93 92 FORMAT(//15F15.5,2F20.51) CL2 3226
94 WRITE(K2,93) CL2 3227
95 93 FORMAT(11FOR EACH CHARACTERISTIC GAS THE SUM OF ALL DIRECT INTERCHCL2 3228
96 JANE AREAS WITH A GAS VOLUME AS THE EMITTER MUST EQUAL THEI /1 PRODCL2 3229
97 2UCT OF THE GAS ABSORPTION COEFFICIENT AND THE VOLUME MULTIPLIED PYCL2 3230
98 2 A CONSTANT DE 4.01/23X,IGRAY GAS 1,25X,IGRAY GAS 2,1,25X,IGRAY CL2 3231
99 4 GAS 3,1/15X,1 INTER=AREA1,5X,1ABS*VOL1,10X,1INTER=AREA1,6X,1ABS*VOL2 3232
100 0L1,10X,1INTER=AREA1,5X,1ABS*VOL1//) CL2 3233

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```
101 WRITE(K2,94)(I,(BB(I),M),M=6,11),I=1,NVQL) CL2 3234
102 94 FORMAT(/(15,3I3,2E15,5I1)) CL2 3235
103 CALL WRITE(4,'STAR',WT(1),1) CL2 3236
104 RETURN CL2 3237
105 END CL2 3238
```

```

1 FUNCTION SS(XE,YE,XXR,YYR,NNN,MMM)
2 COMMON // DUMH(2),KK, ICODE, HCODE,
3 A TAU(9), VAREA, HAREA, XLX, XK(3), ACOEF(8,3),
4 A TBRIDG, PRES, FLUET, FLUE(5), XMRX, ISINK,
5 A NCR, HDUTY, HTVAL, FRATE, KFUEL, XAIR, FTEMP,
6 A NSSBLK, NGSBLK, NSGBLK, NGGBLK, NSURE, NVOL,
7 A XSURFX(9), XD, YD, ZLONG, NCOL, NROW, NXSXN,
8 A RSTART, ICODE, SCODE, NGRAY, JGHC,
9 A K1, K2, RCRD(10), TDEP(100), PERM(200)
10 C
11 INTEGER SCODE,TCODE,RSTART,HCODE
12 COMMON/GAUSS/ WT(9),XY(9),ARG(9,9),NPT
13 DIMENSION W(9),Z(9)
14 EQUIVALENCE (XY(1),W(1),Z(1))
15 C NP=1 SURFACE IS HORIZONTAL
16 C NM=2 SURFACE IS VERTICAL
17 C RECEIVER ORIENTATION
18 C MP=1 HORIZONTAL
19 C MM=2 SURFACE IS VERTICAL
20 XE=XXE
21 YE=YYE
22 XR=XXR
23 YR=YYR
24 MM=MMH
25 MM=MMH
26 IF(KK.EQ.4)GO TO 23
27 Z=XK(KK)
28 GO TO 30
29 Z=0.0
30 C J=VARIATION ACROSS EMITTING SURFACE
31 C I=VARIATION ACROSS RECEIVING SURFACE
32 30 CALL PZERO(ARG(1),I,J,81)
33 XX=ABS(XR-XE)
34 YY=ABS(YR-YE)
35 GO TO(31,32),NH
36 31 GO TO(51,41),MM
37 32 GO TO(51,71),MH
38 C CASE 1, NM=1, MM=2
39 C EMITTER IS HORIZONTAL Y CONSTANT
40 C RECEIVER IS VERTICAL X CONSTANT
41 41 IF(XR.GT.XE)GO TO 42
42 X1=XX
43 X2=XX+XU
44 GO TO 43
45 42 X1=XX-XD
46 X2=XX
47 43 IF(YR.LT.YE) GO TO 44
48 Y1=YY
49 Y2=YY+YD
50 GO TO 45

```

SS 3239

SS 3240

SS 3241

SS 3242

SS 3243

SS 3244

SS 3245

SS 3246

SS 3247

SS 3248

SS 3249

SS 3250

SS 3251

SS 3252

SS 3253

SS 3254

SS 3255

SS 3256

SS 3257

SS 3258

SS 3259

SS 3260

SS 3261

SS 3262

SS 3263

SS 3264

SS 3265

SS 3266

SS 3267

SS 3268

SS 3269

SS 3270

SS 3271

SS 3272

SS 3273

SS 3274

SS 3275

SS 3276

SS 3277

SS 3278

SS 3279

SS 3280

SS 3281

SS 3282

SS 3283

SS 3284

SS 3285

SS 3286

SS 3287

SS 3288


```

51 44 Y1=YY=YO SS 3289
52 Y2=VY SS 3290
53 45 DD 47 J=1,NPT SS 3291
54 X=(X2*(1.-W(J))+X1*(1.-W(J)))/2. SS 3292
55 DD 46 I=1,NPT SS 3293
56 Y=(Y2*(1.-Z(I))+Y1*(1.-Z(I)))/2. SS 3294
57 U=SQRT(X**2+Y**2) SS 3295
58 ARG=J*PI-E(ZZ*U)/U**3*XY*(X2=X1)/2.*(Y2=V1)/2. SS 3296
59 46 CONTINUE SS 3297
60 47 CONTINUE SS 3298
61 GO TO 85 SS 3299
62 C CASE 2 HM=2 MM=1 SS 3300
63 C EMITTER IS VERTICAL X CONSTANT SS 3301
64 C RECEIVER IS HORIZONTAL Y CONSTANT SS 3302
65 51 IF(XR.LT.XE)GO TO 52 SS 3303
66 X1=XX SS 3304
67 X2=XX+XD SS 3305
68 GO TO 53 SS 3306
69 52 X1=XX+XD SS 3307
70 X2=XX SS 3308
71 53 IF(YR.GT.YE)GO TO 54 SS 3309
72 Y1=YY SS 3310
73 Y2=VY+YD SS 3311
74 GO TO 55 SS 3312
75 54 Y1=VY-YD SS 3313
76 Y2=VY SS 3314
77 55 DD 57 J=1,NPT SS 3315
78 Y=(Y2*(1.-W(J))+Y1*(1.-W(J)))/2. SS 3316
79 DD 56 I=1,NPT SS 3317
80 X=(X2*(1.-Z(I))+X1*(1.-Z(I)))/2. SS 3318
81 U=SQRT(X**2+Y**2) SS 3319
82 ARG=J*PI-E(ZZ*U)/U**3*XY*(Y2=V1)/2.*(X2=X1)/2. SS 3320
83 56 CONTINUE SS 3321
84 57 CONTINUE SS 3322
85 GO TO 85 SS 3323
86 C CASE 3 MM=1 MM=1 SS 3324
87 C EMITTER IS HORIZONTAL Y CONSTANT SS 3325
88 C RECEIVER IS HORIZONTAL Y CONSTANT SS 3326
89 61 IF(YE.EQ.0.0)GO TO 84 SS 3327
90 Y=YY SS 3328
91 X1=AR=0.0 SS 3329
92 X2=AR+XD SS 3330
93 DD 65 J=1,NPT SS 3331
94 X=AR*(X2+AR*(1.-W(J))+X1+AR*(1.-W(J)))/2. SS 3332
95 IF(XR.EQ.XE)GO TO 62 SS 3333
96 X1=XX-XD+XBAR SS 3334
97 X2=X1+XD SS 3335
98 GO TO 63 SS 3336
99 62 X1=-XBAR SS 3337
100 X2=X1+XD SS 3338

```

```

101 63 DD 64 J=1,NPT
102 X=(X2*(1.+Z/(1+X1*(1.-Z/(1+X1))))/2.
103 U=SQRT(X**2+Y**2)
104 64 ARG(I,J)=F(Z*U)/(U**3*Y**2*(X2BAR-X18AR)/2.+(X2-X1)/2.
105 65 CONTINUE
106 65 GO TO 85
107 CASE 4 NH=2 NH=2
108 C EMITTER IS VERTICAL X CONSTANT
109 C RECEIVER IS VERTICAL X CONSTANT
110 C
111 71 IF((X.EQ.0.0)GO TO 84
112 X=XX
113 Y1BAR=0.
114 Y2BAR=Y0
115 DD 75 J=1,NPT
116 YBAR=(Y2BAR*(1.+W(J))+Y1BAR*(1.-W(J)))/2.
117 IF((YR.EQ.YE)GO TO 72
118 Y1=YY-Y0+YBAR
119 Y2=Y1+YD
120 GO TO 72
121 72 Y1=-YBAR
122 Y2=Y1+YD
123 73 DD 74 J=1,NPT
124 Y=(Y2*(1.+Z/(1+Y1*(1.-Z/(1+Y1))))/2.
125 U=SQRT(X**2+Y**2)
126 ARG(I,J)=F(Z*U)/(U**3*Y**2*(Y2BAR-Y1BAR)/2.+(Y2-Y1)/2.
127 74 CONTINUE
128 75 CONTINUE
129 GO TO 85
130 C SURFACES ARE IN THE SAME PLANE BUT NOT ADJACENT
131 84 SS=0.0
132 GO TO 88
133 85 SS=0.
134 DD 87 J=1,NPT
135 FAC=0.0
136 DD 86 J=1,NPT
137 FAC=FAC+WT(I)*ARG(I,J)
138 86 CONTINUE
139 SS=SS+WT(J)*FAC
140 87 CONTINUE
141 SS=SS/3.1415927
142 88 RETURN
143 END

```

SS 3339
SS 3340
SS 3341
SS 3342
SS 3343
SS 3344
SS 3345
SS 3346
SS 3347
SS 3348
SS 3349
SS 3350
SS 3351
SS 3352
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SS 3360
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SS 3364
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SS 3369
SS 3370
SS 3371
SS 3372
SS 3373
SS 3374
SS 3375
SS 3376
SS 3377
SS 3378
SS 3379
SS 3380
SS 3381

```

1 FUNCTION F(W)
2 C W=ABSORBITIVITY*SQRT(X**2+W**2)
3 W=1.5707963
4 IF(W*GT+.0) GO TO 5
5 F=1.5707963
6 GO TO 99
7
8 IF(W*LE.3.9) GO TO 10
9 IF(W*LE.7.9) GO TO 20
10 IF(W*LE.11.9) GO TO 30
11 IF(W*LE.15.9) GO TO 40
12 IF(W*LE.19.9) GO TO 50
13 F=0.0
14 GO TO 99
15 V=EXP(-W)
16 F=(((-.55633800E-1)*V**3+.24694718E+00)*V**2+.52658248)*V+.8587086F
17 IF(W*GT+.0526692E+.1)*V=.2878833E+02
18 GO TO 99
19 V=EXP(-W/2+.0)
20 F=(((.1056065E+07)*V**5+.61555166E+03)*V**2+.11892488E3)*V
21 IF(W*GT+.0526692E+.1)*V=.26287279E0)*V+.1988744E-2)*V-.0E-2
22 GO TO 99
23 V=EXP(-W/3+.1)
24 F=(((.13272233E+05)*V+.66956509E4)*V**2+.47270165)*V+.59591527E-2)*V
25 IF(W*GT+.0526692E+.1)*V=.2878833E+02
26 GO TO 99
27 V=EXP(-W/4+.1)
28 F=(((-.86991805E+9)*V**3+.20670843E+7)*V+.54843329E+6)*V**3
29 IF(W*GT+.0526692E+.1)*V=.26287279E0)*V+.16454718E-2)*V+.5E-6
30 GO TO 99
31 V=EXP(-W/5+.1)
32 F=(((.16617530E+9)*V+.50842624E+8)*V**3
33 IF(W*GT+.0526692E+.1)*V=.26287279E0)*V+.16454718E-2)*V+.5E-6
34 RETURN
END

```

3382 F
 3383 F
 3384 F
 3385 F
 3386 F
 3387 F
 3388 F
 3389 F
 3390 F
 3391 F
 3392 F
 3393 F
 3394 F
 3395 F
 3396 F
 3397 F
 3398 F
 3399 F
 3400 F
 3401 F
 3402 F
 3403 F
 3404 F
 3405 F
 3406 F
 3407 F
 3408 F
 3409 F
 3410 F
 3411 F
 3412 F
 3413 F
 3414 F
 3415 F

```

1. SUBROUTINE SSCALC
2. C COMPUTATION OF SURFACE TO SURFACE DIRECT INTERCHANGE AREA
3. COMMON // DUMMY(3),KK, ICODE, HCNDE,
4. A TAU(9), VAREA, HAREA, XLX, XK(3), ACDEF(8,3),
5. A TRRIDG, PRES, FLUET, FLUF(5), XMX, TSINK,
6. A NGR, HOUTY, HTVAL, FRATE, KFUEL, XAIR, FTEMP,
7. A NSSBLK, NGSBLK, NSGALK, NGGBLK, NSURF, NVOL,
8. A XSUREX(9), XO, YG, ZLONG, HCOL, NROW, HXSXA,
9. A RSTAR, TCODE, SCODE, NGRAY, JHCHC,
10. A K1, K2, RCRD(10), IDEP(10), PERAI(200), NPRINT
11. C
12. C INTEGER SCODE, ICODE, RSTAR, HCODE
13. C
14. C COMMON/JAZZ2/, SSUM(8,4), GSNM(8,3), SGNM(8,3), GGNM(8,3),
15. 1 ZSS(8), ZGS(8), ZSG(8), ZGC(8)
16. COMMON/SCE2/AA( 60, 60), BB( 60,15), CC( 60,15), ALPHA( 60)
17. CALL READ(1, 'ALP 1', ALPHA(1), 60)
18. C KK= GAS NUMBER
19. CALL PZERO(88(1,1), 600)
20. KMAX=NGRAY+1
21. DO 99 K=1, KMAX
22. CALL PZERO(AA(1,1), 3600)
23. IF(K.EQ.KMAX)GO TO 12
24. KK=K
25. ZZ=XK(KK)
26. GO TO 21
27. 12 KK=4
28. ZZ=0.0
29. C GENERATE ONLY LOWER LEFT OF SURFACE TO SURFACE MATRIX
30. C OBTAIN REMAINDER USING SYMMETRY OF MATRIX
31. C N=NUMBER OF EMITTING SURFACES
32. C M=NUMBER OF RECEIVING SURFACES
33. 21 DO 89 N=1, NSURF
34. CALL ZONE(0, N, XE, YE)
35. NN=1
36. IF(N.GT.2)HCOL=NN*2
37. DO 88 M=1, NSURF
38. CALL ZONE(0, M, XM, YM)
39. MM=1
40. IF(M.GT.2)HCOL=MM*2
41. XX=ABS(XE-XE)
42. YY=ABS(YE-YE)
43. GO TO (31,32), NN
44. 31 GO TO (61,65), MM
45. 32 GO TO (85,61), MM
46. 61 IF(XX+YY.EQ.0.0)GO TO 81
47. GO TO 85
48. C A SURFACE CANNOT VIEW ITSELF
49. 81 AA(M,N)=0.0
50. GO TO 88

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SSCA3416
SSCA3417
SSCA3418
SSCA3419
SSCA3420
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SSCA3427
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SSCA3461
SSCA3462
SSCA3463
SSCA3464
SSCA3465

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51 85 AA(M,N)=SS(XE,YE,XR,YR,NN,MM)
52 IF(M.GT.NCR) AA(M,N)=AA(M,N)*ALPHA(M)
53 IF(N.GT.NCR) AA(M,N)=AA(M,N)*ALPHA(N)
54 88 CONTINUE
55 89 CONTINUE UPPER RIGHT OF MATRIX
56 C COMPLETE UPPER RIGHT OF MATRIX
57 C N ROW L COL
58 90 NN=NSURF-1
59 DO 94 N=1,NN
60 L=H+1
61 DO 93 L=1,NSURF
62 AA(M,L)=AA(L,H)
63 93 CONTINUE
64 94 CONTINUE
65 DO 945 J=1,NSSBLK
66 CALL READ(I,ISS(I),CC(I),, 900)
67 JJ=(J-1)*15
68 NLA=ST+15
69 IF(J.EQ.NSSBLK) NLA=NSURF+JJ
70 DO 943 N=1,NLA
71 DO 941 M=1,NSURF
72 NLA=JJ+1
73 AA(N,MM)=AA(M,MM)*CC(N,M)
74 IF(AA(N,MM).LT.0.) CALL ERROR(I,SSCC(I),N,MM)
75 941 CONTINUE
76 943 CONTINUE
77 945 CONTINUE
78 C NORMALIZED CLEAR GAS SURFACE TO SURFACE INTERCHANGE AREA
79 C SO THAT THEY SUM TO THE AREA OF THE EMITTER
80 IF(K.NE.KMAX) GO TO 301
81 95 NN=2*NCUL
82 DO 209 M=1,NSURE
83 IF(N.GT.NN) GO TO 201
84 AREA=XQ
85 GO TO 203
86 201 IF(N.GT.NCR) GO TO 202
87 AREA=YU
88 GO TO 203
89 202 AREA=YD*2.*ALPHA(N)
90 203 ZZ=0.0
91 DO 205 H=1,NSURF
92 ZZ=ZZ+AA(H,N)
93 205 CONTINUE
94 206 ZZ=AREA/ZZ
95 DO 207 H=1,NSURF
96 AA(H,N)=AA(H,N)*ZZ
97 IF(AA(H,N).LT.0.) CALL ERROR(I,SSZZ(I),H,N)
98 207 CONTINUE
99 209 CONTINUE
100 GO TO 96

```

SSCA3466
SSCA3467
SSCA3468
SSCA3469
SSCA3470
SSCA3471
SSCA3472
SSCA3473
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SSCA3477
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SSCA3513
SSCA3514
SSCA3515

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101 C COMPUTE SUM OF SURFACE TO SURFACE INTERCHANGE AREAS
102 C SO THAT THEY CAN BE LATER NORMALIZED TO THE AREA OF THE EMITTER
103 301 DO 303 N=1, NSURF SSCA3516
104 DO 302 M=1, NSURF SSCA3517
105 RB(N, KK)=BB(N, KK)+AA(M, N) SSCA3518
106 302 CONTINUE SSCA3519
107 303 CONTINUE SSCA3520
108 C WRITE DATA OUT ON DISK SSCA3521
109 96 DO 97 J=1, NSSBLK SSCA3524
110 CALL WRITE(I, SSHM(J, KK), AA(I, 15=J-14), 900) SSCA3525
111 97 CONTINUE SSCA3526
112 IF(X.NE.KMAX)GO TO 99
113 IF(NPRINT.EQ.1)GO TO 99 SSCA3527
114 400 WRITE(K2, 401)KK SSCA3528
115 401 FORMAT(I11, 19X, 1SURFACE TO SURFACE DIRECT INTERCHANGE AREAS, 10X, 1SSCA3530
116 1, K= 1, 15) SSCA3531
117 CALL PRINT(AA, NSURF, NSURF)
118 99 CONTINUE SSCA3532
119 101 RETURN SSCA3533
120 END SSCA3534
SSCA3535

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1 SUBROUTINE GSCALC GSCA3536
2 C COMPUTATION OF SURFACE TO VOLUME DIRECT INTERCHANGE AREA GSCA3537
3 COMMON // DUMMY(3),KK, ICODE, HCODE, GSCA3538
4 A TAIL(9), VAREA, HAREA, XLX, XK(2), ACDEF(8,3), GSCA3539
5 A TBRIGG, PRES, FLUET, FLUE(5), XMX, TSINK, GSCA3540
6 A NCR, HOUTY, HTVAL, FRATE, KEUEL, XAIR, FTEMP, GSCA3541
7 A NSSBLK, NGSBLK, NGBLK, NGGELK, NSURF, NVOL, GSCA3542
8 A XSUBEX(9), XQ, YD, ZLONG, NCOL, IRCH, NXSXX, GSCA3543
9 A RSTART, TCODE, SCODE, NGRAY, JHCHC, GSCA3544
10 A K1, K2, RCRD(10), IDEP(10), PERM(200), NPRNT GSCA3545
11 C
12 INTEGER SCODE,ICODE,SLAET,HCODE GSCA3546
13 COMMON/JAZZ2/ SSM(8,4),GSNM(8,3),SGMH(8,3),GGNM(8,3), GSCA3547
14 /ZSS(8),ZGS(8),ZSG(8),ZGL(8) GSCA3548
15 COMMON/SPCE2/ AA( 60, 60),BB( 60,15),CC( 60,15),ALPHA( 60) GSCA3549
16 XDYDEA(10),XD,YD) GSCA3550
17 CALL READ(1,ASUR,1,BB(1,5), 60) GSCA3551
18 C KK=GAS NUMBER GSCA3552
19 10 DO 1900 KK=1,NGRAY GSCA3553
20 CALL PZERD(AA(1,1), 3600) GSCA3554
21 C N=NUMBER OF EMITTING SURFACE GSCA3555
22 C M=NUMBER OF RECEIVING VOLUME GSCA3556
23 DO 1850 N=1,NSURF GSCA3557
24 CALL ZONE(0,1,XE,VE) GSCA3558
25 DO 1840 M=1,NVOL GSCA3559
26 CALL ZONE(1,M,XR,YR) GSCA3560
27 C WRITE(K2,16)N,XE,VE,M,XR,YR GSCA3561
28 C16 FORHAT(//15,2F15.5) GSCA3562
29 XRA=XR GSCA3563
30 YRA=YR GSCA3564
31 XRB=XR+XD GSCA3565
32 YRB=YR GSCA3566
33 XRC=XR GSCA3567
34 YRC=YR+YD GSCA3568
35 XRD=XR GSCA3569
36 YRD=YR GSCA3570
37 C WRITE(K2,25)XRA,TRA,XRB,YRB,XRC,YRC,XRD,YRD GSCA3571
38 C25 FORNAT(//15,2F15.5) GSCA3572
39 IF(N.GT.2)HCU(IGN TO 37 GSCA3573
40 C HORIZONTAL SURFACES GSCA3574
41 NN=1 GSCA3575
42 IF(YE.GT.YR)GO TO 30 GSCA3576
43 IF(XE=XR)GO 200,300 GSCA3577
44 30 IF(XE=XR)GO 100,100,1200 GSCA3578
45 C VERTICAL SURFACES GSCA3579
46 37 NN=2 GSCA3580
47 IF(XE.GT.XR)GO TO 50 GSCA3581
48 IF(YE=YR)GO 400,800 GSCA3582
49 50 IF(YE=YR)GO 500,700,900 GSCA3583
50 C SURFACE AREA TO GAS VOLUME GSCA3584

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51 C ORIENTATION 1
52 100 S1=1
53 S2=1
54 S3=1
55 S4=1
56 GO TO 1500
57 C ORIENTATION 2
58 200 IF (ABS(XE, YE), EQ, 0, 0) GO TO 210
59 S1=1
60 S2=1
61 S3=1
62 S4=1
63 GO TO 1500
64 210 FAC=XD, SS(XE, YE, XRB, YRB, NN, 2), SS(XE, YE, XRC, YRC, NN, 1) = SS(XE, YE, XRD, YRD, NN, 1)
65 1 YRC, NN, 2)
66 GO TO 1700
67 C ORIENTATION 3
68 300 S1=1
69 S2=1
70 S3=1
71 S4=1
72 GO TO 1500
73 C ORIENTATION 4
74 400 S1=1
75 S2=1
76 S3=1
77 S4=1
78 GO TO 1500
79 C ORIENTATION 5
80 500 S1=1
81 S2=1
82 S3=1
83 S4=1
84 GO TO 1500
85 C ORIENTATION 6
86 600 IF (ABS(XB, XE), EQ, 0, 0) GO TO 610
87 S1=1
88 S2=1
89 S3=1
90 S4=1
91 GO TO 1500
92 610 FAC=YD, SS(XE, YE, XRA, YRA, NN, 1) = SS(XE, YE, XRB, YRB, NN, 2)
93 1 = SS(XE, YE, XRC, YRC, NN, 1)
94 GO TO 1700
95 C ORIENTATION 7
96 700 IF (ABS(XR, XE), XD), LT, XD) GO TO 710
97 S1=1
98 S2=1
99 S3=1
100 S4=1

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GSCA3586
GSCA3587
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GSCA3634
GSCA3635

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101 GO TO 1500
102 710 FAC=YO*SS(XE, YE, XRA, YRA, NN, 1) - SS(XE, YE, XRC, YRC, NN, 1)
103 1*SS(XE, YE, XRD, YRD, NN, 2)
104 GO TO 1700
105 C ORIENTATION 8
106 800 S1=1.
107 S2=1.
108 S3=1.
109 S4=1.
110 GO TO 1500
111 C ORIENTATION 9
112 900 S1=1.
113 S2=1.
114 S3=1.
115 S4=1.
116 GO TO 1500
117 C ORIENTATION 10
118 1000 S1=1.
119 S2=1.
120 S3=1.
121 S4=1.
122 GO TO 1500
123 C ORIENTATION 11
124 1100 IEIABS(ABS(YR=YE), YD), I, XDYD GO TO 1110
125 S1=1.
126 S2=1.
127 S3=1.
128 S4=1.
129 GO TO 1500
130 1110 FAC=XD*SS(XE, YE, XRA, YRA, NN, 1) - SS(XE, YE, XRB, YRB, NN, 2)
131 1*SS(XE, YE, XRD, YRD, NN, 2)
132 GO TO 1700
133 C ORIENTATION 12
134 1200 S1=1.
135 S2=1.
136 S3=1.
137 S4=1.
138 1500 FAC=SS(XE, YE, XRA, YRA, NN, 1) - S1 + SS(XE, YE, XRB, YRB, NN, 2) + S2
139 1*SS(XE, YE, XRC, YRC, NN, 1) + S3 + SS(XE, YE, XRD, YRD, NN, 2) + S4
140 1700 AA=NN*JJ*FAC
141 IF(NOT(NCR) AA(M, N) = FAC*ALPHA(N)
142 1840 CONTINUE
143 1850 CONTINUE
144 DO 1851 J=1, NGSBLK
145 CALL READ(1, ZGS(J), CC(1, 1), 900)
146 JJ=(J-1)*15
147 MLAST=15
148 IF(J=EQ, NGSBLK) JHLAST=NVOL=JJ
149 DO 1852 M=1, MLAST
150 DO 1853 I=1, NVOL

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- GSCA3636
- GSCA3637
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- GSCA3640
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- GSCA3645
- GSCA3646
- GSCA3647
- GSCA3648
- GSCA3649
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- GSCA3682
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- GSCA3684
- GSCA3685

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151 MM=JJ+M GSCA3686
152 AA(H,MM)=AA(N,MM)+CC(N,MM) GSCA3687
153 CONTINUE GSCA3688
154 1852 CONTINUE GSCA3689
155 1851 CONTINUE GSCA3690
156 C WRITE SURFACE TO VOLUME INTERCHANGE AREA ON DISK GSCA3691
157 1860 DO 1862 J=1,NGSBLK GSCA3692
158 CALL WRITE(I,GSNH(J,KK),AA(I,15*J-14),900) GSCA3693
159 1862 CONTINUE GSCA3694
160 C COMPUTE SUM OF INTERCHANGE AREA WITH SURFACE AS EMITTER GSCA3695
161 DO 2002 I=1,NSURF GSCA3696
162 DO 2001 J=1,NVCL GSCA3697
163 RB(N,KK)=BR(H,KK)+AA(M,N) GSCA3698
164 2001 CONTINUE GSCA3699
165 2002 CONTINUE GSCA3700
166 C NORMALIZE SURFACE TO SURFACE INTERCHANGE AREA GSCA3701
167 DO 2011 J=1,NSSBLK GSCA3702
168 CALL READ(I,SSNH(J,KK),AA(I,15*J-14),900) GSCA3703
169 2011 CONTINUE GSCA3704
170 DO 2022 I=1,NSURF GSCA3705
171 FAC=BB(N,5)/BB(N,KK) GSCA3706
172 DO 2021 M=1,NSURE GSCA3707
173 AA(M,N)=AA(M,N)*FAC GSCA3708
174 2021 CONTINUE GSCA3709
175 2022 CONTINUE GSCA3710
176 DO 2031 J=1,US5BLK GSCA3711
177 CALL WRITE(I,SSNH(J,KK),AA(I,15*J-14),900) GSCA3712
178 2031 CONTINUE GSCA3713
179 IF(NPRT.EQ.1)GO TO 2040 GSCA3714
180 4000 WRITE(K2,4001)KK GSCA3715
181 4001 FORMAT(1H1,19X,1SURFACE TO SURFACE DIRECT INTERCHANGE AREA,10X,1 GSCA3716
182 1,1,15) GSCA3717
183 CALL PRIT(AA,NSURF,NSURF) GSCA3718
184 C NORMALIZE SURFACE TO VOLUME INTERCHANGE AREAS GSCA3719
185 2040 DO 2041 J=1,NGSBLK GSCA3720
186 CALL READ(I,GSNH(I,KK),AA(I,15*J-14),900) GSCA3721
187 2041 CONTINUE GSCA3722
188 DO 2052 I=1,NSURE GSCA3723
189 FAC=BB(N,5)/BB(N,KK) GSCA3724
190 DO 2051 M=1,NVCL GSCA3725
191 AA(M,N)=AA(M,N)*FAC GSCA3726
192 2051 CONTINUE GSCA3727
193 2052 CONTINUE GSCA3728
194 DO 2061 J=1,NGSBLK GSCA3729
195 CALL WRITE(I,GSNH(J,KK),AA(I,15*J-14),900) GSCA3730
196 2061 CONTINUE GSCA3731
197 IF(NPRT.EQ.1)GO TO 1870 GSCA3732
198 5000 WRITE(K2,5001)KK GSCA3733
199 5001 FORMAT(1H1,19X,1SURFACE TO VOLUME DIRECT INTERCHANGE AREAS,10X,1KGSCA3734
200 1,1,15) GSCA3735

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201 CALL PRINT(AA,NVOL,NSURF)
202 C OBTAIN VOLUME TO SURFACE DIRECT INTERCHANGE AREA
203 C BY TRANSPOSING MATRIX AA(NVOL,NSURF)
204 C N = ROW DESIGNATION
205 C L = COLUMN DESIGNATION
206 C TRANSPOSE SQUARE PART OF MATRIX
207 1870 NL=MINO(NSURF,NVOL)
208 DO 1872 I=2,NL
209 L2=N-1
210 DO 1871 J=1,L2
211 SAVE=AA(I,J)
212 AA(I,J)=AA(L,N)
213 AA(L,N)=SAVE
214 1871 CONTINUE
215 1872 CONTINUE
216 NZ=HL-1
217 IF(NVOL=NSURF)1873,1878,1874
218 C NSURF,GI,NVOL COLUMNS,GI,ROWS
219 1873 NSTART=1
220 LSTART=Z
221 GO TO 1875
222 C NVOL,GI,NSURF, ROWS,GI,COLUMNS
223 1874 NSTART=NZ
224 LSTART=1
225 1875 DO 1877 I=NSTART,NVOL
226 DO 1876 J=LSTART,NSURF
227 AA(L,N)=AA(I,J)
228 AA(N,L)=J
229 1876 CONTINUE
230 1877 CONTINUE
231 C WRITE VOLUME TO SURFACE INTERCHANGE AREAS ON DISK
232 1878 DO 1879 J=LNSGBLK
233 CALL WRITE(I,SGNH(J,KK),AA(I,15*J-14),900)
234 1879 CONTINUE
235 IF(NPRINT,EQ,1)GO TO 1900
236 6000 WRITE(K2,6001)KK
237 6001 FORMAT(1H1,19X,1VOLUME TO SURFACE DIRECT INTERCHANGE AREA1,10X,1K=,K=GSCA3772
238 1,15)
239 CALL PRINT(AA,NSURF,NVOL)
240 1900 CONTINUE
241 RETURN
242 END

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GSCA3736
GSCA3737
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GSCA3777

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1 SUBROUTINE GGALC GGC3778
2 C COMPUTE DE VOLUME TO VOLUME DIRECT INTER CHANGE AREAS GGC3779
3 COMMON // DUMMY(3),KK, ICODE, HCODE, GGC3780
4 A TAU(9), VAREA, HAREA, XLX, XK(3), ACDEF(8,3), GGC3781
5 A TBRIDG, PRES, FLUET, FLUE(5), XMWX, TSINK, GGC3782
6 A MCK, HDUTY, HVAL, FRATE, KEUEL, XAIR, FTEMP, GGC3783
7 A NSSBLK, NGSBLK, NSGRBK, NGBLK, NSURF, NVOL, GGC3784
8 A XSUBEX(3), XO, YO, ZLONG, NCDL, NROW, NXSXN, GGC3785
9 A RSTART, TCJDE, SCODE, NGRAY, JHCHC, GGC3786
10 A K1, K2, RCRUF(10), IDEP(100), PERPH(200),NPRNT GGC3787
11 C GGC3788
12 INTEGER SCODE,ICODE,RSTART,HCODE GGC3789
13 COMMON/JAZZ2/ SSNM(8,4),GSNM(8,3),SGNM(8,3),GGNM(8,3), GGC3790
14 /ZSS(8),ZSS(8),ZSC(8),ZGG(8) GGC3791
15 COMMON/SPEC2/ AA( 60, 60),BB( 60,15),CC( 60,15),ALPHA( 60) GGC3792
16 C KKGAS NUMBER GGC3793
17 DO 1900 KK=1,NGRAY GGC3794
18 CALL PZERU(AA(1,1),3600) GGC3795
19 C GENERATE ONLY LOWER LEFT OF VOLUME TO VOLUME MATRIX GGC3796
20 C OBTAIN THE REST USING THE SYMMETRY FEATURE OF MATRIX GGC3797
21 C N=NUMBER OF EMITTING VOLUMES GGC3798
22 C M=NUMBER OF RECEIVING VOLUMES GGC3799
23 C DO 1850 M=1,NVOL GGC3800
24 CALL ZONE(1,N,XE,YE) GGC3801
25 DO 1840 M=N,NVOL GGC3802
26 CALL ZONE(1,M,XR,YR) GGC3803
27 C WRITE(K2,5)N,XE,YE,M,XR,YR GGC3804
28 C5 FORMAT(/15,2F15.5) GGC3805
29 C COORDINATES OF SURFACES MAKING UP RECEIVING VOLUME GGC3806
30 XRA=XR GGC3807
31 YRA=YR GGC3808
32 XRB=XR+XO GGC3809
33 YRB=YR GGC3810
34 XRC=XR GGC3811
35 YRC=YR+YO GGC3812
36 XRD=XR GGC3813
37 YRD=YR GGC3814
38 C WRITE(K2,8)XRA,YRA,XRB,YRB,XRC,YRC,XRD,YRD GGC3815
39 C8 FORMAT(10X,2F15.5) GGC3816
40 IF(YE=XR)J=20,20 GGC3817
41 10 IF(XE=XR)45,50,55 GGC3818
42 20 IF(XE=XR)180,180,60 GGC3819
43 30 IF(XE=XR)75,70,65 GGC3820
44 C CALCULATION GGC3821
45 C GAS VOLUME TO GAS VOLUME GGC3822
46 45 S1=1 GGC3823
47 S2=1 GGC3824
48 S3=1 GGC3825
49 S4=1 GGC3826
50 GO TO 1740 GGC3827

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51 C GAS VOLUME TO GAS VOLUME          GGCA3828
52 C ORIENTATION 2                      GGCA3829
53 50 S1=1,                             GGCA3830
54 S2=1,                             GGCA3831
55 S3=1,                             GGCA3832
56 S4=1,                             GGCA3833
57 GO TO 1700                          GGCA3834
58 C GAS VOLUME TO GAS VOLUME          GGCA3835
59 C ORIENTATION 3                      GGCA3836
60 55 S1=1,                             GGCA3837
61 S2=1,                             GGCA3838
62 S3=1,                             GGCA3839
63 S4=1,                             GGCA3840
64 GO TO 1700                          GGCA3841
65 C GAS VOLUME TO GAS VOLUME          GGCA3842
66 C ORIENTATION 4                      GGCA3843
67 60 S1=1,                             GGCA3844
68 S2=1,                             GGCA3845
69 S3=1,                             GGCA3846
70 S4=1,                             GGCA3847
71 GO TO 1700                          GGCA3848
72 C GAS VOLUME TO GAS VOLUME          GGCA3849
73 C ORIENTATION 5                      GGCA3850
74 65 S1=1,                             GGCA3851
75 S2=1,                             GGCA3852
76 S3=1,                             GGCA3853
77 S4=1,                             GGCA3854
78 GO TO 1700                          GGCA3855
79 C GAS VOLUME TO GAS VOLUME          GGCA3856
80 C ORIENTATION 6                      GGCA3857
81 70 S1=1,                             GGCA3858
82 S2=1,                             GGCA3859
83 S3=1,                             GGCA3860
84 S4=1,                             GGCA3861
85 GO TO 1700                          GGCA3862
86 C GAS VOLUME TO GAS VOLUME          GGCA3863
87 C ORIENTATION 7                      GGCA3864
88 75 S1=1,                             GGCA3865
89 S2=1,                             GGCA3866
90 S3=1,                             GGCA3867
91 S4=1,                             GGCA3868
92 GO TO 1700                          GGCA3869
93 C GAS VOLUME TO GAS VOLUME          GGCA3870
94 C ORIENTATION 8                      GGCA3871
95 80 S1=1,                             GGCA3872
96 S2=1,                             GGCA3873
97 S3=1,                             GGCA3874
98 S4=1,                             GGCA3875
99 1700 AAT(M,N)=SG(XE,VE,XRA,YRA,1)*S1+SG(XE,VE,XRC,YRC,2)*S2
100 S1=SG(XE,VE,XRC,YRC,1)+S2+SG(XE,VE,XRD,YRD,2)*S4

```

```

101 GO TO 1840
102 C A VOLUME CAN SEE ITSELF, BUT WE WILL COMPUTE ITS VALUE LATER
103 1800 AA(M,N)=0.0
104 1840 CONTINUE
105 1850 CONTINUE
106 C COMPLETE UPPER RIGHT OF MATRIX
107 C N -- RUN L -- COL
108 1860 M=NVOL-1
109 DO 1880 N=1,N1
110 L=M+1
111 DO 1870 L=1,NVOL
112 AA(N,L)=AA(L,N)
113 1870 CONTINUE
114 1880 CONTINUE
115 DO 5881 J=1,NGCBLK
116 CALL READ(1,ZGG(I),CC(I),J, 900)
117 JJ=(J-1)*15
118 MLAST=15
119 IF(J.EQ.MGCBLK)MLAST=NVOL-JJ
120 DO 5882 M=1,MLAST
121 DO 5883 N=1,NVOL
122 MM=JJ+M
123 AA(N,MM)=AA(N,MM)*CC(N,M)
124 5883 CONTINUE
125 5882 CONTINUE
126 5881 CONTINUE
127 C COMPUTE GAS TO GAS INTERCHANGE AREA FOR VOLUME VIEWING ITSELF
128 MM=MAXO(1,SURE,MMVL)
129 CON=4 *X(KK)*XD*YD
130 DO 1885 J=1,MGCBLK
131 CALL READ(1,SGNH(J,KK),BB(1,1), 900)
132 IF(J.EQ.MGCBLK)GO TO 1881
133 NN=15
134 GO TO 1862
135 1881 NN=NVOL-(NSGBLK-1)*15
136 1882 DO 1884 M=1,NN
137 ZZ=0.
138 MM=NN+(J-1)*15
139 DO 1883 N=1,MM
140 ZZ=ZZ+AA(N,MM)*BD(M,M)
141 1883 CONTINUE
142 AA(NM,MM)=CON=ZZ
143 1884 CONTINUE
144 1885 CONTINUE
145 C WRITE VOLUME TO VOLUME INTERCHANGE AREA ON DISK
146 1890 DO 1892 J=1,NGCBLK
147 CALL WRITE(1,CGNH(J,KK),AA(1,15*J-14), 900)
148 1892 CONTINUE
149 IF(NPRINT.EC.1)GO TO 1900
150 5000 WRITE(K2,5001KK)

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GGCA3878
GGCA3879
GGCA3880
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GGCA3925
GGCA3926
GGCA3927

151 5001 FORMAT(1H1,19X,1VOLUME TO VOLUME DIRECT INTERCHANGE AREA,10X,1K=1GGCA3928
152 1,15) GGCA3929

153 CALL PRINT(AA,NVOL,NVOL) GGCA3930

154 1900 CONTINUE GGCA3931

155 RETURN GGCA3932

156 END GGCA3933

```

1 FUNCTION SG(XXE,YVE,XXR,YYR,NM) SG 3934
2 C THIS FUNCTION IS USED TO CALCULATE SURFACE TO VOLUME INTERCHANGE AREA SG 3935
3 C THE EVALUATION IS MADE UP BY CONSIDERING THE RECEIVING (VOLUME) TO BE SG 3936
4 C MADE UP OF FOUR SURFACES SG 3937
5 COMMON // DUMMY(3),KK, ICODE, HCODE, SG 3938
6 A TAU(3), VAREA, HAREA, XLX, XK(3), ACDEF(8,3), SG 3939
7 A TBRIDG, PRES, FLUET, FLVE(5), XMX, TSINK, SG 3940
8 A NCR, HDUFL, HVAL, FRATE, KEUEL, XAIR, FTEMP, SG 3941
9 A NSSBLK, NCSBLK, NSGBLK, NGGBLK, NSURF, NVOL, SG 3942
10 A XSUREX(3), XU, YD, ZLONG, NCOL, PROW, NXSXD, SG 3943
11 A RSTART, TCODE, SCODE, NCRAY, JHCHC, SG 3944
12 C SG 3945
13 A K1, K2, RCRD(10), TDEP(100), PERM(200) SG 3946
14 INTEGER SCODE,ICODE,START,HCODE SG 3947
15 C INTERCHANGE FULL OF SURFACE TO VOLUME AND USE FUNCTION SS SG 3948
16 C TO OBTAIN SURFACE VOLUME INTERCHANGE AREA CONTRIBUTION SG 3949
17 XOVO=AHIN1(XU,YD) SG 3950
18 XE=XXR SG 3951
19 YE=YYR SG 3952
20 XR=XXE SG 3953
21 YR=YVE SG 3954
22 YRA=XR SG 3955
23 YRA=YR SG 3956
24 XRB=XR+XG SG 3957
25 YRB=YR SG 3958
26 XRC=XR SG 3959
27 YRC=YR+YD SG 3960
28 XRD=XR SG 3961
29 YRD=YR SG 3962
30 C SURFACE ORIENTATION SG 3963
31 C NM=1 HORIZONTAL SURFACE SG 3964
32 C NM=2 VERTICAL SURFACE SG 3965
33 GO TO(20,37),NM SG 3966
34 C HORIZONTAL SURFACES SG 3967
35 20 NM=1 SG 3968
36 IF(YE,GT,YR)GO TO 30 SG 3969
37 IF(XE,XR)100,200,300 SG 3970
38 30 IF(XE,XX)1100,1100,1200 SG 3971
39 C VERTICAL SURFACES SG 3972
40 37 NM=2 SG 3973
41 IF(XE,GT,XF)GO TO 50 SG 3974
42 IF(YE,YY)400,600,800 SG 3975
43 50 IF(YE,YH)500,700,900 SG 3976
44 C SG 3977
45 C ORIENTATION 1 SG 3978
46 100 S1=1. SG 3979
47 S2=-1. SG 3980
48 S3=1. SG 3981
49 S4=1. SG 3982
50 GO TO 1500 SG 3983

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A FORTRAN IV (VER L43) SOURCE LISTING: SG          FUNCTION          03/05/74          PAGE 0097
51 C ORIENTATION 2
52 200 IF (ABS(XR-YE),EQ,0,0)GO TO 210
53 S1=1
54 S2=1
55 S3=1
56 S4=1
57 GO TO 1500
58 210 FAC=YO-SS(XE,YE,XRB,YN,2)-SS(XE,YE,XRC,YN,1)-SS(XE,YE,XRD,2)
59 1YRC,NN,2)
60 GO TO 1700
61 C ORIENTATION 3
62 300 S1=1
63 S2=1
64 S3=1
65 S4=1
66 GO TO 1500
67 C ORIENTATION 4
68 400 S1=1
69 S2=1
70 S3=1
71 S4=1
72 GO TO 1500
73 C ORIENTATION 5
74 500 S1=1
75 S2=1
76 S3=1
77 S4=1
78 GO TO 1500
79 C ORIENTATION 6
80 600 IF (ABS(XR-XE),EQ,0,0)GO TO 610
81 S1=1
82 S2=1
83 S3=1
84 S4=1
85 GO TO 1500
86 610 FAC=YO-SS(XE,YE,XRA,YN,1)-SS(XE,YE,XRB,NN,2)
87 1-SS(XE,YE,XRC,YN,1)
88 GO TO 1700
89 C ORIENTATION 7
90 700 IF (ABS(ALS(XN-XE),XO),1,1,XOYD)GO TO 710
91 S1=1
92 S2=1
93 S3=1
94 S4=1
95 GO TO 1500
96 710 FAC=YO-SS(XE,YE,XRA,YN,1)-SS(XE,YE,XRC,YN,1)
97 1-SS(XE,YE,XRD,NN,2)
98 GO TO 1700
99 C ORIENTATION 8
100 800 S1=1

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SG 3984
SG 3985
SG 3986
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SG 3998
SG 3999
SG 4000
SG 4001
SG 4002
SG 4003
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SG 4031
SG 4032
SG 4033

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101 S2=1, SG 4034
102 S3=1, SG 4035
103 S4=1, SG 4036
104 GO TO 1500 SG 4037
105 C ORIENTATION 9 SG 4038
106 900 S1=1, SG 4039
107 S2=1, SG 4040
108 S3=1, SG 4041
109 S4=1, SG 4042
110 GO TO 1500 SG 4043
111 C ORIENTATION 10 SG 4044
112 1000 S1=1, SG 4045
113 S2=1, SG 4046
114 S3=1, SG 4047
115 S4=1, SG 4048
116 GO TO 1500 SG 4049
117 C ORIENTATION 11 SG 4050
118 1100 IF(ABS(ABS(YR, YE) - YD) .LT. X.DVD) GO TO 1110 SG 4051
119 S1=1, SG 4052
120 S2=1, SG 4053
121 S3=1, SG 4054
122 S4=1, SG 4055
123 GO TO 1500 SG 4056
124 1110 FAC=XD-SS(XE, YE, XRA, YRA, NN, 1) - SS(XE, YE, XRB, YRB, NN, 2) SG 4057
125 1-SS(XE, YE, XRD, YRD, NN, 2) SG 4058
126 GO TO 1700 SG 4059
127 C ORIENTATION 12 SG 4060
128 1200 S1=1, SG 4061
129 S2=1, SG 4062
130 S3=1, SG 4063
131 S4=1, SG 4064
132 1500 FAC=SS(XE, YE, XRA, YRA, NN, 1) + SS(XE, YE, XRB, YRB, NN, 2) * S2 SG 4065
133 1+SS(XE, YE, XRC, YRC, NN, 1) * S3 + SS(XE, YE, XRD, YRD, NN, 2) * S4 SG 4066
134 1700 SG=FAC SG 4067
135 RETURN SG 4068
136 END SG 4069

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1  SUBROUTINE CL3
2  COMMON // DUMM(3),KK, ICODE, HCODE,
3  A TAU(9), VAREA, HAREA, XLX, XK(3), ACOEF(8,3),
4  A TRIDG, PRES, FLUET, FLUE(3), XHWX, TSINK,
5  A NCR, HDUTY, HTVAL, FRATE, KFUEL, XAIR, FTEMP,
6  A NSSBLK, NSGALK, NSGALK, HGSBLK, NSURF, NVOL,
7  A XSURFX(9), XQ, YD, ZLONG, NCOL, NROW, NXSXN,
8  A RSTART, ICODE, SCODE, NGRAY, JCHC,
9  A K1, K2, RGRU(10), TDEP(100), PERM(200)
10 C
11  INTEGER SCODE, TCJDE, RSTART, HCODE
12  COMMON /JAZZ/SSNM(8,4), GSNM(8,3), SGNM(8,3), SR$NM(8,4),
13  ISRGNM(8,3), TSSNM(8,4), TGSNM(8,3), TSGNM(8,3), TGGNM(8,3)
14  COMMON /ALUCK/ ESURE( 60), TSURE( 60), ASURE( 60), AEP( 60)
15  COMMON /SPCE/ AA( 60, 60), BB( 60,15), CC( 60,15)
16  CALL READ(1, ESURE(1), 60)
17  CALL READ(1, ASURE(1), 60)
18  CALL READ(1, TSURE(1), 60)
19  CALL RRRR
20  CALL IIII
21 C  TEST OF COMPUTATION OF TOTAL INTERCHANGE AREA
22 C  (1) SURFACE AS EMITTER
23 C  (2) VOLUME AS EMITTER
24 61  CALL PZER(1, BB(1,1), 660)
25  DO 62 L=1, NSURF
26  BB(L,5)=ESURE(L)*ASURE(L)
27 62  CONTINUE
28 C  SURFACE AS EMITTER
29 C  NSSBLK=NUMBER OF SURFACE TO SURFACE BLOCKS
30 C  NGSBLK=NUMBER OF SURFACE TO GAS BLOCKS
31  KMAX=NGRAY+1
32  DO 69 K=1, KMAX
33  IF (K.EQ.KMAX) GO TO 63
34  KK=K
35  GO TO 64
36 63  KK=4
37 64  DO 65 J=1, NSSBLK
38  CALL READ(1, ISSNM(J, KK), AA(1,15*J-14), 900)
39 65  CONTINUE
40  DO 67 L=1, NSURF
41  DO 66 N=1, NSURF
42
43  BB(L, KK)=BB(L, KK)+AA(N, L)
44 66  CONTINUE
45 67  CONTINUE
46  IF (K.EQ.KMAX) GO TO 90
47  DO 72 J=1, NGSBLK
48  CALL READ(1, IGSNM(J, KK), AA(1,15*J-14), 900)
49 72  CONTINUE
50  DO 74 L=1, NSURF

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CL3 4070

CL3 4071

CL3 4072

CL3 4073

CL3 4074

CL3 4075

CL3 4076

CL3 4077

CL3 4078

CL3 4079

CL3 4080

CL3 4081

CL3 4082

CL3 4083

CL3 4084

CL3 4085

CL3 4086

CL3 4087

CL3 4088

CL3 4089

CL3 4090

CL3 4091

CL3 4092

CL3 4093

CL3 4094

CL3 4095

CL3 4096

CL3 4097

CL3 4098

CL3 4099

CL3 4100

CL3 4101

CL3 4102

CL3 4103

CL3 4104

CL3 4105

CL3 4106

CL3 4107

CL3 4108

CL3 4109

CL3 4110

CL3 4111

CL3 4112

CL3 4113

CL3 4114

CL3 4115

CL3 4116

CL3 4117

CL3 4118

CL3 4119

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51 DO 73 N=1,NVUL
52 BB(L,KK)=BRILL(KK)*AA(N,L)
53 73 CONTINUE
54 74 CONTINUE
55 C GAS AS EMITTER
56 C NSGBLK=NUMBER OF GAS TO GAS BLOCKS
57 C NSGBLK=NUMBER OF GAS TO SURFACE BLOCKS
58 K=6+2*(KK-1)
59 DO 76 J=1,NSGBLK
60 CALL READ(I,ICGNH(I),KK),AA(I,15*(J-1)+14), 900)
61 76 CONTINUE
62 DO 79 L=1,NVUL
63 DO 78 N=1,NVUL
64 BB(L,KOL+BB(L,KO)+1)=AAA(N,L)
65 78 CONTINUE
66 79 CONTINUE
67 DO 81 J=1,NSGBLK
68 CALL READ(I,ISGNH(I),KK),AA(I,15*(J-1)+14), 900)
69 81 CONTINUE
70 DO 86 L=1,NVUL
71 DO 85 N=1,NSURF
72 BB(L,KO)=BF(L,KO)+AA(N,L)
73 85 CONTINUE
74 86 CONTINUE
75 CON=4,*XY(KK)*XD*YD
76 DO 87 L=1,NVUL
77 RB(L,KO+1)=CON
78 87 CONTINUE
79 89 CONTINUE
80 90 WRITE(K2,91)
81 91 FORMAT(11FOR EACH CHARACTERIST GAS THE SUN OF ALL TOTAL INTERCHANGCL3 4150
82 1E AREA WITH THE GAS VOLUME AS THE EMITTER MUST EQUAL THE 11 PRODUCCCL3 4151
83 2 OF THE EMISSIVITY AND THE AREA1/10X,1GRAY GAS 1,5Y,1GRAY GAS 2,CL3 4152
84 3,5X,1GRAY GAS 3,1,1X,1CLEAR GAS,8X,1EMISS*AREA1//)
85 WRITE(K2,92)(I,(IB(I,M),M=1,5),I=1,NSURF)
86 92 FORMAT(15,3F15.5,2E20.5)
87 WRITE(K2,93)
88 93 FORMAT(11E6R EACH CHARACTERIST GAS THE SUM OF THE TOTAL INTERCHANGCL3 4157
89 1E AREAS WITH A GAS VOLUME AS THE EMITTER MUST EQUAL THE 11 PRODUCTCL3 4158
90 2 OF THE GAS ABSORPTION COEFFICIENT AND THE VOLUME MULTIPLIED BY A CL3 4159
91 1 CONSTANT OF 4,1/23X,1GRAY GAS 1,25X,1GRAY GAS 2,1,25X,1GRAY GASCL3 4160
92 23,1,15X,1LITER=AREA1*6X,1ABS * VOL1,10X,1LITER=AREA1*6X,1ABS * VOLCL3 4161
93 3,1,10X,1LITER=AREA1*6X,1ABS * VOL1//)
94 WRITE(K2,94)(I,(IB(I,M),M=1,5),I=1,NSURF)
95 94 FORMAT(/(15,3(5X2F15.5)))
96 RETURN
97 END

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CL3 4120
CL3 4121
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CL3 4166

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1  SUBROUTINE AKRR
2  COMPUTES SURFACE REFLECTIVITIES AND STORE ON DISK 1
3  C (1) = SURFACE AREA AS EMITTER
4  C (2) = GAS VOLUME AS EMITTER
5  COMMON / / DUMMY(3),KK, ICODE, HCODE,
6  A TAU(9),VAREA,HAREA,XY,XK(3),ACDEF(8,3),
7  A TBRIDG,PRES,FLUET,FLUE(5),XMX,TSINK,
8  A NCR,HOUYA,HIVALE,ERATE,KEUEL,XAIR,EYEMP,
9  A NSSBLK,NGSBLK,HSGRIK,NGGBLK,NSURF,NVOL,
10 A XSUREX(9),XU,YO,ZLONG,NCDL,HROW,NXSXN,
11 A RSTART,TCODE,SCODE,NGRAY,JHCHC,
12 A K1,K2,RCR(10),IDEP(10),PERM(20)
13 C
14 INTEGER SCODE,ICODE,RSIART,HCODE
15 COMMON/JAZZ3/SSNH(8,4),GSHM(8,3),SGNH(8,3),GGNH(8,3),SRSNM(8,4),
16 ,SBCNM(8,3),TSSNH(8,4),IGSHM(8,3),TSGNH(8,3),IGGNM(8,3)
17 COMMON/BLOCK/ESURF(60),TSURF(60),ASURF(60),AEP(60)
18 COMMON/SPEC3/AA(60),BB(60),CC(60),D(60),E(60),F(60),G(60),H(60),I(60),J(60),K(60),L(60),M(60),N(60),O(60),P(60),Q(60),R(60),S(60),T(60),U(60),V(60),W(60),X(60),Y(60),Z(60),AA(60),BB(60),CC(60),DD(60),EE(60),FF(60),GG(60),HH(60),II(60),JJ(60),KK(60),LL(60),MM(60),NN(60),OO(60),PP(60),QQ(60),RR(60),SS(60),TT(60),UU(60),VV(60),WW(60),XX(60),YY(60),ZZ(60)
19 DIMENSION RHO(60),FACTR(60)
20 C GENERATE REQUIRED SURFACE PARAMETERS
21 C REFLECTIVITY RHO
22 C AREA / REFLECTIVITY FACTR
23 C AREA * EMISSIVITY/REFLECTIVITY AEP
24 DO 10 J=1,MSURE
25 RHO(JJ)=1,ESURF(JJ)
26 FACTR(JJ)=ASURF(JJ)/RHO(JJ)
27 AEP(JJ)=FACTR(JJ)*ESURF(JJ)
28 10 CONTINUE
29 C KK=GAS NUMBER
30 12 KMAX=1+IGRAY
31 DO 80 K=1,KMAX
32 CALL PZERO(AA(1,1),3600)
33 IF(K.EO.KMAX)GO TO 16
34 KKK
35 GO TO 18
36 16 KKK4
37 C SET UP MATRIX AND INVERT FOR EACH CHARACTERISTIC GAS
38 C MATRIX EQUALS S-S DIRECT INTERCHANGE AREA WITH
39 C DIAGONAL TERMS ADJUSTED FOR AREA/REFLECTIVITY TERM
40 C NSSBLK = NUMBER OF SURFACE TO SURFACE BLOCKS
41 18 DO 20 J=1,NSSBLK
42 CALL READ(1,SSHM(J,KK),AA(1,15),J=14),900)
43 20 CONTINUE
44 DO 21 J=1,MSURE
45 AA(J,J)=AA(J,J)+FACTR(JJ)
46 21 CONTINUE
47 C OBTAIN INVERSE OF OUTGOING FLUX DENSITY FOR EACH
48 C CHARACTERISTIC GAS -- SAVE SINCE IT CAN BE USED
49 C FOR BOTH EMITTERS( SURFACE AREA AND GAS VOLUME )
50 23 KODE=0

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RRRR4167
RRRR4168
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RRRR4170
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RRRR4208
RRRR4209
RRRR4210
RRRR4211
RRRR4212
RRRR4213
RRRR4214
RRRR4215
RRRR4216

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51 CALL INVERT(NSURF, 60, AA, CC, KODE)
52 26 IE(KODE, 1), GO TO 31
53 WRITE(K2, 29)
54 29 FORMAT(1, 'TROUBLE IN INVERT', 1)
55 STOP
56 C REFLECTIVITIES WITH SURFACE AS EMITTER
57 C OBTAINED BY MATRIX - VECTOR MULTIPLICATION
58 C MATRIX PREVIOUSLY OBTAINED INVERSE
59 C VECTOR NEGATIVE OF S-S DIRECT INTERCHANGE
60 C AREA * EMISSIVITY OF EMITTER
61 C NSSBLK = NUMBER OF SURFACE BLOCKS
62 31 DO 49 J=1, NSSBLK
63 CALL READ(1, SSNM(J, KK), BB(1, 1), 900)
64 JJ=J*(J+1)
65 IF(J.EQ.NSSBLK) GO TO 33
66 JJMAX=J
67 GO TO 34
68 32 JJMAX=NSURF-(NSSBLK-1)*15
69 34 DO 38 JJ=1, JJMAX
70 DO 36 JJ=1, NSURF
71 J2=J1+JJ
72 BB(N, JJ)=BB(N, JJ)*ESURE(J2)
73 36 CONTINUE
74 38 CONTINUE
75 CALL PZERO(CC(1, 1), 900)
76 DO 46 JJ=1, JJMAX
77 DO 44 N=1, NSURF
78 DO 42 L=1, NSURF
79 CC(N, JJ)=CC(N, JJ)+AA(N, L)*BB(L, JJ)
80 42 CONTINUE
81 44 CONTINUE
82 46 CONTINUE
83 CALL WRITE(1, SRSUM(J, KK), CC(1, 1), 900)
84 49 CONTINUE
85 C TEST TO SEE IF WE HAVE FINISHED THE CLEAR GAS
86 C THAN COMPUTATION IS FINISHED
87 IF(K.EQ.KMAX) GO TO 90
88 C REFLECTIVITY AS GAS AS EMITTER (GAS TO SURFACE)
89 C OBTAINED BY MATRIX VECTOR MULTIPLICATION
90 C MATRIX PREVIOUSLY OBTAINED INVERSE
91 C VECTOR NEGATIVE OF G-S DIRECT INTERCHANGE AREA
92 C NSGBLK = NUMBER OF GAS TO SURFACE BLOCKS
93 DO 69 J=1, NSGBLK
94 CALL READ(1, SSNM(J, KK), BB(1, 1), 900)
95 IF(J.EQ.NSGBLK) GO TO 52
96 JJMAX=J
97 GO TO 54
98 52 JJMAX=JUL=(NSGBLK-1)*15
99 54 CALL PZERO(CC(1, 1), 900)
100 DO 66 JJ=1, JJMAX

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RRRR4217
RRRR4218
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RRRR4220
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RRRR4264
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RRRR4266

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101	DD 64 N1,ISURF	RRRR4267
102	DD 62 L1,LSURB	RRRR4268
103	CC(N,JJ)=CC(N,JJ)-AA(N,L)#BB(L,JJ)	RRRR4269
104 62	CONTINUE	RRRR4270
105 64	CONTINUE	RRRR4271
106 66	CONTINUE	RRRR4272
107	CALL WRITE(1,SRGNH(J,KK),CC(L1), 900)	RRRR4273
108 69	CONTINUE	RRRR4274
109 60	CONTINUE	RRFR4275
110 90	RETURN	RRRR4276
111	END	RRRR4277

```

1  SUBROUTINE INVERT (NEG,MAX,A,E,KERR)
2  REAL A(MAX,1),E(1)
3  KERR=0
4  NN=NEG
5  10 DO 16 I=1,NN
6  DO 17 J=1,I
7  IF(Q.NE.0.0)GO TO 12
8  KK=10
9  GO TO 30
10 12 DO 13 J=1,NN
11  A(I,J)=A(I,J)/Q
12 13 CONTINUE
13  A(I,I)=1./Q
14  IF(I.EQ.NN)GO TO 20
15  L=I+1
16  DO 15 K=L,NN
17  RA(K,I)
18  IF(R.EQ.0)GO TO 15
19  DO 14 J=L,NN
20  A(K,J)=A(K,J)-RA(K,I)*A(I,J)
21 14 CONTINUE
22  A(K,I)=R/Q
23 15 CONTINUE
24 16 CONTINUE
25 20 DO 24 L=2,NN
26  L=L+1
27  K=L+1
28  DO 21 J=K,NN
29  E(J)=A(I,J)
30  A(I,J)=0.0
31 21 CONTINUE
32  DO 23 J=L,NN
33  DO 22 M=K,NN
34  A(I,J)=A(I,J)+E(M)*A(M,J)
35 22 CONTINUE
36 23 CONTINUE
37 24 CONTINUE
38 30 RETURN
39  END
INVE4278
INVE4279
INVE4280
INVE4281
INVE4282
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INVE4314
INVE4315
INVE4316

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51 DO 22 J=1,NSGBLK
52 CALL REALT(SRGUM(J,KK),AA(L,J),L4,900)
53 22 CONTINUE
54 DO 25 I=1,NVOL
55 DO 24 L=1,NSURF
56 AA(L,N)=AA(L,N)+AEP(L)
57 24 CONTINUE
58 25 CONTINUE
59 DO 27 J=1,NSGBLK
60 CALL WRITE(LTSGUM(J,KK),AA(L,J),L4,900)
61 27 CONTINUE
62 C SURFACE TO GAS TOTAL INTERCHANGE AREA
63 C SINCE G-S=5=C ALL THAT NEEDS TO BE DONE IS
64 C TRANSPOSE SURFACE TO GAS MATRIX
65 C NSGBLK=NUMBER OF SURFACE TO GAS BLOCKS
66 30 N=NSURF*NSURF
67 DO 32 I=2,N
68 L2=N-I
69 DO 31 L=1,L2
70 SAVE(AA(L,I))
71 AA(I,L)=AA(L,I)
72 AA(L,I)=SAVE
73 31 CONTINUE
74 32 CONTINUE
75 IZ=NL+1
76 IE(NSURF=NVOL),33,38,34
77 C NVOL,GT,NSURF
78 33 NSTART=I
79 LSTART=I
80 GO TO 35
81 C NSURF,GT,NVOL
82 34 NSTART=I
83 LSTART=I
84 35 DO 37 N=1,NSURF
85 DO 36 L=1,NSURF
86 AA(L,N)=AA(L,I)
87 AA(N,L)=0
88 36 CONTINUE
89 37 CONTINUE
90 38 DO 372 I=1,NSURF
91 DO 371 L=1,NVOL
92 FIXS(H,KK)=FIXS(H,KK)+AA(L,N)
93 371 CONTINUE
94 372 CONTINUE
95 DO 39 J=1,NSGBLK
96 CALL WRITE(LTSGUM(J,KK),AA(L,J),L4,900)
97 39 CONTINUE
98 C GAS TO GAS TOTAL INTERCHANGE AREA
99 C THIS INTERCHANGE AREA HAS TO COMBINATIONS
100 C (1) G-G VIA REFLECTION FROM SURFACES

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101 C      (2) G-G VIA DIRECT INTERCHANGE
102 C      COMPUTE (1) FIRST BY MATRIX MULTIPLICATION
103 C      MATRIX SURFACE TO GAS REFLECTIVITY
104 C      VECTOR SURFACE TO GAS DIRECT INTERCHANGE AREA
105 C      ADD (2) TO (1) TO GET TOTAL INTERCHANGE AREA
106 C      NGGBLK = NUMBER OF GAS TO GAS BLOCKS
107 C      NGSBLK = NUMBER OF SURFACE TO GAS BLOCKS
108 41     CALL PZERO(AA(1,1), 3600)
109         DO 42 J=1,NGSBLK
110         CALL READ(1,GSUM(J,KK),AA(1,15+J,1), 900)
111         CONTINUE
112         DO 49 J=1,NSGBLK
113         CALL PZERO(CC(1,1), 900)
114         CALL READ(1,SRGM(J,KK),BB(1,1), 900)
115         IF(J.EQ.NSGBLK)GO TO 43
116         NMAX=15
117         GO TO 44
118 43     NMAX=NVOL-(NSGBLK-1)*15
119 44     DO 47 N=1,NMAX
120         DO 46 L=1,NVOL
121         DO 45 M=1,SURF
122         CC(L,N)=CC(L,H)+RB(H,N)*AA(L,M)
123 45     CONTINUE
124 46     CONTINUE
125 47     CONTINUE
126         CALL WRITE(1,TGGM(H,J,KK),CC(1,1), 900)
127 49     CONTINUE
128         DO 59 J=1,NGGBLK
129         CALL PZERO(AA(1,1), 900)
130         CALL READ(1,GGNM(J,KK),BB(1,1), 900)
131         CALL READ(1,TGGNM(J,KK),CC(1,1), 900)
132         IF(L.EQ.NGGBLK)GO TO 51
133         NMAX=15
134         GO TO 52
135 51     NMAX=NVOL-(NGGBLK-1)*15
136 52     DO 56 N=1,NMAX
137         DO 55 L=1,NVOL
138         AA(L,N)=B(L,H)+CC(L,N)
139 55     CONTINUE
140 56     CONTINUE
141         CALL WRITE(1,TGGM(J,KK),AA(1,1),900)
142 59     CONTINUE
143 60     CONTINUE
144 C      NORMALIZE INTERCHANGE AREAS
145 63     DO 96 K=1,KMAX
146         IF(K.EQ.KMAX)GO TO 65
147         KK=K
148         GO TO 66
149 65     KK=4
150 66     DO 67 N=1,NSURE

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151     FIXS(N,KK)=ESURF(N)*ASURF(N)/FIXS(N,KK)
152 67     CONTINUE
153     CALL PZERO(AA(1,1), 3600)
154     DO 68 J=1,NSSBLK
155     CALL READ(1,TSSNH(J,KK),AA(1,15*J-14), 900)
156 68     CONTINUE
157     DO 72 N=1,NSURF
158     DO 71 L=1,NSURE
159     AA(L,N)=AA(L,N)*FIXS(N,KK)
160 71     CONTINUE
161 72     CONTINUE
162     DO 73 J=1,NSSBLK
163     CALL WRITE(1,TSSNH(J,KK),AA(1,15*J-14), 900)
164 73     CONTINUE
165     IF(NPRINT.EQ.1)GO TO 74
166 4000  WRITE(2,4001)KK
167 4001  FORMAT(11,19X,1SURFACE TO SURFACE TOTAL INTERCHANGE AREA,10X,1K
168        ,1,15)
169     CALL PRINT(AA,NSURF,NSURE)
170     CALL PRINT(FIXS(1,KK),NSURE,1)
171 74     IF(K.EQ.KMAX)GO TO 99
172     CALL PZERO(AA(1,1), 3600)
173     DO 76 J=1,NGSBLK
174     CALL READ(1,IGSNH(J,KK),AA(1,15*J-14), 900)
175 76     CONTINUE
176     DO 78 H=1,NSURE
177     DO 77 L=1,NVOL
178     AA(L,H)=AA(L,H)*FIXS(N,KK)
179 77     CONTINUE
180 78     CONTINUE
181     DO 79 J=1,NGSBLK
182     CALL WRITE(1,IGSNH(J,KK),AA(1,15*J-14), 900)
183 79     CONTINUE
184     IF(NPRINT.EQ.1)GO TO 80
185 4010  WRITE(2,4011)KK
186 4011  FORMAT(11,19X,1SURFACE TO VOLUME TOTAL INTERCHANGE AREA,10X,1K
187        ,1,15)
188     CALL PRINT(AA,NVOL,NSURE)
189 80     NL=HTNO(NSURF,NVOL)
190     DO 82 N=1,NL
191     LZ=N-1
192     DO 81 L=1,LZ
193     SAVE=AA(L,L)
194     AA(N+1,AA(L,H))
195     AA(L,N)=SAVE
196 81     CONTINUE
197 82     CONTINUE
198     NZ=NL+1
199     IF(NVOL=NSURF)83,870,84
200 C     NSURE.GI.NVOL

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201 83 NSTART=1
202 LSTART=NZ
203 GO TO 85
204 C NVOL,GI,NSURF
205 84 NSTART=NZ
206 LSTART=1
207 85 DO 87 N=1,NVOL
208 DO 86 L=1,LSTART,NSURF
209 AA(L,N)=AA(N,L)
210 AA(N,L)=0
211 86 CONTINUE
212 87 CONTINUE
213 87 DO 89 N=1,NVOL
214 Z(L)=0
215 DO 80 L=1,NSURF
216 Z(L)=Z(N)+AA(L,N)
217 88 CONTINUE
218 89 CONTINUE
219 DO 90 J=1,NSGBLK
220 CALL WRITE(L,IGSUM(J,KK),AA(1,15*NJ=14), 900)
221 90 CONTINUE
222 IF(INPRT.EQ.1)GO TO 900
223 4020 WRITE(K2,4021)KK
224 4021 FORMAT(14L,19X,1VOLUME TO SURFACE TOTAL INTERCHANGE AREA,10X,1K,1
1,15)
225 CALL PRINT(AA,NSURF,NVOL)
226 CALL PRINT(Z,NVOL,1)
227 900 CONTINUE
228 900 CONE4,0*XD*YJ*KK(KK)
229 CALL PZERO(AA(1,1), 3600)
230 DO 91 J=1,NSGBLK
231 CALL READ(1,IGSUM(J,KK),AA(1,15*NJ=14), 900)
232 91 CONTINUE
233 DO 94 N=1,NVOL
234 Z(N)=0
235 DO 92 L=1,NVOL
236 Z(N)=Z(N)+AA(L,N)
237 92 CONTINUE
238 Z(N)=CON-Z(N)/ZZ
239 DO 93 L=1,NVOL
240 AA(L,N)=AA(L,N)*ZZ
241 93 CONTINUE
242 94 CONTINUE
243 DO 95 J=1,NSGBLK
244 CALL WRITE(L,IGSUM(J,KK),AA(1,15*NJ=14), 900)
245 95 CONTINUE
246 IF(INPRT.EQ.1)GO TO 96
247 4030 WRITE(K2,4031)KK
248 4031 FORMAT(14L,19X,1VOLUME TO VOLUME TOTAL INTERCHANGE AREA,10X,1K,1,
115)
249 CALL PRINT(AA, NVOL,NVOL)
250

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A FORTRAN IV (VER L43) SOURCE LISTING: TTTT SUBROUTINE 03/09/74 PAGE 0110
251 96 CONTINUE TTTT4567
252 99 RETURN TTTT4568
253 END TTTT4569

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1  FUNCTION LOC(KIK) LOC 4570
2  C  L LOC CODE FOR GAS VOLUME ORIENTATION LOC 4571
3  C  K KK GAS VOLUME NUMBER LOC 4572
4  COMMON // DUMMY(3),KK, ICODE, HCODE, LOC 4573
5  A TAU(9), VAREA, HAREA, XLX, XK(3), ACDEF(8,3), LOC 4574
6  A TRIDG, PRES, FLUET, FLUE(5), XHXY, TSIHK, LOC 4575
7  A HCR, HDUTY, HTVAL, FRATE, KFUEL, XAIR, FTEMP, LOC 4576
8  A WSSOLK, NCSOLK, USGOLK, HGGOLK, HSURE, DVOL, LOC 4577
9  A XSURFX(9), XO, YO, ZLNG, NCOL, NROW, NXSXN, LOC 4578
10 A RSTART, ICODE, SCODE, NGEAY, JHCHC, LOC 4579
11 A K1, K2, KCRU(10), TDEP(100), PERM(200) LOC 4580
12 C
13 INTEGER SCODE,TCODE,RSTART,HCODE LOC 4581
14 COMMON/GAS/ NX1,NX2,NY1,NY2,HT,HTI,XIEST,ALFA(3),BETA(3),GAMA(3), LOC 4582
15 DELT(3),GMX(120),GMY(120),HC( 60),JX1,JX2,JY1,JY2 LOC 4584
16 COMMON/HT/ IV(120,2),IS(120,2) LOC 4585
17 10 K=KIK LOC 4586
18 CALL PZERO(ALFA(1),3) LOC 4587
19 CALL PZERO(BETA(1),3) LOC 4588
20 CALL PZERO(GAMA(1),3) LOC 4589
21 CALL PZERO(DELT(1),3) LOC 4590
22 C FOR GAS VOLUME OBTAIN LOC 4591
23 C JR FOR NUMBER LOC 4592
24 C JG COLUMN NUMBER LOC 4593
25 JR=0 LOC 4594
26 JC=K LOC 4595
27 12 JR=JR+1 LOC 4596
28 IF(JC.LE.NCOL)GO TO 14 LOC 4597
29 JC=JC+NCPL LOC 4598
30 GO TO 12 LOC 4599
31 C BULK FLOW INDICIES LOC 4600
32 C JX1 X DIRECTION IN LOC 4601
33 C JX2 OUT LOC 4602
34 C JY1 Y DIRECTION IN LOC 4603
35 C JY2 OUT LOC 4604
36 14 JX1=(JR-1)*(NCOL+1)+JC LOC 4605
37 JX2=JX1+1 LOC 4606
38 JY1=K LOC 4607
39 JY2=K+NCU1 LOC 4608
40 C COMPLETE VALUE OF L AND NX1,NX2,NY1,NY2 LOC 4609
41 16 IF(JR.NE.1)GO TO 21 LOC 4610
42 IF(JC.NE.1)GO TO 17 LOC 4611
43 C SURF VOL SURF VOL LOC 4612
44 L=L1 LOC 4613
45 NX1=2*NCU1+1 LOC 4614
46 NX2=K+1 LOC 4615
47 NY1=L1 LOC 4616
48 NY2=K+NCU1 LOC 4617
49 GO TO 61 LOC 4618
50 17 IF(JC.EQ.NCOL)GO TO 19 LOC 4619

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51 C IP(NXSXN,NE,0)GO TO 31

LOC 4620

52 C VOL VOL SURF VOL

LOC 4621

53 18 L=2

LOC 4622

54 NX1=K+1

LOC 4623

55 NX2=K+1

LOC 4624

56 NX1=K

LOC 4625

57 NY2=K+NCOL

LOC 4626

58 GO TO 81

LOC 4627

59 19 L=3

LOC 4628

60 C VOL SURF SURF VOL

LOC 4629

61 NX1=K+1

LOC 4630

62 NX2=2*NCOL+NRQW+1

LOC 4631

63 NV1=K

LOC 4632

64 NY2=K+NCOL

LOC 4633

65 GO TO 101

LOC 4634

66 21 IF(JR,NE,MR)GO TO 25

LOC 4635

67 IF(JC,NE,1)GO TO 22

LOC 4636

68 L=7

LOC 4637

69 C SURR VOL VOL SURF

LOC 4638

70 NX1=2*NCOL+ARROW

LOC 4639

71 NX2=K+1

LOC 4640

72 NY1=K+NCOL

LOC 4641

73 NY2=NCOL+1

LOC 4642

74 GO TO 181

LOC 4643

75 22 IF(JC,EQ,NCOL)GO TO 24

LOC 4644

76 IF(NXSXN,NE,0)GO TO 31

LOC 4645

77 23 L=8

LOC 4646

78 C VOL VOL VOL SURF

LOC 4647

79 NX1=K+1

LOC 4648

80 NX2=K+1

LOC 4649

81 NY1=K+NCOL

LOC 4650

82 NY2=NCOL+JC

LOC 4651

83 GO TO 201

LOC 4652

84 24 L=9

LOC 4653

85 C VOL SURF VOL SURF

LOC 4654

86 NX1=K+1

LOC 4655

87 NX2=NCR

LOC 4656

88 NY1=K+NCOL

LOC 4657

89 NY2=2*NCOL

LOC 4658

90 GO TO 221

LOC 4659

91 25 IF(JC,NE,1)GO TO 26

LOC 4660

92 L=4

LOC 4661

93 C SURF VOL VOL VOL

LOC 4662

94 NX1=2*NCOL+JR

LOC 4663

95 NX2=K+1

LOC 4664

96 NY1=K+NCOL

LOC 4665

97 NY2=K+NCOL

LOC 4666

98 GO TO 121

LOC 4667

99 26 IF(JC,NE,NCOL)GO TO 27

LOC 4668

100 L=6

LOC 4669

101 C	VOL SURF	VOL	VOL	LOC 4670
102	NY1=K+1			LOC 4671
103	NY2=2*NCOL+NRROW+JR			LOC 4672
104	NY1=K+NCUL			LOC 4673
105	NY2=K+NCUL			LOC 4674
106	GO TO 161			LOC 4675
107 27	IF(NXSXN.NE.0)GO TO 31			LOC 4676
108 28	L=5			LOC 4677
109 C	VOL	VOL	VOL VOL	LOC 4678
110	NY1=K+1			LOC 4679
111	NY2=K+1			LOC 4680
112	NY1=K+NCUL			LOC 4681
113	NY2=K+NCUL			LOC 4682
114	GO TO 141			LOC 4683
115 C	INTERMEDIATE SURFACE PRESENT			LOC 4684
116 C	SURFACE ON LEFT SIDE OF GAS VOLUME			LOC 4685
117 C	L=11,OR,13,OR,15			LOC 4686
118 31	XX=XD*ELCAT(JC=1)			LOC 4687
119	DO 32 J=1,NXSXN			LOC 4688
120	IF(ABS(XX-XSURF(J)))GT.XTEST)GO TO 32			LOC 4689
121	NSN=J			LOC 4690
122	GO TO 33			LOC 4691
123 32	CONTINUE			LOC 4692
124	GO TO 41			LOC 4693
125 33	IF(JR.NE.1)GO TO 34			LOC 4694
126	L=11			LOC 4695
127 C	SURF	VOL	SURF VOL	LOC 4696
128	NY1=NCB+(NSN=1)*NRROW+1			LOC 4697
129	NY2=K+1			LOC 4698
130	NY1=K			LOC 4699
131	NY2=K+NCUL			LOC 4700
132	GO TO 261			LOC 4701
133 34	IF(JR.NE.NROW)GO TO 35			LOC 4702
134	L=13			LOC 4703
135 C	(?)	VOL VOL	VOL SURF	LOC 4704
136	NY1=NCB+(NSN=1)*NRROW+JR			LOC 4705
137	NY2=K+1			LOC 4706
138	NY1=K+NCUL			LOC 4707
139	NY2=K+NCUL			LOC 4708
140	GO TO 301			LOC 4709
141 35	L=15			LOC 4710
142 C	SUR	VOL	VOL SURF	LOC 4711
143	NY1=NCB+NSN*NRROW			LOC 4712
144	NY2=K+1			LOC 4713
145	NY1=K+NCUL			LOC 4714
146	NY2=K+NCUL			LOC 4715
147	GO TO 341			LOC 4716
148 C	SURFACE ON RIGHT SIDE OF GAS VOLUME			LOC 4717
149 C	L=10,OR,12,OR,14			LOC 4718
150 41	XX=XX+XD			LOC 4719

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151 DD 42 J=1,NX5XN LUC 4720
152 IF(ABS(XX-XS)SURF(I))GT.XTEST)GO TO 42 LUC 4721
153 NSH=J LUC 4722
154 GO TO 43 LUC 4723
155 42 CONTINUE LUC 4724
156 IF(JR.EQ.1)GO TO 18 LUC 4725
157 IF(JR.EQ.NROW)GO TO 23 LUC 4726
158 GO TO 28 LUC 4727
159 43 IF(JR.NE.1)GO TO 44 LUC 4728
160 L=10 LUC 4729
161 C VOL SURF SURF VOL LUC 4730
162 NX1=K-1 LUC 4731
163 NX2=NCR+(NSH=1)*NROW+1 LUC 4732
164 NY1=K LUC 4733
165 NY2=NK+NCOL LUC 4734
166 GO TO 241 LUC 4735
167 44 IF(JR.EQ.NROW)GO TO 45 LUC 4736
168 L=12 LUC 4737
169 C VOL SURF VOL VOL LUC 4738
170 NX1=K-1 LUC 4739
171 NX2=NCR+(NSH=1)*NROW+JR LUC 4740
172 NY1=K+NCOL LUC 4741
173 NY2=NK+NCOL LUC 4742
174 GO TO 281 LUC 4743
175 45 L=14 LUC 4744
176 C VOL SURF VOL SURF LUC 4745
177 NX1=K-1 LUC 4746
178 NX2=NCR+SH*NROW LUC 4747
179 NY1=K+NCOL LUC 4748
180 NY2=NCOL+JC LUC 4749
181 GO TO 321 LUC 4750
182 C COMPUTE HEAT TRANSFER AND BULK FLOW TERMS LUC 4751
183 C L=1 LUC 4752
184 61 HX=HC(NX1)MYO LUC 4753
185 HY=HC(NY1)*XU LUC 4754
186 HT=HX+HY LUC 4755
187 HTT=HX*TS(NX1,1)+HY*TS(NY1,1) LUC 4756
188 IF(GHX(JX1,1)62,64,63 LUC 4757
189 62 GX=GHX(JX1)*CP(TV(K,1)) LUC 4758
190 ALFA(2)=GX LUC 4759
191 ALFA(3)=GMX(JX1)*HV(TV(K,1))+GX*TV(K,1) LUC 4760
192 GO TO 64 LUC 4761
193 63 ALFA(3)=GMX(JX1)*HV(TEMP) LUC 4762
194 64 IE=GHX(JX2,1)65,67,66 LUC 4763
195 65 GX=GHX(JX2)*CP(TV(NX2,1)) LUC 4764
196 GAMA(2)=GX LUC 4765
197 GAMA(3)=GMX(JX2)*HV(TV(NX2,1))+GX*TV(NX2,1) LUC 4766
198 GO TO 67 LUC 4767
199 66 GX=GHX(JX2)*CP(TV(K,1)) LUC 4768
200 GAMA(1)=GX LUC 4769

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201 GAMA(3)=GMX(JX2)*HV(TV(K,1))-GX*TV(K,1) LOC 4770
202 IF(GMY(JY1)18,7,69) LOC 4771
203 68 GY=GMY(JY1)*CP(TV(K,1)) LOC 4772
204 BETA(2)=GY LOC 4773
205 RETA(3)=-GMY(JY1)*HV(TV(K,1))+GY*TV(K,1) LOC 4774
206 GO TO 70 LOC 4775
207 69 RETA(3)=-GMY(JY1)*HV(FTEHP) LOC 4776
208 70 IF(GMY(JY2)17,99,72) LOC 4777
209 71 GY=GMY(JY2)*CP(TV(NY2,1)) LOC 4778
210 DELT(2)=GY LOC 4779
211 DELT(3)=GMY(JY2)*HV(TV(NY2,1))-GY*TV(NY2,1) LOC 4780
212 GO TO 99 LOC 4781
213 72 GY=GMY(JY2)*CP(TV(K,1)) LOC 4782
214 DELT(1)=GY LOC 4783
215 DELT(3)=-GMY(JY2)*HV(TV(K,1))-GY*TV(K,1) LOC 4784
216 GO TO 99 LOC 4785
217 C L=2 LOC 4786
218 81 HT=HC(JY1)XQ LOC 4787
219 HT=HT*TS(JY1) LOC 4788
220 IF(GMX(JX1)18,84,82) LOC 4789
221 82 GX=GMX(JX1)*CP(TV(K,1)) LOC 4790
222 ALFA(2)=GX LOC 4791
223 ALFA(3)=-GMX(JX1)*HV(TV(K,1))+GX*TV(K,1) LOC 4792
224 GO TO 84 LOC 4793
225 83 GX=GMX(JX1)*CP(TV(NX1,1)) LOC 4794
226 ALFA(1)=GX LOC 4795
227 ALFA(3)=-GMX(JX1)*HV(TV(NX1,1))+GX*TV(NX1,1) LOC 4796
228 84 IF(GMX(JX2)15,87,86) LOC 4797
229 85 GX=GMX(JX2)*CP(TV(NX2,1)) LOC 4798
230 GAMA(2)=GX LOC 4799
231 GAMA(3)=GMX(JX2)*HV(TV(NX2,1))-GX*TV(NX2,1) LOC 4800
232 GO TO 87 LOC 4801
233 86 GX=GMX(JX2)*CP(TV(K,1)) LOC 4802
234 GAMA(1)=GX LOC 4803
235 GAMA(3)=GMX(JX2)*HV(TV(K,1))-GX*TV(K,1) LOC 4804
236 87 IF(GMY(JY1)18,9,89) LOC 4805
237 88 GY=GMY(JY1)*CP(TV(K,1)) LOC 4806
238 BETA(2)=GY LOC 4807
239 BETA(3)=-GMY(JY1)*HV(TV(K,1))+GY*TV(K,1) LOC 4808
240 GO TO 90 LOC 4809
241 89 RETA(3)=-GMY(JY1)*HV(FTEHP) LOC 4810
242 90 IF(GMY(JY2)19,99,92) LOC 4811
243 91 GY=GMY(JY2)*CP(TV(NY2,1)) LOC 4812
244 DELT(2)=GY LOC 4813
245 DELT(3)=GMY(JY2)*HV(TV(NY2,1))-GY*TV(NY2,1) LOC 4814
246 GO TO 99 LOC 4815
247 92 GY=GMY(JY2)*CP(TV(K,1)) LOC 4816
248 DELT(1)=GY LOC 4817
249 DELT(3)=-GMY(JY2)*HV(TV(K,1))-GY*TV(K,1) LOC 4818
250 GO TO 99 LOC 4819

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251 C L=3 LOC 4820
252 101 HX=HC(NX2)*XO LOC 4821
253 HY=HC(NY1)*XO LOC 4822
254 HT=HX*HY LOC 4823
255 HTT=HX*TS(NX2,1)+HV*TS(NY1,1) LOC 4824
256 IF(GHX(JX1)+102+104+108 LOC 4825
257 102 GX=GMX(JX1)*CP(TV(K,1)) LOC 4826
258 ALFA(2)=GX LOC 4827
259 ALFA(3)=GMX(JX1)*HV(TV(K,1))+GX*TV(K,1) LOC 4828
260 GO TO 104 LOC 4829
261 103 GX=GMX(JX1)*CP(TV(NX1,1)) LOC 4830
262 ALFA(1)=GX LOC 4831
263 ALFA(3)=GMX(JX1)*HV(TV(NX1,1))+GX*TV(NX1,1) LOC 4832
264 104 IF(GHX(JX2)+105+107+108 LOC 4833
265 105 GAMA(3)=GMX(JX2)*HV(FTEMP) LOC 4834
266 GO TO 107 LOC 4835
267 106 GX=GMX(JX2)*CP(TV(K,1)) LOC 4836
268 GAMA(1)=GX LOC 4837
269 GAMA(3)=GMX(JX2)*HV(TV(K,1))+GX*TV(K,1) LOC 4838
270 107 IF(GMY(JY1)+109+110+112 LOC 4839
271 108 GY=GMV(JY1)*CP(TV(K,1)) LOC 4840
272 BETA(2)=GY LOC 4841
273 BETA(3)=GMV(JY1)*HV(TV(K,1))+GY*TV(K,1) LOC 4842
274 GO TO 111 LOC 4843
275 109 BETA(3)=GMV(JY1)*HV(FTEMP) LOC 4844
276 110 IF(GMY(JY2)+111+109+112 LOC 4845
277 111 GY=GMV(JY2)*CP(TV(NY2,1)) LOC 4846
278 DELI(2)=GY LOC 4847
279 DELI(3)=GMV(JY2)*HV(TV(NY2,1))+GY*TV(NY2,1) LOC 4848
280 GO TO 999 LOC 4849
281 112 GY=GMV(JY2)*CP(TV(K,1)) LOC 4850
282 DELI(1)=GY LOC 4851
283 DELI(3)=GMV(JY2)*HV(TV(K,1))+GY*TV(K,1) LOC 4852
284 GO TO 999 LOC 4853
285 C L=4 LOC 4854
286 121 HT=HC(NX1)*YO LOC 4855
287 HT*HT*TS(NX1,1) LOC 4856
288 IF(GMX(JX1)+122+124+123 LOC 4857
289 122 GX=GMX(JX1)*CP(TV(K,1)) LOC 4858
290 ALFA(2)=GX LOC 4859
291 ALFA(3)=GMX(JX1)*HV(TV(K,1))+GX*TV(K,1) LOC 4860
292 GO TO 124 LOC 4861
293 123 ALFA(3)=GMX(JX1)*HV(FTEMP) LOC 4862
294 124 IF(GMX(JX2)+125+127+126 LOC 4863
295 125 GX=GMX(JX2)*CP(TV(NX2,1)) LOC 4864
296 GAMA(2)=GX LOC 4865
297 GAMA(3)=GMX(JX2)*HV(TV(NX2,1))+GX*TV(NX2,1) LOC 4866
298 GO TO 127 LOC 4867
299 126 GX=GMX(JX2)*CP(TV(K,1)) LOC 4868
300 GAMA(1)=GX LOC 4869

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301	GAMA(3)=GMX(JX2)*HV(TV(K,1))-GX*TV(K,1)	LOC 4870
302	IF(GMY(JY1))128,130,129	LOC 4871
303	GY=GMY(JY1)*CP(TV(K,1))	LOC 4872
304	BETA(2)=GY	LOC 4873
305	BETA(3)=GMY(JY1)*HV(TV(K,1))+GY*TV(K,1)	LOC 4874
306	GO TO 130	LOC 4875
307	GY=GMY(JY1)*CP(TV(NY1,1))	LOC 4876
308	BETA(1)=GY	LOC 4877
309	BETA(3)=GMY(JY1)*HV(TV(NY1,1))+GY*TV(NY1,1)	LOC 4878
310	IF(GMY(JY2))131,999,132	LOC 4879
311	GY=GMY(JY2)*CP(TV(NY2,1))	LOC 4880
312	DELTA(2)=GY	LOC 4881
313	DELTA(3)=GMY(JY2)*HV(TV(NY2,1))+GY*TV(NY2,1)	LOC 4882
314	GO TO 999	LOC 4883
315	GY=GMY(JY2)*CP(TV(K,1))	LOC 4884
316	DELTA(1)=GY	LOC 4885
317	DELTA(3)=GMY(JY2)*HV(TV(K,1))-GY*TV(K,1)	LOC 4886
318	GO TO 999	LOC 4887
319	C L=5	LOC 4888
320	14: HI=0.0	LOC 4889
321	HT=0.0	LOC 4890
322	IF(GMX(JX1))142,144,143	LOC 4891
323	GX=GMX(JX1)*CP(TV(K,1))	LOC 4892
324	ALFA(2)=GX	LOC 4893
325	ALFA(3)=GMX(JX1)*HV(TV(K,1))+GX*TV(K,1)	LOC 4894
326	GO TO 144	LOC 4895
327	GX=GMX(JX1)*CP(TV(NX1,1))	LOC 4896
328	ALFA(1)=GX	LOC 4897
329	ALFA(3)=GMX(JX1)*HV(TV(NX1,1))+GX*TV(NX1,1)	LOC 4898
330	IF(GMX(JX2))145,147,146	LOC 4899
331	GX=GMX(JX2)*CP(TV(NX2,1))	LOC 4900
332	GAMA(2)=GX	LOC 4901
333	GAMA(3)=GMX(JX2)*HV(TV(NX2,1))+GX*TV(NX2,1)	LOC 4902
334	GO TO 147	LOC 4903
335	GX=GMX(JX2)*CP(TV(K,1))	LOC 4904
336	GAMA(1)=GX	LOC 4905
337	GAMA(3)=GMX(JX2)*HV(TV(K,1))+GX*TV(K,1)	LOC 4906
338	IF(GMY(JY1))148,150,149	LOC 4907
339	GY=GMY(JY1)*CP(TV(K,1))	LOC 4908
340	BETA(2)=GY	LOC 4909
341	BETA(3)=GMY(JY1)*HV(TV(K,1))+GY*TV(K,1)	LOC 4910
342	GO TO 150	LOC 4911
343	GY=GMY(JY1)*CP(TV(NY1,1))	LOC 4912
344	BETA(1)=GY	LOC 4913
345	BETA(3)=GMY(JY1)*HV(TV(NY1,1))+GY*TV(NY1,1)	LOC 4914
346	IF(GMY(JY2))151,999,152	LOC 4915
347	GY=GMY(JY2)*CP(TV(NY2,1))	LOC 4916
348	DELTA(2)=GX	LOC 4917
349	DELTA(3)=GMY(JY2)*HV(TV(NY2,1))+GY*TV(NY2,1)	LOC 4918
350	GO TO 999	LOC 4919

351	152	GY=GHY(JY2)*CP(TV(K,1))	LOC 4920
352		DEL(T,1)=GX	LOC 4921
353		DEL(T,3)=+GHY(JY2)*HV(TV(K,1))-GY*TV(K,1)	LOC 4922
354		GO TO 999	LOC 4923
355	C	L=6	LOC 4924
356	161	HT=HC(NX2)*YD	LOC 4925
357		HT=HT*TS(NX2,1)	LOC 4926
358		IF(GMX(JX1))162,164,163	LOC 4927
359	162	GX=GMX(JX1)*CP(TV(K,1))	LOC 4928
360		ALFA(2)=GX	LOC 4929
361		ALFA(3)=GMX(JX1)*HV(TV(K,1))+GX*TV(K,1)	LOC 4930
362		GO TO 164	LOC 4931
363	163	GX=GMX(JX1)*CP(TV(NX1,1))	LOC 4932
364		ALFA(1)=GX	LOC 4933
365		ALFA(3)=GMX(JX1)*HV(TV(NX1,1))+GX*TV(NX1,1)	LOC 4934
366	164	IF(GMX(JX2))165,167,166	LOC 4935
367	165	GAMA(3)=GMX(JX2)*HV(FTEMP)	LOC 4936
368		GO TO 167	LOC 4937
369	166	GX=GMX(JX2)*CP(TV(K,1))	LOC 4938
370		GAMA(1)=GX	LOC 4939
371		GAMA(3)=GMX(JX2)*HV(TV(K,1))-GX*TV(K,1)	LOC 4940
372	167	IF(GMX(JY1))168,170,169	LOC 4941
373	168	GY=GHY(JY1)*CP(TV(K,1))	LOC 4942
374		BETA(2)=GY	LOC 4943
375		BETA(3)=GHY(JY1)*HV(TV(K,1))+GY*TV(K,1)	LOC 4944
376		GO TO 173	LOC 4945
377	169	GY=GHY(JY1)*CP(TV(NY1,1))	LOC 4946
378		BETA(1)=GY	LOC 4947
379		BETA(3)=GHY(JY1)*HV(TV(NY1,1))+GY*TV(NY1,1)	LOC 4948
380	170	IF(GHY(JY2))171,199,172	LOC 4949
381	171	GY=GHY(JY2)*CP(TV(NY2,1))	LOC 4950
382		DEL(T,2)=GX	LOC 4951
383		DEL(T,3)=GHY(JY2)*HV(TV(NY2,1))-GY*TV(NY2,1)	LOC 4952
384		GO TO 999	LOC 4953
385	172	GY=GHY(JY2)*CP(TV(K,1))	LOC 4954
386		DEL(T,1)=GX	LOC 4955
387		DEL(T,3)=+GHY(JY2)*HV(TV(K,1))-GY*TV(K,1)	LOC 4956
388		GO TO 999	LOC 4957
389	C	L=7	LOC 4958
390	181	HX=HC(NX1)*YD	LOC 4959
391		HV=HC(NY2)*XD	LOC 4960
392		HT=HX*HY	LOC 4961
393		HT=HX*TS(NX1,1)+HY*TS(NY2,1)	LOC 4962
394		IF(GMX(JX1))182,184,183	LOC 4963
395	182	GX=GMX(JX1)*CP(TV(K,1))	LOC 4964
396		ALFA(2)=GX	LOC 4965
397		ALFA(3)=GMX(JX1)*HV(TV(K,1))+GX*TV(K,1)	LOC 4966
398		GO TO 184	LOC 4967
399	183	ALFA(3)=GMX(JX1)*HV(FTEMP)	LOC 4968
400	184	IF(GMX(JX2))185,187,186	LOC 4969

LOC	FUNCTION	LOC
401 185	GX=GMX(JX2)*CP(TV(NX2,1))	LDC 4970
402	GAMA(2)=GX	LDC 4971
403	GAMA(3)=+GMX(JX2)*HV(TV(NX2,1))=GX*TV(NX2,1)	LDC 4972
404	GO TO 187	LDC 4973
405 186	GX=GMX(JX2)*CP(TV(K,1))	LDC 4974
406	GAMA(1)=GX	LDC 4975
407	GAMA(3)=+GMX(JX2)*HV(TV(K,1))=GX*TV(K,1)	LDC 4976
408 187	IF(GHY(JY1))188,190,189	LDC 4977
409 188	GY=GHY(JY1)*CP(TV(K,1))	LDC 4978
410	BETA(2)=GY	LDC 4979
411	BETA(3)=+GHY(JY1)*HV(TV(K,1))=GY*TV(K,1)	LDC 4980
412	GO TO 190	LDC 4981
413 189	GY=GMX(JY1)*CP(TV(NY1,1))	LDC 4982
414	BETA(1)=GY	LDC 4983
415	BETA(3)=+GMX(JY1)*HV(TV(NY1,1))=GY*TV(NY1,1)	LDC 4984
416 190	IF(GHY(JY2))191,192,192	LDC 4985
417 191	DELTA(3)=+GMX(JY2)*HV(TEMP)	LDC 4986
418	GO TO 995	LDC 4987
419 192	GY=GHY(JY2)*CP(TV(K,1))	LDC 4988
420	DELTA(1)=GY	LDC 4989
421	DELTA(3)=+GHY(JY2)*HV(TV(K,1))=GY*TV(K,1)	LDC 4990
422	GO TO 999	LDC 4991
423 C	L=8	LDC 4992
424 201	HT=HC(NY2)*XO	LDC 4993
425	HT=HT*(NY2,1)	LDC 4994
426	IF(GHX(JX1))202,204,203	LDC 4995
427 202	GX=GMX(JX1)*CP(TV(K,1))	LDC 4996
428	ALFA(2)=GX	LDC 4997
429	ALFA(3)=+GMX(JX1)*HV(TV(K,1))=GX*TV(K,1)	LDC 4998
430	GO TO 204	LDC 4999
431 203	GX=GMX(JX1)*CP(TV(NX1,1))	LDC 5000
432	ALFA(1)=GX	LDC 5001
433	ALFA(3)=+GMX(JX1)*HV(TV(NX1,1))=GX*TV(NX1,1)	LDC 5002
434 204	IF(GHX(JX2))205,207,205	LDC 5003
435 205	GX=GMX(JX2)*CP(TV(NX2,1))	LDC 5004
436	GAMA(2)=GX	LDC 5005
437	GAMA(3)=+GMX(JX2)*HV(TV(NX2,1))=GX*TV(NX2,1)	LDC 5006
438	GO TO 207	LDC 5007
439 206	GX=GMX(JX2)*CP(TV(K,1))	LDC 5008
440	GAMA(1)=GX	LDC 5009
441	GAMA(3)=+GMX(JX2)*HV(TV(K,1))=GX*TV(K,1)	LDC 5010
442 207	IF(GHY(JY1))208,210,209	LDC 5011
443 208	GY=GHY(JY1)*CP(TV(K,1))	LDC 5012
444	BETA(2)=GY	LDC 5013
445	BETA(3)=+GHY(JY1)*HV(TV(K,1))=GY*TV(K,1)	LDC 5014
446	GO TO 210	LDC 5015
447 209	GY=GHY(JY1)*CP(TV(NY1,1))	LDC 5016
448	BETA(1)=GY	LDC 5017
449	BETA(3)=+GHY(JY1)*HV(TV(NY1,1))=GY*TV(NY1,1)	LDC 5018
450 210	IF(GHY(JY2))211,199,212	LDC 5019

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451 211 DELT(3)=+GMY(JY2)*HV(FTEMP) LOC 5020
452 GO TO 999 LOC 5021
453 212 GY=GMY(JY2)*CP(TV(K ,1)) LOC 5022
454 DELT(1)=GY LOC 5023
455 DELT(3)=+GMY(JY2)*HV(TV(K,1))=GY*TV(K,1) LOC 5024
456 GO TO 999 LOC 5025
457 C L=9 LOC 5026
458 221 HX=HC(NX2)+XU LOC 5027
459 HY=HC(HY2)*XU LOC 5028
460 HT=HX-HY LOC 5029
461 HTT=HX*TS(NX2,1)=HY*TS(HY2,1) LOC 5030
462 IF(GHX(JX1)+22+224,223 LOC 5031
463 222 GX=GHX(JX1)*CP(TV(K,1)) LOC 5032
464 ALFA(2)=GX LOC 5033
465 ALFA(3)=GX*(JX1)*HV(TV(K,1))+GX*TV(K,1) LOC 5034
466 GO TO 224 LOC 5035
467 223 GX=GHX(JX1)*CP(TV(NX1,1)) LOC 5036
468 ALFA(1)=GX LOC 5037
469 ALFA(3)=GX*(JX1)*HV(TV(NX1,1))+GX*TV(NX1,1) LOC 5038
470 224 IF(GHX(JX2)+225+227,226 LOC 5039
471 225 GAMA(3)=+GHX(JX2)*HV(FTEMP) LOC 5040
472 GO TO 227 LOC 5041
473 226 GX=GHX(JX2)*CP(TV(K,1)) LOC 5042
474 GAMA(1)=GX LOC 5043
475 GAMA(3)=+GHX(JX2)*HV(TV(K ,1))=GX*TV(K ,1) LOC 5044
476 227 IF(GAY(JY1)+228+230+229 LOC 5045
477 228 GY=GMY(JY1)*CP(TV(K ,1)) LOC 5046
478 BETA(2)=+GY LOC 5047
479 BETA(3)=GMY(JY1)*HV(TV(K ,1))+GY*TV(K ,1) LOC 5048
480 GO TO 230 LOC 5049
481 229 GY=GMY(JY1)*CP(TV(NY1,1)) LOC 5050
482 BETA(1)=GY LOC 5051
483 BETA(3)=GMY(JY1)*HV(TV(NY1,1))+GY*TV(NY1,1) LOC 5052
484 230 IF(GMY(JY2)+231+232 LOC 5053
485 231 DELT(3)=+GMY(JY2)*HV(FTEMP) LOC 5054
486 GO TO 999 LOC 5055
487 232 GY=GMY(JY2)*CP(TV(K ,1)) LOC 5056
488 DELT(1)=GX LOC 5057
489 DELT(3)=+GMY(JY2)*HV(TV(K,1))=GY*TV(K,1) LOC 5058
490 GO TO 999 LOC 5059
491 C L=10 LOC 5060
492 241 HX=HC(NX2)+YU/2, LOC 5061
493 HY=HC(NY1)*XU LOC 5062
494 HT=HX-HY LOC 5063
495 HTT=HX*TS(NX2,1)=HY*TS(NY1,1) LOC 5064
496 IF(GHX(JX1)+242+244+243 LOC 5065
497 242 GX=GHX(JX1)*CP(TV(K,1)) LOC 5066
498 ALFA(2)=GX LOC 5067
499 ALFA(3)=GMY(JX1)*HV(TV(K,1))+GX*TV(K,1) LOC 5068
500 GO TO 244 LOC 5069

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501 243 GX=GMX(JX1)*CP(TV(NX1,1)) LOC 5070
502 ALFA(1)=GX LOC 5071
503 ALFA(3)=GMX(JX1)*HV(TV(NX1,1))+GX*TV(NX1,1) LOC 5072
506 244 IF(GMX(JX2)1245,247,246) LOC 5073
505 245 GX=GMX(JX2)*CP(TV(K+1,1)) LOC 5074
506 GAMA(2)=GX LOC 5075
507 GAMA(3)=+GMX(JX2)*HV(TV(K+1,1))-GX*TV(K+1,1) LOC 5076
509 247 GO TO 247 LOC 5077
509 246 GX=GMX(JX2)*CP(TV(K,1)) LOC 5078
510 GAMA(1)=GX LOC 5079
511 GAMA(3)=+GMX(JX2)*HV(TV(K,1))-GX*TV(K,1) LOC 5080
512 247 IF(GMY(JY1)1248,250,249) LOC 5081
513 248 GY=GMX(JY1)*CP(TV(K,1)) LOC 5082
514 BETA(2)=GY LOC 5083
515 BETA(3)=+GMX(JY1)*HV(TV(K,1))+GY*TV(K,1) LOC 5084
516 GO TO 250 LOC 5085
517 249 BETA(3)=+GMX(JY1)*HV(FTEMP) LOC 5086
518 250 IF(GMY(JY2)1251,252) LOC 5087
519 251 GY=GMX(JY2)*CP(TV(NY2,1)) LOC 5088
520 DELT(2)=GY LOC 5089
521 DELT(3)=+GMX(JY2)*HV(TV(NY2,1))-GY*TV(NY2,1) LOC 5090
522 GO TO 259 LOC 5091
523 252 GY=GMX(JY2)*CP(TV(K,1)) LOC 5092
524 DELT(1)=GY LOC 5093
525 DELT(3)=+GMX(JY2)*HV(TV(K,1))-GY*TV(K,1) LOC 5094
526 GO TO 259 LOC 5095
527 C L=1 LOC 5096
528 261 HX=HC(NX1)*YD/2. LOC 5097
529 HV=HC(NY1)*XD LOC 5098
530 HT=HX*HY LOC 5099
531 HTT=HX*TS(NX1,1)+HY*TS(NY1,1) LOC 5100
532 IF(GMX(JX1)1262,264,263) LOC 5101
533 262 GX=GMX(JX1)*CP(TV(K,1)) LOC 5102
534 ALFA(2)=GX LOC 5103
535 ALFA(3)=+GMX(JX1)*HV(TV(K,1))+GX*TV(K,1) LOC 5104
536 GO TO 264 LOC 5105
537 263 GX=GMX(JX1)*CP(TV(K-1,1)) LOC 5106
538 ALFA(1)=GX LOC 5107
539 ALFA(3)=+GMX(JX1)*HV(TV(K-1,1))+GX*TV(K-1,1) LOC 5108
540 264 IF(GMX(JX2)1265,267,266) LOC 5109
541 265 GX=GMX(JX2)*CP(TV(NX2,1)) LOC 5110
542 GAMA(2)=GX LOC 5111
543 GAMA(3)=+GMX(JX2)*HV(TV(NX2,1))-GX*TV(NX2,1) LOC 5112
544 GO TO 267 LOC 5113
545 266 GX=GMX(JX2)*CP(TV(K,1)) LOC 5114
546 GAMA(1)=GX LOC 5115
547 267 GAMA(3)=+GMX(JX2)*HV(TV(K,1))-GX*TV(K,1) LOC 5116
548 267 IF(GMY(JY1)1268,270,269) LOC 5117
549 268 GY=GMX(JY1)*CP(TV(K,1)) LOC 5118
550 BETA(2)=GY LOC 5119

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551 BETA(3)=-GMV(JY1)*HV(TV(K ,1))+GY*TV(K ,1) LOC 5120
552 GO TO 270 LOC 5121
553 269 BETA(3)=-GMV(JY1)*HV(FTEMP) LOC 5122
554 270 IF(GMV(JY2)+271,999,292 LOC 5123
555 271 GY=GMV(JY2)*CP(TV(NY2,1)) LOC 5124
556 DELT(2)=-GY LOC 5125
557 DELT(3)=-GMV(JY2)*HV(TV(NY2,1))=GY*TV(NY2,1) LOC 5126
558 GO TO 999 LOC 5127
559 272 GY=GMV(JY2)*CP(TV(K ,1)) LOC 5128
560 DELT(1)=-GY LOC 5129
561 DELT(3)=-GMV(JY2)*HV(TV(K,1))=GY*TV(K,1) LOC 5130
562 GO TO 999 LOC 5131
563 C L=12 LOC 5132
564 281 HT=HC(NX2)+YB/2, LOC 5133
565 HT= HT*TS(NX2,1) LOC 5134
566 IF(GMX(JX1)+282,284,283 LOC 5135
567 282 GX=GMX(JX1)*CP(TV(K,1)) LOC 5136
568 ALFA(2)=-GX LOC 5137
569 ALFA(3)=-GMX(JX1)*HV(TV(K,1))+GX*TV(K,1) LOC 5138
570 GO TO 284 LOC 5139
571 283 GX=GMX(JX1)*CP(TV(NX1,1)) LOC 5140
572 ALFA(1)=-GX LOC 5141
573 ALFA(3)=-GMX(JX1)*HV(TV(NX1,1))+GX*TV(NX1,1) LOC 5142
574 284 IF(GMX(JX2)+285,287,286 LOC 5143
575 285 GX=GMX(JX2)*CP(TV(K+1,1)) LOC 5144
576 GAMMA(2)=-GX LOC 5145
577 GAMMA(3)=-GMX(JX2)*HV(TV(K+1,1))=GX*TV(K+1,1) LOC 5146
578 GO TO 287 LOC 5147
579 286 GX=GMX(JX2)*CP(TV(K ,1)) LOC 5148
580 GAMMA(1)=-GX LOC 5149
581 GAMMA(3)=-GMX(JX2)*HV(TV(K ,1))=GX*TV(K ,1) LOC 5150
582 287 IF(GMV(JY1)+288,290,289 LOC 5151
583 288 GY=GMV(JY1)*CP(TV(K ,1)) LOC 5152
584 BETA(2)=-GY LOC 5153
585 BETA(3)=-GMV(JY1)*HV(TV(K ,1))+GY*TV(K ,1) LOC 5154
586 GO TO 290 LOC 5155
587 289 GY=GMV(JY1)*CP(TV(NY1,1)) LOC 5156
588 BETA(1)=-GY LOC 5157
589 BETA(3)=-GMV(JY1)*HV(TV(NY1,1))+GY*TV(NY1,1) LOC 5158
590 290 IF(GMV(JY2)+291,999,292 LOC 5159
591 291 GY=GMV(JY2)*CP(TV(NY2,1)) LOC 5160
592 DELT(2)=-GY LOC 5161
593 DELT(3)=-GMV(JY2)*HV(TV(NY2,1))=GY*TV(NY2,1) LOC 5162
594 GO TO 999 LOC 5163
595 292 GY=GMV(JY2)*CP(TV(K ,1)) LOC 5164
596 DELT(1)=-GY LOC 5165
597 DELT(3)=-GMV(JY2)*HV(TV(K,1))=GY*TV(K,1) LOC 5166
598 GO TO 999 LOC 5167
599 C L=13 LOC 5168
600 301 HT=HC(NX1)+YD/2, LOC 5169

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601 HTT=HT*TS(NX1,1) LOC 5170
602 IF(GHX(JX1))302,304,303 LOC 5171
603 302 GX=GMX(JX1)*CP(TV(K,1)) LOC 5172
604 ALFA(2)=GX LOC 5173
605 ALFA(3)=GMX(JX1)*HV(TV(K,1))+GX*TV(K,1) LOC 5174
606 GO TO 304 LOC 5175
607 303 GX=GMX(JX1)*CP(TV(K,1,1)) LOC 5176
608 ALFA(1)=GX LOC 5177
609 ALFA(3)=GMX(JX1)*HV(TV(K,1,1))+GX*TV(K,1,1) LOC 5178
610 304 IF(GMX(JX2))305,307,306 LOC 5179
611 305 GX=GMX(JX2)*CP(TV(NX2,1)) LOC 5180
612 GAHA(2)=GX LOC 5181
613 GAHA(3)=GMX(JX2)*HV(TV(NX2,1))+GX*TV(NX2,1) LOC 5182
614 GO TO 307 LOC 5183
615 306 GX=GMX(JX2)*CP(TV(K,1)) LOC 5184
616 GAHA(1)=GX LOC 5185
617 GAHA(3)=GMX(JX2)*HV(TV(K,1))+GX*TV(K,1) LOC 5186
618 307 IF(GMY(JY1))308,310,309 LOC 5187
619 308 GY=GMY(JY1)*CP(TV(K,1)) LOC 5188
620 BETA(2)=GY LOC 5189
621 BETA(3)=GMY(JY1)*HV(TV(K,1))+GY*TV(K,1) LOC 5190
622 GO TO 310 LOC 5191
623 309 GY=GMY(JY1)*CP(TV(NY1,1)) LOC 5192
624 BETA(1)=GY LOC 5193
625 BETA(3)=GMY(JY1)*HV(TV(NY1,1))+GY*TV(NY1,1) LOC 5194
626 310 IF(GMY(JY2))311,999,312 LOC 5195
627 311 GY=GMY(JY2)*CP(TV(NY2,1)) LOC 5196
628 DELT(2)=GY LOC 5197
629 DELT(3)=GMY(JY2)*HV(TV(NY2,1))+GY*TV(NY2,1) LOC 5198
630 GO TO 999 LOC 5199
631 312 GY=GMY(JY2)*CP(TV(K,1)) LOC 5200
632 DELT(1)=GY LOC 5201
633 DELT(3)=GMY(JY2)*HV(TV(K,1))+GY*TV(K,1) LOC 5202
634 GO TO 999 LOC 5203
635 C L=14 LOC 5204
636 321 HX=HC(NX2)*YD/2. LOC 5205
637 HY=HC(NY2)*XU LOC 5206
638 HT=HX*HY LOC 5207
639 HTT=HX*TS(NX2,1)+HY*TS(NY2,1) LOC 5208
640 IF(GHX(JX1))322,324,323 LOC 5209
641 322 GX=GMX(JX1)*CP(TV(K,1)) LOC 5210
642 ALFA(2)=GX LOC 5211
643 ALFA(3)=GMX(JX1)*HV(TV(K,1))+GX*TV(K,1) LOC 5212
644 GO TO 324 LOC 5213
645 323 GX=GMX(JX1)*CP(TV(NX1,1)) LOC 5214
646 ALFA(1)=GX LOC 5215
647 ALFA(3)=GMX(JX1)*HV(TV(NX1,1))+GX*TV(NX1,1) LOC 5216
648 324 IF(GHX(JX2))325,327,326 LOC 5217
649 325 GX=GMX(JX2)*CP(TV(K,1,1)) LOC 5218
650 GAHA(2)=GX LOC 5219

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651	GAMA(3)=+GMX(JX2)*HV(TV(K,1))=GX*TV(K,1,1)	LOC 5220
652	GO TO 327	LOC 5221
653	GX=GMX(JX2)*CP(TV(K,1))	LOC 5222
654	GAMA(1)=GX	LOC 5223
655	GAMA(3)=+GMX(JX2)*HV(TV(K,1))=GX*TV(K,1)	LOC 5224
656	IF(GMY(JY1))328,330,329	LOC 5225
657	GY=GMY(JY1)*CP(TV(K,1))	LOC 5226
658	BETA(2)=GY	LOC 5227
659	BETA(3)=GMY(JY1)*HV(TV(K,1))+GY*TV(K,1)	LOC 5228
660	GO TO 330	LOC 5229
661	GY=GMY(JY1)*CP(TV(NY1,1))	LOC 5230
662	BETA(1)=GY	LOC 5231
663	BETA(3)=GMY(JY1)*HV(TV(NY1,1))+GY*TV(NY1,1)	LOC 5232
664	IF(GMY(JY2))331,999,332	LOC 5233
665	DELTA(3)=+GMY(JY2)*HV(FTEMP)	LOC 5234
666	GO TO 999	LOC 5235
667	GY=GMY(JY2)*CP(TV(K,1))	LOC 5236
668	DELTA(1)=GY	LOC 5237
669	DELTA(3)=GMY(JY2)*HV(TV(K,1))=GY*TV(K,1)	LOC 5238
670	GO TO 999	LOC 5239
671	C L=15	LOC 5240
672	HX=HC(HX1)+VD/2.	LOC 5241
673	HY=HC(NY2)*XD	LOC 5242
674	HT=HX-HY	LOC 5243
675	HTT=HX*TS(NX1,1)=HY*TS(NY2,1)	LOC 5244
676	IF(GMX(JX1))342,344,343	LOC 5245
677	GX=GMX(JX1)*CP(TV(K,1))	LOC 5246
678	ALFA(2)=GX	LOC 5247
679	ALFA(3)=GMX(JX1)*HV(TV(K,1))+GX*TV(K,1)	LOC 5248
680	GO TO 344	LOC 5249
681	GX=GMX(JX1)*CP(TV(K,1,1))	LOC 5250
682	ALFA(1)=GX	LOC 5251
683	ALFA(3)=GMX(JX1)*HV(TV(K,1,1))+GX*TV(K,1,1)	LOC 5252
684	IF(GMX(JX2))345,347,346	LOC 5253
685	GX=GMX(JX2)*CP(TV(NX2,1))	LOC 5254
686	GAMA(2)=GX	LOC 5255
687	GAMA(3)=+GMX(JX2)*HV(TV(NX2,1))=GX*TV(NX2,1)	LOC 5256
688	GO TO 347	LOC 5257
689	GX=GMX(JX2)*CP(TV(K,1))	LOC 5258
690	GAMA(1)=GX	LOC 5259
691	GAMA(3)=+GMX(JX2)*HV(TV(K,1))=GX*TV(K,1)	LOC 5260
692	IF(GMY(JY1))348,350,349	LOC 5261
693	GY=GMY(JY1)*CP(TV(K,1))	LOC 5262
694	BETA(2)=GY	LOC 5263
695	BETA(3)=GMY(JY1)*HV(TV(K,1))+GY*TV(K,1)	LOC 5264
696	GO TO 350	LOC 5265
697	GY=GMY(JY1)*CP(TV(NY1,1))	LOC 5266
698	BETA(1)=GY	LOC 5267
699	BETA(3)=GMY(JY1)*HV(TV(NY1,1))+GY*TV(NY1,1)	LOC 5268
700	IF(GMY(JY2))351,999,352	LOC 5269

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701 351 DELT(3)=GMY(JY2)*HV(FTEMP) LOC 5270
702 GO TO 999 LOC 5271
703 352 GY=GMY(JY2)*CP(TV(K ,1)) LOC 5272
704 DELT(1)=GY LOC 5273
705 DELT(3)=GMY(JY2)*HV(TV(K,1))=GY*TV(K,1) LOC 5274
706 999 LOC=L LOC 5275
707 RETURN LOC 5276
708 END LOC 5277
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1  SURROUTINE CL4 CL4 5278
2  COMPUTATION OF TOTAL INTERCHANGE AREA --- REAL GAS CL4 5279
3  COMPUTATION HAS TWO PARTS CL4 5280
4  C HCDEF=0 INITIAL CALCULATION OF GAS VOLUME INTERCHANGE AREAS CL4 5281
5  C =10 UPDATE INTERCHANGE AREAS WITH NEW TEMPERATURES CL4 5282
6  C ICDEF=0 INITIAL CALCULATION OF SURFACE AREA INTERCHANGE AREAS CL4 5283
7  C =10 UPDATE INTERCHANGE AREA WITH NEW TEMPERATURES CL4 5284
8  C COMMON // DIMENS(3),KK, ICDEF,HCDEF CL4 5285
9  A TAU(9), VAREA, HAREA, XLX, XK(3), ACDEF(8,3), CL4 5286
10 A IBRIDG, PRES, FLUET, ELUELS, XUMX, ISINK, CL4 5287
11 A NCR, HDUTY, HTVAL, FRATE, KFUEL, XAIR, FTEMP, CL4 5288
12 A NSSBLK, NGSBLK, NSGBLK, NGGBLK, NSURE, NVOL, CL4 5289
13 A XSURFX(9), XO, YO, ZLONG, NCOL, NROW, NXSXN, CL4 5290
14 A KSTART, ICDEF, SCODE, NGRAY, JHCHC, CL4 5291
15 A K1, K2, RCRD(10), TDEP(100), PERM(200), NPRINT CL4 5292
16 C
17 INTEGER SCODE,TCODE,RSTART,HCDEF
18 COMMON/SRCE4/AA(-60,60),BB(-60,15)
19 COMMON/JAZZ4/TSSM(8,4), TGSNM(8,3), TSGNM(8,3), TGGNM(8,3),
20 /SS(8),GS(8),SG(8),GG(8)
21 DIMENSION T(60),Z(60)
22 CALL READ(1,XLUM,Z(1),60)
23 IJK=HCDEF+ICDEF
24 IF(IJK.EQ.0)GO TO 11
25 IF(ICDEF.EQ.10)GO TO 11
26 IF(ICDEF.EQ.10)GO TO 31
27 11 CONTINUE
28 CALL READ(2,ITEMG,T(1),60)
29 CALL WRITE(3,ITEMG,T(1),60)
30 C KK=GAS NUMBER
31 C GAS TO SURFACE INTERCHANGE AREA
32 CALL PZERO(AA(1),1),3600)
33 DO 18 KK=1,NGRAY
34 DO 17 J=1,NSGBLK
35 MM=15*(J-1)
36 CALL READ(1,ISGNH(J,KK),BB(1,1),900)
37 IF(J.EQ.NSGBLK)GO TO 13
38 NMAX=15
39 GO TO 14
40 13 NMAX=NVOL/(NSGBLK-1)+1
41 14 DO 16 N=1,NMAX
42 H=MM*N
43 ZZ=EXP(EQUA(T(M)/1000,ACDEF(1,KK)))**Z(M)
44 DO 15 L=1,NSURE
45 AA(L,H)=AA(L,H)+BB(L,N)*ZZ
46 15 CONTINUE
47 16 CONTINUE
48 17 CONTINUE
49 18 CONTINUE
50 DO 19 J=1,NSGBLK

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51 CALL WRITE(2,SG(J),AA(1,15*J-14), 900) CL4 5328
52 CONTINUE CL4 5329
53 6000 IF(NPRINT.EQ.1)GO TO 22 CL4 5330
54 WRITE(K2,5001)(I(N),4,1,NVOL) CL4 5331
55 5001 FORMAT(1H,19X,1GAS VOLUME TEMPERATURES USED IN EVALUATION OF GAS CL4 5332
56 1VOLUMES1/20X,1TEMPERATURE DEPENDENT INTERCHANGE AREA,DEG. R1//125X,CL4 5333
57 26F15.31)
58 WRITE(K2,6001) CL4 5334
59 6001 FORMAT(11,1,20X,1VOLUME TO SURFACE INTERCHANGE AREA1) CL4 5335
60 CALL PR1(I,AA,NSUR,1VDL) CL4 5337
61 C GAS TO GAS INTERCHANGE AREA CL4 5338
62 22 CALL PZERO(AA(1,1), 3600) CL4 5339
63 DO 29 KK=1,NGRAY CL4 5340
64 DO 27 J=1,NGGBLK CL4 5341
65 HM=15*(J-1) CL4 5342
66 CALL READ(I,ICGMH(J,KK),88(1,1), 900) CL4 5343
67 IF(J.EQ.NGGBLK)GO TO 23 CL4 5344
68 MAX=15 CL4 5345
69 GO TO 24 CL4 5346
70 23 NMAX=NV1-(NGGBLK-K-1)*15 CL4 5347
71 24 DO 26 N=1,NMAX CL4 5348
72 H=H*H CL4 5349
73 ZZ=EXPECUA(T(H)/1000.,ACDEF(1,KK))*Z(M) CL4 5350
74 DO 25 L=1,1VDL CL4 5351
75 AA(L,M)=AA(L,M)+88(L,N)*ZZ*(L) CL4 5352
76 25 CONTINUE CL4 5353
77 26 CONTINUE CL4 5354
78 27 CONTINUE CL4 5355
79 28 CONTINUE CL4 5356
80 DO 29 J=1,NGGBLK CL4 5357
81 CALL WRITE(2,GG(J),AA(1,15*J-14), 900) CL4 5358
82 29 CONTINUE CL4 5359
83 IF(NPRINT.EQ.1)GO TO 30 CL4 5360
84 6010 WRITE(K2,6002) CL4 5361
85 6002 FORMAT(11,1,20X,1VOLUME TO VOLUME INTERCHANGE AREA1) CL4 5362
86 CALL PR1(AA,NVOL,NVOL) CL4 5363
87 30 CONTINUE CL4 5364
88 IF(LJK.EQ.0)GO TO 31 CL4 5365
89 GO TO 67 CL4 5366
90 C PART 2 SURFACE AREA TEMPERATURE DEPENDENT CL4 5367
91 31 CALL READ(2,ITEMS1,T(1), 60) CL4 5368
92 CALL WRITE(3,ITEMS1,T(1), 60) CL4 5369
93 C SURFACE TO SURFACE INTERCHANGE AREA CL4 5370
94 C KK=GAS NUMBER CL4 5371
95 CALL PZERO(AA(1,1), 3600) CL4 5372
96 KMAX=1+NGRAY CL4 5373
97 DO 45 K=1,KMAX CL4 5374
98 IF(K.EQ.KMAX)GO TO 33 CL4 5375
99 KK=K CL4 5376
100 GO TO 34 CL4 5377

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101 33      KK=4          CL4 5378
102 34      DD 44 J=1,NSSBLK CL4 5379
103      MM=15*(J=1)    CL4 5380
104      CALL READ(J,KK,1,88,(J), 900) CL4 5381
105      IF(J.EQ.NSSBLK)GO TO 36      CL4 5382
106      NMAX=15        CL4 5383
107      GO TO 37      CL4 5384
108 36      NMAX=NSURF-(NSSBLK=1)+15 CL4 5385
109 37      DD 43 N=1,NMAX CL4 5386
110      M=MM*N        CL4 5387
111      IF(KK.EQ.4)GO TO 38          CL4 5388
112      ZZ=EXP(EQUA(I(H)/1000.,ACDEF(I,KK))) CL4 5389
113      GO TO 41          CL4 5390
114 38      ZZ=1.        CL4 5391
115      DD 40 I=1,GRAY          CL4 5392
116      ZZ=EXP(EQUA(I(H)/1000.,ACDEF(I,I))) CL4 5393
117 40      CONTINUE          CL4 5394
118 41      DD 42 L=1,NSURF      CL4 5395
119      AA(L,N)=AA(L,H)+RB(L,N)*ZZ CL4 5396
120 42      CONTINUE          CL4 5397
121 43      CONTINUE          CL4 5398
122 44      CONTINUE          CL4 5399
123 45      CONTINUE          CL4 5400
124      DD 47 J=1,NSSBLK      CL4 5401
125      CALL WRITE(2,SS(J),AA(1,15*J-14), 900) CL4 5402
126 47      CONTINUE          CL4 5403
127 7000   IF(NPRT.EQ.1)GO TO 52   CL4 5404
128      WRITE(4,2,5002)(I(N),V(I,NSURF)) CL4 5405
129 5002   FORMAT(1H19X,'SURFACE AREA TEMPERATURE USED IN EVALUATING SURFACE CL4 5406
130      LAREA/20X,'TEMPERATURE DEPENDENT INTERCHANGE AREA=DEC R//(25X,6F15 CL4 5407
131      2.3))
132      WRITE(2,7001)
133 7001   FORMAT(/11,1,20X,'SURFACE TO SURFACE INTERCHANGE AREA1) CL4 5410
134      CALL PRINT(AA,NSURF,ISURE) CL4 5411
135 C     SURFACE TO SURFACE INTERCHANGE AREA CL4 5412
136 C     KK=GAS NUMBER          CL4 5413
137 52     CALL PZERO(AA(1,1), 3600) CL4 5414
138      DD 58 KK=1,NGAS        CL4 5415
139      DD 57 J=1,NGSBLK      CL4 5416
140      MM=(J=1)+15          CL4 5417
141      CALL READ(1,TGSNH(J,KK),BB(1,1), 900) CL4 5418
142      IF(J.EQ.NGSBLK)GO TO 53 CL4 5419
143      NMAX=15              CL4 5420
144      GO TO 54              CL4 5421
145 53     NMAX=NSURF-(NGSBLK=1)+15 CL4 5422
146 54     DD 56 N=1,NMAX      CL4 5423
147      M=MM*N                CL4 5424
148      ZZ=EXP(EQUA(I(H)/1000.,ACDEF(I,KK))) CL4 5425
149      DD 55 L=1,HVUL        CL4 5426
150      AA(L,H)=AA(L,H)+BB(L,N)*ZZ*(L) CL4 5427

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151 55 CONTINUE CL4 5428
152 56 CONTINUE CL4 5429
153 57 CONTINUE CL4 5430
154 58 CONTINUE CL4 5431
155 00 59 J=1,NGSBLK CL4 5432
156 CALL WRITE(2,GS(J),AA(1,15*NJ-14), 900) CL4 5433
157 59 CONTINUE CL4 5434
158 I=INPRN1,EG,1)GO TO 67 CL4 5435
159 7010 WRITE(K27011) CL4 5436
160 7011 FORHAI(71,1,20X,(SURFACE TO VOLUME INTERCHANGE AREA)) CL4 5437
161 CALL PRI:(AA,NVOL,NSURF) CL4 5438
162 67 RETURN CL4 5439
163 END CL4 5440
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1 SUBROUTINE CL5
2 C GAS VOLUME HEAT BALANCE CL5 5441
3 COMMON / / DUMHY(3),KK, ICODE, HCODE, CL5 5442
4 A TAU(9), VALEA, HAREA, XLX, XK(3), ACOEF(8,3), CL5 5443
5 A TARIDG, PRES, FLUET, FLUE(5), XHMX, TSINK, CL5 5444
6 A XCR, HQUY, HVAL, ERATE, KEVEL, XAIR, ETEMP, CL5 5445
7 A NSSBLK, NGSBLK, NSGBLK, NGBLKB, NSURF, NVOL, CL5 5447
8 A XSUREX(2), XQ, YQ, ZICNC, NCOL, NROW, NXSXN, CL5 5448
9 A RSTART, TCODE, SCODE, NGRAY, JHCHC, CL5 5449
10 A K1, K2, RCRD(10), IDEP(100), PEKH(200), NPRINT CL5 5450
11 C
12 INTEGER SCODE,ICODE,RSTART,HCODE CL5 5451
13 EQUIVALENCE (DUMHY(1),NFMX),(PERM(199),DHTCL5) CL5 5453
14 COMMON/GAS/ NY,NX,NZ,NY,NZ,HT,HTI,XTEST,ALFA(3),BETA(3),GAMA(3), CL5 5454
15 I DELT(3),GNX(120),GMV(120),HC( 60),JX1,JX2,JY1,JY2 CL5 5455
16 COMMON/TT/TV(12,2),TS(120,2) CL5 5456
17 COMMON/JAZZ5/ GS(8),SG(8),GG(8) CL5 5457
18 COMMON/CPHV/CPCP(11),VHV(12) CL5 5458
19 DIMENSION AA( 60, 60),RHS( 60),AAA( 60, 61),ET( 60),ZZ( 60),MM( 60CL5 5459
20 )
21 EQUIVALENCE (AA(1,1),AAA(1,1)),(RHS(1),AAA(1, 61)),(ZZ(1),MM(1)) CL5 5461
22 DATA SIG /0.1713E-8/ CL5 5462
23 HCODE=1 CL5 5463
24 NFIX=0 CL5 5464
25 XTEST=.10*XD CL5 5465
26 C RETRIEVE DATA CL5 5466
27 C SURFACE AND VOLUME TEMPERATURES CL5 5467
28 C HEAT RELEASE PATTERN CL5 5468
29 C BULK FLOW PATTERN CL5 5469
30 C GAS --- SURFACE HEAT TRANSFER COEFFICIENT CL5 5470
31 CALL READ(2,'TEMG',TV(1,1), 60) CL5 5471
32 CALL READ(2,'ITEMS',TS(1,1), 50) CL5 5472
33 CALL READ(2,'HGAS',ET(1), 60) CL5 5473
34 NX=(NCOL+1)*NROW CL5 5474
35 NY=(NROW+1)*NCOL CL5 5475
36 CALL READ(2,'GMV',GMV(1), NY) CL5 5476
37 CALL READ(2,'GNX',GNX(1), NX) CL5 5477
38 CALL READ(2,'HC',HC(1), 60) CL5 5478
39 CALL READ(2,'CPCP',CPCP(1),11) CL5 5479
40 CALL READ(2,'HV',VHV(1),12) CL5 5480
41 C COMPUTE TEMPERATURE FACTORS (T**3 AND T**4)
42 DO 4 J=1,NSURE CL5 5481
43 TS(J,2)=TS(J,1)**3 CL5 5482
44 C CONTINUE CL5 5483
45 10 DO 11 J=1,NVCL CL5 5484
46 IV(J,2)=TV(J,1)**3 CL5 5485
47 11 CONTINUE CL5 5486
48 C PUT SURFACE TO GAS INTERCHANGE AREA IN AA CL5 5487
49 CALL PZERD(AA(1,1), 3600) CL5 5489
50 DO 15 J=1,NGSBLK CL5 5490

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51 CALL READ(2,GS(J),AA(1,15*J-14), 900)
52 CONTINUE
53 C COMPUTE S-G CONTRIBUTION TO RHS --- SUM OVER SURFACE EMITTER FOR
54 C EACH GAS RECEIVER ACCOUNTING FOR TEMPERATURE OF EMITTER
55 DO 17 I=1,NVUL
56 RHS(I)=0.0
57 DO 16 J=1,NSURF
58 RHS(I)+RHS(I)+AA(I,J)*S(J,2)
59 CONTINUE
60 RHS(I)+RHS(I)*(-SIG)
61 CONTINUE
62 C PUT GAS TO SURFACE AREA IN AA
63 CALL PZERD(AA(1,1), 3600)
64 DO 23 J=1,NSGK
65 CALL READ(2,SG(J),AA(1,15*J-14), 900)
66 CONTINUE
67 C COMPUTE G-S CONTRIBUTION TO DIAGONAL OF MATRIX AA AND SAVE IN
68 C TEMPORARY STORAGE --- SUM OVER SURFACE RECEIVER FOR EACH GAS
69 C EMITTER AND STORE IN ZZ
70 DO 25 J=1,NVUL
71 ZZ(J)=0.0
72 DO 24 I=1,HSURF
73 ZZ(J)+ZZ(J)+AA(I,J)
74 CONTINUE
75 CONTINUE
76 C PUT G-G TOTAL INTERCHANGE AREA IN AA
77 CALL PZERD(AA(1,1), 3600)
78 DO 27 J=1,NSGK
79 CALL READ(2,GG(J),AA(1,15*J-14), 900)
80 CONTINUE
81 C COMPUTE G-G CONTRIBUTION TO DIAGONAL OF MATRIX AA AND SAVE IN
82 C TEMPORARY STORAGE ALONG WITH G-S CONTRIBUTIONS --- SUM OVER GAS
83 C RECEIVER FOR EACH GAS EMITTER AND ADD IN TEMPORARY STORAGE ZZ
84 C WHEN FINISHED MULTIPLY BY MINUS SIGMA
85 DO 29 J=1,NVUL
86 DO 28 I=1,NSURF
87 ZZ(J)+ZZ(J)+AA(I,J)
88 CONTINUE
89 ZZ(J)+ZZ(J)*(-SIG)
90 CONTINUE
91 C MULTIPLY AA BY SIMGA
92 DO 32 J=1,NVUL
93 DO 31 I=1,NSURF
94 AA(I,J)=AA(I,J)*SIG
95 CONTINUE
96 CONTINUE
97 C EACH GAS VOLUME MUST BE ANALYZED INDIVIDUALLY TO DETERMINE
98 C CONVECTIVE HEAT TRANSFER TERMS
99 C 1 -- BULK FLOW ADJACENT SURFACE AND VOLUMES
100 C 2 -- SURFACE HEAT TRANSFER INTO GAS VOLUME

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CL5 5491
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CL5 5540

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101      I=1          CL5 5541
102 50      LL=LOC(I)  CL5 5542
103      AA(I,I)=AA(I,I)+(HT+ALFA(2)+BETA(2)+GAMA(1)+DELT(1))/TV(I,2)+ZZ(I) CL5 5543
104      RHS(I)=RHS(I)+(HT+ALFA(3)+BETA(3)+GAMA(3)+DELT(3))/EI(I)  CL5 5544
105      GO TO(51,52,53,54,55,56,57,58,59,510,511,512,513,514,515),LL  CL5 5545
106 C      LL=1      CL5 5546
107 51      AA(I,NX2)=AA(I,NX2)+GAMA(2)/TV(NX2,2)  CL5 5547
108      AA(I,NY2)=AA(I,NY2)+DELT(2)/TV(NY2,2)  CL5 5548
109      GO TO 60  CL5 5549
110 C      LL=2      CL5 5550
111 52      AA(I,NX1)=AA(I,NX1)+ALFA(1)/TV(NX1,2)  CL5 5551
112      AA(I,NX2)=AA(I,NX2)+GAMA(2)/TV(NX2,2)  CL5 5552
113      AA(I,NY2)=AA(I,NY2)+DELT(2)/TV(NY2,2)  CL5 5553
114      GO TO 60  CL5 5554
115 C      LL=3      CL5 5555
116 53      AA(I,NX1)=AA(I,NX1)+ALFA(1)/TV(NX1,2)  CL5 5556
117      AA(I,NY2)=AA(I,NY2)+DELT(2)/TV(NY2,2)  CL5 5557
118      GO TO 60  CL5 5558
119 C      LL=4      CL5 5559
120 54      AA(I,NX2)=AA(I,NX2)+GAMA(2)/TV(NX2,2)  CL5 5560
121      AA(I,NY1)=AA(I,NY1)+BETA(1)/TV(NY1,2)  CL5 5561
122      AA(I,NY2)=AA(I,NY2)+DELT(2)/TV(NY2,2)  CL5 5562
123      GO TO 60  CL5 5563
124 C      LL=5      CL5 5564
125 55      AA(I,NX1)=AA(I,NX1)+ALFA(1)/TV(NX1,2)  CL5 5565
126      AA(I,NX2)=AA(I,NX2)+GAMA(2)/TV(NX2,2)  CL5 5566
127      AA(I,NY1)=AA(I,NY1)+BETA(1)/TV(NY1,2)  CL5 5567
128      AA(I,NY2)=AA(I,NY2)+DELT(2)/TV(NY2,2)  CL5 5568
129      GO TO 60  CL5 5569
130 C      LL=6      CL5 5570
131 56      AA(I,NX1)=AA(I,NX1)+ALFA(1)/TV(NX1,2)  CL5 5571
132      AA(I,NY1)=AA(I,NY1)+BETA(1)/TV(NY1,2)  CL5 5572
133      AA(I,NY2)=AA(I,NY2)+DELT(2)/TV(NY2,2)  CL5 5573
134      GO TO 60  CL5 5574
135 C      LL=7      CL5 5575
136 57      AA(I,NX2)=AA(I,NX2)+GAMA(2)/TV(NX2,2)  CL5 5576
137      AA(I,NY1)=AA(I,NY1)+BETA(1)/TV(NY1,2)  CL5 5577
138      GO TO 60  CL5 5578
139 C      LL=8      CL5 5579
140 58      AA(I,NX1)=AA(I,NX1)+ALFA(1)/TV(NX1,2)  CL5 5580
141      AA(I,NX2)=AA(I,NX2)+GAMA(2)/TV(NX2,2)  CL5 5581
142      AA(I,NY1)=AA(I,NY1)+BETA(1)/TV(NY1,2)  CL5 5582
143      GO TO 60  CL5 5583
144 C      LL=9      CL5 5584
145 59      AA(I,NX1)=AA(I,NX1)+ALFA(1)/TV(NX1,2)  CL5 5585
146      AA(I,NY1)=AA(I,NY1)+BETA(1)/TV(NY1,2)  CL5 5586
147      GO TO 60  CL5 5587
148 C      LL=10     CL5 5588
149 510     AA(I,NX1)=AA(I,NX1)+ALFA(1)/TV(NX1,2)  CL5 5589
150      AA(I,I)=AA(I,I)+GAMA(2)/TV(I,I+2)  CL5 5590

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151 AA(I,NY2)=AA(I,NY2)+DELTA(2)/TV(NY2,2) CL5 5591
152 GO TO 60 CL5 5592
153 C LL=11 CL5 5593
154 511 AA(I,I=1)=AA(I,I=1)+ALFA(1)/TV(I=1,2) CL5 5594
155 AA(I,NX2)=AA(I,NX2)+GAMA(2)/TV(NX2,2) CL5 5595
156 AA(I,NY2)=AA(I,NY2)+DELTA(2)/TV(NY2,2) CL5 5596
157 GO TO 60 CL5 5597
158 C LL=12 CL5 5598
159 512 AA(I,NX1)=AA(I,NX1)+ALFA(1)/TV(NX1,2) CL5 5599
160 AA(I,I=1)=AA(I,I=1)+GAMA(2)/TV(I=1,2) CL5 5600
161 AA(I,NY1)=AA(I,NY1)+BETA(1)/TV(NY1,2) CL5 5601
162 AA(I,NY2)=AA(I,NY2)+DELTA(2)/TV(NY2,2) CL5 5602
163 GO TO 60 CL5 5603
164 C LL=13 CL5 5604
165 513 AA(I,I=1)=AA(I,I=1)+ALFA(1)/TV(I=1,2) CL5 5605
166 AA(I,NX2)=AA(I,NX2)+GAMA(2)/TV(NX2,2) CL5 5606
167 AA(I,NY1)=AA(I,NY1)+BETA(1)/TV(NY1,2) CL5 5607
168 AA(I,NY2)=AA(I,NY2)+DELTA(2)/TV(NY2,2) CL5 5608
169 GO TO 60 CL5 5609
170 C LL=14 CL5 5610
171 514 AA(I,NX1)=AA(I,NX1)+ALFA(1)/TV(NX1,2) CL5 5611
172 AA(I,I=1)=AA(I,I=1)+GAMA(2)/TV(I=1,2) CL5 5612
173 AA(I,NY1)=AA(I,NY1)+BETA(1)/TV(NY1,2) CL5 5613
174 GO TO 60 CL5 5614
175 C LL=15 CL5 5615
176 515 AA(I,I=1)=AA(I,I=1)+ALFA(1)/TV(I=1,2) CL5 5616
177 AA(I,NX2)=AA(I,NX2)+GAMA(2)/TV(NX2,2) CL5 5617
178 AA(I,NY1)=AA(I,NY1)+BETA(1)/TV(NY1,2) CL5 5618
179 60 IF(I.EQ.NVOL)GO TO 61 CL5 5619
180 I=I+1 CL5 5620
181 GO TO 50 CL5 5621
182 C FOR VOLUMES WITH KNOWN TEMPERATURE SET DIAGONAL OF AA EQUAL TO CL5 5622
183 C 1.0 AND RHS=T**4 CL5 5623
184 61 CALL REAL(2,ICONV1,MH1),60} CL5 5624
185 DO 63 I=1,NVOL CL5 5625
186 IF(MH1.EQ.0)GO TO 63 CL5 5626
187 DO 62 J=1,NVOL CL5 5627
188 AA(I,J)=0.0 CL5 5628
189 62 CONTINUE CL5 5629
190 AA(I,I)=1. CL5 5630
191 RHS(I)=TV(I,1)**4 CL5 5631
192 63 CONTINUE CL5 5632
193 C SOLVE FOR TEMPERATURE OF GAS VOLUME RAISED TO THE FORTH POWER AND CL5 5633
194 C THAN EXTRACT THE FOURTH ROOT CL5 5634
195 N=NVOL+1 CL5 5635
196 DO 67 I=1,NVOL CL5 5636
197 AAA(I,N)=RHS(I) CL5 5637
198 67 CONTINUE CL5 5638
199 IF(NPRINT.EQ.1)GO TO 681 CL5 5639
200 67 WRITE(K2,6900) CL5 5640

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201 6000 FORMAT(1H1,19X,'GAS VOLUME ENERGY BALANCE!')
202 CALL PRINT(AAA,NVOL,1)
203 681 CALL ISINEQ(AAA, 60, 61,NVOL)
204 DT=0.0
205 DD 69 I=1,NVOL
206 RHS(I)=SQRT(SQRT(AAA*(I,N)))
207 DT=AMAX1(ABS(RHS(I)-TV(I,1)),DT)
208 DEL=RHS(I)-TV(I,1)
209 TV(I,1)=TV(I,1)+SIGN(AMIN1(ABS(DEL),250.0),DEL)
210 69 CONTINUE
211 71 NFIX=NFIX+1
212 IF(DT.LT.5.0)WHICH(5,OR,NFIX,60,NEHAX)GO TO 81
213 IF(DT.LT.250.0)GO TO 10
214 GO TO 85
215 C COMPARE TEMPERATURES OBTAINED FROM GAS VOLUME HEAT BALANCE WITH
216 C THOSE USED IN OBTAINING GAS VOLUME TEMPERATURE DEPENDENT
217 C INTERCHANGE AREA (G-G AND G-S)
218 81 CALL READ(3,ITENG,ZZ(I), 60)
219 DT=0.0
220 DD 82 I=1,NVOL
221 DT=AMAX1(ABS(ZZ(I)-TV(I,1)),DT)
222 82 CONTINUE
223 IF(DT.LT.DHTCL5)HCODE=2
224 85 CALL WRITE(2,ITENG,TV(I,1), 60)
225 WRITE(6,3003)DT
226 IF(NPRINT.EQ.1)GO TO 86
227 WRITE(2,3002) (TV(N,1),N=1,NVOL)
228 3002 FORMAT(12X,1COMPUTED GAS VOLUME TEMPERATURES,DEC,R1//125X,6E15,3CL5 5668
229 1))
230 3003 FORMAT(12X,1MAX TEMPERATURE DIFFERENCE FOUND IN COMPUTING GAS VOLUC15 5670
231 1ME1,F10,3)
232 86 RETURN
233 END
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1 SUBROUTINE CL6 CL6 5674
2 SURFACE AREA HEAT BALANCE CL6 5675
3 COMMON // DUMMY(3),KK, ICODE, HCODE, CL6 5676
4 A TAU(9), VAREA, HAREA, XLX, XK(3), ACDEE(L8,3), CL6 5677
5 A TBRIDG, PRES, FLUET, FLUE(5), XIMX, TSINK, CL6 5678
6 A NCR, HJUV, HTVAL, ERATE, KEUEL, XAIR, FTEMP, CL6 5679
7 A NSSBLK, NSGOLK, NSGOLK, HGRAY, NSURF, NVOL, CL6 5680
8 A XSUREX(2), XB, YB, ZLONC, NCOL, HGRAY, NXSXN, CL6 5681
9 A RSTART, TCODE, SCODE, HGRAY, JHCHC, CL6 5682
10 A K1, K2, RCFD(10), TDEP(100), PERH(200), NPRINT CL6 5683
11 C CL6 5684
12 INTEGER SCODE, TCODE, RSTART, HCODE CL6 5685
13 EQUIVALENCE (DUMMY(2), NFIX), (PERM(200), DHTCL6) CL6 5686
14 COMMON /JZZ/ S(8), S(8), S(8) CL6 5687
15 DIMENSION AA( 60, 60), RHS( 60), AAA( 60, 61), ET( 60), ZZ( 60), MM( 60) CL6 5688
16 1, TV( 60, 2), IS( 60, 2), IP( 60), HC( 60, 3) CL6 5689
17 EQUIVALENCE (AA(1,1), AAA(1,1)), (RHS(1), AAA(1, 61)), (ZZ(1), MM(1)) CL6 5690
18 DATA SIG /0.1713E-8/ CL6 5691
19 ICODE=1 CL6 5692
20 NFIX=0 CL6 5693
21 C RETRIEVE DATA CL6 5694
22 C SURFACE VOLUME AND PROCESS TEMPERATURES CL6 5695
23 C HEAT RELEASE PATTERN CL6 5696
24 C ALL THREE HEAT TRANSFER COEFFICIENTS CL6 5697
25 CALL READ(2), TEMG, TV(1,1), 60) CL6 5698
26 CALL READ(2), TEMEL, TS(1,1), 60) CL6 5699
27 CALL READ(2), TEMPI, TP(1), 60) CL6 5700
28 CALL READ(2), HSUEI, ET(1), 60) CL6 5701
29 CALL READ(2), HC(1,1), 60) CL6 5702
30 CALL READ(2), HCP(1,2), 60) CL6 5703
31 CALL READ(2), HCPPI, HC(1,3), 60) CL6 5704
32 C COMPUTE TEMPERATURE FACTORS (I=3 AND I=4) CL6 5705
33 DO 8 J=1, NVOL CL6 5706
34 TV(J,2)=TV(J,1)**4 CL6 5707
35 8 CONTINUE CL6 5708
36 10 DO 11 J=1, NSURF CL6 5709
37 TS(J,2)=TS(J,1)**3 CL6 5710
38 11 CONTINUE CL6 5711
39 C PUT GAS TO SURFACE INTERCHANGE AREA IN AA CL6 5712
40 CALL PZERO(AA(1,1), 3600) CL6 5713
41 DO 13 J=1, NSGOLK CL6 5714
42 CALL READ(2), SG(J), AA(1,15+J-14), 900) CL6 5715
43 13 CONTINUE CL6 5716
44 C COMPUTE G-S CONTRIBUTION TO RHS -- SUM OVER GAS EMITTER FOR EACH CL6 5717
45 C SURFACE RECEIVER ACCOUNTING FOR TEMPERATURE OF EMITTER CL6 5718
46 DO 16 I=1, NSURF CL6 5719
47 RHS(I)=0.0 CL6 5720
48 DO 15 J=1, NVOL CL6 5721
49 RHS(I)=RHS(I)+AA(I,J)*TV(J,2) CL6 5722
50 15 CONTINUE CL6 5723

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51  RHS(I)=RHS(I)*(-SIG)          CL6 5724
52 16 CONTINUE                   CL6 5725
53 C PUT SURFACE TO GAS INTERCHANGE AREA IN AA
54 CALL PZERO(AA(I,1), 3600)      CL6 5726
55 DO 21 J=1,NGSRLK              CL6 5727
56 CALL READ(2,GS(I),AA(I,15),J=14), 900) CL6 5728
57 21 CONTINUE                   CL6 5729
58 C COMPUTE S-G CONTRIBUTIONS TO DIAGONAL OF MATRIX AA AND SAVE IN
59 C TEMPORARY STORAGE -- SUM OVER GAS RECEIVER FOR EACH SURFACE EMITTER
60 C AND STORE IN ZZ              CL6 5730
61 DO 23 J=1,NSURF              CL6 5731
62 ZZ(J)=0.C                    CL6 5732
63 DO 22 I=1,NVUL               CL6 5733
64 ZZ(I)=ZZ(I)+AA(I,I)          CL6 5734
65 22 CONTINUE                   CL6 5735
66 23 CONTINUE                   CL6 5736
67 C PUT SURFACE TO SURFACE INTERCHANGE AREA IN AA
68 CALL PZERO(AA(I,1), 3600)      CL6 5737
69 DO 27 J=1,MSSBLK             CL6 5738
70 CALL READ(2,SS(J),AA(I,15),J=14), 900) CL6 5739
71 27 CONTINUE                   CL6 5740
72 C COMPUTE S-S CONTRIBUTION TO DIAGONAL OF MATRIX AA AND SAVE IN
73 C TEMPORARY STORAGE ALONG WITH S-G CONTRIBUTION -- SUM OVER SURFACE
74 C RECEIVER FOR EACH SURFACE EMITTER AND STORE IN ZZ, WHEN
75 C FINISHED MULTIPLY BY MINUS SIGMA
76 DO 29 J=1,NSURF              CL6 5741
77 DO 28 I=1,NSURF              CL6 5742
78 ZZ(I)=ZZ(I)+AA(I,I)          CL6 5743
79 28 CONTINUE                   CL6 5744
80 ZZ(I)=ZZ(I)*(-SIG)           CL6 5745
81 29 CONTINUE                   CL6 5746
82 C MULTIPLY AA THROUGH BY SIGMA
83 DO 37 J=1,NSURF              CL6 5747
84 DO 36 I=1,NSURF              CL6 5748
85 AA(I,J)=AA(I,J)*SIG          CL6 5749
86 36 CONTINUE                   CL6 5750
97 37 CONTINUE                   CL6 5751
88 C COMPLETE MATRIX AND RHS IN TWO STEPS
89 C 1 -- RADIANT AND SOURCE TERMS
90 C 2 -- CUMULATIVE TERMS
91 DO 38 I=1,NSURF              CL6 5752
92 AA(I,I)=AA(I,I)+ZZ(I)        CL6 5753
93 RHS(I)=RHS(I)+ET(I)          CL6 5754
94 38 CONTINUE                   CL6 5755
95 DD49 I=1,NSURF              CL6 5756
96 CALL IGAS(I,K,I1,I2)          CL6 5757
97 IF(I.GT.2)CJL)GU TO 99       CL6 5758
98 XY=XD                          CL6 5759
99 GU TO 46                       CL6 5760
100 39 XY=YD                       CL6 5761

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101 46 GO TO (47,48),K
102 C K=1 ----- OUTER SURFACE
103 47 AA(I,1)=AA(I,1)-(HC(I,1)+HC(I,2)+HC(I,3))*XY/TS(I,2)
104 RHS(I)=RHS(I)-(HC(I,1)*TV(I,1,1)+HC(I,2)*TP(I,1,3)+TSINK)*XY
105 GO TO 49
106 C K=2 ----- INNER SURFACE
107 48 AA(I,1)=AA(I,1)-(HC(I,1)+HC(I,2))*XY/TS(I,2)
108 RHS(I)=RHS(I)-(HC(I,1)*TV(I,1,1)+TV(I,2,1,1))/2+HC(I,2)*TP(I,1,3)*XY
109 49 CONTINUE
110 C FOR SURFACES WITH KNOWN TEMPERATURE SET DIAGONAL OF AA EQUAL TO
111 C 1.0 AND RHS EQUAL TO TS**4
112 CALL READ(2,ICONS,MM(1),-60)
113 DO 54 I=1,NSURF
114 IF(MM(I),EQ,0)GO TO 54
115 DO 53 J=1,NSURF
116 AA(I,J)=0.0
117 53 CONTINUE
118 AA(I,I)=1.
119 RHS(I)=TS(I,1)**4
120 54 CONTINUE
121 C SOLVE FOR TEMPERATURE OF SURFACES ARE RAISED TO THE FOURTH POWER AND
122 C THEN EXTRACT THE FOURTH ROOT
123 N=NSURF+1
124 DO 56 I=1,NSURF
125 AAA(I,N)=RHS(I)
126 56 CONTINUE
127 IF(NPRT,EQ,1)GO TO 581
128 571 WRITE(K2,6000)
129 6000 FORMAT(11,19X,'SURFACE AREA ENERGY BALANCE')
130 CALL PRINT(AAA,NSURF,N)
131 581 CALL ISIEQ(AAA,60,61,NSURF)
132 DISO=0
133 DO 62 I=1,NSURF
134 RHS(I)=SRT(SURF(AAA(I,N)))
135 DT=AMAX1(ABS(RHS(I))-TS(I,1)),DT)
136 DEL=RHS(I)-TS(I,1)
137 TS(I,1)=TS(I,1)+SIGN(AMIN1(ABS(DEL),250.0),DEL)
138 62 CONTINUE
139 71 NFIX=NFIX+1
140 IF(DT,LT,5.0*DHITCL6,OR,NEIX,EQ,NEMAX)GO TO 81
141 IF(DT,LT,250.)GO TO 10
142 GO TO 85
143 C COMPARE AREA
144 C COMPARE TEMPERATURES OBTAINED FROM SURFACE AREA HEAT BALANCE WITH
145 C THOSE USED IN OBTAINING SURFACE AREA TEMPERATURE DEPENDENT
146 C INTERCHANGE AREASIS=5 AND S=6)
147 81 CALL READ(3,ITENS1,ZZ(1),60)
148 DTRO=
149 DO 82 I=1,NSURF
150 DT=AMAX1(ABS(ZZ(I))-TS(I,1)),DT)

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CL6 5774
CL6 5775
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A FORTRAN IV (VER L43) SOURCE LISTING: CL6 SUBROUTINE 03/05/74 PAGE 0138
151 82 CONTINUE CL6 5824
152 85 CALL WRITE(2,ITEMS1,TS(1,1),60) CL6 5825
153 IF(OT.LE.DHTCL6)ICDDE=2 CL6 5826
154 WRITE(2,3002)OT CL6 5827
155 IF(NPRINT.EQ.1)GO TO 86 CL6 5828
156 WRITE(2,3001) (TS(N,1),N=1,NSURF) CL6 5829
157 3001 FORMAT(//20X'COMPUTED SURFACE AREA TEMPERATURES,DEG.R'/(25X,6F15CL6 5830
158 1-3)) CL6 5831
159 3002 FORMAT(2X,'MAX TEMPERATURE DIFFERENCE IN SURFACE ARAE CALCULATION CL6 5832
160 1, F12.3)
161 86 RETURN CL6 5834
162 END CL6 5835

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1 SUPROUTINE IGAS(I1,KK,IG1,IG2) IGAS5836
2 C SUBROUTINE COMPUTES THE INDEX OF GAS VOLUMES ADJACENT TO SURFACE ARIGAS5837
3 C I1 SURFACE AREA INDEX IGAS5838
4 C KKK NUMBER OF ADJACENT GAS VOLUMES IGAS5839
5 C IGL2 INDEX OF ADJACENT GAS VOLUMES IGAS5840
6 COMMON // DUMMY(I2),KK, ICODE, HCJDE, IGAS5841
7 A TAU(9), VAREA, HAREA, XLX, XK(3), ACOEF(3,3), IGAS5842
8 A TRIDG, PRES, FLUET, FLUE(5), XENX, ISIPK, IGAS5843
9 A NCR, HDITY, HTVAL, FRATE, KFUEL, XAIR, FTEMP, IGAS5844
10 A NSSBLK, NSGALK, NSGALK, NSGALK, NSURE, NVOL, IGAS5845
11 A XSURFX(9), XJ, YD, ZLONG, NCOL, NROW, NXSN, IGAS5846
12 A RSTART, ICODE, SCODE, NGRAY, JHGH, IGAS5847
13 A K1, K2, RCRD(10), TDEP(100), PERM(200) IGAS5848
14 C IGAS5849
15 INTEGER SCODE,TCODE,RSTART,HCODE IGAS5850
16 I=1 IGAS5851
17 I1=0 IGAS5852
18 I2=0 IGAS5853
19 K=1 IGAS5854
20 IF(I1.GT.NCOL)GO TO 11 IGAS5855
21 C TOP OF FURNACE IGAS5856
22 I1=1 IGAS5857
23 GO TO 19 IGAS5858
24 11 IF(I1.GT.2*NCOL)GO TO 12 IGAS5859
25 C BOTTOM OF FURNACE IGAS5860
26 I1=NCOL*(I1-1)+1 IGAS5861
27 GO TO 19 IGAS5862
28 12 IF(I1.GT.2*NCOL+NROW)GO TO 13 IGAS5863
29 C LEFT SIDE OF FURNACE IGAS5864
30 I1=NCOL*(I1-2)+1 IGAS5865
31 GO TO 19 IGAS5866
32 13 IF(I1.GT.NCOL)GO TO 14 IGAS5867
33 C RIGHT SIDE OF FURNACE IGAS5868
34 I1=(I1-2)*NCOL+NROW)IGAS5869
35 GO TO 19 IGAS5870
36 14 K=2 IGAS5871
37 I=1+NCR IGAS5872
38 C INTER-SURFACE HENCE TWO GAS VOLUMES IGAS5873
39 DO 17 J=1,9 IGAS5874
40 IF(I1.GT.NROW)GO TO 15 IGAS5875
41 I=(I1-1)*NCOL+INT(XSURFX(J)/XD+.1) IGAS5876
42 I2=I+1 IGAS5877
43 GO TO 19 IGAS5878
44 15 I=1+NROW IGAS5879
45 17 CONTINUE IGAS5880
46 19 KKK=K IGAS5881
47 IGL=I1 IGAS5882
48 IGL2=I2 IGAS5883
49 RETURN IGAS5884
50 END IGAS5885

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1  SUBROUTINE CL7          CL7 5886
2  C  FEMALE OUTPUT      CL7 5887
3  COMMON // DUMMY(3),KK, ICODE, HCODE,          CL7 5888
4  A TAU(9), VAREA, HAREA, XLX, XK(3), ACDEF(8,3), CL7 5889
5  A TBRIDG, PRES, FLUET, FLUE(5), XMAX, TSINK, CL7 5890
6  A NGR, HDUTY, HTVAL, FRATE, KEUEL, XAIR, FTEMP, CL7 5891
7  A NSSBLK, NSGULK, NSGULK, NIGGULK, NSURF, NVOL, CL7 5892
8  A XSUREX(4), X0, Y0, Z0, NC0, NRC0, XMAX, CL7 5893
9  A KSTART, TC0DE, SCODE, NGRAY, JHCHC, CL7 5894
10 A K1, K2, RGRD(10), TDEF(10), PERH(200) CL7 5895
11 COMMON/TUBE2/IND, TX(100), OT(4), QFF CL7 5896
12 C
13 INTEGER SCODE, TCODE, KSTART, HCODE
14 REAL I1, G0, V1, G1, Z1, SO, HIDENT, G0, GMY(120) CL7 5897
15 DATA IN3/1/
16 HDONE=KK
17 IF (NDUNE.EQ.0) GO TO 65
18 WRITE(K2,63)
19 63  FORMAT(11,14X,'CASE CONVERGED',15X ,14(1-1)) CL7 5904
20 GO TO 70
21 65  WRITE( K2,66)
22 66  FORMAT(11,14X,'CASE NOT CONVERGED',15X,18(1-1)) CL7 5906
23 70  CALL READ(2,ITEMG,T(1), 60)
24 DO 71 J=1,NVOL
25 IF (T(N).EQ.0.0) GO TO 71
26 T(J)=T(J)+460.
27 71  CONTINUE
28 JJSO
29 TBR=0.0
30 NY=(AROW+1)*NGOL
31 CALL READ(2,IGMY,IGMY(1), NY)
32 DO 710 J=1,NGOL
33 IF (GMY(J).GE.0.0) GO TO 710
34 JJSJJ+1
35 TBR=TBR+T(J)
36 710 CONTINUE
37 TBR=TBR/FLDRT(JJ)
38 712 WRITE(K2,72)(T(N),N=1,NVOL)
39 72  FORMAT(11/20X,'FEMALE GAS VOLUME TEMPERATURE, DEG. F.
40 11/((25X,6E15+1))
41 CALL READ(2,ITEM5,T(1), 60)
42 DO 78 N=1,NSURE
43 IF (T(N).EQ.0.0) GO TO 78
44 T(N)=T(N)+60.
45 78  CONTINUE
46 WRITE(K2,79)(T(N),N=1,NSURE)
47 79  FORMAT(11/20X,'FINAL SURFACE AREA TEMPERATURES, DEGREES F.11/((25X,
48 16E15+1))
49 80  CALL READ(2,ITEM1,V(1), 60)
50 DO 82 N=1,NSURE

```

```

51 IF(V(N),EQ,0.0)GO TO 82
52 V(N)=V(N)+.660
53 82 CONTINUE
54 CALL READ(2, HCP, I, Z(1), 60)
55 DO 85 N=1, NSURF
56 HDER(N)=Z(N)*T(N)+V(N)
57 85 CONTINUE
58 IF(HAREA, EQ, 0.0)GO TO 860
59 DO 86 N=1, NCR
60 HDER(H)=HTDEN(N)/HAREA
61 86 CONTINUE
62 860 IF(I*XSX+EQ, 0)GO TO 48
63 IN=NCR+1
64 DO 87 N=1, NSURE
65 HTDEN(N)=HTDEN(N)/VAREA
66 87 CONTINUE
67 88 WRITE(K2, 89) (HTDEN(N), N=1, NSURF)
68 162 FORMAT(1, /20X, 'SURFACE TO AREA COEFFICIENTS', /27X, 6F15.1)
69 89 FORMAT(1, /20X, 'COMPUTED HEAT DENSITIES, BTU/HR/SQUARE FOOT OF TUBE SURFACE', /25X, 6F15.1)
70 SURFACE=1.56/ZLOG
71 HCOMB=HCOMB+.56/ZLOG
72 HFIN=FLUET*X*HAMB+H*(FTEMP)
73 CALL READ(2, HCPPI, Z(1), 60)
74 TSINKF=TSINK-460.
75 HAMB=0.0
76 DO 91 N=1, NCR
77 HAMB=HAMB+Z(N)*T(N)-TSINKF
78 91 CONTINUE
79 HPROC=0.0
80 M=2*WCU
81 DO 92 N=1, NIN
82 HPROC=HPROC+HTDEN(N)*XC*WAREA
83 92 CONTINUE
84 N=NIN+1
85 DO 93 N=1, NCR
86 HPROC=HPROC+HTDEN(N)*YO*HAREA
87 93 CONTINUE
88 IFC XSX*EQ, 0)GO TO 95
89 DO 94 N=1, NCR
90 HPROC=HPROC+HTDEN(N)*YC*VAREA
91 94 CONTINUE
92 95 HNET=FLUET*X*HAMB+H*(TBR+460.)
93 HNET=HCOMB+HFIN+HAMB-HPROC-HFOUT
94 WRITE(K2, 96) HCOMB, HFIN, HAMB, HPROC, HNET
95 OFF=HPROC
96 96 FORMAT(1, /14X, 'FURNACE OVERALL HEAT BALANCE, BTU/HR/FOOT OF FURNACE', /11X, 5F15.1)
97 151, 15X, 56(1.1) /20X, 'HEAT IN', /25X, 'COMBUSTION', F21.0/25X, 'FLUE GAS', /25X, 'FURNACE', F24.0/25X, 'PROCESS FLUID', /25X, '2AS1', F23.0/25X, 'HEAT GAIN', /25X, 'AMBIENT', F24.0/25X, 'PROCESS FLUID', /25X, '3F18.0/25X, 'FLUE GAS', F23.0/25X, 'NET HEAT BALANCE (HEAT IN-HEAT OUT)', /25X, '411, F20.0)
98 99
99 99
100 100

```

```

101 IF(HPROC.LE.0.0)WRITE(K2,103)HPROC,XD,YD,HAREA,VAREA CL7 5986
102 103  FORMAT(I1,HPROC=1,E8.3,I1,XD=1,E8.3,I1,YD=1,E8.3,I1,HAREA=1,E8.3, CL7 5987
103 1 VAREA=1,F8.3) CL7 5988
104 WRITE(K2,97) CL7 5989
105 97  FORMAT(I1) CL7 5990
106 HEAT=HCQIN+HFIM+HAMB-HPROC CL7 5991
107 ENTH=HEAT/FLUET/XMWX CL7 5992
108 YSTOP=9000./460. CL7 5993
109 TT=600.-460. CL7 5994
110 TOL=.01 CL7 5995
111 99  IF(WAYAI*(TT+460.),ENTH,TOL,TT,TSTOP,1)99,105,100 CL7 5996
112 100  WRITE(K2,101)ENTH,TT CL7 5997
113 101  FORMAT(15X,'BRIDGE WALL TEMPERATURE CANNOT BE COMPUTED/15X42(1-1) CL7 5998
114 1//20X,'REQUIRED ENTHALPY,BTU/LB',F20.3/20X,'LAST VALUE OF BRIDGE CL7 5999
115 2 WALL TEMPERATURE, DEG F',F20.3) CL7 6000
116 GO TO 110 CL7 6001
117 105  WRITE(K2,106)ENTH,TT CL7 6002
118 106  FORMAT(15X,'BRIDGE WALL TEMPERATURE COMPUTION/15X 35(1-1) CL7 6003
119 1//20X,'REQUIRED ENTHALPY,BTU/LB',F20.3/20X,'BRIDGE WALL TEMPERATURE, DEG F' CL7 6004
120 2 ,F15.3) CL7 6005
121 110  TT=6.0 CL7 6006
122 IF(IN3.GT.1)GO TO 999 CL7 6007
123 IN3=IN3+1 CL7 6008
124 N=1 CL7 6009
125 120  Y(N)=TT CL7 6010
126 Y(N)=WV*(TT+460.) CL7 6011
127 Z(N)=CP*(TT+460.) CL7 6012
128 IF(TT.GE.4000.)GO TO 130 CL7 6013
129 N=N+1 CL7 6014
130 Y=TT+100. CL7 6015
131 GO TO 120 CL7 6016
132 130  NN=N CL7 6017
133 WRITE(K2,131)(Y(N),V(N),Z(N),N=1,NN) CL7 6018
134 131  FORMAT(I1,14X,'ELUE GAS ENTHALPY AND SPECIFIC HEAT DATA/15X40(1-1) CL7 6019
135 1) //20X,'TEMP, DEG F ',5X,'ENTHALPY,BTU/LB',5X,'SPECIFIC HEAT,BTU/L CL7 6020
136 2B/LB/DEG F',F20.3,F21.3,F25.6) CL7 6021
137 999  RETURN CL7 6022
138 END CL7 6023

```

```

1 FUNCTION WAYA(A,ANS,TOL,START,STOP,LEVEL)
2 ROUTINE TO CONVERGE ON SINGLE VALUED FUNCTION
3 C A =CURRENT VALUE OF DEPENDENT VARIABLE
4 C ANS =DESIRED VALUE OF DEPENDENT VARIABLE
5 C TOL =TOLERANCE
6 C START =CURRENT VALUE OF INDEPENDENT VARIABLE, A BETTER VALUE RETURNED
7 C STOP =LIMIT OF INDEPENDENT VARIABLE ANSWER BETWEEN START AND STOP
8 C LEVEL =1,2,3 AS A INDEX FOR MULTILEVEL USE
9 C WAYA WILL VARY START BETWEEN ITS INITIAL VALUE AND STOP UNTIL
10 C ABS(AUS-A) LE-TOL OR 30 TRIALS TAKEN
11 C ON EXIT WAYA IS
12 C = FOR SET C=CONVERGED, REPEAT CALCULATIONS WITH A NEW VALUE IN START
13 C 0 CONVERGED IN LIMITS OR 30 TRIALS TAKEN
14 C * FOR CALCUOT COVERAGE START OR STOP WILL BE INITIAL VALUE
15 C WHICHEVER GIVES LESSER ERROR, OR ITS INITIAL VALUE IF LEVEL IS
16 C NEGATIVE
17 DIMENSION X1(10),X2(10),Y1(10),Y2(10),KOUNT(10)
18 DATA KOUNT(10)/0
19 C SET X , Y , AND LEVEL
20 X=START
21 Y=ANS-A
22 L=IABS(LEVEL)
23 WAYA=1.0
24 C SEE IF CONVERGED
25 IF (ABS(Y).LE.TOL) GO TO 70
26 C NOT CONVERGED SEE WHICH CALL
27 IF (KOUNT(L)) GO TO 30,10
28 C SECOND OR HINGER CALL SEE IF Y AND Y1(L) BRACKET ANSWER
29 10 IF (Y*Y1(L).LT.0.) GO TO 20
30 C NO Y=Y1 BRACKET SEE IF SECOND OR HIGHER CALL
31 IF (KOUNT(L).GT.1) GO TO 30
32 C NO BRACKET AT ALL REDD AT START IF THAT LIMIT IS CLOSER OR IF LEVEL
33 C MINUS
34 IF (ABS(Y).LE.ABS(Y1(L)).AND.LEVEL.GT.0) GO TO 80
35 X=X1(L)
36 KOUNT(L)=1
37 GO TO 60
38 C Y=Y1 BRACKET STORE X AND Y IN X2(L) AND Y2(L)
39 20 X2(L)=X
40 Y2(L)=Y
41 GO TO 40
42 C FIRST CALL OR CONVERGING Y=Y1 BRACKET CALL
43 C STORE RESULT IN X AND Y IN XU AND YI
44 30 X1(L)=X
45 Y1(L)=Y
46 X=STOP
47 IF (KOUNT(L).EQ.0) GO TO 50
48 C INTERPOLATE NEW X AND CONTINUE OR QUIT DEPENDING ON KOUNT(L)
49 40 X=(X1(L)*(3.*Y2(L)-Y1(L))+X2(L))*(Y2(L)-3.*Y1(L))/(4.*(Y2(L)-Y1(L)
50 )))

```

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WAYA6024
WAYA6025
WAYA6026
WAYA6027
WAYA6028
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WAYA6071
WAYA6072
WAYA6073

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```
51 IF(KOUNT(L).GE.30)GO TO 70
52 50 KOUNT(L)=KOUNT(L)+1
53 60 WAYA=1.
54 GO TO 90
55 C CONVERGED OR TOO MANY TRAILS
56 70 WAYA=0.0
57 80 KOUNT(L)=0
58 C SET NEW VALUE OF INDEPENDENT VARIABLE
59 90 START=X
60 RETURN
61 END
```

```
WAYA6074
WAYA6075
WAYA6076
WAYA6077
WAYA6078
WAYA6079
WAYA6080
WAYA6081
WAYA6042
WAYA6083
WAYA6084
```



```
1 SUBROUTINE PZERO(A,N)
2 DIMENSION A(1),HH(1)
3 DO 1 K=1,N
4   A(K)=0
5 RETURN
6 ENTRY NZERO(HH,N)
7 DO 2 K=1,N
8   HH(K)=0
9 RETURN
10 END
```

PZER0085
PZER0086
PZER0087
PZER0088
PZER0089
PZER0090
PZER0091
PZER0092
PZER0093
PZER0094

```

1  FUNCTION FITIT ( X, Y, ND, MAX, C, LN, A )      FIT 6095
2  C                                              EIT 6096
3  C WILL FIT POLYNOMIAL OF ORDER MAX ( MAX .LT. 7 ) TO ND Y VS. X DATAFIT 6097
4  C POINTS SUPPLIED IN ARRAYS Y AND X. COEFFICIENTS RETURNED IN ARRAY EIT 6098
5  C C IN FURN NEEDED BY FUNCTION EQUA. STANDARD DEVIATION OF Y RETURN EIT 6099
6  C U AS FITIT.
7  C
8  C LN = LOG TRANSFORMATION CODE 1 = Y VS. X
9  C 2 = LN Y VS. X
10 C 3 = Y VS. LN X
11 C 4 = LN Y VS. LN X
12 C
13 C A = INTERCEPT CODE ZERO = INTERCEPT = 0.0
14 C NONZERO = INTERCEPT CALCULATED
15 C
16 C DOUBLE PRECISION D(5),XY,0
17 C DIMENSION X(1), Y(1), C(1), D(7), S(7), XY(7,7)
18 C REAL*4 LUG
19 C
20 C SET CONTROLS AND ZEROS AND XY.
21 C
22 C N = ND
23 C M = MINO ( MAX + 1, 7)
24 C L = MINO ( 4, MAXO ( 1, LN ) )
25 C Z = N
26 C DO 10 I = 1, M
27 C S(I) = 0.0
28 C DO 10 J = 1, M
29 C 10 XY(I, J) = 0.0
30 C
31 C FOR EACH DATUM, MOVE Y AND X TO D(1) AND D(2), GET LOGS IF NEEDED
32 C AND POWERS OF X, AND ACCUMULATE SUHS, SQUARES, AND CROSS PRODUCTS
33 C IN S AND XY.
34 C
35 C DO 80 K = 1, N
36 C D(1) = X(K)
37 C D(2) = X(K)
38 C GO TO ( 50, 20, 40, 30 ), L
39 C 20 D(1) = LOG ( D(1) )
40 C GO TO 50
41 C 30 D(1) = LOG ( D(1) )
42 C 40 D(2) = LOG ( D(2) )
43 C 50 DO 60 I = 3, M
44 C 60 D(I) = D(2) * D(I - 1)
45 C DO 70 I = 1, M
46 C S(I) = S(I) + D(I)
47 C DO 70 J = 1, M
48 C 70 XY(I, J) = XY(I, J) + D(I) * D(J)
49 C 80 CONTINUE
50 C

```

```

51 C GET REDUCED SQUARES AND CROSS PRODUCTS IF A NONZERO AND FOLD XY FIT 6145
52 C OVER. FIT 6146
53 C
54 IF ( A.EQ. 0.0 ) GO TO 110 FIT 6147
55 DO 100 I = 1, M FIT 6148
56 Q = S(I) / Z FIT 6149
57 DO 90 J = 1, M FIT 6150
58 90 XY(I, J) = XY(I, J) + Q * S(I) FIT 6151
59 100 S(I) = Q FIT 6152
60 110 DO 120 J = 1, M FIT 6153
61 DO 120 I = J, M FIT 6154
62 120 XY(I, J) = XY(I, J) FIT 6155
63 C
64 C SOLVE REGRESSION MATRIX AND GET STANDARD DEVIATION OF Y. FIT 6157
65 C
66 DO 160 J = 2, M FIT 6158
67 Q = XY(I, I) FIT 6159
68 XY(I, J) = 1.0 FIT 6160
69 DO 130 J = 1, M FIT 6161
70 130 XY(I, J) = XY(I, J) / Q FIT 6162
71 DO 150 K = 1, M FIT 6163
72 IF ( K.EQ. 1 ) GO TO 150 FIT 6164
73 Q = XY(K, I) FIT 6165
74 XY(K, I) = Q + Q FIT 6166
75 DO 140 J = 1, M FIT 6167
76 140 XY(K, J) = XY(K, J) + XY(I, J) * Q FIT 6168
77 150 CONTINUE FIT 6169
78 160 CONTINUE FIT 6170
79 Q = (MAX0(N-M, 1)) FIT 6171
80 FITIT=0.0 FIT 6172
81 IF(XY(1,1).GT.0.)FITIT=DSORT(XY(1,1))/Q FIT 6173
82 C STORE COEFFICIENTS IN C ARRAY. FIT 6174
83 C FIT 6175
84 C FIT 6176
85 C(1) = M - 1 FIT 6177
86 C(2) = 0.0 FIT 6178
87 DO 170 I = 2, M FIT 6179
88 S(I) = S(I) - S(I) * XY(I, 1) FIT 6180
89 170 C(I + 1) = XY(I, 1) FIT 6181
90 IF ( A.EQ. 0.0 ) C(2) = S(I) FIT 6182
91 RETURN FIT 6183
92 C FIT 6184
93 END FIT 6185
FIT 6186
FIT 6187

```

1 FUNCTION EQUA (X, C)
2 C
3 C THIS FUNCTION EVALUATES A SET OF POLYNOMIAL COEFFICIENTS BY
4 C NESTED EXPANSION ----- AS GENERATED BY FUNCTION FITT,
5 C
6 C $Y = A0 + A1X + A2X^2 + \dots + AMX^M$
7 C
8 C $M = C(1)$
9 C
10 C $A0 = C(2)$
11 C $A1 = C(3)$
12 C $A2 = C(4)$
13 C \dots
14 C \dots
15 C $AM = C(M+2)$
16 C
17 REAL C(1)
18 C
19 $M = C(1)$
20 $Y = C(M+2)$
21 $MM = M+2$
22 DO 1 J=1,M
23 K=MM-J
24 $Y = YXX + C(K)$
25 1 CONTINUE
26 EQUA = Y
27 RETURN
28 END

```

1 SUBROUTINE READ(IJ,NAME,X,N)
2 COMMON/SLURP(66),NVOL,NSURF,SLURP2(32),NPRINT
3 COMMON/ZREAD/ID
4 DIMENSION X(1),XX(60),K(3),KU(150,3),NAME(150,3)
5 DATA K/3*0/,KH/1,149*0,1,149*0,1,149*0/,NAMES/450*1 /
6 DATA STAR/LSIAR/
7 J=IJ
8 IF(NAME.EQ.STAR.OR.IJ.EQ.4)GO TO 50
9 IF(K(J).EQ.0)GO TO 100
10 KK=K(J)
11 DO 1 I=1,KK
12 IF(NAME.EQ.NAMES(I,J))GO TO 10
13 CONTINUE
14 ERROR HAS OCCURED
15 100 CALL ERROR(NAME,KK,J)
16 10 ID=KN(I+J)
17 J=J+19
18 IF(ELJAIN/ 60).EQ.FLOAT(N)/ 60.160 TO 20
19 READ(J,I)(X(NN),NN=1,N)
20 FMD(J,I,D)
21 J=J-19
22 RETURN
23 20 INUM=N/ 60
24 DO 21 NN=1,INUM
25 NNX=(NN-1)* 60+1
26 NNY=NN*MAX-1
27 READ(J,I)(X(NN),NN=NX,NY)
28 FMD(J,I,D)
29 21 CONTINUE
30 RETURN
31 50 ID=1
32 READ(23:ID)K,KU,NAMES,NMAX
33 READ(23:ID)SLURP,NVOL,NSURF,SLURP2,NPRINT
34 WRITE(6,50)K,KU,NAMES,NMAX
35 K(3)=0
36 RETURN
37 743 CONTINUE
38 JL=K(I)+1
39 JI=K(J)+1
40 DO 51 I=1,J1
41 READ(24:II)(XX(NN),NN=1,NMAX)
42 WRITE(20:II)XX(31),NN=1,NMAX)
43 51 CONTINUE
44 K(2)=I3
45 DO 53 J2=1,14
46 53 KN(J2)=J2
47 J2=K(2)+1
48 J2=KN(J2)=1
49 M=0
50 DO 52 I=1,13

```

READ6216
 READ6217
 READ6218
 READ6219
 READ6220
 READ6221
 READ6222
 READ6223
 READ6224
 READ6225
 READ6226
 READ6227
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 READ6262
 READ6263
 READ6264
 READ6265

```

51 L=1 READ6266
52 M=1 READ6267
53 NMAX1=NMAX READ6268
54 IF(I.EQ.3)NMAX1=1 READ6269
55 IF(I.EQ.4)NMAX1=1 READ6270
56 IF(I.EQ.6)ER=1E+7)NMAX1=2 READ6271
57 READ(251M,ERR=59)(XX(NN),NN=1,NMAX1) READ6272
58 WRITE(2111)(XX(NN),N=1,NMAX1) READ6273
59 52 CONTINUE READ6274
60 RETURN READ6275
61 59 WRITE(2902)I,K READ6276
62 902 FORMAT(1X,ERRUR III READ DATA SET=25 RECORD=1,13,1 NMAX=1,13,1 TYPE=READ6277
63 IE TO CONTINUE PROGRAM TYPE 2 TO STOP') READ6278
64 RETURN READ6279
65 ENTRY WRITE(IJ,NAME,X,N) READ6280
66 IF(NAME.EQ.'STAR_OR_IJ.EQ.4)GO TO 150 READ6281
67 J=I READ6282
68 IF(K(I).EQ.0)GO TO 115 READ6283
69 KK=K(I) READ6284
70 DO 2 I=1,KK READ6285
71 IF(NAME.EQ.'NAMES(I,J))GO TO 120 READ6286
72 2 CONTINUE READ6287
73 115 K(J)=K(I)+1 READ6288
74 KK=K(I) READ6289
75 NMAX=MAX0(MVOL,NSURF) READ6290
76 GO TO 200 READ6291
77 120 KK=1 READ6292
78 200 NAMES(KK,J)=NAME READ6293
79 ID=KN(KK,J) READ6294
80 J=J+1 READ6295
81 IF(FLOAT(N/ 60).EQ.FLOAT(N)/ 60.)GO TO 30 READ6296
82 WRITE(JID),X(NN),NN=1,N READ6297
83 J=J-1 READ6298
84 KN(KK,J)=ID READ6299
85 RETURN READ6300
86 30 I=J+N/ 60 READ6301
87 DO 31 NN=1, I*HUM READ6302
88 NNX=(NN+1)* 60+1 READ6303
89 NNY=NNX+1 MAX=1 READ6304
90 31 WRITE(JID),X(NN),NN=NXX,NNY) READ6305
91 J=J-1 READ6306
92 KN(KK,J)=ID READ6307
93 RETURN READ6308
94 150 ID=1 READ6309
95 WRITE(6,901)K,KN,NAMES,NMAX READ6310
96 901 FORMAT(111,20X,IK(1)=1,13,3X,IK(2)=1,13,3X/1 1,20X,READ6311
97 1KN VALS1//3(6(2515//1//1)1,40X 1NAMES1//18(25(1X,A4))//10NMAX=1,READ6312
98 23) READ6313
99 WRITE(231D)K,KN,NAMES,NMAX READ6314
100 WRITE(231D)SLURP,NVOL,NSURF,SLURP2,NBENT READ6315

```

A FORTRAN IV (VER L43) SOURCE LISTING READ SUBROUTINE 03/05/74 PAGE 0151
101 RETURN READ6316
102 END READ6317

```

1 SUBROUTINE PRINT(AA,N1,N2)
2 REAL AA(1)
3 COMMON//SLURP(89),K2,SLURP2(310),K3
4 IF(K3.EQ.1)RETURN
5 IF(N2.EQ.1)GO TO 20
6 NJ=N2/6
7 NR=N2-NJ*6
8 IF(NR.NE.0)NJ=NJ+1
9 NC=0
10 KK=5
11 DO 1 J=1,NJ
12 KK=KK*6
13 KL=KK+5
14 IF(J*6.GT.N2)KL=KK+NR*1
15 NC=NC+N1+2
16 IF(NJ.GT.61)GO TO 4
17 IF(NC.GT.61)NC=N1+2
18 NC=0
19 3 FORMAT(111)
20 4 WRITE(K2,2)(I=1,KK,KL)
21 2 FORMAT(/27X,6(6X)3,5X)
22 DO 1 IX=1,11
23 NF=NX+(KK=1)*60
24 NL=NF+5*60
25 IF(J*6.GT.N2)NL=NF+(NR=1)*60
26 1 WRITE(K2,10)MX=1AA(NV),NY=NE,NL=60)
27 10 FORMAT(20X,13,4X,6(1PE14,6))
28 RETURN
29 20 WRITE(K2,11)(AA(NV),NV=1,N1)
30 11 FORMAT(27X,1PE14,6,5E14,6)
31 RETURN
32 END

```

```

PRINT6318
PRINT6319
PRINT6320
PRINT6321
PRINT6322
PRINT6323
PRINT6324
PRINT6325
PRINT6326
PRINT6327
PRINT6328
PRINT6329
PRINT6330
PRINT6331
PRINT6332
PRINT6333
PRINT6334
PRINT6335
PRINT6336
PRINT6337
PRINT6338
PRINT6339
PRINT6340
PRINT6341
PRINT6342
PRINT6343
PRINT6344
PRINT6345
PRINT6346
PRINT6347
PRINT6348
PRINT6349

```


1 FUNCTION LOG(X)
2 REAL*4 LOG
3 LOG=ALOG(X)
4 RETURN
5 END

LOG 6350
LOG 6351
LOG 6352
LOG 6353
LOG 6354

1	SUBROUTINE ERROR(NAME,N1,N2)	ERR 6355
2	C ALL UNRECOVERABLE ERRORS COME HERE	ERR 6356
3	COMMON//SLURP(89),K2	ERR 6357
4	WRITE(2,10)NAME,N1,N2	ERR 6358
5	10 FORMAT(11,20X,1AN ERROR HAS OCCURED IN SUBROUTINE1,2X,A4,2I10)	ERR 6359
6	CALL WRITE(1,1\$STAR1,X,NN)	ERR 6360
7	STOP	ERR 6361
8	END	ERR 6362

```

1  SUBROUTINE ISIMEQ(C, HMAX, NNMAX, NN)
2  REAL C(HMAX, NNMAX)
3  C  CONVERT LOWER LEFT TO ZERO AND DIAGONAL TO 1.0
4  C  NROW  NCOL  NLEN
5  DO 73 N=1, NN
6  IF(N=1) GO, 30, 30
7  C  SET ZERO VALUES
8 30  N1=1
9  DO 50 N=1, NN1
10  HOLD=C(N, N)
11  IF (HOLD) 32, 50, 32
12 32  CONTINUE
13 332  C(N, M)=0
14  N1=N+1
15  DO 40 N=1, NN
16 40  C(H, K)=C(H, K)+HOLD*C(K, K)
17  C(N, NN+1)=C(N, NN+1)-HOLD*C(N, NN+1)
18 50  CONTINUE
19  C  SET DIAGONAL EQUAL TO 1.0
20 66  HOLD=C(H, H)
21  IF (HOLD) 63, 200, 63
22 63  CONTINUE
23 663  C(N, N)=1.0
24  IF (H, EQ, N) GO TO 72
25 68  N1=NN+1
26  DO 70 N=1, N1, 4H
27 70  C(N, M)=C(N, M)/HOLD
28 72  C(N, NN+1)=C(N, NN+1)/HOLD
29 73  CONTINUE
30  C  CLEAR UPPER RIGHT BY BACK SUBSTITUTION
31  C  STARTING WITH K=N NN=1
32 74  DO 90 J=2, NN
33  N=NN+1-J
34  J1=J+1
35  DO 87 K=1, J1
36  M=NN+1-K
37  HOLD=C(M, H)
38  IF (HOLD) 75, 87, 75
39 75  CONTINUE
40  C75  C(H, M)=0.0
41  C(N, NN+1)=C(N, NN+1)+HOLD*C(M, NN+1)
42 87  CONTINUE
43 90  CONTINUE
44  RETURN
45 200  CALL ERROR('ISIQ', N, H)
46  RETURN
47  END

```

SMEQ6363
SMEQ6364
SMEQ6365
SMEQ6366
SMEQ6367
SMEQ6368
SMEQ6369
SMEQ6370
SMEQ6371
SMEQ6372
SMEQ6373
SMEQ6374
SMEQ6375
SMEQ6376
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SMEQ6380
SMEQ6381
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SMEQ6394
SMEQ6395
SMEQ6396
SMEQ6397
SMEQ6398
SMEQ6399
SMEQ6400
SMEQ6401
SMEQ6402
SMEQ6403
SMEQ6404
SMEQ6405
SMEQ6406
SMEQ6407
SMEQ6408
SMEQ6409

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1 BLOCK DATA DATA6410
2 COMMON/JAZZ2/SSNM(B,4),GSUM(B,3),SGMM(B,3),GGMM(B,3),ZSS(B), DATA6411
3 ZGS(B),ZSG(B),ZGG(B) DATA6412
4 C SURFACE TO SURFACE DIRECT INTERCHANGE AREAS DATA6413
5 DATA SSNI/DSSAI, DSSB, DSSC, DSSD, DSSD, DSSD, DSSFI, DSSGI, DATA6414
6 1 DSSH, DSSII, DSSJ, DSSK, DSSL, DSSM, DSSN, DSSO, DSSP, DSSQ, DSSR, DSSS, DSSU, DSSV, DSSW, DSSX, DSSY, DSSZ, DSS3, DSS4, DSS5, DSS6, DATA6415
7 2, DSSO, DSSP, DSSQ, DSSR, DSSS, DSSU, DSSV, DSSW, DSSX, DSSY, DSSZ, DSS3, DSS4, DSS5, DSS6, DATA6416
8 3, DSSX, DSSY, DSSZ, DSS3, DSS4, DSS5, DSS6, DATA6417
9 C SURFACE TO GAS DIRECT INTERCHANGE AREAS DATA6418
10 DATA GSNW/DGSAI, DGSB, DGSC, DGSD, DGSE, DGSEI, DGSGI, DATA6419
11 1 DGSII, DGSIII, DGSJ, DGSK, DGLI, DGLM, DGSNI DATA6420
12 2, DGSO, DGSPI, DGSQ, DGSRI, DGSST, DGSU, DGSVI, DGSXI, DATA6421
13 3, DGSX, DGSY, DGSZ, DATA6422
14 C GAS TO SURFACE DIRECT INTERCHANGE AREA DATA6423
15 DATA GSNW/DGSAI, DGSB, DGSC, DGSD, DGSE, DGSEI, DGSGI, DATA6424
16 1 DGSII, DGSIII, DGSJ, DGSK, DGLI, DGLM, DGSNI DATA6425
17 2, DGSO, DGSPI, DGSQ, DGSRI, DGSST, DGSU, DGSVI, DGSXI, DATA6426
18 3, DGSX, DGSY, DGSZ, DATA6427
19 C GAS TO GAS DIRECT INTERCHANGE AREA DATA6428
20 DATA GCH/DGCAI, DGCBI, DGCCL, DGCCL, DGCCL, DGCCL, DGCCL, DATA6429
21 1 DGGHI, DGGII, DGGJI, DGGKI, DGGLI, DGGMI, DGGNI DATA6430
22 2, DGGO, DGGPI, DGGQ, DGGRI, DGGST, DGGU, DGGVI, DGGXI, DATA6431
23 3, DGGX, DGGY, DGGZ, DATA6432
24 C BET TRANSMISSIVITY SURFACE TO SURFACE DATA6433
25 DATA ZSS/ZSSI, ZSS2, ZSS3, ZSS4, ZSS5, ZSS6, ZSS7, ZSS8, ZSS9, DATA6434
26 C NET TRANSMISSIVITY SURFACE TO GAS DATA6435
27 DATA ZSG/ZSGI, ZSG2, ZSG3, ZSG4, ZSG5, ZSG6, ZSG7, ZSG8, ZSG9, DATA6436
28 C NET TRANSMISSIVITY GAS TO SURFACE DATA6437
29 DATA ZGS/ZGSI, ZGS2, ZGS3, ZGS4, ZGS5, ZGS6, ZGS7, ZGS8, ZGS9, DATA6438
30 C NET TRANSMISSIVITY GAS TO GAS DATA6439
31 DATA ZGG/ZGGI, ZGG2, ZGG3, ZGG4, ZGG5, ZGG6, ZGG7, ZGG8, ZGG9, DATA6440
32 COMMON /GAUSS/WT(9),XY(9),ARG(9),PI DATA6441
33 C GAUSSIAN QUADRATURE METHOD USING ZERO OF LEGENDRE DATA6442
34 C POLYNOMIALS AND THE CORRESPONDING WEIGHTS DATA6443
35 C WEIGHTS --- WT DATA6444
36 DATA WT(9),0.06127439, 0.11064816, 0.26061070, 0.31234708, DATA6445
37 1 0.38023936, 0.31234708, 0.26061070, 0.18064816, 0.08127439, DATA6446
38 C ABSCISSAS --- XY DATA6447
39 DATA XY(9),0.9681624, 0.83603111, 0.61337143, 0.32425342, 0.0, DATA6448
40 1 0.32425342, 0.61337143, 0.83603111, 0.96816024, DATA6449
41 C NUMBER OF QUADRATURE POINTS DATA6450
42 DATA NPT /9/ DATA6451
43 END DATA6452

```

```

1 BLOCK DATA DATA6453
2 COMB/JA23/SSN(8,4),CSN(8,3),SCM(8,3),CGN(8,3),SRSH(8,4), DATA6454
3 1SRGN(8,3),TSSM(8,4),TGNM(8,3),TSGN(8,3),TGGN(8,3) DATA6455
4 C SURFACE TO SURFACE DIRECT INTERCHANGE AREAS DATA6456
5 DATA SSN/IDSSA1, IDSSB1, IDSSC1, IDSSD1, IDSSE1, IDSSF1, IDSSG1, DATA6457
6 1 IDSSH1, IDSSH1, IDSSJ1, IDSSK1, IDSSL1, IDSSM1, IDSSN1 DATA6458
7 2, IDSSO1, IDSSP1, IDSSQ1, IDSSR1, IDSSS1, IDSSST1, IDSSU1, IDSSV1, IDSSW1, DATA6459
8 3, IDSSX1, IDSSY1, IDSSZ1, IDSS11, IDSS21, IDSS31, IDSS41, IDSS51, IDSS61, DATA6460
9 C SURFACE TO GAS DIRECT INTERCHANGE AREAS
10 DATA GSN/IDGSA1, IDGSB1, IDGSC1, IDGSD1, IDGSE1, IDGSE1, IDGSG1, DATA6461
11 1 IDGSH1, IDGSH1, IDGSJ1, IDGSK1, IDGSL1, IDGSM1, IDGSN1 DATA6462
12 2, IDGSO1, IDGSP1, IDGSQ1, IDGSR1, IDGSS1, IDGST1, IDGSU1, IDGSV1, IDGSW1, DATA6464
13 3, IDGSX1/ DATA6465
14 C GAS TO SURFACE DIRECT INTERCHANGE AREA DATA6466
15 DATA SGN/IDSGA1, IDSGB1, IDSGC1, IDSGD1, IDSGE1, IDSGF1, IDSGG1, DATA6467
16 1 IDSGH1, IDSGH1, IDSGJ1, IDSGK1, IDSGL1, IDSGM1, IDSGN1 DATA6468
17 2, IDSGO1, IDSGP1, IDSGQ1, IDSGR1, IDSGS1, IDSGT1, IDSGU1, IDSGV1, IDSGW1, DATA6469
18 3, IDSGX1/ DATA6470
19 C GAS TO GAS DIRECT INTERCHANGE AREA
20 DATA GGN/IDGGA1, IDGGB1, IDGGC1, IDGGD1, IDGGE1, IDGGE1, IDGGG1, DATA6471
21 1 IDGGH1, IDGGH1, IDGGJ1, IDGGK1, IDGGL1, IDGGM1, IDGGN1 DATA6473
22 2, IDGGO1, IDGGP1, IDGGQ1, IDGGR1, IDGGS1, IDGGT1, IDGGU1, IDGGV1, IDGGW1, DATA6474
23 3, IDGGX1/ DATA6475
24 C SURFACE REELECTIVITY WITH SURFACE AS THE EMITTER DATA6476
25 DATA SRSH/ISRSA1, ISRSB1, ISRSC1, ISRSD1, ISRSE1, ISRSF1, ISRSG1, DATA6477
26 1 ISRSH1, ISRSH1, ISRSJ1, ISRSK1, ISRSL1, ISRSM1, ISRSN1 DATA6478
27 2, ISRSO1, ISRSP1, ISRSQ1, ISRSR1, ISRS11, ISRS21, ISRS31, ISRS41, ISRS51, ISRSW1, DATA6479
31SRSX1, ISRSY1, ISRSZ1, ISRS11, ISRS21, ISRS31, ISRS41, ISRS51, ISRS61, DATA6480
29 C SURFACE REFLECTIVITY WITH GAS AS THE EMITTER
30 DATA SRG/ISRGA1, ISRGB1, ISRGC1, ISRGD1, ISRGE1, ISRGE1, ISRGG1, DATA6482
31 1 ISRGH1, ISRSH1, ISRGJ1, ISRGI1, ISRGL1, ISRGM1, ISRGN1 DATA6483
32 2, ISRGO1, ISRGP1, ISRGG1, ISRGI1, ISRGS1, ISRGT1, ISRGU1, ISRGV1, ISRGG1, DATA6484
33 3 ISRGX1/ DATA6485
34 C SURFACE TO SURFACE TOTAL INTERCHANGE AREA DATA6486
35 DATA TSSM/ITSSA1, ITSSB1, ITSSC1, ITSSD1, ITSSE1, ITSSF1, ITSSG1, DATA6487
36 1 ITSSH1, ITSSH1, ITSSJ1, ITSSK1, ITSSL1, ITSSM1, ITSSN1 DATA6488
37 2, ITSSO1, ITSSP1, ITSSQ1, ITSSR1, ITSSS1, ITSSST1, ITSSU1, ITSSV1, ITSSW1, DATA6489
38 3, ITSSX1, ITSSY1, ITSSZ1, ITSS11, ITSS21, ITSS31, ITSS41, ITSS51, ITSS61, DATA6490
39 C SURFACE TO GAS TOTAL INTERCHANGE AREA
40 DATA TGSN/ITGSA1, ITGSB1, ITGSC1, ITGSD1, ITGSE1, ITGSE1, ITGSG1, DATA6491
41 1 ITGSH1, ITGSH1, ITGSJ1, ITGSK1, ITGSL1, ITGSM1, ITGSN1 DATA6493
42 2, ITGSO1, ITGSP1, ITGSQ1, ITGSR1, ITGSS1, ITGST1, ITGSU1, ITGSV1, ITGSW1, DATA6494
43 3, ITGSX1/ DATA6495
44 C GAS TO SURFACE TOTAL INTERCHANGE AREA DATA6496
45 DATA TGNM/ITGNA1, ITGNB1, ITGNC1, ITGND1, ITGNE1, ITGNE1, ITGNG1, DATA6497
46 1 ITGNH1, ITGNH1, ITGNJ1, ITGNK1, ITGNL1, ITGNM1, ITGNI1, DATA6498
47 2, ITGNO1, ITGNP1, ITGNQ1, ITGNR1, ITGNS1, ITGNT1, ITGOU1, ITGOU1, ITGOW1, DATA6499
48 3, ITGNX1/ DATA6500
49 C GAS TO GAS TOTAL INTERCHANGE AREA
50 DATA TGGN/ITGGA1, ITGGB1, ITGGC1, ITGGD1, ITGGE1, ITGGE1, ITGGG1, DATA6502

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51 1 1TGGH1,1TGGI1,1TGGJ1,1TGGK1,1TGL1,1TGM1,1TGN1 DATA6503
52 2 1TGGH1,1TGGI1,1TGGJ1,1TGGK1,1TGL1,1TGM1,1TGN1,1TGGV1,1TGGW1, DATA6504
53 3 1TGGX1/ DATA6505
54 END DATA6506

```

1 BLOCK DATA DATA6517
2 COMMON/JAZZAZ/ TSSNM(8,4),IGSNM(8,3),ISGNM(8,3),ISS(8), DATA6518
3 1 GS(8),SG(8),GG(6) DATA6519
4 C SURFACE TO SURFACE TOTAL INTERCHANGE AREA
5 DATA TSS:M/ISSA1,ITSSB1,ITSSC1,ITSSD1,ITSE1,ITSSFI,ITSSGI, DATA6510
6 1 ITSSLL,ITSSL1,ITSSJ1,ITSSK1,ITSSL1,ITSSM1,ITSSN1 DATA6511
7 2,ITSSO1,ITSSP1,ITSSQ1,ITSSR1,ITSSS1,ITSSST1,ITSSU1,ITSSV1,ITSSW1, DATA6512
8 3,ITSSX1,ITSSY1,ITSSZ1,ITSS1,ITSS2,ITSS3,ITSS4,ITSS5,ITSS6, DATA6513
9 C SURFACE TO GAS TOTAL INTERCHANGE AREA
10 DATA IGS:M/IGSAL,IGSBL,IGSC1,IGSD1,IGSE1,IGSEFI,ITGSG1, DATA6515
11 1 ITGSH1,ITGSI1,ITGSJ1,ITGSK1,ITGSL1,ITGSM1,ITGSN1 DATA6516
12 2,ITGSO1,ITGSP1,ITGSQ1,ITGSR1,ITGSS1,ITGST1,ITGSU1,ITGSV1,ITGSW1, DATA6517
13 3,ITGSX1/ DATA6518
14 C GAS TO SURFACE TOTAL INTERCHANGE AREA
15 DATA TSG:M/ITSGA1,ITSGU1,ITSGC1,ITSGD1,ITSGE1,ITSGFI,ITSGGI, DATA6520
16 1 ITSGH1,ITSGI1,ITSGJ1,ITSGK1,ITSGL1,ITSGM1,ITSGN1 DATA6521
17 2,ITSGO1,ITSGP1,ITSGQ1,ITSGR1,ITSGS1,ITSGT1,ITSGU1,ITSGV1,ITSGW1, DATA6522
18 3,ITSGX1/ DATA6523
19 C GAS TO GAS TOTAL INTERCHANGE AREA
20 DATA IGG:M/IGGAL,IGGB1,IGGC1,IGGD1,IGGE1,IGGEFI,ITGGGI, DATA6525
21 1 ITGGH1,ITGGI1,ITGGJ1,ITGGK1,ITGGL1,ITGGM1,ITGGN1 DATA6526
22 2,ITGGO1,ITGGP1,ITGGQ1,ITGGR1,ITGGS1,ITGGT1,ITGGU1,ITGGV1,ITGGW1, DATA6527
23 3,ITGGX1/ DATA6528
24 C SURFACE TO SURFACE INTERCHANGE AREA -- REAL GAS
25 DATA SS/ISS=11,ISS=21,ISS=31,ISS=41,ISS=51,ISS=61,ISS=71,ISS=81/ DATA6529
26 C SURFACE TO GAS INTERCHANGE AREA -- REAL GAS
27 DATA GS/IGS=11,IGS=21,IGS=31,IGS=41,IGS=51,IGS=61,IGS=71,IGS=81/ DATA6530
28 C GAS TO SURFACE INTERCHANGE AREA REAL GAS
29 DATA SG/ISG=11,ISG=21,ISG=31,ISG=41,ISG=51,ISG=61,ISG=71,ISG=81/ DATA6531
30 C GAS TO GAS INTERCHANGE AREA -- REAL GAS
31 DATA GG/IGG=11,IGG=21,IGG=31,IGG=41,IGG=51,IGG=61,IGG=71,IGG=81/ DATA6532
32 END DATA6533

```

```
1      BLOCK DATA
2      COMMON/JAZZ5/GS(8),SG(8),GG(8)
3 C    SURFACE TO GAS INTERCHANGE AREA == REAL GAS
4      DATA GS/1GS=11,1GS=21,1GS=31,1GS=41,1GS=51,1GS=61,1GS=71,1GS=81/
5 C    GAS TO SURFACE INTERCHANGE AREA REAL GAS
6      DATA SG/1SG=11,1SG=21,1SG=31,1SG=41,1SG=51,1SG=61,1SG=71,1SG=81/
7 C    GAS TO GAS INTERCHANGE AREA == REAL GAS
8      DATA GG/1GG=11,1GG=21,1GG=31,1GG=41,1GG=51,1GG=61,1GG=71,1GG=81/
9      END
DATA6539
DATA6540
DATA6541
DATA6542
DATA6543
DATA6544
DATA6545
DATA6546
DATA6547
```



```

1  BLOCK DATA
2  COMMON /JAIZ6/ SG(8),GS(0),SS(8) DATA6548
3  C  SURFACE TO SURFACE INTERCHANGE AREA -- REAL GAS DATA6549
4  DATA SS/ISS=11,ISS=21,ISS=31,ISS=41,ISS=51,ISS=61,ISS=71,ISS=81/ DATA6550
5  C  SURFACE TO GAS INTERCHANGE AREA -- REAL GAS DATA6551
6  DATA GS/IGS=11,IGS=21,IGS=31,IGS=41,IGS=51,IGS=61,IGS=71,IGS=81/ DATA6552
7  C  GAS TO SURFACE INTERCHANGE AREA REAL GAS DATA6553
8  DATA SG/ISG=11,ISG=21,ISG=31,ISG=41,ISG=51,ISG=61,ISG=71,ISG=81/ DATA6554
9  END DATA6555

```